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State of Indiana

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25 January, 2018

Attention: Incoming Application to Heath Hartleyept of Environmetal Management

100 North Senate Avenue

MC 61-53 IGCN 1003

Indianapolis, IN 46204-2251

JAN 2 5 2018

Dept. of Environmental Mgmt Office of Air Quality

Subject:

Air Emissions Source Construction Permit Application for Riverview Energy Corporation

Dear Mr. Hartley,

Please find attached for your review and consideration an application to construct a Direct Coal Hydrogenation (DCH) at a site in Spencer County, near Dale, Indiana by Riverview Energy Corporation. Two copies of the application package are being provided IDEM. Riverview requests IDEM to schedule a public meeting during the draft construction permit comment period.

Please note that the dispersion modeling protocol and modeling report have been separately submitted to Mr. Cody Jones of the IDEM Technical Support and Modeling Section.

Please contact Mr. Stephen Lang (713-753-7580) with any questions that you may have regarding this application.

Regards,

Stephen A. Lang

KBR

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Attachments

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Dept. of Environmental Mgmt Office of Air Quality

Application

to the

Indiana Department of Environmental Management

for a

Construction Permit

to build a

Direct Coal Hydrogenation Facility

to be located in

Spencer County, Near Dale, Indiana

Ву

Riverview Energy Corporation

Application Prepared By

KBR 601 Jefferson Ave., Houston, TX 77002

January, 2018

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### 1. Application Overview

This air pollutant emission source construction permit application package is for a direct coal hydrogenation facility. This facility will utilize a cutting-edge approach to a technology with proven performance and reliability. It is called the Veba Combi Cracker® (VCC) technology and it is licensed in the United States by Kellogg Brown and Root (KBR).

The permit application package for this project is organized as shown on the Table of Contents. Tables have been utilized whenever feasible in order to minimize the number of forms that needed to be included. These tables have been structured to reproduce in exact order the information required by their parent forms, which we anticipate will facilitate review of this package.

Specific application elements that are best addressed as separate items are included as individual attachments to the core package. These attachments include the proposed fugitive dust control plan. The modeling protocol and related modeling information have been submitted separately from this package.

It is important to note that this fuel conversion facility is not a petroleum refinery in any sense. It does not process crude oil or petroleum or petroleum derived feedstocks. Therefore, it is not subject to NSPS and NESHAPs that are applicable to oil refineries. It does convert solid fuel (coal) into high quality ultra low sulfur diesel and naphtha boiling range products likely to be used as blend stock by fuel refiners and marketers. It is only subject to coal conversion-related regulatory packages.

## Forms and Supporting Figures/Tables

All of the application forms are provided in a single attachment. Their supporting figures and tables are kept in separate, adjacent attachments for ease of review.

The emission summaries are contained in the Forms section described above. Because of their importance, they are being described here in detail. The total emissions from each emitter and from the facility as a whole are critical for determining the applicability of different emission control requirements, ranging from Indiana's regulations to the applicability of federal New Source Performance Standards (NSPS) and National Emission Standards for Hazardous Air Pollutants (NESHAPs). A separate attachment has been dedicated to the many tables that are needed to characterize the emissions, equipment specifications and other information needed for IDEM to complete its determinations in order to provide an enforceable, environmentally protective construction permit for this facility.

Tables 1 through 8 are the potential emissions after emission controls have been applied to the various operations that will comprise this facility. These controls include both hardware (e.g.,

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baghouse) and work practice programs (e.g., roadway dust controls). They form the basis of this application package.

### Environmental Data Sheets

The project definition has been developed by Kellogg Brown & Root, LLC (KBR) and current system design details of major emission units are captured on summary load/data sheets. These data sheets are the basis upon which the permit application emissions inventory has been generated.

### **BACT Determinations**

The BACT determinations for this project were made using the top-down approach recommended in USEPA guidance. The determinations made for this project are addressed in this section.

### Fugitive Dust Plans

This facility is required to have a fugitive dust control plan for its Coal Preparation and Processing scope under the provisions of 40 CFR 60 Subpart Y. This plan has been provided in a dedicated attachment. It includes the paving of parking areas and plant roads in areas of coal handling, with a work practices program to maintain fugitive dust control in these areas. As coal is delivered by rail only, conveyed, stacked, and reclaimed by dedicated automatic equipment without equipment traffic, fugitive losses are minimized by design. Transfer into the VCC process area's thermal drying and milling operations are also addressed in the dust control plan.

# New Source Performance Standards (NSPS) and National Emissions Standards for Hazardous <u> Air Pollutants (NESHAPs)</u>

Separate sections have been generated to address the applicable NSPS and NESHAPs requirements for this facility. The individual Subparts are identified and discussed in these sections.

### Preventative Maintenance Plans

Every Preventative Maintenance Plan (PMP) for control equipment is similar. All PMPs require the operation and maintenance of the piece of control equipment to comply with manufacturer's recommendations for maintenance and for the operation of the device to comply with its design specifications and manufacturer's guarantee requirements/limitations. For each piece of equipment or operation that requires a PMP, the PMP will identify the job title of the individual responsible for inspecting, maintaining and repairing the subject equipment or operation, describe the item/condition to be inspected, and include an inspection schedule for the specified items/conditions. The PMP will also identify the stock replacement parts to be kept in stock and specify the number to be maintained in the site inventory to allow quick replacement.

## 2. Project Overview and Process Descriptions

The Applicant is currently planning to construct a fuel conversion facility at a site in Spencer County near Dale, Indiana. The facility will utilize a process technology with proven performance and reliability, called Veba Combi Cracking® (VCC), which is licensed in the United States by Kellogg Brown and Root (KBR). Table 2-1 identifies the overall DCH Facility's process blocks and attached reference block flow diagrams which are subject for this application.

	Table 2-1: DCH Facility Pro	cess Blocks
Block ID	Facilities	Block Flow Diagram
1000	Coal Handling	H102-1000-EV-DWG-EV2-0001
1500	Additives Handling	H102-1500-EV-DWG-EV2-0001
2000	VCC Unit	H102-2000-EV-DWG-EV2-0001
3000	Sulfur Recovery	H102-3000-EV-DWG-EV2-0001
3000	Sulfur Recovery – Amine Recovery	H102-3000-EV-DWG-EV2-0003
3000	Sulfur Recovery - Amine Storage	H102-3000-EV-DWG-EV2-0004
4000	Offsites	H102-4000-EV-DWG-EV2-0001
5000	Residue Solidification	H102-5000-EV-DWG-EV2-0001
6000	Utilities	H102-6000-EV-DWG-EV2-0001
6500	Water Supply & Treatment	H102-6500-EV-DWG-EV2-0001
7000	Hydrogen Unit	H102-7000-EV-DWG-EV2-0001
8000	Waste Water Treatment	H102-8000-EV-DWG-EV2-0001

The following process block descriptions provide a more comprehensive overview of the interrelationships of the VCC Process Unit with its supporting Offsites and Utility infrastructure comprising the proposed DCH Facility.

# 2A. Process Block 1000 Description - Coal Handling

The coal handling from rail receipt to transfer into the VCC process includes the following system components, which include point and fugitive emission sources addressed in the emissions inventory:

- 1. Rail Car Dump Unloading Facility (Shelter Type)
- 2. Rail Unloading Conveyor 1 (Enclosed Pipe)
- 3. Conveyor 1 Transfer Station (Enclosed Structure)
  - a. Transfer to Feed Conveyor 2 (Enclosed Pipe) to Stacker 1
  - b. Transfer to Feed Conveyor 3 (Enclosed Pipe) to Stacker 2
- 4. Stacker 1 Boom Conveyor 2A (Enclosed) to Discharge Chute (for creating adjacent Stockpiles #1 & #2)
- 5. Coal Stockpile #1 (Radial Conical Ring)
- 6. Coal Stockpile #2 (Radial Conical Ring)

- 7. Stacker 2 Boom Conveyor 3A (Enclosed) to Discharge Chute (for creating adjacent Stockpiles #3 & #4)
- 8. Coal Stockpile #3 (Radial Conical Ring)
- 9. Coal Stockpile #4 (Radial Conical Ring)
- 10. Reclaimer 1 (500 ton/hr. reclaim capacity from Stockpiles #1 & #2
- 11. Reclaimer 1 Transfer Conveyor 4 (Enclosed) to Reclaim Transfer Structure
- 12. Reclaimer 2 (500 ton/hr. reclaim capacity from Stockpiles #3 & #4)
- 13. Reclaimer 2 Transfer Conveyor 5 (Enclosed) to Reclaim Transfer Structure
- 14. Transfer Station 1 Conveyor 9 to Reclaim Transfer Structure (for direct feed to VCC process from coal unloading bin)
- 15. Reclaim Transfer Structure (Enclosed)
- 16. Reclaim Transfer Conveyor 6 (Enclosed) to Milling/Drying Building
- 17. Milling/Drying Building Crushed coal feed conveyor/coal feeder
- 18. Coal Milling & Drying System
- 19. Pulverized Coal Baghouse
- 20. Coal Hopper with Filter
- 21. Closed Screw Conveying to Coal-Oil Slurry Mixing VCC Feed Stream Preparation

# Overview of Coal Receipt, Handling, and Storage

Illinois Number 6 or equivalent Indiana coal will be delivered to the site by 100-car unit trains and unloaded in an enclosed building via continuous rapid unloading, a process in which bottom dump railcars unload coal into receiving hoppers located beneath the railroad tracks. The railcars are "indexed" through the unloading spot, with the unloading hopper scraper discharging to an 84-inch wide conveyor belt, which transports the coal through an elevated transfer station to one or both of the two separate transfer conveyors to the stockpiling locations. A separate conveyor is provided from the transfer station for direct coal feed to the VCC unit.

Two radial stackers are provided which have capability for continuous and independent stacking and reclaiming. Stacker/Reclaimer 1 will be used for creating and maintaining two coal stockpiles (#1A & #1B). The radial stackers/reclaimers create a conical, kidney-shaped stockpile configuration over an approximate 180 degree arc, with a vertical rise of ~100 ft. A second radial stacker/reclaimer creates stockpiles #2A & #2B, also within the coal rail loop area. The stacker/reclaimers operate without the need for any routine traffic on, across, or around the coal pile which would generate fugitive emissions.

While the unloading conveyor systems and stackers have high capacity to enable rapid unloading of the unit trains (5000 tons per hour), the reclaiming systems operate at much lower rates (500 tons per hour), i.e., to match the VCC design feed rate and intermittently provide catch-up transfer rates to the coal milling/drying operations. Reclaimer 1 and Reclaimer 2 have independent transfer conveyors to the Reclaim Transfer Station which provides redundancy in meeting the VCC design coal feed demand. A final Reclaim Transfer Conveyor exits the Reclaim Transfer Structure to deliver coal feed to the VCC Coal Milling/Dryer Building, wherein

the dry pulverized coal feed is produced and screw conveyed to the VCC coal hopper and final conveying/weighing into the coal-oil slurry vessel.

# Coal Preparation for VCC Unit - Coal Milling and Drying

A mill unit, a baghouse, a recycle gas blower, and a fired heater comprise the coal milling and drying unit, which pulverizes feed coal received as 30 - 40 mm sized material into a coal size range of roughly 50% less than 75 microns and maximum of 250 microns and dries the coal to a specified moisture content.

Crushed coal is fed to the coal mill where it is pulverized in a process where warm gas enters the mill bottom to heat and dry the coal. Gas carries pulverized coal particles out of the mill to the pulverized coal baghouse, while larger, heavier coal particles remain in the milling process. In the pulverized coal baghouse, solids are separated and filtered, and "dust-free" gas is sent to the recycle gas blower for circulation back to the coal mill. A fired heater, normally operated on fuel gas, generates hot flue gas used to warm the circulation gas before it enters the mill; surface and absorbed moisture evaporated from coal enters circulation gas flow. To maintain conditions above the dew point temperature in the coal baghouse, a fraction of warm gas is diverted around the mill to the baghouse and also a purge from the recirculating gas loop is used for both pressure control and to eliminate accumulated moisture.

# 2B. Process Block 1500 Description - Feed Additives Unit

# Solid Additive Handling and Feed Preparation

A separate set of solid handling systems is required for each feed additive from receipt to storage and from storage to the VCC coal-oil slurry station dosing/mixing vessels. The fine and coarse additives are received by rail car while the sodium sulfide (Na₂S) additive is received by truck transport. Each additive is stored in a silo and must be kept free of moisture, thus nitrogen is used as carrier gas in the pneumatic conveying systems and as a storage blanket gas. Each step of the handling process is generically described below.

As fine additive may be the same material as coarse additive, i.e., only differing in size distribution, a "Fine Additive Production System" package is provided in the scope as backup for direct delivery.

# Pneumatic Transport, Solid Storage, Solid Dosing

Pneumatic transport shall consist of an open loop transfer system designed for batch operation. The conveying system will transfer solid feed via unloading facilities from nitrogen-blanketed rail cars and trucks and transfer the solid to appropriate storage vessels. Carrier gas and blanketing nitrogen will be supplied as a utility at required pressures to the unloading spots. Dilute phase conveying will be employed with an option to convert to dense phase conveying with closed loop design to minimize nitrogen consumption. Solid storage will include a dust filter baghouse

on top to separate nitrogen from conveyed solids. Nitrogen will also be used for pulse jet cleaning of the baghouse filters.

Solid dosing systems will consist of a rotary feeder solid weigh scale, a solid dosing master control system, and a solid screw conveyor, which will be precalibrated based on material transport rates. In normal operation, each rotary feeder will feed the solid weighing scale pot in batch mode based on the level measurements on the pot. The system will be controlled via a solid dosing master controller.

### Na<sub>2</sub>S Slurry Preparation

In addition to solid handling, a solvent mixture system is required for feed preparation of the sodium sulfide to ensure adequate mixing of Na<sub>2</sub>S powder with the feedstock. Solvent used will be VGO from the VCC unit's vacuum tower.

From the Na<sub>2</sub>S screw conveyor, solid Na<sub>2</sub>S is sent, along with solvent, to the Na<sub>2</sub>S mixing drum, which will be blanketed with low pressure nitrogen. The suspension is pumped from the Na₂S mixing drum to the coal-oil-additive premix drum for transport into the VCC process.

### Coal Slurry Feed Preparation

Solvent from the VCC Unit fractionation section, including fractionator bottoms and vacuum gas oil (VGO) from the VCC Unit's vacuum column is routed to the VCC Unit's Feed Premix Drum. Coal feed from the Coal Milling and Drying section is gravity fed to the Coal Hopper and further fed for mixing to the Feed Premix Drum through the Screw Feeder; similarly, coarse additive and fine additive are gravity fed from conveyors to the Feed Premix Drum, where coal, catalyst, additive, solvent, and Na<sub>2</sub>S are combined. All solids are passed through sieves to remove large solids and other materials prior to mixing in feed premix drum.

A control unit regulates the coal to liquid ratio in the Feed Premix Drum by setting the coal rate via the weighing system in relation to the recycled solvent flow rate. The other solid feeds will be controlled by using the related dosing screw, and their rates set as a function of coal feed rate. The recycle solvent from VGO recycle drum is routed to the Feed Premix Drum. An internal mixer is required in the Feed Premix Drum to disperse solids in the feed and to establish a stable suspension. In addition to the internal mixer, a recirculated solid slurry stream is recycled from suction of the HP Feed Pump to the Feed Premix Drum; during normal operation the vessel is filled with 50 wt% solids.

After mixing, the slurry is routed to the Feed Surge Drum (V-0102) via the Feed Premix Pump to the reactor section of the VCC unit.

# 2C. Process Block 2000 Description - Veba Combi Cracking (VCC) Unit

VCC technology is commercially proven, with decades of commercial operations and innovation. It is the most mature and versatile technology of its kind in the market today. VCC is

the only slurry-phase hydro-cracking technology proven to convert coal to higher value distillate products. The Riverview Energy VCC Unit is designed to process a nominal 200 metric tons per hour, on a moisture and ash free basis, of run-of-mine (ROM) coal into premium ultra-low sulfur content distillate products. The VCC technology's main processing steps may be summarized as:

- Coal Feedstock & Additive Solids Handling
- Coal + Solvent Slurry Feed preparation
- Pressurization and preheating of the feed
- Liquid phase reaction (LPH: hydro-cracking & hydrogenation) and separation of the primary products
- Gas phase reaction (GPH: hydro-treating & hydrogenation) of the primary product in a trickle bed reactor and heat recovery
- GPH Reactor Effluent Separation Section
- Product Fractionation (Naphtha & Diesel)
- Recycle Gas Compression (Hydrogen & hydrocarbon)
- System depressurization and Stripping
- Makeup hydrogen compression
- Vacuum distillation of the LPH reactor unconverted material (hydrocarbon recovery)
- Solidification of the Vacuum Residue

The VCC process feedstock is a slurry of finely ground dry coal, additives, and catalyst carried in a heavy gas oil which is injected into the high pressure section of the process. After adding makeup hydrogen the feed stream is preheated by heat recovery from the reactor effluents and a fired heater. The feed mixture is converted in a cascade of multiple slurry or liquid phase hydro-cracking (LPH) reactors operated at high pressure. The LPH reactors' effluent of converted coal, additives, and the process catalyst are separated from the vaporized reaction products in a hot separator.

The hot separator vapor effluent is sent to the VCC gas phase hydro-treating (GPH) stage while the separator's bottom liquid product is further heated and fed to a vacuum flasher for additional distillate recovery. The vacuum column's bottom product is termed residue and sent to a solidification unit for shipping to offsite consumers.

The GPH stage is a single reactor vessel with catalytic beds for hydro-treating, followed by additional beds for further hydro-cracking to maximize diesel production. After leaving the GPH the effluent is cooled, condensed and separated from the non-condensable gas fraction. The stripped vapors are further processed into sweet LPG for use as process feedstock in the Complex's Hydrogen Manufacturing Unit. The separated liquids are further processed in a fractionator to produce high quality naphtha, ultra-low sulfur diesel fuel and fractionator bottoms. The bottoms are recycled back to the GPH and converted to diesel. A small portion of the bottoms is purged back to the LPH for further hydro-cracking in order to prevent buildup of polynuclear aromatics in the process loop and products.

The VCC Unit contains auxiliary systems including a water injection system, a sour water collection system which sends effluent to the OSBL Sulfur Recovery Plant, gas Amine Absorbers, from which rich amine will be sent to the OSBL Amine Regeneration Unit, and an Emergency De-pressure System to collect and contain solid-containing slurry material during an emergency depressurizing of the high pressure reactor systems.

# 2D. Process Block 3000 Description - Sulfur Recovery Unit

Due to the VCC's high pressure liquid phase hydro-cracking and gas phase hydro-treating steps, the sulfur recovery from feedstock coal is very high and in turn the sulfur content of the process products is very low. Nearly all of the feedstock coal's sulfur content is converted to hydrogen sulfide and is recovered either via the amine treating of produced gas or collection of sour water generated in the process. These recovery systems produce the feed to the Sulfur Block operations which has two parallel Sulfur Recovery Plants, each rated at 70% of expected loading to provide reliability and allow for VCC Unit turndown to 70% rate if one of the plants experience a shutdown. The amine, sour water, sulfur recovery, and product handling are described in the following narrative.

### Amine Regeneration

So-called "lean amine" solution, which contains only trace amounts of H₂S after stripping, is recirculated from the Amine Regeneration Unit (ARU) to the VCC unit where it is contacted with sour gas and LPG streams in high pressure and low pressure absorbing towers. The resulting absorber bottoms streams, now as "rich amine" solutions carrying the recovered hydrogen sulfide (H<sub>2</sub>S) and ammonia (NH3) are regenerated by medium temperature stripping, allowing concentrated processing of recovered H2S and NH3 gases in the Sulfur Recovery Plants (SRP) and the lean amine solution to be recycled.

The amine-water contacting solution is comprised of ~40% methyl diethanolamine (MDEA) in water and has extremely low vapor pressure, minimizing losses to product streams as well as fugitive emissions from processing equipment. Its use in the VCC process allows the diesel and naphtha products to meet product quality specifications as well as the VCC by-product streams used as feedstock to the Hydrogen Plants or alternatively sent to the fuel gas system, e.g., those streams internally described as "sweet", e.g., Sweet Offgas and Sweet LPG.

Rich amine from the VCC unit enters the rich amine flash drum where entrained oil is removed from the stream. The amine is then heated and sent to the amine regenerator, where the amine is reboiled by a steam exchanger to remove H<sub>2</sub>S and ammonia (NH<sub>3</sub>) from the solution. These overhead gases are cooled to condense water which has boiled up through the column with the H<sub>2</sub>S and NH<sub>3</sub> prior being sent to the sulfur recovery plant. The recovered water is returned as reflux to the column and purged to the Sour Water system.

The lean amine from the bottom of the column is cooled against rich amine feed to the amine regenerator, then cooled further with an air cooler. After cooling, the amine stream is filtered via

cartridge filters and a carbon bed absorber to remove any trace decomposition or oil contaminants before beginning another recovery cycle in the VCC unit.

### Sour Water Stripping

Sour water stripping is conducted in a two stage system to first separate ammonia and then hydrogen sulfide (H<sub>2</sub>S) from the sour water feed. This processing configuration reduces ammonia load on the Sulfur Recovery Plant (SRP) and NOx generation in the SRP's tail gas treatment unit (TGTU).

In the NH<sub>3</sub> Stripper, ammonia and any water containing trace H<sub>2</sub>S remaining in the steam are stripped out. The NH<sub>3</sub> reboiler uses LP steam to drive stripping of the sour water, which is used either as reflux on the ammonia stripper or as internal recycle and returned to the sour water degassing drum. Overhead gas from the NH3 stripper is cooled and the resulting gas and liquid are separated in the NH<sub>3</sub> reflux drum. NH<sub>3</sub> rich gas is liquefied to be sold as product and stored onsite.

Sour water exiting the bottom of the NH3 stripper column is sent to the H2S Stripper column with non-phenolic sour water produced in the VCC unit. The non-phenolic sour water will be sent to sour water stripping, after oils are separated out prior to preheating and entering the H<sub>2</sub>S stripper. In the H<sub>2</sub>S stripper column, H<sub>2</sub>S is removed by heat application. The H<sub>2</sub>S rich gas is quenched and any ammonia content washed out via cold stripped water, prior to leaving the top of the column. H<sub>2</sub>S gas is let down in pressure, heated, and then jacketed prior to being sent to sulfur recovery. Bottoms are reboiled with MP steam and used for preheating feed prior surge and reuse/recycling in the VCC Unit.

A small portion of sour water, mainly from the VCC Unit's vacuum tower, contains phenolic compounds which are handled in a parallel sour water system, including tankage and stripping. The separate parallel systems (phenolic and non-phenolic) are provided to keep phenolics from concentrating in product streams from the recycling of stripped sour water to the process.

### Sulfur Recovery

Acid gases containing primarily H<sub>2</sub>S from the amine regeneration process and sour water stripping process are sent to two SRPs, which use the Claus process with tail gas treating units (TGTU) to produce elemental sulfur product. The process configuration has 2 x 70% VCC capacity SRPs to allow for shut down of one Claus unit and turndown of the VCC to a nominal 70% production rate to minimize any need for flaring of H2S/NH3 bearing gases.

In the SRP process, feed gases and are burned with sufficient air to combust 1/3 of the H2S content to promote the Claus reactions. Hot burner gases are cooled in a waste heat boiler, producing steam, before being mixed with additional acid gas and fed into the first stage of a catalytic converter. Partially converted gas from the first stage converter is cooled, removing the condensed sulfur product.

Unconverted acid gas compounds are then heated prior to entering the second stage of the converter; the effluent from the second stage is again cooled to remove condensed sulfur compounds, before the gas is reheated and sent to the third stage converter. Effluent from the third stage converter is cooled with sulfur product and sent in molten form to the sulfur pit, while unconverted gas is sent to the tail gas treating unit.

The resulting tail gas from the Claus process contains trace sulfur compounds, so the stream is partially recycled back to the SRP feed stream to recover additional sulfur. The main tail gas is heated prior to being fed to a hydrogenation reactor where all sulfur containing compounds are converted to H<sub>2</sub>S. The stream is cooled, producing steam, and cooled further using cooling water. Produced H<sub>2</sub>S is removed in an amine contactor, from which the remaining sweet gas is incinerated and vented to atmosphere.

Sulfur produced may contain up to ~300 ppmw H<sub>2</sub>S, partly chemically bound as polysulfides and partly physically dissolved. Sulfur product is degassed by air injection via spargers into the liquid sulfur pit, with this purge gas stripping H<sub>2</sub>S from the sulfur, promoting decomposition of polysulfides, and oxidizing the product to elemental sulfur. The purge gas is recycled to the SRP feed stream. The Sulfur pit contents with < 10 ppmw free H2S are pumped to the heated sulfur storage tanks for loading into railcars for shipment.

# 2E. Process Block 4000 Description - Offsite Facilities

The offsite facilities for the Riverview Energy Corp. complex include flares, storage tanks, and product loading operations.

#### <u>Flares</u>

Four flares service the Riverview Energy Corp. complex. No routine flaring occurs from the VCC process; each of three flares associated with VCC Unit processes will operate normally on standby, contributing minimal emissions from the burning of small quantities of pilot and purge gases.

Each flare system is comprised of a vent header from process unit, a knock out drum, a molecular (velocity) seal, and a flare tip with multiple pilots. Pilot status is monitored by thermocouple.

The High Pressure (HP) Flare and Low Pressure (LP) Flare are supported by a common derrick within the coal loop area. The HP Flare's primary purpose is to control overpressure reliefs from control and safety valves at the VCC complex, while the LP Flare primarily serves the Hydrogen Production Complex. The controlling overpressure event which acts as a flare sizing basis is major power failure at the complex. A power failure would trigger the VCC Unit's Emergency De-pressure System (EDS), which results in fast de-pressuring of VCC unit's LPH and/or GPH reactors; hot solid material and effluent from the LPH and GPH reactors are sent to the VCC Unit's Emergency De-pressure Drum, where vapor flashes off, is cooled, and is sent to the HP

Flare system with an alternative case being the shut down of hydrogen production and the short term flaring of VCC feedstock streams. The Low Pressure (LP) Flare's primary purpose is to control overpressure reliefs from control and safety valves at the complex's hydrogen production units. The hydrogen units are fed gas from the VCC Unit, supplemented by natural gas from pipeline.

The Sulfur Block Flare is supported on a dedicated derrick within the coal loop area. The Sulfur Block Flare's primary purpose is to control overpressure reliefs from control and safety valves in the complex's Sulfur Recovery Plants, Amine Regeneration Unit, Sour Water Stripping Unit, and sulfur product loading operations.

The Loading Flare is supported on a dedicated derrick adjacent to the product loading spots. The Loading Flare will control venting from the complex's loading operations for diesel, naphtha, and ammonia product.

#### **Product Tanks**

Product diesel from the VCC Unit will be stored onsite in three fixed roof type tanks and one internal floating roof type tank. One diesel storage tank is to be constructed as internal floating roof type to serve as a swing tank for naphtha service if required.

Product naphtha from the VCC Unit will be stored onsite in two internal floating roof type tanks.

Molten sulfur will be stored in a fixed roof that will be heated to maintain product at a flowable viscosity.

Product ammonia will be stored in 12 horizontal pressurized vessels.

### Intermediate Tanks

Hydrogenated residue, vacuum residue, and vacuum gas oil (VGO) are intermediates associated with the VCC process, which will be stored in heated, fixed roof tanks. These materials have very low vapor pressures and need to be kept warm to maintain their liquid state.

#### Other Tanks

Additional tankage at the complex will contain liquids associated with utilities and auxiliary processes, including diesel fuel, slop, amines, sour waters, a variety of water treatment chemicals (sulfuric acid, caustic, etc.), as well as potable water, firefighting water, and demineralized water, and will be stored in fixed roof tanks.

### **Loading Operations**

A loading rack servicing up to 8 railcars simultaneously will be provided for diesel and naphtha product loading at 2500 gpm each. The railcar loading system is submerged fill type to minimize vapor loads sent to the Loading Flare.

A single railcar loading spot is dedicated for loading anhydrous ammonia.

A single railcar loading spot is dedicated for loading liquid sulfur.

Two railcar loading spots are dedicated for loading solidified residue; one load spot is equipped for truck loading as a secondary means of product shipping.

# 2F. Process Block 5000 Description - Residue Solidification Unit

Residue from the VCC Unit Vacuum Tower bottoms will be fed directly to SANDVIK technology ROTOFORM 3000 units for solidification into pastilles. Residue will be alternatively fed to a tank, from which heated residue will be pumped to the solidification units. 1236 STPD of hydrogenated residue is solidified in 12 operating units + 4 spare units.

All heat supplied to the system to maintain the residue in flowable, liquid form will be electrically generated.

Each unit includes a prefilter, a fine filter, and a pastillator (ROTOFORMER TM) discharging residue onto a steel belt with a dedicated, under-belt water cooling system. The pastilles are of uniform hemi-spherical shape, ~ 5-6 millimeters in diameter. Given the high melting point of the residue and immediate cooling on the belt, the pastilles rapidly form a glassy coat as they travel along the ~130 foot length of the cooling belt to a discharge point. The belt cooler is enclosed and provided with an exhaust vent for a purge air stream. Four units are exhausted to a common blower and discharged to a vent above the solidification building roof to the atmosphere. A small amount of hydrocarbon is initially released from the pastilles' surface, i.e., evaporated vacuum gas oil which is dissolved in the residue. The temperature profile along the cooling belt indicates surface evaporation occurs only for approximately the first third of the belt travel length.

The belt cooling water recirculates and is never in contact with the residue product. The fully solidified pastilles, each 5-6 mm diameter, are dropped off the belt via discharge knife and conveyed to loading spots for railcar (primary), truck (secondary) or other containers such as supersacks, or bulk containers (tertiary) for shipping.

The pastilles have a significant strength and are not friable. Their handling is essentially dustless.

# 2G. Process Block 6000 Description - Utilities

The VCC Unit will require auxiliary systems to provide utilities to sustain the plant's process. The utility systems contributing to air emissions are detailed below; additional utility systems to be installed include raw water treatment, wastewater treatment, plant and instrument air, electrical infrastructure, etc.

A three-cell, mechanic draft cross flow cooling tower will provide cooling water for various process and utility units in the Riverview Energy Corp. complex. The cooling tower will be equipped with drift eliminators capable of achieving drift to 0.0005% of the tower's recirculation rate (~32,000 gpm). Well water from the Dale Complex will be used as cooling tower makeup supply.

A package boiler will provide 40,000 lb/hr of 650 psig/750 degree F superheated steam to meet steam demand for start-up of the complex's VCC unit. The package boiler will operate at a turndown rate of ~30% during normal plant operations.

Diesel drivers are provided for emergency operation of equipment in the case of power failure for 1) essential power demands and 2) firewater pump services.

- The essential power diesel generator set will be provided by Caterpillar and will meet EPA Tier 2 emissions standards. The diesel generator is presented as an intermittently operating source; it will be turned on for a maximum of 1-2 hours per week (i.e., 100 hrs per year as its Potential to Emit basis) for engine reliability testing and maintenance. Operation of the diesel generator in excess of this Potential to Emit period will only occur in the event of power failure.
- The diesel driven firewater pump will be provided by Caterpillar and will meet EPA Tier 2 emissions standards for this special service. The diesel driven firewater pump is presented as an intermittently operating source; it will be turned on for a maximum of 1-2 hours per week plus an additional allowance of 100 hours per year (i.e., 200 hrs per year Potential to Emit basis) for engine reliability testing and maintenance plus fire water system pressure testing and purging periods. Operation of the diesel fire water pump in excess of this Potential to Emit period will only occur in the event of a major fire event.

Plant air and instrument air will be generated onsite for use in various units within the Riverview Energy Corp. complex as a basic utility system. Air is filtered and compressed, moisture condensed and discharged from these air systems. No regulated emissions to atmosphere are generated by the plant and instrument air systems' operation.

Nitrogen will be generated onsite for use in various units within the Riverview Energy Corp. complex for purging lines and other support operations. The site's nitrogen generating unit will utilize pressure-swing adsorption (PSA) technology to produce high purity nitrogen from air. No regulated emissions to atmosphere are generated by PSA unit's operation.

# 2H. Process Block 6500 Description - Water Supply and Treatment

Water supply to the Riverview Energy facility is proposed to be from the Ohio River, conveyed to the site by a pipeline, as a groundwater supply does not currently appear feasible. Treatment

steps will include lime softening prior use as cooling tower make-up and then removal of dissolved solids to generate boiler feed water.

The lime-softening step will require receipt and handling of either bulk quantities of dry "quicklime" or slaked-hydrated lime (Ca(OH)2). Truck receipt is currently proposed with pneumatic conveying into a storage silo. Feed from the storage silo to the water treatment system is conveyed by enclosed screw feeder line with no emissions. The storage silo PM emissions from displaced air headspace flow during truck unloading is controlled by a dust collector. No other air emissions are associated with the water treatment areas.

# 21. Process Block 7000 Description - Hydrogen Production

Hydrogen supply is essential to the VCC process, as coal is predominantly carbon and the fuel conversion to liquid products is essentially a hydrogen addition or hydrogenation technology. The extent of hydrogen addition is determined by the available feedstock and desired product composition and quality. In order to maximize the flexibility of processing low cost available feeds, the hydrogen capacity must be robust. Two Hydrogen Plants, each with 105 MMSCFD of 99.9% hydrogen purity are specified for the DCH facility.

The main process steps of the Hydrogen Manufacturing Unit consist of feed preparation, i.e., desulfurization, steam methane reforming (SMR), shift conversion and hydrogen purification. The hydrogen feedstock is first mixed with recycled hydrogen. Desulfurization occurs in two process steps; first, organic sulfur compounds are converted to H2S in the presence of a hydrogenation catalyst, then H2S is adsorbed.

The desulfurized feed is mixed with process steam at an optimized steam-to-carbon ratio and superheated before entering the high temperature primary reformer furnace. A catalyst converts the mixed feed into a reformed synthesis gas containing H2, CO2, CH4, N2 and steam inside the primary reformer's tubes. CO in the reformed synthesis gas is water gas shifted to produce more hydrogen.

In the hydrogen purification unit, hydrogen is separated from the shift gas stream by pressure swing absorption (PSA) with multiple trains cycling to provide relatively constant hydrogen product flow rates. The PSA tail-gas is recycled as fuel to the reformer furnace to recover its heating value.

The primary reformer radiant section is heated by firing the PSA tail-gas from the hydrogen purification unit and by supplemental fuel gas with burners in its top section. The necessary combustion air is routed by a combustion air fan to the furnace burners after preheating against flue gas exiting unit. The gas path from the furnace includes refractory-lined ducting to a convection section where steam production and process heat recovery occur in a series of heat exchanger coils, as well as NOx reduction by a selective catalytic reduction (SCR) bed, and lastly the combustion air preheat exchanger prior being routed to the flue gas stack.

Steam generated by waste heat from the SMR reformed gas is utilized as process steam, with the excess exported for other plant needs.

# 2J. Process Block 8000 Description - Waste Water Treatment Unit

Wastewater generated from the DCH Project is characterized under federal and state regulations as contact, non-contact, storm water run-off, and sanitary flows. It is noted that the Dale site's industrial water supply is provided from wells adjacent to the Ohio River by pipeline and is treated prior use by Riverview for utility and process services. Potable water supply is provided from the City of Dale drinking water distribution system and used directly by Riverview with no further treatment.

The liquid effluent management scheme for the units in the DCH Project will have provisions for the segregation of liquid effluents and wastewater sources, non-contact stormwater, effluent collection, routing, treatment, and monitoring.

All process wastewater from the DCH Units is treated and combined with utility blowdowns and treated sanitary wastewater and leaves the site by pipeline for conveyance to an outfall to the Ohio River.

The design will endeavor to minimize impacts and ensure the effluent discharges are within the limits specified by the applicable State and Federal regulations incorporated into the facility NPDES permit. There are no directly applicable effluent guidelines for the DCH facility under regulations at 40 CFR 414.

Contact wastewater is generally "process" wastewater or water that comes into contact with process streams, intermediate or commercial products. As process piping, vessels, etc. are considered primary containment, secondary containment is provided for potential leak sources, e.g., storage tanks and pumping locations, critical process equipment, and for general spill and emergency release protection areas.

Dedicated wastewater drain collection and conveyance systems are provided for oily, sour, and amine contaminated flows. These systems are designed as closed or water sealed systems in order to control fugitive emissions. Additional wastewater treatment equipment scope may need to be addressed as part of future FEED phase development and is not addressed in this application.

The potentially contaminated storm water runoff from the DCH process area drainage (PAD) will be routed to PAD Containment Sumps for holding and testing before release. Contaminated storm water from ACRO 2 will be routed to the wastewater treatment system as needed and become tributary to the normal dry-weather flow to the plant's Ohio River outfall. Clean storm

water will be routed to the plant's clean water ditches tributary to the Norfolk Southern rail line right-of-way drainage to Little Pigeon Creek.

In the OSBL chemical handling and storage areas, Riverview uses secondary containment, curbing, and diking design concepts to enable a hold and release approach for potential spill incidents generating contact wastewater. While storm water from such areas is assumed potentially contaminated, it is normally non-contaminated and released after testing or checking into the non-contact surface drainage system tributary to the Norfolk Southern rail line right-ofway drainage to Little Pigeon Creek..

# Storage Tanks / Containers Subject To Secondary Containment Design (Finalized in FEED Phase)

- Diesel
- Naphtha
- VGO
- Amine
- Sour Water
- Residue
- Sulfuric Acid
- Sodium Hydroxide
- Cooling Water Treatment Chemicals
- Boiler Feed Water & Boiler Treatment Chemicals

### Non-Contact Wastewater

Non-contact wastewaters are those which normally do not come into direct contact with the facility products, raw materials or intermediate process streams, i.e., nominal utility related flows. The primary direct sources of non-contact utility wastewater discharge from the DCH Project will be:

- Filtered Water and DI Water Treatment Waste Streams
- Cooling Tower Blowdown
- **Boiler Feed Water Services**
- Steam Drum Blowdown
- Steam Condensate Flows, Pump Base Plate and Drains
- Steam Condensate Recovery and Steam Trap Losses
- Sample Coolers' cooling water streams
- Fire Water System Blowdowns (Purges) & Miscellaneous Uses and Losses
- Potable Water System Blowdowns (Purges)
- Utility/Industrial Water System Blowdowns

Non-contact wastewater streams will be combined with the treated wastewater streams and sent to the Ohio River Outfall.

Stormwater and Spill Control Clean stormwater from the DCH Project's non-developed or non-industrial areas will be routed to the Riverview NPDES Outfalls tributary to Little Pigeon Creek. Miscellaneous perimeter areas of the plant are also believed to drain to Little Pigeon Creek via the Norfolk Southern rail line drainage.

Stormwaters may be differentiated within the Riverview Stormwater Pollution Prevention Plans (SWPPP) for both the construction period and the operating facility. This document addresses the expected construction period volumes and flows per a preliminary PDP Phase study conducted. Best management practices for the DCH Project's impacted areas will be established specifically during the FEED Phase in advance of construction to control sediment erosion and other potential contaminants such as fuels, lubricants, and miscellaneous chemicals used in commissioning activities. Incorporation into Riverview's larger drainage strategy and SWPPP for the site is outside of the present Project's scope.

New equipment considered for inclusion in Riverview's SPCC Plan from the DCH Project due to oil inventory from transformers and high voltage capacitors include:

- Transformers at the new Utility Substation (~ area of 60 ft x 15 ft dimension)
- Transformers at the new VCC Substation (~ area of 72 ft x 22 ft dimension)
- HV Capacitors at Utility Substation (Others TBD in FEED)

Civil works including preliminary grading and paving plans will be used to finalize stormwater drainage scope and effluent flow rates to Riverview NPDES Outfall 001.

### Sanitary Wastewater

There will be sanitary wastewater generation from approximately 100 personnel at the Riverview buildings which include: Gate House, Administration, Maintenance Shops, Warehouse, Control Room / Lab Building. The flow will be collected at lift stations and conveyed to the City of Dale.

# 2K. DCH Facility Emission Inventory Overview

The Applicant's emission units addressed in this application and contributing to the DCH facility's emission inventory are listed in Table 2-2.

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		Tab	able 2-2 : Emission mean	2	Emission Inventory	n Emist	sion Inv	entory		
		one of the Coppe			כוממכת			-		Remarks
		DCH Facility Scope	Emission Basis	PM10/	Š	8	<b>S02</b>		HAPs	
Block	Emission	Emission Source Description		C. ZIMIC. C		!	1	i	L	
	DINC NAME OF	Coal Unloading Station	Process weight rate	CIL		1		1		
	2001	Transfer Station 1	Process weight rate	CI.			1	1	1	
	EU-1001	Stacker 1 Boom Chute	Process weight rate	YES		1	1	,		
	EU-1002	Coal Pile 1A/1B	Stack and Met Data	YES		\ \ \	1	1	-	
	EU-1003	Court in Brom Chute	Process weight rate	YES	:					
1000	EU-1004	Stacker & Doom	Stack and Met Data	YES	ı	1		1	1	
	EU-1005	Coal File Zven	Process weight rate	YES	Į	1		1	VEV	Natural Gas Fuel
	EU-1006	Reclaim Transfer Station	Elring Rate	YES	YES	YES	YES	25	3	
	EU-1007	Coal Dryer Heater	Oxidation A I - O	YES			!	1	-	
	F11-1008	Coal Drying Loop Purge	COal Moustaile	VES	1	1	1	ì	1	
	4504	Coarse Additive Storage Filter	Volumetric Displacement	2 :		!	     	<u> </u>	l	
	201-01	T. A Latino Storage Filter	Volumetric Displacement	2	  -  -		-	1	1	
	EU-1502	Fine Additive Stolego	Volumetric Displacement	YES	1	1	1			
1500	EU-1503	NA2S Additive Storage Filter	tnement	YES	1	1	!	!	1	
	EU-1504	Fine Additive Production System	Volumetric Displacement	VEC	YES	YES	YES	YES	YES	Natural Gas Fuel
	ghF11-2001	+	Firing Kate	2 \ Z	VES	YES	YES	YES	YES	Natural Gas Fuel
	E11-2002	-	Firing Rate	3 3	VES	YES	YES	YES	YES	Natural Gas Fuel
		+-	Firing Rate	YES VEC	YES LES	-	YES	YES	YES	Natural Gas Fuel
3		+	Firing Kate	_		-	;	,	!	
	LO-200	-	Volumetric Displacement	_	-			ļ   		

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		Tal	able 2-2 : Emission Inventory Overview	ory Overvic	Me		-	1		
		Soul Facility Scope		드	Included in Emission Inventory	n Emis	ion Inv	entory		Remarks
		DOD Laciny coops	T. Bacis	PM10/	Š	8	<b>S02</b>	၁၀ %	HAPs	
Block	Emission Unit Number	Emission Source Description	EIMISSIOII Dasis	PM2.5				•		
	EU-2006	Coarse Additive Handling	Volumetric Displacement	YES	ı	1	1	1	!	
		Fine Additive Handling System	Volumetric Displacement	YES	ı	ļ	ŀ	١	l	
	EU-2007	Filter		7,10		1	ŀ	1		
	EU-2008	Na2S Handling System Filter	Volumetric Displacement	7ES	VFS	YES	YES	YES	YES	2 x 50% Capacity
	EU-3001	TGTU Stack A	FIIIIB nate		31,	VEC	YES	YES	YES	Units; Natulal Cas Fuel
3000	F11-3002	TGTU Stack B	Firing Kate	YES	153	3	N N N	VES	YES	Natural Gas Fuel
			Standby Pilots & Purge	YES	YES	YES	3	3		Matural Gas File!
	EU-4001	Loading Flare	Standby Pilots & Purge	YES	YES	YES	YES	YES	YES	Matulai Gas i aci
	EU-4002	Sulfur Block Flare	Chandley Dilote & Purpe	VES	YES	YES	YES	YES	YES	Natural Gas Fuel
4000	EU-4003	LP Flare	Standay Filots & Mis-	3		VEC	VEV	YES	YES	Natural Gas Fuel
	E11 4004	HP Flare	Standby Pilots & Purge	YES	TES	2	2			And
	101		Process Weight Rate	YES	1	ł	1	YES	ŀ	race Amounts rivi
	5001A/B/C/D	Residue Pastilators Stach 1						YES	1	Trace Amounts PM
	EU-	Residue Pastilators Stack 2	Process Weight Rate	YES	1	1		1		VO standard
	3002A2006			VEC	-	-	-	YES	1	I race Amounts rivi
	EU- 5003A/B/C/D	Residue Pastilators Stack 3	Process Weight Kate	YES				752	1	Trace Amounts PM
	EU-	Docidio Pastilators Stack 4	Process Weight Rate	YES	1	1	1	2		
5000	5004A/B/C/D		State Rate	VFS	 	1	1	YES	!	Trace Amounts
8	EU-5005	Residue Railcar Loading	Process weight hate					YES	1	Trace Amounts
	9003	Residue Railcar Loading	Process Weight Rate	YES	;			2 2		Trace Amounts
	D000-03		Process Weight Rate	YES	1	1	1	2		
	EU-5007	Residue Rail/Truck Loading	otes Woight Rate	VES	;	1	l	YES	1	Trace Amounts
	EU-5008	Residue Rail/Truck Loading	Process weight have					VES	!	Trace Amounts
	EU-5009	Residue Bulk Container	Process Weight Rate	YES	1	1	1	3		
										Daga 21

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		Inch	<u> </u>	Included in Emission Inventory	1 Emissi	on Inve	ntory		•
	DCH Facility Scope		- 1			-	200		Remarks
		Emission Basis	PM10/	NOX	8	S02	) %	HAPs	
Emission	Emission Source Description		C.2M7			-	YES		Trace Amounts
	Doordue Bail Silo Filter	Volumetric Displacement	YES	-  -	1		1 5		
EU-50'IU	ביים ביים ביים ביים ביים ביים ביים ביים	Volumetric Displacement	YES	ı	;	1	2		
EU-5011	Residue Swing Silo Filter	0+00	YFS	YES	YES	YES	YES	YES	Natural Gas Fuel
E11-6000	Package Boiler	FILING Kate					YFS	ŧ	
	\ = \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \	Recirculation Rate	YES	1	1	-	}		
EU-6001	Cooling Tower Cell A	Registraliation Rate	YES	1	ı		YES	1	
EU-6002	Cooling Tower Cell B	otto acit-l	25/2		1	1	YES	1	
FU-6003	Cooling Tower Cell C	Recirculation nate	2			1	YES		
111 6008	Eng Diesel Tank	Tank and Met Data		1		0 137	VEC	VFS	
		Operating HP-Hrs	YES	YES	YES	7.5	2		
EU-6006	Emergency Diesel Generator	operation of the state of the s	!	;	1	1	YES	1	
EU-6007	EDFWP Diesel Tank	Tank and Met Data				77,	\ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \	YES	
0000	Emergency Diesel Fire Water	Operating HP-Hrs	YES	YES	YES	<u>a</u>	ን   -	}	
EU-buus	Pump		VES	1	1	ł	1	ł	
EU-6501	Lime Silo Filter	Volumetric Displacement	3	1	1		1	 	CO2 & Inerts
E11-6507	Deaerator Vent	BFW Rate	1		757	VEC	YES	YES	Natural Gas and
2000	1 August Dlant 1 Reformer	Firing Rate	YES	YES	2	3	3	VEC	Process Tail Gas
EU-/001	Hydrogen Figure 1	Firing Rate	YES	YES	YES	YES	ZE AES		
EU-7002	Hydrogen Plant 2 Reformer	ct-cl			YES	l	YES	YES	Methanol HAP
EU-7003	Hydrogen Plant 1 DA Vent	Licensor Data		\ \ \ \	YES	1	YES	YES	
7007	Hydrogen Plant 2 DA Vent	Licensor Data							

# 3. Applicable Federal New Source Performance Standards (NSPS)

Considerations for granting a permit are based upon the scope of regulatory applicability and upon the technical acceptability of the submissions under New Source Review - Prevention of Significant Deterioration (NSR-PSD) and State Implementation Plan (SIP) regulations at 40 CFR 51 & 52 et. seq. incorporated by reference by IDEM.

As noted in Section 1, the Riverview DCH facility is defined as a Fuel Conversion Facility, one of the 28 PSD Source Categories with 100 ton/yr Major Source Thresholds. See Table 3-1 for that listing. The current DCH Project emissions inventory has NOx, CO, SO2 and VOC emissions exceeding the PSD major source threshold and Green House Gase (GHG) emissions also exceed the current major source threshold of 75,000 ton/yr.

Table 3-1: PSD Source Categories	with 100 TPY Major Source Thresholds
<ol> <li>Coal cleaning plants (with thermal dryers)</li> </ol>	15. Coke oven batteries
2. Kraft pulp mills	16. Sulfur recovery plants
3. Portland cement plants	17. Carbon black plants (furnace process)
3. Portiand Certient plants	18. Primary lead smelters
4. Primary zinc smelters	19. Fuel conversion plants
5. Iron and steel mills	20. Sintering plants
6. Primary aluminium ore reduction plants	21. Secondary metal production plants
<ul><li>7. Primary copper smelters</li><li>8. Municipal incinerators capable of charging more than 250 tons of refuse per day</li></ul>	22. Chemical process plants
9. Hydrofluoric acid plants	23. Fossil-fuel boilers (or combination thereof) totaling more than 250
10. Sulfuric acid plants	24. Petroleum storage and transfer units with a total storage capacity exceeding 300,000 barrels
	25. Taconite ore processing plants
11. Nitric acid plants	26. Glass fiber processing plants
12. Petroleum refineries	27 Charcoal production plants
<ul><li>13. Lime plants</li><li>14. Phosphate rock processing plants</li></ul>	28. Fossil fuel-fired steam electric plants of more than 250 million British thermal units per hour hear input

Section 3 addresses the federal New Source Performance Standards (NSPS) at 40 CFR 60 et. seq., incorporated by reference by IDEM that have been identified for the Applicant's DCH facility.

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# 3A. Coal Preparation and Processing Plants (40 CFR 60, Subpart Y)

Coal transfer, coal storage, and the coal crusher are regulated under "Standards of Performance Coal Preparation and Processing Plants," 40 CFR 60, Subpart Y. This regulation limits opacity coal processing and conveying equipment, coal storage systems, or coal transfer and loading

# 3B. Process Heaters and Boilers (40 CFR 60, Subpart Db or DC)

The boiler and most of the process heaters at this facility are subject to the requirements contained in 40 CFR 60 Subparts Db or Dc that apply to gas-fired units. The requirements contained in Subpart Db for gaseous fuel-fired units are applicable to the Feed Heater (128.4 MMBTUH) and the Fractionator Feed Heater (156.0 MMBTUH). The requirements contained in Subpart Dc for gaseous fuel-fired units are applicable to the Package Boiler (68.5 MMBTUH), the Coal Drying Heater (55.8 MMBTUH), and the Treat Gas Heater (52.8 MMBTUH). The design of this facility complies with all applicable requirements of these regulations.

# 3C. Internal Combustion Engines (40 CFR 60, Subpart IIII & 40 CFR 63, Subpart ZZZZ)

Stationary reciprocating internal combustion engines (RICE) will be used for emergency purposes (exclusively) at the facility (e.g., as emergency generators or to drive fire protection water pumps). Stationary RICE are subject to EPA's New Source Performance Standards for compression-ignition engines (Subpart IIII). Engines may also be subject to requirements under the RICE MACT standard (40 CFR 63, Subpart ZZZZ). The requirements that apply to stationary RICE depend on design, date of manufacture, use, fuel type, size, and whether the engines will be located at a facility that is a major source for HAPs. An estimate of emissions from the planned units is included with the facility emissions. The magnitude of estimated annual emissions from these units qualifies as insignificant activities. Once specified, Riverview Energy intends to purchase engines that comply with the applicable rules and will implement procedures to demonstrate compliance.

# 4. National Emission Standards for Hazardous Air Pollutants (NESHAPS)

Considerations for granting a permit are based upon the scope of regulatory applicability and upon the technical acceptability of the submissions under New Source Review - Prevention of Significant Deterioration (NSR-PSD) and State Implementation Plan (SIP) regulations at 40 CFR 51 & 52 et. seq. incorporated by reference by IDEM.

The National Emission Standards for Hazardous Air Pollutants (NESHAPs) program developed by USEPA under the federal Clean Air Act Amendments of 1990 are comprised of packages of regulatory requirements that are applicable to operations that satisfy the qualifying criteria

specified for each package. The current DCH Project emissions inventory has has a single HAP exceeding the major source threshold of 10 tons per year emissions (methanol). Methanol and other identified HAP emissions are modeled as part of the IDEM Risk Assessment methodology presented in the air dispersion modeling section of this application.

Section 4 addresses the federal NESHAPs at 40 CFR 61 & 63 et. seq., incorporated by reference by IDEM that have been identified for the Applicant's DCH facility.

# 4A. Industrial, Commercial and Institutional Boilers and Process Heaters (40 CFR 63, Subpart DDDDD)

The following units are subject to Subpart DDDDD: the Package Boiler, the Coal Drying Heater, the Feed Heater, the Treat Gas Heater, the Vacuum Column Feed Heater, and the Fractionator Feed Heater. The applicable requirement of Subpart DDDDD is addressed for these units in this application package. The table below identifies the applicable provisions of Subpart DDDDD for each affected unit:

# 4B. Organic Liquids Distribution (Non-Gasoline, 40 CFR 63, Subpart EEEE)

None of the Applicant's equipment is subject to control under this NESHAP, based upon the criteria identified in Table 2 of these standards because they have neither the requisite vapor pressure nor specified HAP components in Table 1 of these standards.

# Storage Tanks (40 CFR 63.2343(b)(1) through (3))

Tanks impacted by this NESHAP are: the Naphtha Product Tanks, Diesel Product Tanks, Diesel Product Swing Tank, the Slop Tank, and the Diesel Fuel Storage Tank. These storage tanks are subject to the requirements listed in 40 CFR 63.2343(b)(1) through (3).

# Transfer Racks (40 CFR 63.2343(c)(1) through (3))

No transfer rack that is subject to Subpart EEEE is subject to control at the facility, based upon the criteria specified in Table 2, items 7 through 10. However, the requirements specified in 40 CFR 63.2343(c)(1) through (3) are applicable to them.

# Equipment Leak Components (40 CFR 63.2346(c))

The pumps, valves and sampling connections in organic liquids service at this facility are addressed in 63.2346(c). None of the tanks are subject to Table 2 control requirements.

# Transport Vehicles (40 CFR 63.2346(c), Table 2)

None of the racks at the Applicant's facility are subject to control requirements based upon Table 2 criteria, so this subsection is inapplicable.

# 5. Best Available Control Technology (BACT) Analyses

The PSD permit regulations are designed to ensure that NAAQS and the PSD air quality increments are protected. One of the requirements of the rules designed to meet this objective is the requirement to install the best available control technology (BACT) for certain pollutant emitters. This requirement is included in Federal regulations (40 CFR Part 60 series) and in the Indiana PSD provisions at 326 IAC 2-2-1(i). The key requirement of this rule is that new major stationary sources must apply BACT for pollutants that the source has the potential to emit in significant amounts.

BACT is defined in 326 IAC 2-2-1(i) as follows:

"Best available control technology" or "BACT" means an emissions limitation, including a visible emissions standard, based on the maximum degree of reduction for each regulated NSR pollutant that would be emitted from any proposed major stationary source or major modification, that the commissioner, on a case-by-case basis, taking into account energy, environmental, and economic impacts and other costs, determines is achievable for the source or modification through application of production processes or available methods, systems, and techniques, including fuel cleaning or treatment or innovative fuel combustion techniques for control of the pollutant. In no event shall application of BACT result in emissions of any pollutant that would exceed the emissions allowed by any applicable standard under 40 CFR Part 60 and 40 CFR Part 61. If the commissioner determines that technological or economic limitations on the application of measurement methodology to a particular emissions unit would make the imposition of an emissions standard not feasible, a design, equipment, work practice, operational standard, or combination thereof may be prescribed instead to satisfy the requirements for the application of BACT. The standard shall, to the degree possible, set forth the emissions reduction achievable by implementation of the design, equipment, work practice, or operation and shall provide for compliance by means that achieve equivalent results.

The definition of a significant amount is provided in 326 IAC 2-2-1(ww). For Riverview Energy, these significant pollutants are PM, PM10, PM2.5, CO, VOCs, SO2, and NOx. Control technologies and practices that control PM10 and PM2.5 will also control PM. Therefore, PM, PM10 and PM2.5 are addressed together. The pollutants CO, VOC, SO2, and NOx are addressed separately, noting that CO & NOx control is inter-related, as both are associated only with combustion sources.

Greenhouse Gas (GHG) emissions sources are required to undergo a BACT analysis because the facility exceeds the applicable threshold for this facility. The GHG emissions will also be addressed separately.

# 5A. Best Available Control Technology Determinations – Top-Down Methodology

The BACT analysis presented in this report is based on a "top-down" approach, consistent with the draft top-down BACT guidance document issued by EPA on March 15, 1990, which is reflected in EPA's Draft New Source Review Workshop Manual (EPA 1990).

In the EPA's top-down methodology, available control technology options are identified based on knowledge of the source and previous regulatory decisions for other identical or similar sources (Step 1). If the top control alternative is technically infeasible or is otherwise rejected as inappropriate after considering site-specific impacts, it is rejected and the next most stringent alternative is then considered (Step 2). The alternatives are then ranked in descending order of control effectiveness (i.e., the "top" option is the most stringent) (Step 3). The feasibility or appropriateness of each alternative as BACT is first based on its technical feasibility. This appropriateness of each alternative is determined to be achievable after weighing the economic, energy, and environmental impacts (Step 4). This alternative is then selected as BACT (Step 5).

The BACT analyses for the Applicant's facility consistently adopted the highest performing technically feasible and reasonable approaches that were found in the EPA's RACT/BACT/LAER Clearinghouse. This eliminated the need to perform relative cost analyses.

# Identification of Available Control Technologies

To determine which control technologies or techniques were available for consideration for the proposed project, the following resources were consulted:

- EPA's Office of Air Quality Planning and Standards MACT developmental data;
- EPA Air Pollution Control Cost Manual (EPA 2002); EPA Air Pollution Control Cost Manual (EPA 2002);
- EPA's Reasonably Available Control Technology (RACT)/Best Available Control Technology (BACT)/Lowest Achievable Emission Rate (LAER) Clearinghouse (RBLC);
- EPA white papers on GHG control measures;
- Permits for similar sources issued in other states; and
- Applicant knowledge.

The RBLC database, made available through EPA's Office of Air Quality Planning and Standards' Technology Transfer Network, lists technologies that have previously been approved as BACT. It was used as a basis for the following determinations.

## 5B. Fugitive Particulate Matter

Fugitive particulate matter (PM) emissions will be produced from coal unloading, coal storage, coal reclaiming, and coal processing in Process Blocks 1000 and 1500 of the DCH facility. Riverview Energy evaluated measures to control fugitive PM from these emission categories. The control options identified are shown in Table 5-1.

**Table 5-1. Fugitive PM BACT Control Options** 

able 5-1. Fugitive PM BACT Emission Unit	
Coal unloading	Chemical or water dust suppression, enclosure of dump pit with baghouse
Coal piles	Wind fence, dust suppression, pile compaction, reduced drop heights, telescopic chutes
Coal handling	Wind screen, wet suppression, enclosure, fabric filter
Coal crushing	Enclosure, wet suppression, fabric filter
Roadways	Paving, reduce speed limit, sweeping, watering, good housekeeping measures, chemical suppression

Enclosure of the bottom dump pit in a shed with a fan exhaust to a baghouse has been selected for control of rail load-in. It is equal to or more effective than other potential BACT selections (e.g., wet suppression, wind screens), since baghouse control exceeds 99% for all particulate size ranges. Although a more conservative capture value has been assumed for emission calculation purposes, a full shed enclosure provides up to 95% capture of fugitive particulates.

#### Coal Conveying

Total enclosure of coal conveyors in tube-like enclosures eliminates virtually any PM fugitive emissions. The resultant control effectiveness exceeds partial enclosure with exhaust to a fabric filter and provides the maximum control effectiveness observed for this activity. The coal transfer stations will be provided with baghouse filter/induced draft fan systems to control ventilation of the enclosures and fugitive dust from drop chutes at the stations.

### Coal Storage & Reclaiming

Coal storage pile emissions are generally controlled by the frequent application of water to the pile, by chemical suppressant application, by covering the pile (tarping), using windbreaks to reduce winds below the entrainment velocity of the material fines, or by enclosing the pile inside a building. Building enclosure is the most effective approach, but the 100 foot high, multi-acre piles planned for this facility to support its operation make building enclosure technically and economically infeasible. The use of chemical suppression is potentially infeasible, since the coal undergoes chemical reactions to form the desired end-product and a chemical suppressant could negatively impact the reaction chemistry. The application of tarps to control emissions has not historically been very effective, requires frequent tarp maintenance and can impact operating efficiency. Windbreaks alone do not assure BACT-level control of coal pile-related PM emissions.

Riverview Energy has chosen an innovative approach to reducing fugitive dust emissions from wind erosion, coal load-in and load-out by selection of BRUKS style Stacker-Reclaimer machinery. The BRUKS style stacker forms two conical, kidney-shaped adjacent piles around each unit. The nearly circular perimeter shaped piles formed around each stacker-reclaimer essentially shields reclaiming load-out activities virtually completely from wind by forming up to a 100 foot high windbreak that surrounds where pile load-out occurs.

Pile stacking load-in emissions will be controlled by low drop height from the automated stacker boom chute and loading to the inside of the pile (as much as feasible) after the initial height of 100 feet is attained. Surface area is minimized by this pile design, reducing the potential fugitive emissions compared to typical pile designs requiring heavy equipment movement and pushing of material over or around the pile. The outer pile surfaces will not be disturbed by fresh coal whenever feasible in order to avoid exposing silt to wind. Water will be applied from the boom chute around the coal flow during load-in activities to further reduce emissions.

The outer surfaces of the piles will be watered to maintain BACT control, i.e., to 10% opacity or less, consistent with Subpart Y requirements). Reclaim load-out emissions to the process equipment will be conducted inside the area enclosed by the piles, where virtually no wind will reach to entrain particulate. This pile design, in conjunction with these work practices and with sufficient water application, provides maximum control of load-in and load-out emissions (the preponderant pollutant emitting activities), as well as wind erosion.

### Coal Milling and Drying

After receipt of VCC Unit's coal feedstock in the Block 1000 Coal Milling and Drying area by conveyor, fugitive PM is controlled by the enclosed systems venting to the dirty side of the coal drying loop. The drying process loop, as described in Section 2, has a baghouse for separating the coal fines feedstock from the recirculating drying loop gas. The collected fines are screw conveyed to Block 1500 for slurry feed preparation.

The purge from the clean side of the drying loop baghouse (EU-1008) is used for pressure control and to control moisture content in the loop gas which has not been otherwise condensed

and recovered. This purge gas vent may have trace amounts of entrained coal fines and is not further controlled.

Roadway dust control is most effectively controlled with either a chemical suppressant application program or by paving the roadways and implementing a pavement watering program. Of these two options, the higher average control effectiveness is maintained with a paved roadway that is watered sufficiently often to maintain low surface silt levels. Maintaining BACT-level performance with a paved roadway is dependent upon consistent implementation of the fugitive dust control program that is applied to it. Riverview Energy proposes to pave all roadways and maintain BACT-level control performance by implementing a watering program of sufficient intensity to maintain a minimum control effectiveness of 80%.

The control technologies shown in Table 5-2 were selected as BACT for the fugitive PM sources as described above.

Table 5-2. BACT for Fugitive PM

able 5-2. BACT for Fu	gitive PM
mission Unit	Control Technology
Coal unloading	Enclosure for rail bottom dump station, exhausted to baghouse
Coal piles	Radial stacker, reduced drop heights, wet suppression
Coal conveyors	Complete enclosure during conveyance
Coal crushing	Enclosure of process in building, wetting material into slurry
Roadways	Paving, watering as needed

# Cooling Tower Point Source PM

There is an additional point source PM emitter that differs from those addressed above. The mechanical draft cooling tower equipment emits particulate matter with the water vapor that escapes during operation. BACT for all ranges of PM emissions due to this phenomenon is the same: mist (drift) eliminators. Virtually every BACT determination found on the RBLC listed drift/mist eliminators as the selection. Riverview Energy proposes to include drift/mist eliminators on its cooling towers. Calculation of cooling tower performance that reflects the use of state-of- the-art drift eliminators is shown in the emission inventory tables of this application.

### 5C. Nitrogen Oxides

Although the VCC is the predominant nitrogen oxides (NOx) generator for this facility, over 38% of the total NOx emissions are from the hydrogen reformer. Thus, the first BACT discussion will

address VCC emissions, while the second portion will address the hydrogen reformer. Due to the wide selection of potential approaches that can be taken to address nitrogen oxide reduction, an overview of potential technologies is being provided to better substantiate that each selected BACT approach is optimal.

### DCH Facility Fuel Gas

All of the DCH Facility's process heater and boiler emission units fire the DCH facility fuel gas supplied from Utility Block 6000. This fuel gas is routinely natural gas and may have small amounts of VCC Unit Off-gas or LPG fractions introduced during intermittent periods. These intermittent flows are when the Hydrogen Plants cannot accept them as feedstock. The Hydrogen Plants primarily fire their process tail gas and only secondarily fire DCH fuel gas, other than at startup when only DCH fuel gas is fired.

## VCC Process Combustion Sources

The combustion sources being addressed as a group in this section include: the package boiler, the coal drying heater, the feed heater, the treat gas heater, vacuum column feed heater, and the fractionator feed heater

The following subsections discuss combustion controls, post-combustion controls (i.e., add-on controls), and their applicability to one or both of the above processes. Combustion controls discussed are flue gas recirculation (FGR), staged combustion and low/ultra-low NOx burners (LNB/ULNBs). Post-combustion controls discussed are selective catalytic reduction (SCR) and selective non-catalytic reduction (SNCR).

### Flue Gas Recirculation (FGR)

FGR recirculates a portion of the flue gas from the stack to the burner windbox. In the windbox, recirculated gas is mixed with combustion air prior to being fed to the burner. The recycled flue gas consists of combustion products which are inert during combustion of the fuel/air mixture. The FGR system reduces NOx emissions by two mechanisms. Primarily, the recirculated gas acts as a diluent to reduce combustion temperatures, thus suppressing the thermal NOx mechanism. To a lesser extent, FGR reduces NOx formation by lowering the oxygen concentration in the primary flame zone. The amount of recirculated flue gas is a key operating parameter influencing NOx emission rates for these systems.

An FGR system is normally used in combination with specially designed low NOx burners that are capable of sustaining a stable flame with the increased inert gas flow resulting from the use of FGR. It is noted that the mechanical systems associated with FGR, i.e., blowers ducting and dampers, increases complexity of operations, both mechanically and combustion control-wise which increases capital costs and impact reliability.

When low NOx burners and FGR are used in combination, these techniques are capable of reducing NOx emissions by 60 to 90 percent (AP-42, Section 1.4, Natural Gas Combustion).

## Staged Combustion Fuel or Air

Staged combustion controls NOx by limiting the oxygen present at temperatures where NOx formation is likely and/or suppressing peak temperatures that increase NOx formation during gas combustion.

Low and Ultra-low NOx Burners Low NOx burners (LNBs) limit NOx formation by controlling the stoichiometric and temperature profiles of the combustion process in each burner zone. The burner design of an LNB may create (1) a reduced oxygen level in the combustion zone to limit fuel NOx formation, (2) a reduced flame temperature that limits thermal NOx formation, and/or (3) a reduced residence time at peak temperature, which also limits thermal NOx formation. Typical control efficiencies for boilers employing LNB range from 40% to 85% (AP-42 Section 1.4, Natural Gas Combustion). Based upon the information in Table 1.4-1 of AP-42, LNB provides an emission rate of 0.049/lb/MMBtu. The use of ultra-low NOx burners consistently reduces the emission rate to 0.036 lb NOx /MMBtu, which represents a reduction that is equivalent to the reduction from the FGR and LNB combination (when the combination is operating at its upper level of performance).

## **Selective Non-Catalytic Reduction**

Selective Non-Catalytic Combustion (SNCR) is a post-combustion technique that involves injecting ammonia or urea into specific temperature zone for a proper duration in the upper furnace or connective pass of a boiler or process heater. The ammonia or urea reacts with NOx in the gas to produce nitrogen and water. The chemical reaction for NO and ammonia is as follows:

Multiple injection locations are required within several different zones of the boiler (or process heater) to respond to variations in the boiler operating conditions. CFD modeling of combustion product flow patterns must be conducted to properly design SNCR injection systems and check that proper time and temperature regimes are present to assure reaction kinetics proceed.

Three difficulties are associated with using SNCR in the heat recovery process involve temperature, initial NOx level, and fouling. The biggest challenge in the implementation of SNCR is the effect of temperature as mentioned, which is a relatively narrow temperature range. In a boiler, there will be adequate residence time at the ideal temperatures if an appropriate steady-state operation is maintained. The required temperature window is 1,600-2,200°F (the most effective range is 1,800–2,100°F). Above these temperatures ammonia begins to react with oxygen rather than NOx (i.e., it is no longer a selective process). At even higher temperatures, more NOx will be formed from nitrogen in the reagent. Below the ideal temperature range, no reaction will occur and ammonia slip will increase, potentially leading to fouling. The Riverview Energy facility will operate at a wide range of load levels, with lower levels potentially unable to provide a furnace temperature profile that maintains the temperature

range needed for effective SNCR control for sufficient residence time to achieve proper emissions control.

Even during proper operation, some ammonia will be emitted, since ammonia slip is need to assure maximum reaction occurs. Additionally, SNCR is most effective for an essentially steady operating level, because transitions between operating levels result in non-stoichiometric operation that will adversely impact control performance. USEPA estimated control performance of SNCR is 30-50% reduction without additional controls.

## Selective Catalytic Reduction

Selective Catalytic Reduction (SCR) is a post-combustion technique similar to SNCR that involves injecting ammonia into flue gas in the presence of a metal-based catalyst to convert NOx emissions to elemental nitrogen and water. The catalyst allows SCR systems to operate at much lower temperatures than SNCR; typical temperatures for application of mediumtemperature SCR are 575-800°F, compared to 1,600-2,200°F for SNCR. The optimum temperature range is 700-750°F (EPA 2002). Low-temperature catalyst systems operating at less than 500°F are commercially available, but tend to be most cost effective for retrofit applications where structural changes to a heater or boiler drive capital cost considerations. obtainable with different catalysts.

SCR reduction efficiencies are substantially better than SNCR, ranging from 70-90+%. Pollutant loading is a key determinant of both economic viability and achievable control efficiency, with high NOx concentrations (100 ppm, for instance) and large unit sizes normally needed to make it economically viable.

Given the low sulfur content fuel gas being fired, concern for ammonium salt formation in the SCR effluent gas path and related fouling and corrosion problems in downstream convection sections or the stack is considered negligible.

### Hydrogen Plant Reformers

The twin hydrogen reformers have a different firing configuration and technology concerns than the more standard process heaters and boiler combustion devices utilized in the VCC, but the reformers share some key characteristics with them. Just as in the case of the process heaters, ultra-low NOx burners can be employed to control nitrogen oxide emissions during the combustion process. The high concentration of NOx in hydrogen reformer exhaust gases makes the use of SCR an economically viable proposition. The discussions for all of the control devices that have been presented for the VCC plant combustion equipment are valid for application with the hydrogen plant reformer with the exception of FGR.

FGR is rarely, if ever used for NOx control in pyrolysis furnaces such as the hydrogen plant reformers due to the high radiant flame temperatures required for the process pyrolysis

reactions. Additionally, the typical high firing rates and thus large combustion product gas flows present in these large "economy of scale" sized units makes recirculation impractical.

However, catalytic reduction approaches also have potential applicability, since they are either built into the convection sections in design or applied as tail end devices that do not impact the process taking place inside the reformer.

### NOx BACT Selections

#### VCC

The use of ULNB is selected as BACT for the boiler and process heaters because it is technically feasible and provides the highest dependable level of control performance of the available options for these units. Use of ULNB is consistent with RBLC BACT determinations for similar gas-fired boilers and process heating combustion equipment. The low NOx concentrations in these units that result from ULNB is supported as BACT in the RBLC.

### Hydrogen Reformers

The design of a hydrogen reformer also allows use of ULNB. ULNB has been selected for the same reasons as above: because it is technically feasible and provides the highest dependable level of control performance of the available options for these units at the burner. However, the high concentration of NOx from this process requires additional control to achieve BACT-level performance.

The process of hydrogen production is a totally separate operation from the VCC process. The hydrogen reformer's pre-control NOx emissions are substantially higher than those from the VCC emitters, which impacts the control economics. In order to control these NOx emissions to a BACT level, the implementation of SCR is proposed. As noted above, SCR is very effective (90% is achievable and proposed here) at controlling NOx emissions. SCR is proposed as the second half of a combined BACT approach for the hydrogen reformer. This approach is further supported by multiple RBLC determinations for hydrogen reformers. It reflects the highest level of BACT control effectiveness.

### 5D. Greenhouse Gases

New PSD/NSR sources that have a potential to emit 75,000 tons/year or more of CO2 equivalent (CO2e) must address their GHG emissions in the NSR and PSD permitting process. Consequently, the requirement to perform a BACT analysis now applies to GHGs. For PSD purposes, GHGs are classified as a single air pollutant that is defined as the aggregate group of the following six gases: CO2, nitrous oxide (N2O), methane (CH4), hydrofluorocarbons, perfluorocarbons, and sulfur hexafluoride. A small quantity of GHG emissions will be from insignificant activities.

The RBLC database ws supplemented with the following resources to identify CO2 control options:

- EPA white papers on GHG control measures for the iron and steel industry,
- Technical reports from engineering studies associated with the power industry, and
- GHG Mitigation Strategies Database
- KBR In-house BACT Assessments for NSR Permitting

#### Green House Gas Control Options

In regard to end-of-pipe technologies, amine solvent based CO2 removal systems offer the greatest emissions reduction potential (> 85%) and are considered technically feasible; however, implementation of such technologies and linkage with available sequestration options such as geological containment is shown to be economically infeasible. Additionally, such systems are unproven at world scale facilities such as Riverview's, which have multiple types of emission sources from which to collect and control GHG. Application of other developing end-of-pipe technologies for carboncapture and sequestration (CCS) are similarly challenged and as a category, end-ofpipe controls cannot be selected as BACT at the Riverview site, leaving smaller-scale mitigation techniques to be chosen by the selection methodology.

Riverview will implement some inherently lower-emitting practices from its proposed burner and convection section designs in in the VCC process heaters and boiler, and in the Hydrogen Plant's pyrolysis furnaces. These base-case or built in conservation approaches represent site-wide source control approach to BACT.

Note: In regard to the use of "lower GHG emitting fuel" EPA has recognized that the initial list of control options for a BACT analysis does not need to include "clean fuel" options that would fundamentally redefine the source. Such options include those that would require a permit applicant to switch to a primary fuel type (i.e., coal, natural gas, or biomass) other than the type of fuel that an applicant proposes to use for its primary combustion process. Following this issue is the consideration that when a permit applicant has incorporated a particular fuel into one aspect of the project design (such as startup or auxiliary applications), this suggests that a fuel is "available" to a permit applicant. In such circumstances, greater utilization of a fuel that the applicant is already proposing to use in some aspect of the project design should be listed as an option in Step 1 unless it can be demonstrated that such an option would disrupt the applicant's basic business purpose for the proposed facility.

For furnaces and boilers, the EPA's RACT/BACT/LAER Clearinghouse (RBLC) database was first investigated to check for any GHG related permit conditions on

record. The RBLC only identifies proper combustion operation and maintenance as BACT controls for GHG without much elaboration or definition of net annualized cost effectiveness. Add-on controls and other potential end-of pipe technologies have not yet been adopted, however, as they are considered emerging technologies, identification is made as being "available".

Note: Under EPA's GHG Permitting Guidance, a control technology is "available" if it has a potential for practical application to the emissions unit and the regulated pollutant under evaluation. Thus, even technologies that are in the initial stages of full development and deployment for an industry, such as CCS, can be considered "available" as that term is used for the specific purposes of a BACT analysis under the PSD program

The available GHG control technologies for the Riverview Project are listed in Table 5-1.

		Table 5-1: Available GHG BACT									
GHG Reduction	Practice	Sub-category Practice	Description	Potential GHG Reductions / Energy Savings / Impacts							
Opportunities	1100000	,	Lish hydrogon	Dependent on % reduction of carbon in							
Source Control	Use of Low- Carbon Content Fuel	natural gas GHG ,> synthetic natural gas	Gaseous fuels (natural gas or high-hydrogen plant tail gas) contain less carbon, and thus have lower CO2 potential, than liquid or solid fuels.	fuel.							
Energy	Burner Tune-	T Julio Fatte	Peep Windows or infrared camera so done without introducing tramp air.	< percentage point improvement for well operated sources							
Efficiency	ups	Inspection CO Monitoring	Done at arch to identify burnout problems								
		O2 Trim Control	Done at arch to control excess air at burners but bias with CO to assure complete combustion	O2 levels are prime indicator of firing efficiency, however site specifics may dictate higher levels for safety or capturing convection section efficiency. Highest accuracy of fuel carbon							
	Instrumen- tation	Fuel Composition	Continuous GC or GC-MS analyses	definition by continuous speciation							
		Analyses Fuel	Fuel Flow Compensation	Continuous compensation of metering improves overall metering accuracy							
		Temperature Fuel Pressure	Fuel Flow Compensation								
		Fuel Density	Fuel Flow Compensation Cross Check	hand release and fuel							
		Fuel Calorimeter	Heat Release Backup to Composition Analyses	Cross check on heat release and fuel composition analyses							
		Fuel Flow	Compensated metering	Accurate fuel firing and GHG account and Air to Fuel ratio control							
		Heater Arch O <sub>2</sub> & CO Monitoring	Process heater radiant section exit analyses on continuous basis	Process firing control							

		7	Table 5-1: Available GHG BACT	
GHG Reduction	Practice	Sub-category Practice	Description	Potential GHG Reductions / Energy Savings / Impacts
Opportunities	ļ -	Stack Femperature Monitoring	Maximum temperature limits indirectly limit GHGs by promoting Heat Recovery	Every 35 °F drop in exhaust gas temp results in ~ 1% increase in thermal efficiency. (w/Temp datum = 77 °F)  Most economically attractive when flue gas temps are > 650 °F.
		Stack CO	Arch vs Stack analyses show tramp air	Energy efficiency . CO Trim Control to ensure optimal combustion
!		Monitoring Stack O <sub>2</sub>	infiltration Arch vs Stack analyses show tramp air	Energy efficiency
	_	Monitoring Stack Flow	infiltration Direct measurement for CEMS	Crosscheck on fuel flow measurement and Method 19 Flow Determination
		Monitoring Stack CO <sub>2</sub> CEMS	Direct Measurement of CO <sub>2</sub>	Accounting GHG-CO2 Fraction  The DCS can make flow meter
	Advanced Process Control	Distributed Control System (DCS) Support	The DCS will host and/or forward GHG related data and calculations to other data servers or systems.	compensation calculations; provide interface for reporting, recordkeeping, and reporting functions.
	Combustion Air / Draft	Burner Management	While considered a safety related system, BMS monitoring and control functions can provide indication of combustion status.	Crosscheck for optimizing combustion efficiency.
	Management	System (BMS)  Damper Controls	Ganged damper actuators (jack shaft	Consistent damper operations and control of excess combustion air  Manage O2 Levels ; Reduce Stack
		Mechanical Draft Design	D ((Decima with Forced	Temperatures otherwise needed in Natural Draft / Tall Stack Sources
		Blower / Fan Driver Variable	Reduce energy demand	Dependent upon service requirements
	Combustion Radiant Zone	Speed Drive Burner & Firebook Sealing &	x Assure controlled, even burner firing	Optimize fuel usage and heat transfer
	Management	Insulation Refractory Coatings	Increase emissivity of refractory to reduce firing rates, provide consistent energy flux to process tubes	Emerging technology, may not have sustained impact due to severe operating conditions
	Convection	Add / Revise	Verify scope with Process Licensor	Pressure drops and heat integration
	Section / Stack / End	Process Coils Add / Revise	Heat Recovery Dependent upon fuel mass rate	Pressure drops and heat integration
	of Stack Heat Recovery	Add / Revise / Preheat Coils	Air Heat Recovery Dependent upon combustion	30300 / 1
		External APH Add / Revise	Heat Recovery Dependent upon water/stear	n Pressure drops and heat integration
		Utility Coils Stack Gas Condensing Heat Exchang	water vapor in exhaust) than conventional economizer. Added benefit of removal of P acid gas, and heavy metals.	yellow, direct savings in fuel cost ~10% increase proces heater efficiencies; tox removal capability similar to that of scrubbing. Payback time ~18 mo.
	Steam	Insulation Stu	dy Thermal Infrared Survey to spot inconsiste	
	System Upgrades	Steam Trap Program	Provide consistent application of steam tra types across site	steam / condensate losses

		•	Table 5-1: Available GHG BACT	
GHG Reduction	Practice	Sub-category Practice	Description	Potential GHG Reductions / Energy Savings / Impacts
Opportunities		Condensate	Increase Condensate Recovery across site;	Original design may have been under much different economic drivers.
		Recovery Boiler Feed Water Pumps Driver Variable	no sewering Reduce energy demand	Dependent upon service requirements
		Speed Drives Minimize direct let-down between steam	Promote energy recovery between steam levels with back pressure or extraction turbines	Check with calibrated steam meters and balances
		levels Minimize Venting	All steam energy recovered	Visual indications may be noted.
End of Pipe Control	Green Chemistry	Flue Gas CO <sub>2</sub> Reaction / Chemical	Flue gas scrubbing with reactive chemicals (example sodium hydroxide used to form sodium carbonate)	Limited by market / uses for product
	Carbon Capture & Storage (CCS)	Recovery  Solvent Absorption, Recovery, Compression, Transport, &	Absorbing solution (nominal amine or other chemical / physical solvent) is contacted with source emission gas, subsequently regenerated to release CO <sub>2</sub> , which is compressed for transport and ultimate	Very high recovery 85-90+% possible based upon source CO2 concentration Application at large scale is limited by costs associated with equipment sizing and energy costs for process steps.
Maintenance	Preventive Maintenance	Sequestration PM and Calibration on Instumentation	sequestration.  Preventative maintenace practices on fuel gas flowmeters, analyzers, etc. to assure good operational monitoring and control	
		PM on Burners	Routine burner tip inspections and cleanings	Based upon experience, increased reliability and steady operations
		PM on Mechanical Components	Routine inspections, monitoring, refurbishment, and cleanings	Based upon experience, increased reliability and steady operations

#### **Source Control**

Use of lower carbon content fuels is considered technically feasible as the DCH facility is using natural gas as fuel gas. Hydrogen is only produced for process use, though some excess production may be fired on an intermittent basis.

#### **Energy Efficiency**

Use of energy efficiency practices and sub-practices identified in Table 5-1 are considered technically feasible but some may be limited in application by site economics, e.g., no home for low grade heat recovered and secondary impacts such as increased NOx emissions for air preheat practices. While many of these practices may be technically feasible, they are best applied in an integrated manner for maximum benefit.

Proposed best practices for the DCH Project include:

- Proper fuel measuring instrumentation
- Burners and draft control, insulation, and heater sealing
- Proper sealing of convection section utility coils

#### **End-of Pipe Control**

Use of Green chemistry options are considered technically feasible but are severely limited by available market and scale of applications not matching the Riverview Project's CO2 emissions inventory.

Use of Carbon Capture and Storage (CCS) technologies are considered technically feasible, though application of capture technologies at large industrial scale has yet to be fully demonstrated.

#### Maintenance

Maintenance of equipment and instrumentation is considered technically feasible in minimizing GHG.

#### Rank According to Effectiveness

Table 5-2 provides ranking of GHG control options considered in the BACT Analysis.

	naryolo.	Table 5-2	: Ranking of	GHG Control Optio	ns Effectiveness	
Rank	GHG Reductio n Opportuni ties	Practice & % Control Effective	Sub- category Practice	Technical Considerations	Energy or Environmental Considerations	Economic Considerations
1	End of Pipe Control	ness Carbon Capture & Storage (CCS)	Solvent Absorption, Recovery, Compressi on, Transport,	Full industrial scale application of CCS has not been proven; equipment scale	High energy consumption for flue gas collection, cooling and dehydration, raising gas	178 \$/ton NACE Value is at multiples of potential cost threshold of reasonableness

Air Per	mit Applica	able 5-2	Ranking of G	HG Control Optior	ns Effectiveness	
Rank Red Opp	HG Puctio	ractice & % Control	Sub- category Practice	Technical Considerations	Energy or Environmental Considerations	Economic Considerations
2 E		6	& Sequestration  Flue Gas CO2 Reaction / Chemical Recovery	issues impact design margins and thus total costs.  Transport pipeline must be routed on public and private right-of ways  Sequestration wells must be located in secure locations, and granted Governmental access rights.  Emerging technologies may use CO2 a near atmospheric pressure.  Market for products not present at sufficient scale	released from products such as bio-fuels may negate favorability	per US EPA (60-90 \$/ton).  Capital investment out of proportion to project costs.  Assumed >100 \$/ton NACE Value.  Low cost CO2 supply is not presently sufficient driving force for adoption of applications. No proposed projects within Spencer Count region. Highly effective
•	Source Control	Use of Low- Carbon Conten		gas firing	be environmental	<< 100 \$/ton NACE Value incorporated into Revamp

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Rank	GHG Reductio n Opportuni ties	Practice & % Control Effective ness	Sub- category Practice	Technical Considerations	Energy or Environmental Considerations	Economic Considerations
		30-80%	natural gas GHG.	Convection	gas fuels, for GHG, SO2, NOx, PM, & trace HAPS (metals)	Associated costs of liquid fuels (storage tanks, fuel line recirculation, burner steam atomization) are avoided.
4	Energy Efficiency	Burner Tune- ups < 1%	Flame Pattern Inspection	Open ports affect firing stability, use peep windows. Metal tube temperatures are monitored which may indicate irregular flames or problems	None. May be supplemented by thermography of furnace walls for units that are being taken down for retubing or other maintenance to find repair/sealing opportunities.	scope for multiple sources
			CO Monitoring O2 Trim Control	Currently accomplished via non-specific Infrared type Combustibles analyzer arch.  Large size of heater radiant zone is problematic. Monitoring at arch or in convection zon most practical.	less rigorous that for CEMS instruments.	Laser based instrumentation capable of scanning across furnace radiant section is being considered but is expensive and has unknown reliability.

		Table 5-2	: Ranking of C	GHG Control Option	15 Lileottyonood	
Rank	GHG Reductio n Opportuni ties	Practice &	Sub- category Practice	Technical Considerations	Energy or Environmental Considerations	Economic Considerations
		ness Instrume	Fuel	GC currently used for fuel	BACT Monitoring - Fuel carbon	Correlation with density may be
		n-tation	Compositio n Analyses	gas composition	content metric	used as backup  Data available
		< 1%	Fuel Temperatu	Currently used on fuel gas	GHG Inventory Basis	for meter compensation
			re Fuel	Currently used	GHG Inventory	within DCS.
			Pressure	on fuel gas	Basis	Restriction Orifice's sizing
			Fuel	Currently used	GHG Inventory Basis	and flow
			Density	on fuel gas	Dasis	calibration basis
						must be revisited for
						post-revamp
						fuels
			Fuel	None.	GHG Inventory	Separate calorimeter
			Calorimete	Į.	Basis	redundant to
			r			GC data used to
						derive heating
						values. Unnecessary
						costs for
						operation and
						maintenenance.  Data available
			Fuel Flow	Restriction	GHG Inventory Basis	for meter
				Orifice with differential	Dasis	compensation
				pressure	Flow bias impact	s within DCS.
				monitoring	emission	Orifice plate sizing and
				currently used.	inventory. Note that flow meterin	
				Orifice plate's sizing and flow	is not in heater	monitoring
				calibration bas	is control loop.	instruments' calibration bein
				must be	_	addressed as
				appropriate for base case fuel		units are
				conditions and		revamped or
				properly		replaced by ne

		Table 5-2:	Ranking of G	HG Control Option	S Ellective less	
Rank	GHG Reductio n Opportuni ties	Practice & % Control Effective ness	Sub- category Practice	Technical Considerations	Energy or Environmental Considerations	Economic Considerations
		11033		compensated for other		metering skids
			Heater	conditions  CO currently indicated via non-specific Infrared type Combustibles analyzer extracting sample at arch location.  Single point extractive system problematic if not in representative location.	Indication of fired source performance.  Calibration of process instrumentation is less rigorous than for CEMS instruments.	Cost of specific compound analyzers. heater sample point monitoring location may be conducted via field testing and/or by CFD modeling to check gas mixing.
			Stack Temperatu re	None. Currently used	BACT Monitoring Parameter	None
			Monitoring Stack CO Monitoring	None.	with burner performance.	Instrumentation Costs
			Stack O2 Monitoring	None.	Scope associated with burner performance and CO2 CEMS concentration correction.	Costs
			Stack Flow Monitoring	1	In-situ monitoring versus fuel combustion basi Method 19	Calibration &

		Table 5-2:	Ranking of G	HG Control Option	1S Effectiveness	
Rank	GHG Reductio n Opportuni ties	Practice & % Control Effective ness	Sub- category Practice	Technical Considerations	Energy or Environmental Considerations	Economic Considerations Cost of
			CEMS	Direct monitoring versus fuel combustion basis options	Parameter	operation and maintenance
		Advance d Process Control (APC)	Distributed Control System (DCS) Support	Input/Output data handling for archiving and calculations must be programmed properly.	Automation via DCS promotes consistency of data handling tasks, such as flow meter compensation and associated GHG recordkeeping and reporting	Value for APC and draft management combined approach.  Cost of programming and additional signal input and data point storage and upkeep.
		Combus tion Air / Draft Manage	Burner Manageme nt System (BMS)	Automation via DCS requires full instrumentation	Maintains approach to optimum firing performance	Expense may not be justified for energy conservation alone.
		ment < 2%	Damper Controls	Consistent operation – ganged jackshaft design	Tighter control of air to fuel ratio, more stable operations	Cost of mechanical component maintenance Energy and
			Air Prehea	Heat Recovery Dependent upon combustion air mass rate and temperature limits	pressure drops require additional	maintenance costs locked in for source, i.e.,

ir Permit Appl			NIC Central Ontion	s Effectiveness	
	Table 5-2:	Ranking of G	HG Control Option	3 Elloutone	
GHG Reductio n Opportuni ties	Practice & % Control Effective	Sub- category Practice	Technical Considerations	Energy or Environmental Considerations	Economic Considerations
		Draft	hot operating temperatures for application. Fan/blower bearings and lube system require upgrading for higher temperature applications  Natural draft design requires high stack.	provides low operating cost.  Mechanical draft may enable more stable burner operations and flame shape.	Energy, operation and maintenance costs.  Energy savings
		Blower / Fan Driver Variable Speed Drive	Reliability for large voltage and power applications	operating costs if variable loads must be followed	minimized by steady state operations may not cover capital costs
	Combus tion Radiant	Burner & Firebox Sealing &		dependent on burner location	Limited opportunity for application while operating
	Zone Manage ment < 1%		The state of the state of	improvement had minor effect on attaining target tube temperatures, small firing difference	limited economic value
	on	Revise	0.2- 0.5 inches H2O. Licensor	Pressure drop energy costs tradeoff with hea savings	80 \$/ton NACE Value.  tradeoff are
	GHG Reductio n Opportuni	Table 5-2:  GHG Reductio n Opportuni ties  Control Effective ness  Combus tion Radiant Zone Manage ment < 1%  Convection Section Stack /	Table 5-2: Ranking of G Reductio n Opportuni ties  Reflective ness  Mechanical Draft Design  Blower / Fan Driver Variable Speed Drive  Combus tion Radiant Zone Manage ment  Convecti on Manage ment  Convecti on Sealing & Insulation Refractory Coatings  Coils	Table 5-2: Ranking of GHG Control Option  GHG Reductio n Opportuni ties  Mechanical Draft Design  Mechanical Not operating temperatures for application. Fan/blower bearings and lube system require upgrading for higher temperature applications  Natural draft design requires high stack.  Reliability for large voltage and power applications  Natural draft design requires high stack.  Sealing & Insulation  Refractory Coatings  Short term gain: only, ~ 3 months sustained performance  Convecti on Revise Process Coils  Add / Revise Process Coils  Gas side pressure drops 0.2- 0.5 inches Process Coils	Table 5-2: Ranking of GHG Control Options Effectiveness  GHG Reductio n Opportuni ties  Mechanical Draft Design  Mechanical Mechanical Mechanical Mechanical Mechanical Ambient versus hot operating temperatures for application. Fant/blower bearings and lube system require upgrading for higher temperature applications  Natural draft design requires high stack.  Reliability for large voltage and power applications  Natural draft may enable more stable burner operating costs and power applications  Natural draft may enable more stable burner operations and flame shape.  Lower driver operating costs if variable loads must be followed  Impacts during pre- planned furnaco outage.  Refirectory Coatings  Nort term gains only, ~ 3 months sustained performance  Emissivity improvement and minor effect on attaining target tube temperatures, small firing difference Pressure drops on Section / Process Coils  Convecti on Stack / Coils  Considerations  Technical Considerations  Natural draft provides low operating cost.  Mechanical frovides low operating cost.  Mechanical frovides low operating oost.  Mechanical frovides low operating cost.  Mechanical fraft may enable more stable burner operations  Mechanical frovides low operating cost.  Mechanical draft may enable more stable burner operations  Mechanical frovides low operating cost stable burner operations  Shatural draft design requires high stack.  Short term gains only, ~ 3 months sustained performance  Emergy operations  Far/blower operations  Mechanical frovides low operating operating cost starle burner operations  Mechanical frovides low operating operatives for applications  Natural draft design requires high stack.  Mechanical may enable more stable burner operations  Mechanical frame have operations  Shot term gains of fractions  Combus frame have operations  Shot ter

	ir Permit Appl	Table 5-2:	Ranking of G	HG Control Option	s Effectiveness	
Rank	GHG Reductio n Opportuni ties	Practice & % Control Effective	Sub- category Practice	Technical Considerations	Energy or Environmental Considerations	Economic Considerations
	ties -	ness Stack Heat Recover y < 2%	Add / Revise Fuel Preheat	Gas side pressure drops 0.2- 0.5 inches H2O Fuel mass may not	Pressure drop energy costs tradeoff with heat savings	minimal if low pressure drop changes made. Energy costs tradeoff are minimal if low pressure drop changes made.
			Add / Revise Air Preheat Coils or External APH	be large enough to carry significant heat load Gas side pressure drops 0.2- 0.5 inches H2O Combustion air side mechanical design for high pressure drops and temperatures.	Pressure drop energy costs tradeoff with heat savings	Energy costs tradeoff are minimal if low pressure drop changes made.
			Add / Revise Utility Coils	Equipment occupies more space. Gas side pressure drops. Steam / BFW mass	Pressure drop energy costs tradeoff with heat savings Stack ga exhaust at less than 300 °F  Application considered least intrusive to original heater design purpose as economizers	s Energy costs tradeoff are minimal if low pressure drop changes made.

		Table 5-2:	Ranking of Gl	HG Control Option	- Inconvenior	
Rank	GHG Reductio n Opportuni ties	Practice & % Control Effective ness	Sub- category Practice	Technical Considerations	Considerations	Economic Considerations
					convection section	
			Condensin de Heat	Gas side pressure drops. Home for heat recovered.	Pressure drop	Capital and operating costs
					Stack gas exhaust at less than 150 °F Energy costs	
					tradeoff	100 ¢/top
		Steam System Upgrade s ~ 2% attainabl e without	Insulation Study	None. Currently implemented, though seasonal interests per steam balance	None	182 \$/ton NACE Value for Economizers to raise BFW temperature 30- 35 °F to claim 2% Fuel efficiency improvement
		significa nt seconda ry impacts	Steam Trap Program	None. Recovery currently implemented across site.	Steam traps are properly sized and condensate substantially recovered	None
			Condensat e Recovery			Some flows are too small for economic recovery such as DPG
			Boiler Feed Water Pumps Driver Variable	Reliability for large voltage and power applications	Less impact expected with consistent near design operations such as ethylene plant	Energy, operation and maintenance costs not significantly reduced

	<u> </u>	Table 5-2:	Ranking of G	HG Control Option	is Effectiveness	
Rank	GHG Reductio n Opportuni ties	Practice & % Control Effective ness	Sub- category Practice	Technical Considerations	Energy or Environmental Considerations	Economic Considerations
5	Maintena	Preventi ve Mainten ance <1%	direct let- down between steam levels  Minimize Venting	i	None  Cost of lost LP steam minimal  None  None  None	None  Cost of lost LP steam recovery uneconomic.  36 \$/ton NACE Value for site-wide PM approach of monitoring for problems and instrument calibration  Labor cost  Labor cost  Labor / vendor supplier costs

#### **Evaluate the Most Effective Controls**

CCS is the top ranked means of GHG control on the basis of percent pollutant removed, however its technical considerations, energy usage, and economic impacts are significant obstacles to its application. Assuring the reliability of the VCC process heaters and boiler and the Hydrogen plant Pyrolysis furnaces, which operate at small differences from atmospheric pressure (inches of water gauge) is essential and they must be protected from being tripped by pressure surges for safety and overall plant production assurance.

It is noted that the energy-intensive Carbon Removal System (CRS) process of flue gas treatment requires significant new utilities to be constructed to sustain its operation. A new large cooling tower much larger than the DCH Facility's presently scoped tower would require additional makeup water supply and would be a contributing source of particulate matter and other regulated pollutants to the site emissions inventory. Additionally in an "all electric" driver case, high continuous electrical load would be created, estimated at multiples of the present electrical load expected at the Riverview site.

While there are potential areas of cost reduction or energy efficiency for the Base Case CRS, these are not seen as driving cost effectiveness to approach the EPA's 60-90 \$/ton threshold range of acceptable cost.

CCS cannot currently be justified as present day BACT and should be eliminated from further consideration.

The second ranked control option, Green Chemistry, is seen to have significant future control potential, especially if flue gas may be handled and CO2 recovered from it or utilized at near atmospheric pressures, eliminating the most costly and energy intensive unit operations from CCS systems. Emerging technologies such as algae based bio-fuels, direct catalytic synthesis of acetic acid from CH4 and CO2 at low temperatures, and membrane bioreactor production of acetic acid from CO2 and H2, e.g., using BR-446 (genus Acetobacterium) will be of continuing interest in developing relevant CO2 sinks. It is noted that CO2 use in "green chemistry" applications such as producing bio-fuels may be considered temporary sequestration as the carbon content will be released upon fuel usage. As with all emerging technology, these options are severely constrained in moving from research to pilot, to demonstration, and to full scale application due to a combination of current day technical and economic factors. Green Chemistry cannot be justified as present day BACT and should be eliminated from further consideration.

The third ranked option, use of low carbon content fuel is currently used at the site given use of utility natural gas supply.

The remaining control measures identified generically as energy efficiency, and maintenance, yield much lower GHG reductions than end-of-pipe or source controls. Though these options are far less energy-intensive and a very small fraction of the cost of CCS, they must be addressed in a coordinated manner so as not to create internal conflicts. To the degree that they can be integrated, they would be considered practical BACT which could be adopted or incorporated in any new fired eqiupment designs. As such, an evaluation of their energy, environmental, and economic impacts of the proposed measures is not deemed necessary for an application. These options will approach if not come in under the EPA's 60-90 \$/ton threshold of acceptable cost for GHG control, and are considered best applied on a site-wide basis.

The use of low carbon content natural gas fuel and the adoption of integrated control measures identified generically as energy efficiency, and maintenance would be considered practical BACT for the Riverview DCH Project.

#### **General Measures**

Systems to monitor and track the performance of critical equipment and processes in the plant can help optimize plant operation. Using process information management systems, scientific research on the behavior of any type of machinery and equipment can be efficiently conducted, as could energy efficiency studies and other critical industrial cost saving measures such as predictive maintenance.

Scheduled preventive maintenance and rotation of redundant equipment helps minimize equipment downtime and optimize process operation. Training programs and good housekeeping programs help decrease energy consumption throughout the plant.

General measures for energy efficiency optimization, like using a process information management system, scheduled preventive maintenance, and training programs are all feasible options for the proposed Riverview Energy facility.

#### **Summary of Energy Efficiency Measures**

The energy efficiency measures that were identified to be technically feasible include energy efficient equipment design, coal moisture control, and other general measures discussed above. Additionally, a process information management system will be integrated into plant operations to monitor and track equipment performance, production, and power consumption, as well as to predict and schedule preventive maintenance on critical equipment. A process information system tracks the

performance of critical equipment and processes in the plant to help optimize plant operation.

#### CO2 Transportation and Sequestration

No matter which CO2 capture technology is used, to take credit for the reduced CO2 emissions, the captured CO2 must either be reused (onsite or sold) or liquefied, transported, and "permanently" stored. Pipelines are the most common method of transporting large amounts of CO2 over long distances. The CO2 must be compressed to very high pressures for pipeline transportation, which requires considerable energy consumption. Water must also be eliminated from CO2 pipeline systems to avoid the formation of carbonic acid, which is extremely corrosive to carbon steel pipe. In addition to compressors at the source, booster compressors may be needed along the length of the pipeline. The pipelines must also be monitored for leaks and overpressure to avoid release of the captured CO2.

The oldest long-distance CO2 pipeline in the United States is the 225 km Canyon Reef Carriers Pipeline (in Texas), which began service in 1972 for enhanced oil recovery in regional oil fields (Parfomak and Folger 2007). Thirteen other large CO2 pipelines constructed since then, mostly in the Western United States, have expanded the CO2 pipeline network for enhanced oil recovery. Many smaller CO2 pipelines connect sources with specific customers. However, there are no existing CO2 pipelines within 500 miles of the planned Riverview Energy facility.

DOE is currently exploring several CO2 storage options in the United States. These include storage in geological formations like exhausted oil and gas fields and saline formations, liquid storage under the ocean, solid storage in the form of solid carbonates, and terrestrial sequestration. Of these options, geologic storage, particularly saline formations, offers the most potential for CO2 storage. Globally, only four commercial CCS facilities are sequestering captured CO2 into deep geologic formations and applying a suite of technologies to monitor and verify that the CO2 remains sequestered (DOE 2010b).

While projects to transport and store CO2 are starting to be funded and developed, transportation and storage of CO2 from the Riverview Energy plant is not feasible in the near future due to the lack of adequate CO2 pipeline and storage infrastructure.

#### **Summary of Carbon Capture and Sequestration Options**

Pre-combustion capture and oxy-combustion are not technically feasible for this application. Of the available technologies presented above for the post-combustion capture of CO2, only solvent-based capture processes have been used commercially.

All the other technologies require either high CO2 concentration or high partial pressures. Currently, several solvent-based capture processes are available for lower capacity industrial level applications, but they have not yet been demonstrated at the scale required for the purposes of GHG emissions mitigation at a typical power plant or commercial facility. Consequently, there is considerable uncertainty associated with capacities at volumes necessary for commercial deployment. Many projects are in the planning stages for demonstration scale-up, including the Alstom chilled ammonia process and several amine-based processes [e.g., Fluor (Econamine), ABB/Lummus, Mitsubishi Heavy Industries, HTC Purenergy, Aker Clean Carbon, Cansolv et al.] (Simmonds et al. 2002). In addition, a variety of processes employing solvents, sorbents, and membranes are at varying stages of development.

The key technical challenges for CCS are summarized below:

- Energy Impact: A significant amount of auxiliary power is required to operate currently available CO2 capture technologies. A large quantity of energy is required to regenerate the solvent in commercially available CO2 capture technologies (approximately 1,550-3,000 Btu/lb of CO2 removed). To enable storage, significant power is required to compress the captured CO2 to typical pipeline levels (1,500-2,200 psia depending on storage scheme and location).
- Environmental Impact: Although CCS offers environmental benefits by reducing GHG emissions, it does not minimize emissions without other impacts to the environment.
- For an absorption-based CO2 capture process, which is the prevalent commercially available CO2 capture technology, the solvent can enter the environment through four pathways, which include entrainment in the treated gas, reclaimer waste, fugitive emissions, and accidental release.
- Flue Gas Contaminants: Constituents in the flue gas, particularly sulfur, can contaminate CO2 capture technologies, leading to increased operational expenses.
- Water Use: A significant amount of water use is required for CO2 capture and compression cooling.
- Transportation and Storage: Transporting captured CO2 in relatively limited quantities is possible by truck, rail, and ship, but moving large quantities of CO2 requires a dedicated pipeline network. There are very few existing CO2 pipelines in the United States and none within 500 miles of the proposed facility. Largescale CO2 storage projects associated with enhanced oil recovery are currently in operation in the United States, but CO2 storage in geologic formations has not been demonstrated on a commercial scale.

Cost Effectiveness: Recent studies conducted by the National Energy Technology Laboratory (NETL) show that current technologies are expensive and energy intensive. DOE-funded studies conducted by NETL estimate the typical cost of CCS in coal-fired power plants to range from \$50 to \$75/ton of CO2 avoided depending on technology. Cost estimates for Integrated Gasification Combined Cycle plants ranged from \$35 to \$46/ton of CO2 avoided (DOE 2008). The Interagency Task Force on CCS, established in 2010, reports CO2 capture costs of \$55-\$104/ton of CO2 avoided (Simmonds et al. 2002) for power plants. A more recent analysis of the techno-economic data for CO2 capture from power generation by the IEA, based on estimates published over the last 5 years in major engineering studies for about 50 CO2 capture installations at power plants, found that CO2 capture costs ranged from \$36 to \$116/ton of CO2 avoided (IEA 2011). However, these costs cover only capture and compression but not transportation and storage. While the transportation and storage cost is often cited at the flat figure of \$4-\$9/ton CO2 removed, studies conducted by the NETL on estimating CO2 transport, storage, and monitoring costs indicated that this is only true for pipeline lengths of less than 100 miles (DOE 2010a). Their studies showed that T&S avoided costs increase almost linearly with pipeline length and can range from \$10 to \$65/ton of CO2 avoided (in 2007\$) for pipeline lengths of 100-500 miles.

For these reasons, existing CO2 capture technologies and CO2 pipeline and storage infrastructure in the United States will need be improved before CCS becomes a viable option. In addition, the substantial energy required to pump CO2 for a long distance will result in substantial criteria pollutant emissions, which have a much more substantial and direct effect upon health and welfare than the CO2.

#### 5E. Sulfur Dioxide

Sulfur dioxide (SO2) emissions from the VCC are predominantly from the Sulfur Recovery Plant Tail Gas Treatment Unit (TGTU) and the Sulfur Block Flare. The emissions from the TGTU are for a generic Claus unit with 95% SO2 reduction, which is consistent with the NSPS emission limit for sulfur oxides enumerated for oil refineries at 40 CFR 60.104(2)(i) of 250ppm @ 0% excess air for an SO2 emissions concentration leaving a refinery sulfur recovery unit. However, it appears that a sulfur recovery level of 99.8% for the Riverview fuel conversion plant is achievable and would reflect BACT per TCEQ reference. This has been calculated as equivalent to ~150 ppm SO2

emission concentration and has been used as the BACT-level performance benchmark to inventory the TGTU emissions for this permit application.

As with all of the other flares at this facility (except as noted above) the Sulfur Block Flare is in place as a safety device that operates during process upset conditions (except for the pilot, which is continuously operating). There is no SO2 control equipment that can be used to achieve the dual goals of safety and emissions reduction that is more effective. Flaring is BACT for SO2 emission control in this application.

#### 5F. Volatile Organic Compounds

There are three primary sources of volatile organic compound (VOC) emissions at the Applicant's facility: fugitive emissions leaks, the hydrogen reformers, and the hydrogen deaerators. The hydrogen reformers and deaerators are both part of the hydrogen plant, which consists of twin process trains that are identically equipped. These three primary VOC sources are addressed below.

#### Fugitive Emission Leaks

The overwhelmingly predominant source of volatile organic compound emissions at this facility will be fugitive emission leaks from pumps, valves, flanges, seals and the other equipment. Both federal and state guidance establish that control of these leaks is best attained with a Leak Detection and Repair (LDAR) program. However, LDAR programs differ greatly in their depth and scope, since they are frequently used either to control HAP emissions to a MACT level or VOC emissions to a BACT (or LAER) level. In addition, different industrial categories have their own unique requirements (i.e., 40 CFR Subpart VVa, etc.) for LDAR. Since this facility is not in any of the industrial categories addressed by these standards, a general approach has been employed using TCEQ references.

The generation of a BACT-level program to address leaks has been simplified by a guidance document that was generated by the Texas Council Environmental Conservation (TCEQ) entitled, "Air Permit Guidance for Chemical Sources: Equipment Leak Fugitives". This guidance, expands upon the information provided in USEPA's "Protocol for Equipment Leak Emissions Estimates" (EPA 453/R-95-017, November 1995) and "Preferred and Alternate Methods for Estimating Fugitive Emissions from Equipment Leaks" (STAPPA/ALAPCO/EPA, November 1996) have been used to define and quantify the emissions reductions from a BACT-level LDAR program. None of the streams associated with the operations of this facility are known to qualify for any NESHAP-related LDAR program, so only NSPS criteria must be addressed. Further,

this location is in NAAQS attainment status for ozone, so LAER is not required. Thus, a 10,000 ppm VOC threshold is the BACT criterion that is the basis of the LDAR program.

KBR has estimated the total number of fittings, valves and other items that will be present at the facility utilizing factored counts from representative process flow diagrams for the VCC configuration. These estimates are provided on attachments. Emission reductions for the proposed level of LDAR program are based upon these component estimates. The emission reductions that result from this approach have been identified for each equipment category and are accounted in the facility emission summaries in this permit application. These reductions are consistent with the aforementioned guidance document information.

#### Hydrogen Plant Sources

This hydrogen plant is similar in all respects to the hydrogen plants used at refineries to produce ultra-low sulfur diesel (ULSD) fuel. Both the hydrogen reformers and the hydrogen deaerators emit VOC. A comprehensive review of the USEPA's RACT/BACT/LAER Clearinghouse (RBLC) for both hydrogen reformers and deaerators produced very limited results. These results indicate that the current BACT level of control for VOC emissions from these sources is as follows:

Hydrogen Reformer Furnace Vent Stacks: Proper design, operation and good engineering practices

Deaerators: None

Riverview Energy proposes proper design, operation and good engineering practices for the hydrogen reformer and for the deaerator as BACT for these sources. Proper operation will be defined as adherence to manufacturer's published operating and maintenance requirements.

#### 5G. Carbon Monoxide

CO primarily results from incomplete combustion, except in cases where a noncombustion chemical reaction occurs. All of the CO emissions from the flare pilots and VCC plant equipment are due to combustion. The hydrogen reformers generate approximately two-thirds of the total CO emission footprint for this facility because CO is a byproduct of the reformer process chemistry and of combustion. The VCC plant CO emissions all result from combustion.

There is no control equipment to address CO from combustion. The accepted BACT-level approach is to optimize combustion efficiency, since combustion-generated CO is the result of incomplete combustion. Combustion efficiency will be optimized by utilizing state-of-the-art automated combustion systems in conjunction with the ULNBs that have previously been described, good engineering practice and manufacturer-specified maintenance. This approach is consistent with the most stringent RBLC determinations that were identified for similar equipment.

#### 5H. Summary of BACT Determination

A summary table compilation of the BACT determinations that have been described in this section has been included as Table 5-3, below. It addresses all of the determination categories, with the exception of particulate matter (PM), since PM was tabulated individually due to its complexity.

Table 5-3: Summary of BACT Determinations

Pollutant	Emission Unit	Control Options	BACT Selection
\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\		Flue gas recirculation	ULNB
NOx	All VCC units in Note 1	Staged combustion	
		Low-NOx burners (LNB)	
		Ultra-low NOx burners (ULNB)	
		Selective non-catalytic combustion	
		Hot-side SCR	
		Tail-end SCR	
		As above for VCC units	ULNB, See Note 2
	Hydrogen reformer	AS above for yee arms	
Greenhouse	Plantwide	Energy efficiency	Energy efficiency
Gases	Plantwide	Carbon sequestration	
	Tail gas treatment unit	flaring (Note 3)	Flare
502	Fugitive Emission Leaks	leak detection and repair (LDAR)	LDAR (Note 4)
VOC	Hydrogen reformer	SCR (described previously)	All listed
	LIAGIOSEILICIONIS	good operating practice	***
		good engineering practice	
		proper design	***************************************
CO	All VCC units in Note 1	automated combustion systems	All listed
CO	, and the same of		(optimze comb.
		ULNB	eff.)
		Good engineering practice	-
		Manufacturer-specified maintenance	All listed for VCC
•	All flare pilots	As above for VCC units	All listed for VCC
	Hydrogen reformer	As above for VCC units	Mi librea io.
PM		All PM emissions are separately tabulate	d

<sup>1)</sup> Package boiler, coal drying heater, feed heater, treat gas heater, fractionator feed heater, vacuum NOTES:

<sup>2)</sup> The hydrogen reformer will have SCR that controls other criteria pollutants and SCR will also reduce NOx.

<sup>3)</sup> Flare control was selected because it is the most effective control approach

<sup>4)</sup> Various LDAR program levels are in the regulations. The one chosen was for BACT from NSPS.

#### 6. Modeling Results Summary

An air dispersion modeling analysis was conducted as part of this air permit application to predict ambient concentrations of criteria pollutants and hazardous air pollutants, as well as address potential visibility impacts resulting from the proposed DCH facility. Details of the modeling are presented in the attached modeling report and protocol. and the quantitative modeling results for criteria pollutants is provided in the report's Table 2-1, presented below as Table 6-1.

In regard to de-minimus or significant impact level (SIL) screening values, the following results are noted:

- All modeled annual impacts are below the applicable SIL values, i.e., those forNO2, SO2, and PM2.5
- The modeled 24-hr impacts for SO2 and PM10 are below their applicable SIL values, while only PM2.5 exceeded its 24-hr SIL value.
- The modeled 8-hr impacts for CO are below its applicable SIL value.
- The modeled 3-hr impacts for SO2 are below its applicable SIL value.
- The modeled 1-hr impacts for CO is below its applicable SIL value, while those for NO2 and SO2 exceeded their applicable SIL values.

Given that impacts below SIL values are the basis for no further analysis or assessment, only short term impacts from 24-hr PM2.5 and 1-hour impacts from NO2 and SO2 emissions are required by IDEM guidance to be further addressed. First, the significant impact area (SIA) was determined for each pollutant. The SIA was then used to determine the necessity of acquiring and modeling regional non-project, off-site emission sources not represented by the background air quality data.

As modeling results show, the distances and directions to significant impacts are very proximate to the Riverview property fence line, especially for the impacts associated with PM2.5. Given these very short distances to the SIA's and the isolation of the proposed DCH project sources relative to other regional emission sources, the likelihood of overlapping and cumulative impacts from any regional sources is highly unlikely. Therefore, no additional modeling of off-site source inventory is considered necessary.

In regard to modeled project impacts versus National Ambient Air Quality Standards (NAAQS) plus background concentrations, all results were well within the NAAQS. Additionally, consumption of PSD Class II Increments ranged from only 2-15%.

In regard to screening for potential toxicological impacts, see the modeling report's Attachment O, presented below as Table 6-2 following IDEM guidance which shows no expected impacts.

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In regard to screening for visibility impacts, emissions were modeled following EPA guidance with their VISCREEN software and showed no expected impacts.

The modeling analyses for criteria pollutants, hazardous air pollutants, and visibility impacts are found to support a finding of minimal impact from the proposed DCH facility emissions on local air quality.

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				trong Daniel	Tahle 2-1:	Table 6-1  Table 2-1: Summary of Modeling Results	Modeling Rest	ults			
			) JOIMI)	nellug vehor		pundand	Modeled +	NAAQS	Estimated	PSD	Modeled
Pollutant	Averaging Period	Rank	Modeled Ground- level Conc.	Significant Impact Level (SIL)	Modeled vs SIL	Conc. (µg/m3)	Background Impact	(hg/m3)	Impact vs NAAQS	Class II Increment (µg/m3)	Increment
			(µg/m3)	(hg/m3)		00	17.60	100	17.6%	25	3%
0.1	le lica A	THE	0.6990	_	%6.69	16.9	00.7	2 '	L	1	
NO <sub>2</sub>	Ailliagi 4 br	표 도 도	19.3073	7.5	257.4%	1000	85.23	188.6	45.2%	l.	1
		표	11.2806	,	, , ,	73.80	4 71	80	2.9%	20	3%
Ç	le i da A	三	0.5107	-	51.1%	7.4		1	•	1	- 30
00°	1-hr	HIH	14.8503	7.8	190.4%	53.7	64.21	196.2	32.7%	91	0/.71
	-	H4H	10.5071	1	,00,00	00:		1	ŧ	1 1	,00
	3-hr	HIH	9.8166	25	39.3%	37.7	46.87	1300	3.6%	512	0,7
	:	H2H	9.1701	1	70 00/	5	E	1	1		1
	24-hr	HIH	3.8977	5	0.0%	16.3	19.76	362	5.4%		ì
	i I	H2H	3.4629	1 0	, OE 40/	9.5	9.76	12	81.3%	4	0/,0
MO	Annual	보도	0.2562	0.3	440 00/	2	-	ı	•	- (	460/
IVI2.5	24-hr	HH	1.4252	1.2	110.070		•	1	-	S	0/07
		H2H	1.3683	ı	-	20	23.13	35	66.1%	,	E .
		표 표	1.1252	1		777			•	1	i
740	24-hr	포포	1.7812	5	35.6%	22.7	35.12	150	23.4%	30	%9
F 1410	-	H9H	1.4234	L	1	33.1	,	-	-	•	-
9	4-br	工工	20.9654	2000	1.0%	0 3000	3416 03	40000	8.5%	1	E.
3	<u> </u>	12. 12.	19.2304	1	L	0.0866	2 1		1	1	1
	8-hr	HH	13.4179	200	2.7%	2000 B	2035.20	10000	20.4%	,	*
	:	HZH	12.3979	-	-	2022.0					

Riverview Energy Corporation Air Permit Application

(MC	deling Re	(Modeling Report Attachment O	ment O - T	oxicologica	al Screening	g Analysis	for HAPS,	- Toxicological Screening Analysis for HAPs, Hydrogen Sunds and Control Chronic			
		Acute	83	     							Target
Pollutant	CAS	Modeled 24-Hour	24-hour MRL	Modeled Annual Conc	Cancer URF,	Source	Cancer Risk	Non-Cancer Chronic RfC, ug/m3	Source of IDEM RfC	Hazard Quotient (HQ)	Organs / Inhalation Critical
		(mg/m3)	(ng/m3)	(ng/m3)	(2006)			00 0000	Sidi	6.57E-05	
		0.0057		1.31				20000.00	214		Neurological
Methanol	67561	1067.8		0.40				700.00	IRIS	2.15E-04	(PNS)
Hexane	110543	1.2214	2100	61.0			4 OSE OR	9.80	ATSDR	8.34E-05	Respiratory system
Formaldehyde	20000	0.0055	49	0.0008	1.3E-05	<u>자</u>	200.1			30 230 0	Neurological
	40883	1 2379	3700	0.15				2000.00	IRIS	3.05E-03	(CNS)
Toluene	200001				7 95 08	IRIS	4.44E-07	30.00	IRIS	1.90E-03	Carcinogen
Benzene	71432	0.4621	160	9 0.0 0	7.0E-00				C	1 14E-04	Inhalation
				2000 05	2 4F-04	IRIS	5.49E-09	0.20	AISDR	1	Carcinogen
Nickel	7440020	0.0002	1	2.285-03						4 OCE 03	Pulmonary, Resniratory
	1444	44 7805	1200	1.86				100.00	<u> </u>	1.00.1 1.00.1	system
Ammonia	/00441/							2.00	IRIS	1.69E-02	Nasal
חסט	7783064	0.2594	280	0.03						20 740	Neurological
070		_	0007	0 10				100.00	RIS	1.91E-US	(CNS)
Xylenes	1330207	1.5515	4300	6.2						4 02E-05	Respiratory system. Liver,
lo no 10	108952	0.0165		0.002				200.00	CAL	20.1	Kidneys
Presso								175.00	Region 9	2.32E-05	
o-Cresol (2-	95487	0.0330		0.004					1	3 39E-06	
Methylphenol)	10000	0.0465		0.002				000.00	TA L	-	
m-, p-Cresols	1318/13	4			Cumulative Cancer Risk =	ancer Risk	= 4.60E-07		Total Hazard Index (HI)	11	
					Cumulance metric =	anco metric	= < 1E-06			< 1	
			•		Прем сошри	allee memo	4				

RESERVED PAGE

January 25, 2018

Attachment A. IDEM Air Permit Application Forms



#### AIR PERMIT APPLICATION COVER SHEET

State Form 50639 (R4 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM – Office of Air Quality – Permits Branch
100 N. Senate Avenue, MC 61-53 Room 1003
Indianapolis, IN 46204-2251
Telephone: (317) 233-0178 or
Toll Free: 1-800-451-6027 x30178 (within Indiana)
Facsimile Number: (317) 232-6749
www.lN.gov/idem

NOTES:

- The purpose of this cover sheet is to obtain the core information needed to
  process the air permit application. This cover sheet is required for <u>all</u> air
  permit applications submitted to IDEM, OAQ. Place this cover sheet on
  top of all subsequent forms and attachments that encompass your air
  permit application packet.
- Submit the completed air permit application packet, including all forms and attachments, to IDEM Air Permits Administration using the address in the upper right hand corner of this page.
- IDEM will send a bill to collect the filing fee and any other applicable fees.
- Detailed instructions for this form are available on the Air Permit Application Forms website.

	FOR OFFICE USE ONLY
PERMIT N	MBER:
DATE AP	LICATION WAS RECEIVED:
	State of Indiana
	JAN 25 2018 JB

Dept or Environmetal Management

1.	Tax ID Number:

	e plant site as a whole and NC  Name: Riverview Energy Corpor		3. Plant ID: —
Source / Company	15 E Putnam Ave, Suite#		
Billing Address:	15 E Puthani Ave, Outer	State: CT	<b>ZIP Code:</b> 06830 –
City: Greenwich Permit Level:	☐ Exemption ☐ Registration	□ SSOA □ MSOP	☐ FESOP ☐ TVOP ☐ PBR
Application Summ choices selected be Initial Permit Review Request	<ul><li>☐ Renewal of Operating F</li><li>☐ Revocation of Operating</li><li>☐ Relocation of Portable S</li></ul>	Permit	Asphalt General Permit Alternate Emission Factor Request Acid Deposition (Phase II)
Site Closure	☐ Emission Reduction Cr	edit Registry	То:
☐ Transition (betw	een permit levels) From:  mendment: Company Name  Correction to No	Change n-Technical Information	☐ Change of Responsible Officia☐ Notice Only Change
☐ Modification:	☐ New Emission Unit or Control Dev ☐ New Applicable Permit Requireme ☐ Prevention of Significant Deteriora	nt Change to Applica	n Unit or Control Device ability of a Permit Requirement ☐ MACT Preconstruction Revie

			PART B: Pre-Application Meeting
art B specif	ies whether	a meetir	ng was held or is being requested to discuss the permit application.
Was a mee	eting held betwe	een the co	ompany and IDEM prior to submitting this application to discuss the details of the
	⊠ Yes:	Date:	10/25/2017
). Would you project?	like to schedul	e a meeti	ng with IDEM management and your permit writer to discuss the details of this
⊠ No	☐ Yes:	Propos	sed Date for Meeting:
			To O Calcutial Business Information
		PAR	T C: Confidential Business Information
art C ident	ifies permit a is kept separ	ipplication ate fron	ons that require special care to ensure that confidential business in the public file.
et out in the l	indiana Adminis	strative Co	e at the time the information is submitted to IDEM, and must follow the requirements ode (IAC). To ensure that your information remains confidential, refer to the IDEM, of confidential business information. For more information on confidentiality for please review IDEM's Nonrule Policy Document Air-031-NPD regarding Emission
)ata		医抗血性多点的	
)ata		医抗血性多点的	
Data. <b>11. I</b> s any o	f the informa	tion con	tained within this application being claimed as Confidential
Data 11.Is any o Busines	f the information	tion con	
Data. <b>11. I</b> s any o	f the informa	tion con	
Data 11.Is any o Busines	f the information	tion con	
Data 11. Is any o Busines \times No	f the information of the informa	tion con	tained within this application being claimed as Confidential
Data.  11. Is any or Busines  No  Part D is the	f the information of the informa	tion con on?  D: Cer tification	tained within this application being claimed as Confidential  tification Of Truth, Accuracy, and Completeness that the information contained within the air permit application packet that we receive without a signe
Data.  11. Is any or Busines  No  Part D is the is truthful, a certification defined in 32	PART  e official cert  accurate, and will be deer  Operating Per 6 IAC 2-7-1(34)	tion con on?  D: Cer tification d comple med inco mit (TVO) ) must ce	tification Of Truth, Accuracy, and Completeness I that the information contained within the air permit application packet. Any air permit application packet that we receive without a signer complete and may result in denial of the permit.  P) or a Source Specific Operating Agreement (SSOA), a "responsible official" as rifly the air permit application. For all other applicants, this person is an "authorized"
Part D is the is truthful, a certification.  For a Part 70 defined in 32 Individual" as	PART  e official cert accurate, and will be deer Operating Per 6 IAC 2-7-1(34) defined in 326	tion con on?  D: Certification d completed incompleted	tification Of Truth, Accuracy, and Completeness I that the information contained within the air permit application packet. Any air permit application packet that we receive without a signe complete and may result in denial of the permit.  P) or a Source Specific Operating Agreement (SSOA), a "responsible official" as rifly the air permit application. For all other applicants, this person is an "authorized"
Part D is the is truthful, a certification.  For a Part 70 defined in 32 Individual" as state.	PART	tion con on?  D: Certification d completed incompleted	tification Of Truth, Accuracy, and Completeness I that the information contained within the air permit application packed I that the information contained within the air permit application packed I that the information contained within the air permit application packed I that the information permit application packed that we receive without a signed I that the information permit application packed that we receive without a signed I that the information packed that we
Part D is the is truthful, a certification.  For a Part 70 defined in 32 Individual" as state.  Gregory Merent State.	PART  PART  The official cert  accurate, and a will be deer  Operating Per  For Inc. 100 (100)  For Inc. 100  For Inc.	tion con on?  D: Certification d completed incompleted	tification Of Truth, Accuracy, and Completeness I that the information contained within the air permit application packet. Any air permit application packet that we receive without a signe amplete and may result in denial of the permit.  P) or a Source Specific Operating Agreement (SSOA), a "responsible official" as rtify the air permit application. For all other applicants, this person is an "authorized 1-1(1).
Part D is the is truthful, a certification.  For a Part 70 defined in 32 Individual" as state.	PART  PART  The official cert  accurate, and a will be deer  Operating Per  For Inc. 100 (100)  For Inc. 100  For Inc.	tion con on?  D: Certification d completed incompleted	rtification Of Truth, Accuracy, and Completeness In that the information contained within the air permit application packet Interest and may result in denial of the permit.  P) or a Source Specific Operating Agreement (SSOA), a "responsible official" as riffy the air permit application. For all other applicants, this person is an "authorized 1-1(1).  The word of the permit application and belief formed after reasonable inquiry, the proposition of the permit application are true, accurate, and complete.  President Title
Data.  11. Is any or Busines  No  Part D is the istruthful, a certification  For a Part 70 defined in 32 Individual" as I certification  Gregory Mere	PART  PART  The official cert  accurate, and a will be deer  Operating Per  For Inc. 100 (100)  For Inc. 100  For Inc.	tion con on?  D: Certification d completed incompleted	tification Of Truth, Accuracy, and Completeness I that the information contained within the air permit application packet. Any air permit application packet that we receive without a signer complete and may result in denial of the permit.  P) or a Source Specific Operating Agreement (SSOA), a "responsible official" as riffy the air permit application. For all other applicants, this person is an "authorized 1-1(1).  The word that, based on information and belief formed after reasonable inquiry, the proposal contained in this application are true, accurate, and complete.  President

# Continued on Next Page

# JAQ AIR PERMIT APPLICATION — FORMS CHECKLIST state Form 51607 (R5 / 1-10) INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM – Office of Air Quality – Pe Branch 100 N. Senate Avenue, MC 61-53 Noom 1003 Indianapolis, IN 46204-2251

Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749

www.IN.gov/idem

NOTES:

Check the appropriate box indicating whether each application form is applicable for the current permit application. The source must submit only those forms pertinent to the current The purpose of this checklist is to help the applicant and IDEM, OAQ ensure that the air permit application packet is administratively complete. This checklist is a required form.

Place this checklist between the cover sheet and all subsequent forms and attachments that encompass your air permit application packet.

Air Permit Application

Indiana Department of Environmental Management Office of Air © 4ity State Form £ 7 (R5 / 1-10) Ap

		Part	Part B: Process Information	ormation
Applicable?	Form ID	Title of Form	State Form	When should this form be included in my application packer?
			51860	Submit if you are requesting to use an emission factor other than AP-42.
N⊠ Y□	AEF-01	Alternate Emission Factor Request	20010	Include one form for each process for which there is not a specific PI form.
Z  X	PI-01	Miscellaneous Processes	52534	Include of the form of the second of the sec
	PI-02A	Combustion Unit Summary	52535	Include one form to suffillialize all colleges or filmace (Indexs SSOA).
	PI-02B	Combustion: Boilers, Process Heaters, & Furnaces	52536	Include one form for each boiler, process fleater, or unitace (unless
Z A	PI-02C	Combustion: Turbines & Internal Combustion Engines	52537	Include one form for each turbille of internal companies. SSOA).
N N	PI-02D	Combustion: Incinerators & Combustors	52538	Include one form for each incinerator or combustor (unless 5000).
>	PI-02F	Combustion: Kilns	52539	Include one form for each kiln (unless SSUA).
	PI-02F	Combustion: Fuel Use	52540	Include one form for each combustion unit (unless SSOA).
	PI-02G	Combustion: Emission Factors	52541	Include one form for each compustion unit (unless SSOA).
N □ X	PI-02H	Combustion: Federal Rule Applicability	52542	Include one form of cash commercials.
>	PI-03	Storage and Handling of Bulk Material	52543	Include if the process involves the storage and training of
	-	Asphalt Plants	52544	Include for each asphalt plant process (unless general portion)
z z 3 2 - >		Brick / Clay Products	52545	Include for each brick and/or clay products process.
	_	Electroplating Operations	52546	Include for each electroplating process.
	-	Welding Operations	52547	Include for each welding process.
		Concrete Batchers	52548	Include for each concrete batcher (unless SSOA)
		Degreasing	52549	Include for each degreasing process (united Secry):
1	I PI-10	Dry Cleaners	52550	Include for each dry dreaming process
N N D	I PI-11	Foundry Operations	52551	Include for each orain elevator (unless SSOA).
N 🛛		Grain Elevators	52553	Include for each lime manufacturing process.
ļ		Linit Organic Compound Storage	52554 (doc)	-
z z	PI-14	-	52555 (xls)	
1		Pod	52556	Include for each Portland cement manufacturing process.
1		Reinforced Plastics & Composites	52557	Include for each reinforced plastics and composites process.
<u>×</u> ≻	임		Continued on Next Page	Next Page

Page 3 of 6 

Indiana Department of Environmental Management

Include for each woodworking or plastic machining process (unless SSOA). Include for each surface coating or printing process (unless SSOA). Include if the process involves mineral processing (unless SSOA). When should this form be included in my application packet? Include for each blasting process (unless SSOA) Include for each soil remediation process. Include for each ethanol plant. Part B: Process Information State Form 52560 52570 52558 None Number 52559 52561 Surface Coating & Printing Operations Ethanol Plants (Under Development) Woodworking / Plastic Machining Blasting Operations Mineral Processing Site Remediation Title of Form Form ID PI-19 PI-20 PI-18 (R5 / 1-10) PI-21 PI-17 Office of Air C 'ty State Form 5 (F z X z X z 🛭 Applicable? z | z Ø ≻  $\succeq$ **≻**  $\succeq$ **≻** 

PI-22

z X

 $\vdash$ 

		Part	Part C: Control Equipment	uipment
Applicable?	Form ID	Title of Form	State Form Number	When should this form be included in my application packet?
		Viennani Simmary	51904	Include if add-on control equipment will be used for the process.
N □ × ⊠	CE-01	Control Equipment Carmers	51053	Include for each baghouse or fabric filter.
N □ × ⊠	CE-02	Particulates - Baghouse / Fabric Filter	00000	Indude for each evolone.
N N	CE-03	Particulates – Cyclone	27070	illorace of cach proceedatic precipitator.
2 2 2 2	CE-04	Particulates - Electrostatic Precipitator	52621	Include to reach electrostate process
	2 2	Particulates – Wet Collector / Scrubber /	52622	Include for each wet collector, sclubber, or absorber.
z X X	SO-11	Absorber		
		Oxidizer / Incinerator	52623	Include for each flare, oxidizer, or incluerator.
N □ × ⊠	CE-06	Organics - rigie / Oxidical / Inchine	10000	Include for each adsorber.
Z X	CE-07	Organics - Adsorbers	4707C	Joseph Company
	L	Organics - Condenser	52625	Include Tor each condensati
z ⊠ ≻	CE-08	Olganics Condense:	80808	Include for each control device using reduction technology (e.g., oc.)
N 🛭	CE-09	Reduction Technology	25050	SNCR).
			E0436	Include one form for equipment for which there is not a specific CE form.
N N	CE-10	Miscellaneous Control Equipment	02430	

Applicable?       Form ID       Title of Form         □ Y       □ N       BACT-01       Analysis of Best Available Control Technology         □ Y       □ N       BACT-01a       Background Search: Existing BAC Determinations         □ Y       □ N       BACT-01b       Cost/Economic Impact Analysis         □ Y       □ N       BACT-02       Summary of Best Available Control Technology         □ Y       □ N       PSD / Emission Offset Checklist		State Form When should this form be included in my application packet?  Number None Include for every BACT application.  None Include for every PSD application and every NSR application emission offsets.
- C T I	State Form Number None None None None	

art F: Emission Credit Registry	State Form When should this form be included in my application packet?  Number	and the modification results in emission reductions.			51/84 Submit Wileliever regions of emission credits for offsets. 51785 Include if the modification requires the use of emission credits for offsets.		Submit if vol. are looking for emission credits for offsets.	
Part F: Emissi	Title of Form		Generation of Emission Credits	Torro doisoing to make	l'ansier di Ellission dicara	Use of Emission Credits	1	Emission Credit Request
	Applicable? Form ID		□ × ⊠ N EC-01		□ Y ⊠ N EC-02	14 Z 7 13	N ⊠ Y ☐	□Y ⋈N EC-04

			Part H: Air Toxics	oxics
Applicable? Form ID	Form ID	Title of Form	State Form Number	State Form When should this form be included in my application packet?  Number
				OF Part 61 NESHAP, and 40
N⊠ ⊁□	FED-01	Summary of Federal Requirements –	53512	CFR Part 63 NESHAP applicable to the process.
				Year of the second of modifying a process subject to a Part 63
N □ X	FED-02	MACT Pre-Construction Review	51905	Include It constituting of including of Programmer NESHAP.
				The factor is expelled on the LLS FPA website. Completed notifications
N N N	No Form ID	□ Y ⊠ N No Form ID MACT Initial Notification	None	should be submitted to the IDEM Compliance Branch.

Permits	rt I: Special Permits State Form When should this form be included in my application packet? Number		Submit if you are applying for or modifying an asphalt plant general permit.	Submit if you are a nower plant or if you have opted in to the NO <sub>x</sub> budget	subfill I you are a power promise trading program.	Submit if you are applying for, modifying, or renewing a Phase 2 Acid Kalli	permit.
Part I: Special Permits	State Form Number	None	None	2	None	None	
à	Form ID Title of Form	A Section Asserts	Interim Approva	☐ Y ☒ N ASPHALT Asphalt General Permit	NO <sub>x</sub> Budget Permit		☐ Y 図 N ACIDRAIN Phase 2 Acid Kain Permin
	Form ID		INTERIM	ASPHALT	NOXBTP		ACIDRAIN
	Applicable?		N X	z ⊠ ≻□	N ⊠ ≻ □		N ⊠ ≻□

ant of Environmental Management

Office of Air L. ..ty State Form 51607 (R5 / 1-10)

ndiana Dep?

Submit if you are applying for or modifying a SSOA for external combustion Submit if you are applying for or modifying a SSOA for internal combustion Submit if you are applying for or modifying a SSOA for coal mines and coal Submit if you are applying for or modifying a SSOA for ready-mix concrete Submit if you are applying for or modifying a SSOA for surface coating or graphic arts operations. Submit if you are applying for or modifying a SSOA for abrasive cleaning Submit if you are applying for or modifying a SSOA for sand and gravel Submit if you are applying for or modifying a Source Specific Operating ö Submit if you are applying for or modifying a SSOA for grain elevators. Submit if you are applying for or modifying a SSOA for crushed stone commercial surface coating operations not subject to 326 IAC 8-2; graphic arts operations not subject to 326 IAC 8-5-5. Submit if you are applying for or modifying a SSOA for woodworking Submit if you are applying for or modifying a SSOA for degreasing Submit if you are applying for or modifying a SSOA for automobile Submit if you are applying for or modifying a SSOA for industrial or When should this form be included in my application packet? refinishing operations. Part J: Source Specific Operating Agreements (SSOA) preparation plants. processing plants. batch plants. operations. Agreement. operations. sonrces. sonices plants. State Form 53448 53449 53450 53451 53446 53447 53445 53443 53444 53442 53439 53440 53438 53441 Coal Mines And Coal Preparation Plants Automobile Refinishing Operations (326 IAC 2-9-11) Industrial / Commercial Surface Coating External Combustion Sources (326 IAC 2-9-13) Crushed Stone Processing Plants (326 IAC 2-9-8) Ready-Mix Concrete Batch Plants (326 Internal Combustion Sources (326 IAC 2-9-14) Degreasing Operations (326 IAC 2-9-12) Woodworking Operations (326 IAC 2-9-4) Abrasive Cleaning Operations (326 IAC 2-9-5) Sand And Gravel Plants (326 IAC 2-9-7) Summary of Application and Existing Operations -OR- Graphic Arts Surface Coating or Graphic Arts Operations (326 IAC 2-9-2.5) Grain Elevators (326 IAC 2-9-6) Operations (326 IAC 2-9-3) (326 IAC 2-9-10) Agreements IAC 2-9-9) Title of Form OA-13 OA-14 OA-10 0A-11 **OA-12** OA-08 OA-06 OA-09 Form ID OA-04 OA-05 **OA-07** OA-03 OA-02 OA-01 z Ø Z z Ø Z z z z 🛛 Z Z z Ø Z Z Applicable?  $\boxtimes$  $\boxtimes$ Ø  $\boxtimes$  $\boxtimes$  $\boxtimes$  $\boxtimes$  $\boxtimes$  $\boxtimes$  $\boxtimes$ <u>≻</u>  $\succeq$ ≻  $\vdash$  $\succeq$ ≻□ <u>≻</u>  $\succeq$  $\vdash$ <u>≻</u>  $\succeq$ ≻□  $\vdash$  $\vdash$ 



NOTES:

### OAQ GENERAL SOURCE DATA APPLICATION GSD-01: Basic Source Level Information

State Form 50640 (R5 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT diana

State of Indiana

IDEM - Office of Air Quality - Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or oji Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 www.IN.gov/idem

JAN 25 2018

The purpose of GSD-01 is to provide essential information about the entire Source of air pollutant emissions. GSD-01 is a required form.

Detailed instructions for this form are available on the Air Peganit Application Forms website.

All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for public inspection.

PART A: Source	e / Company	Location Info	rmation	
Piverview Energy			2. Plant ID:	
4 Address 4704 East County Road 2				
		State: IN	ZiP Code: 475	523 –
	5	Township N	lame: Carter	
. County Name: Spencer . Geographic Coordinates: Latitude: 38.18 degrees N		Longitude:	86.97 degrees W	
. Universal Transferal Mercadum Coordinate Zone: 16S Horizon		20m E	Vertical:	4226392m N
. Adjacent States: Is the source located within	Illinois (IL)	Michigan (	VII) LI Onio (On)	⊠ Kentucky (KY)
<ul> <li>No</li></ul>	$\underline{nt}(s)$ . $\square$ CC	LIPO LIN	O <sub>x</sub>	☐ PM <sub>10</sub> ☐ PM <sub>2.5</sub> ☐ SO <sub>2</sub>
P/	ART B: Source	e Summary		
<ul> <li>11. Company Internet Address (optional):</li> <li>12. Company Name History: Has this source op No ☐ Yes – Provide information reg</li> </ul>	garding past o	ompany name.	s in Paπ I, Compa	ny Name History.
42 Portable Source Location History, Will the	location of th	e portable soul	ce be changing in	the near future?
Not Applicable		AH I DAMANA	Source Location $\Gamma$	History, and ion of Portable Source.
<b>14. Existing Approvals</b> : Have any exemptions,  ☑ No ☐ Yes – List these permits and	their corresp	onding emissio	ns units in Part IVI,	ource? , Existing Approvals.
45 Uppermitted Emissions Units: Does this s	ource have a	ny unpermitted	emissions units?	
☑ No ☐ Yes – List all unpermitted en	nissions units	in Part N, Unp	ermittea Emission	s Units.
45 Now Source Review Is this source proposi	ing to constru	ct or modify an	y emissions units	?
☐ No ☐ Yes – List all proposed new	construction i	n Part O, New	or Woaltied Ethiss	SIONS UNIIS.
17. Risk Management Plan: Has this source si	ubmitted a Ri	sk Managemer	t Plan?	
Not Required □ No □ Yes → Date			EPA Facility Identi	fier:

Indiana Department of Environmental Management Office of Air Quality State Form 50640 (R5 / 1-10)

PART C: Source		. the strict in this section.
DEM will send the original, signed permit dec	ision to the personed ted source.	n Identified in this section.
This person MUST be an employee of the permit	tea coares	
8. Name of Source Contact Person: Gregory Merle		
9. Title (optional): President		
20. Mailing Address: 15 E Putnam Ave, Suite# 210	State: CT	ZIP Code: 06830 -
City: Greenwich		
1. Electronic Mail Address (optional): Greg.Merle@Rive	23. Facsimile Nun	nher (optional): ( ) -
2. Telephone Number: (203) 979 - 3993	23. Facsiline Num	inder (optionary)
PART D: Authorized Individu	al/Responsible Officia	al Information
	the person indicated	In this section, it the pathorized
DEM will send a copy of the permit decision to the individual or Responsible Official is different from	n the Source Conta	ct specified in Part C.
24. Name of Authorized Individual or Responsible Off		
25. Title:		
26. Mailing Address:	State:	ZIP Code: -
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FMIL O. 1.90	nt Information	
. Company Name of Agent: KBR		
Type of Agent: ⊠ Environmental Consultant □	Attorney 🔲 Other	r (specify):
. Name of Agent Contact Person: Stephen A. Lang		
. Mailing Address: 601 Jefferson St		77000
City: Houston	State: TX	<b>ZIP Code</b> : 77002 –
. Electronic Mail Address (optional): Stephen.La	ang@kbr.com	
T-lambona Number: (713) 753 - 7580	46. Facsimile Nun	
<ol> <li>Request for Follow-up: Does the "Agent" wish to receid during the public notice period (if applicable) and a copy</li> </ol>	ve a copy of the prelir  of the final determina	11111 C. 1 1111 C. 1
PART H: Local l	Library Information	
8. Date application packet was filed with the local libra	ary:	
<ol> <li>Name of Library: 1. Lincoln Heritage Public Library.</li> <li>Chrisney Library</li> </ol>	and	
0. Name of Librarian (optional):		
<ol> <li>Mailing Address: 1. Lincoln Library: 105 North Walla</li> <li>Chrisney Library: 228 North Street</li> </ol>		47500
City: 1. Lincoln Library: Dale, IN 47523 2. Chrisney Llbrary: Chrisney, IN 47611	State: IN	<b>ZIP Code</b> : 47523 –
2. Internet Address (optional):		
53. Electronic Mail Address (optional):		· (antionol): (
54. Telephone Number:(  ) <del>-</del>	55. Facsimile Nu	umber (optional): ( ) -
PART I: Company N	lame History (if appli	cable)
Complete this section only if the source has previously op-	dunder e legal r	name that is different from the name listed
above in Section A.		
above in Section A.		57. Dates of Use
above in Section A.  56. Legal Name of Company		<b>57. Dates of Use</b> 11/12/14 to
above in Section A.  56. Legal Name of Company  Riverview Energy Corporation (CURRENT)		57. Dates of Use  11/12/14 to  10/22/08 to 11/12/2014
above in Section A.  56. Legal Name of Company  Riverview Energy Corporation (CURRENT)  Clean Coal Refining Corporation  NOTE: Name change preceded any source operation		57. Dates of Use  11/12/14 to  10/22/08 to 11/12/2014
above in Section A.  56. Legal Name of Company  Riverview Energy Corporation (CURRENT)		57. Dates of Use  11/12/14 to  10/22/08 to 11/12/2014
above in Section A.  56. Legal Name of Company  Riverview Energy Corporation (CURRENT)  Clean Coal Refining Corporation  NOTE: Name change preceded any source operation		57. Dates of Use  11/12/14 to  10/22/08 to 11/12/2014  to
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Indiana Department of Environmental Management Office of Air Quality State Form 50640 (R5 / 1-10)

### PART J: Portable Source Location History (if applicable)

Complete this section only if the source is portable and the location has changed since the previous permit was issued. The current location of the source should be listed in Section A.

). Plant ID	60. Location of the Portable Source	61. Dates at this Location
7. 1 10.110 1 -		to
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_		to
		to
-		to
		to
AND THE RESERVE THE PARTY OF TH		to
		to
-		to

PART K: Request to Chan	ge Location of Portable S	ource (if applicable)	
Complete this section to request a change of location	on for a portable source.		
62. Current Location:			
Address:			
City:	State:	ZIP Code:	
County Name:			
63. New Location:			
Address:			
City:	State:	ZIP Code:	
County Name:			

	: Source Process Description		
Complete this section to summarize the main pro	cesses at the source.		
64. Process Description	65. Products	66. SIC Code	67. NAICS Code
Veba Combi Cracker (VCC)	Diesel abd Naphtha Fuel	2999	3241999

PART M: Existing Approvals (if applicable)  Complete this section to summarize the approvals issued to the source since issuance of the main operating permit.						
68. Permit		70. Expiration Date				
NA						

# Complete this section only if the source has emission units that are not listed in any permit issued by IDEM, OAQ. 71. Emissions Unit ID 72. Type of Emissions Unit Unit ID 73. Actual Dates Began Completed Construction Operation

				78. Estimat	ted Dates	
74. Emissions Unit ID	75. NEW	76. MOD	77. Type of Emissions Unit	Begin Construction	Complete Construction	Begin Operation
See Table 17	Х		See Table 17 for all information			



### OAQ GENERAL SOURCE DATA APPLICATION GSD-02: Plant Layout Diagram

State Form 51605 (R3 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch

100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana)

ree: 1-800-451-6027 X30176 (with Hold Facsimile Number: (317) 232-6749 www.lN.gov/idem

### NOTES:

- The purpose of GSD-02 is to provide a diagram of the entire plant site. This form and a Plant Layout diagram are required for all air permit applications. If you do not provide the necessary information, applicable to your source, the application process may be stopped.
- IDEM, OAQ has provided detailed instructions for this form and an example of a basic plant layout diagram on the Air Permit Application Forms website.

Part A: Basic Plant Layout

All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality.
 Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for public inspection.

Part /	A provides IDEM, OAQ with the appropriate the plant site. Please use this table	iate in	formation about all buildings and a checklist. You must provide scale	access ed drav	-limiting features in and wings, with the actual scale
chow	nd the plant site. Please use this table n. All dimensions and units must be cle ving (All measurements should be giver	carry n	jalcatod with a street	what	is being snown. Include the
1.	☑ Building Location and Dimensions		and the same of th		
2.	□ Property Lines and Access-Limiting	Featu	res		
3.	☑ Surrounding Building Location and [	)imen	sions		
	☑ Distances to Property Lines and Acc				
	□ UTM Location Coordinates     □ UTM Location Coordin	6.		7.	⊠ Scale
<del>ن</del> .	W O I W Location Cocionates	<u> </u>			
			art B: Stack Information		
	B provides IDEM, OAQ with the appropriate to the second se		s u hand all stocks roof m	onitor	s control devices, and process
Part	B provides IDEM, OAQ with the appropriate the plant site. Please use this tab	ie as	a checklist. You must show the lo	cation	of all applicable emission
poin	s at the plant site. Please use this tab ts and include all relevant stack and en tify <u>each</u> of these emission points unde	nission	is unit identification numbers for each Identification" on form GSD-04.	acn. ir Stack	Vent Information. Include the
idan	tify <u>each</u> of these emission points unde wing ( <i>All measurements should be in fe</i>	l Orac	ck (denumcation) of form 300 0 %		
	Wing (All Measurements enedic 22	· /			
8.					
9.	Process Vents	onitor			
10.	☐ Roof Monitors ☐ No Roof M				
11.	☐ Control Devices ☐ No Control		15	rocess	ses vented inside a building)
12.		vents	Doors and Windows (16) p		
		Pa	rt C: Roadway Information		Diago.
Par	t C provides IDEM, OAQ with the appro	opriate follov	information about the roadways in wing (All measurements should be	n and a in feet	around the plant site. Please f.):
13.	☐ Adjacent Roadways ☐ Interi	or Roa	adways		
-	57 - Confirm Description (gr:	avel, d	irt, paved, etc.)		
14.	57.1. I		*See Fugitive Du	ust Co	ntrol Plan
15.	M MULLINE OF Larges				

Air Perr, pplication FORM GSD-02 Page 2 of 4

> Indiana D. ...ment Of Environmental Management Office Of Air Quality State Form 51605 (R3 / 1-10)

20. Distance & direction to	the nearest residence (feet & compass coordinate)											
This table provides detailed information about each building at the plant site that is part of the source. If additional space is incorred, you may be given in feet.)  The plant of the source in additional space is incorred, you may be given in feet.)	line or access limiting feature (feet & compass coordinate)											
oulding at the plant site	18. Building Dimensions  Length Width Height  (feet) (feet)											
nation about each be given in feet.)	18. Buildin Length (feet)											
This table provides detailed information about each table. (All measurements should be given in feet.)	17. Building Description											
his table pro able. ( <i>All me</i>	16. Building ID	See Table 10										

Air Pen, pplication FORM GSD-02 Page 3 of 4

> Indiana D. ...ment Of Environmental Management Office Of Air Quality State Form 51605 (R3 / 1-10)

Indiana D. ment Of Environmental Management Office Of Air Quality
State Form 51605 (R3 / 1-10)

# Part F: Plant Layout Diagram

This space provides a place for a hand drawn plant layout diagram. It is **optional** to use this space to create your plant layout, but you must include the diagram with your application. If you choose to submit the plant layout in a different format, state "plant layout attached" in the space provided, and submit the information with your application. IDEM, OAQ has provided an example of a basic plant layout diagram on the Air Permit Applications Forms website.

See Plant Layout Diagram



### OAQ GENERAL SOURCE DATA APPLICATION GSD-03: Process Flow Diagram

State Form 51599 (R3 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch
100 N. Senate Avenue, MC 61-53 Room 1003
Indianapolis, IN 46204-2251
Telephone: (317) 233-0178 or
Toll Free: 1-800-451-6027 x30178 (within Indiana)
Facsimile Number: (317) 232-6749
www.IN.gov/idem

### NOTES:

- The purpose of GSD-03 is to provide a checklist for identifying the information to be included on each Process Flow diagram.
- Complete this form and submit a process flow diagram for each process included in your air permit application.
- IDEM, OAQ has provided detailed instructions for this form and an example of a basic process flow diagram on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims
  of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326
  IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for
  public inspection.

4 & provides basic information	Part A: Process Flow	Diagram	
part A provides pasic information and icate that you have included the pounds per hour.):	on to understanding the nature of the the following items on your process	e process. Please use this flow diagram ( <i>All throughp</i>	table as a checklist to outs should be given in
	VCC		
	3. Raw Material Input	4. Process Throu	ughput
Dolation	ons  Modifications		
Use the space below to briefly e	explain the impacts of the additional sed modification. (If additional space below that additional informations)	equipment, the reason for ce is needed, please attacl tion is attached.)	h a separate sheet with the
N/A Initial construction applicati	tion		
· <del>- ·</del>			
	Part B: Process Opera	tion Schedule	
Part B indicates the actual (or e	estimated actual) hours of operation	for the process.	
	hedule 24 Hours per Day 7	Days per Week <u>52</u>	Weeks Per Year
	Use the space below to include as ress. (If additional space is needed, ow that additional information is atta	picaco atra-	wn about scheduled periods sheet with the information and
	Part C: Emissions Po	int Information	
Part C provides information ab as a checklist to indicate that y be given in pounds per hour.):	bout each potential outlet of air polli you have included the following iter		osphere. Please use this table agram (All throughputs should
	ation		
8. Stack / Vent Informat			

Air Pen, pplication FORM GSD-03 Page 2 of 2

Indiana D. ment Of Environmental Management Office Of Air Quality State Form 51599 (R3 / 1-10)

# Part D: Process Flow Diagram

the diagram with your application. If you choose to submit the process flow diagram in a different format, state "process flow diagram attached" in the space provided, and submit the information with your completed application. IDEM, OAQ has provided an example of a basic process flow diagram on the Air Permit Applications Forms website. This space provides a place for a hand drawn process flow diagram. It is optional to use this space to create your process flow diagram, but you must include

See Process Flow Diagrams

### OAQ GENERAL SOURCE DATA APPLICATION GSD-04: Stack / Vent Information

INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

Toll Free: 1-800-451-6027 x30178 (within Indiana) IDEM -- Office of Air Quality -- Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 Facsimile Number: (317) 232-6749 Telephone: (317) 233-0178 or Indianapolis, IN 46204-2251 www.lN.gov/idem

NOTES:

The purpose of this form is to provide basic information about each stack or vent that has the potential to emit air pollutants. If you do not provide enough information to adequately describe each process vent and/or stack, the application process may be stopped. This form is required for all air permit applications.

Detailed instructions for this form are available online on the Air Permit Application Forms website.

All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. becoming a public record, available for public inspection.

Related Stacks / This table provides detailed information about each stack or vent through which air pollutants could be released into the atmosphere. If an air stream is vented 6 <u>В</u> Р ω. Temperature 7. Outlet Gas (Degrees F) inside a building, the vent does not need to be listed on this form. If additional space is needed, you may make a copy of this form. Maximum Outlet Flow Rate (acfm) Stack / Vent Information 5. Height (feet) Dimensions (feet) Outlet 4 ô 3. Shape <u>ဂ</u> ô M H ≥ 2. Type See Table 11 Vent ID Stack /

# OAQ GENERAL SOURCE DATA APPLICATION

State Form 51610 (R3 / 1-10) INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT GSD-05: Emissions Unit Information

Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 IDEM – Office of Air Quality – Permits pranch 100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 www. IN gov/idem

The purpose of this form is to provide basic information about each emissions unit that has the potential to emit air pollutants. This form is required for all air permit applications.

Detailed instructions for this form are available online on the Air Permit Application Forms website.

NOTES:

All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for public inspection.

	ns unit that has the potential to emit air pollutants to the atmosphere. Accurate information is recover a serough information to adequately describe each emissions unit, the application process may be	7. Maximum 8. Stack/										
	o the atmosphere. emissions unit, the	6. Installation										
ation	emit air pollutants trately describe each (	Manifacturer										
<b>Emissions Unit Information</b>	at has the potential to information to adequa				-							
En	each emissions unit the one of provide enough	stopped. If additional space is needed, you may make a copy of this lonn.	4. Description									
	This table provides detailed information about each emission to determine the total potential to emit. If you do not provide	e is needed, you ma	3. Serial 4. Number									
	provides detailed	If additional space	2. Model Number									Ş
	This table	stopped.	1. Unit	See Table 12								

OAQ GENERAL SOURCE DATA APPLICATION GSD-06: Particulate Emissions Summary

State Form 51612 (R3 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

Indianapolis, IN 46204-2551 Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 IDEM – Office of Air Quality – Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 www.IN.gov/idem

NOTES:

The purpose of this form is to provide basic information about each source of particulate emissions. This form is required for all air permit applications.

Detailed instructions for this form are available on the Air Permit Application Forms website.

All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for public inspection.

Part A: Particulate Matter Emissions

Indiana D ment Of Environmental Management Office Of Air Quality State Form 51612 (R3 / 1-10)

Air Perr. pplication FOKM GSD-06 Page 3 of 4

**2** Date Submitted: Date Submitted: ☐ Yes ☐ No 13, Control Plan 2 Date Submitted: ☐ Yes ☐ № Date Submitted: Date Submitted: Date Submitted: ☐ Yes ☐ No Date Submitted: Date Submitted: Part C gathers information about how each source of particulate emissions is controlled. If you do not provide enough information to adequately describe how each source of particulate emissions is controlled, the application process may be stopped. If additional space is needed, you may make a copy of this table. ∏ Yes ☐ Yes ☐ Yes ☐ Yes ☐ Yes Part B: Control of Particulate Emissions 12. Control Measure Description Dust Suppression **Dust Suppression Dust Suppression Dust Suppression Dust Suppression** Dust Suppression **Dust Suppression Dust Suppression** 10. Emissions Point ID | 11. Control Measure No Control No Control ☐ No Control No Control No Control ☐ No Control ☐ No Control No Control Other: Other: Other: Other: Other: Other. Other: Other: See Table 13

Air Perr, pplication FORM GSD-06 Page 4 of 4

Indiana Dt., ... iment Of Environmental Management Office Of Air Quality State Form 51612 (R3 / 1-10)

Air Permitting Rules 326 IAC 6-4 and 326 IAC 6-5 require fugitive dust to be controlled as needed to prevent dust from visibly crossing property lines. Parts C and D summarize sources of fugitive particulate emissions from process operations and unpaved roads.

PART C: Fugitive Dust (if applicable)	art C identifies measures implemented for controlling fugitive particulate emissions from process operations and unpaced.	4. Dust Control Plans. Check all that apply.	☐ Wet ⊠ Dry	ck Piles:	oads: Watered? ☐ Yes 🗵 No	See fugitive dust control plan section:    See fugitive dust control plan section:   See fugitive dust control pla	her (specify):	her (specify):	PART D: Vehicular Traffic on Onlywood 1998.  Part D gathers information on vehicular traffic patterns when the site contains unpaved roads. All data should be provided assuming peak hours of vehicular property and D gathers information on vehicular traffic patterns when the site contains and leaving the property lines), the distance from the plant to the property traffic. Two one-way trip distance	paved Roads: NA	19. Distance of one- 20. Max. vehicle 7.1. Max. 9.000 speed weight (fully loaded) (miles/trip) (mph)				
	art C identifies mea	4. Dust Control Pl	⊠ Conveving:	Stock Piles:	☐ Unpaved Ros	Other (specify)	Other (specify):	Other (specify):	Part D gathers infor traffic. Two one-we line is the one-way	16 Average Silt C	17. Vehicle Description	ΑΝ			



### GSD-07: Criteria Pollutant Emissions Summary OAQ GENERAL SOURCE DATA APPLICATION

State Form 51602 (R3 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 IDEM - Office of Air Quality - Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 www.IN.gov/idem

The purpose of this form is to provide the actual and potential emissions of each criteria pollutant emitted from the source. This form is required for all air permit applications.

Detailed instructions for this form are available on the Air Permit Application Forms website.

NOTES:

All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for public inspection.

do not provide enough information to		5. Potential To Emit	Standard Units Tons Per Year	-							
Part A: Unit Emissions Summary	Part A provides the actual and potential emissions of each criteria pollutant emitted from each emissions from each emissions unit, the application process may be stopped.	A Actual Emissions	Standard Units Tons Per Year								
Part A:	Part A provides the actual and potential emissions of each criteria pollutant emitted from each emission. Part A provides the actual and potential emissions of each emissions unit, the application process may be stopped		2. Stack / Vent ID 3. Criteria Pollutant								
	Part A provides the actual and pol	adequately describe the enhasion	1. Unit ID 2. Stack / Vent ID	See Table 14							

Air Perr. pplication FOrtM GSD-07 Page 2 of 3

Indiana D<sub>c.</sub> ment Of Environmental Management Office Of Air Quality State Form 51602 (R3 / 1-10)

Air Perr pplication FOKM GSD-07 Page 3 of 3

> Indiana Dt., , (ment Of Environmental Management Office Of Air Quality State Form 51602 (R3 / 1-10)

Part B:	Part B: Pollutant Emissions Summary	microns units and fligitive emissions at
Part B provides the total actual and potential emissions of each criteria pollutant emitted from the source (including all emissions arms are stopped.	ia pollutant emitted from the source (including all	on process may be stopped.
the source). If you do not provide enough information to adequately	SUCCESSION OF THE PROPERTY OF	8. Potential To Emit
6. Criteria Pollutant	Actual Emissions	Standard Units Tons Per Year
	Standard Units	
Carbon Monoxide (CO)	See Table 14	
(Ph)		
Load ( V)		
Nitrogen Oxides (140X)		
Particulate Matter (PM)		
Particulate Matter less than 10µm (PM₁0)		
Particulate Matter less than 2.5µm (PM <sub>2.5</sub> )		
Sulfur Dioxide (SO <sub>2</sub> )		
Volatile Organic Compounds (VOC)		
Other (specify):		
	C. Eirive VOC Emissions (if applicable)	
Fair Complete this table if you are source and estimates VOC emissions from these emission points. Complete this table if you are	ource and estimates VOC emissions from these	emission points. Complete this table if you are
Part C summarizes the sources of lugitive 100 and 100 July 100 Jul	IAC 2-2 or 326 IAC 2-3.	49 Headplied Potential To Emit
		12. Office in care.

Part C: Tuglitive VOC emissions at the source and estimates VOC emissions from these emission points. Complete this table if you are required to provide fugitive emissions data pursuant to 326 IAC 2-2 or 326 IAC 2-3.  9. Fugitive Emissions Source Compressor Seals Flanges Open-Ended Lines Part C: Remission Factor Tone Per Hour Tons Per Year Tons Per Year  Compressor Seals Flanges Open-Ended Lines Part C: Remission Factor Tons Per Year Tons Per Year  Pump Seals Pump Seals Pump Seals Pump Seals Pump Seals	Valves Other (specify):
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### Continued on Next Page

# GSD-08: Hazardous Air Pollutant Emissions Summary OAQ GENERAL SOURCE DATA APPLICATION

State Form 51604 (R3 / 1-10) INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana) IDEM – Office of Air Quality – Permits eranch 100 N. Senate Avenue, MC 61-53 Room 1003 Facsimile Number: (317) 232-6749

www.IN.gov/idem

NOTES:

The purpose of this form is to provide the actual and potential emissions of each hazardous air pollutant emitted from the source. This form is required for all air permit applications.

Detailed instructions for this form are available on the Air Permit Application Forms website.

All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. becoming a public record, available for public inspection.

and and amyide enough information to	Part A provides the actual and potential emissions of each hazardous air pollutant emitted from each emissions unit. If you do not provide and potential emissions of each hazardous air pollutant emitted from each emissions unit the annication process may be stopped.	6. Potential To Emit	Standard Units Tons Per Year								
	ch emissions unit. oed.	eions	Tons Per Year								
Part A: Unit Emissions Summary	Part A provides the actual and potential emissions of each hazardous air pollutant emitted from each er	Succession I contact T	Standard Units								
Part A	each hazardous	Olls unit, in e depo	4. CAS Number								
	potential emissions of	ions from each emissi	3. Hazardous Air Pollutant								
	s the actual and	scribe the emiss	2. Stack / 3	See Table 15							
	Part A provide:	adequately de:	1. Unit ID								

Air Perr. pplication FOKM GSD-08 Page 2 of 2

Indiana Derestiment Of Environmental Management Office Of Air Quality State Form 51604 (R3 / 1-10)

	Part B: P	Part B: Pollutant Emissions Summary	ry the source (inclu	ding all emissions units and f	fugitive
Part B provides the total actual and potential emissions of each hazardous air pollutain eminical northead actual and potential emissions, the application process may be stopped.	ions of each hazard	lous air pollutarit erimted iron adequately describe the total	source emissions	, the application process may	y be stopped.
emissions at the source). If you do not provide		9 Actual Emissions	sions	10. Potential To Emit	Emit
7. Hazardous Air Pollutant	8. CAS Number	Standard Units	Tons Per Year	Standard Units	Tons Per Year
See Table 15					

	Part C: Fugi	C: Fugitive HAP Emissions (if applicable)	cable)	mission points. Complete	this table if you are	
Part C summarizes the sources of fugitive HAP emissions at the	P emissions at the source	se and estimates HAP emissi 326 IAC 2-3.	Ons morn mese e			
required to provide fugitive emissions data pulsualit to 320 mode.	Suail to 320 in to 1		44 Number	15. Uncontrolled Potential To Emit	itial To Emit	
11. Fugitive Emissions Source	12. Hazardous Air Pollutant	ractor	Leaking	Pounds Per Hour	Tons Per Year	
Compressor Seals	See Table 15					
Flanges						
Open-Ended Lines						
Pressure Relief Seals						
Pump Seals						,
Sampling Connections						·····
Valves						
Other (specify):						



### OAQ GENERAL SOURCE DATA APPLICATION GSD-10: Insignificant Activities

State Form 51596 (R4 / 1-10) INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT IDEM - Office of Air Quality - Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251

Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 www.IN.gov/idem

### NOTES:

- The purpose of this form is to identify all trivial and insignificant activities in operation at the source. This form is required for all air permit applications.
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for public inspection. public inspection.

correspo	entifies all trivial activities in operation at the source as defined in 326 IAC 2-7-1(40). Frease documentifies all trivial activities in operation at the source as defined in 326 IAC 2-7-1(40). Frease documentifies to the case item and sub-item that applies. If applicable, provide the Emissions Unit Identification to the Plant Layout and Process Flow diagrams.	Citation (326 IAC)							
Unit ID	Description of Trivial Activity	2-7-1(40)(A)							
See Table 16	Any activity or emission unit:  In not regulated by a NESHAP, with potential uncontrolled emissions are equal to or less than one (1)  pound per day on an emission unit basis for any single HAP or combination of HAPs; and pound per day on an emission unit basis for any single HAP or combination of HAPs; and pound per day on an emission unit basis for any single HAP or combination of HAPs; and pound per day on an emission unit basis for any single HAP or combination of HAPs; and pound per day on an emission unit basis for any single HAP or combination of HAPs; and pound per day on an emission unit basis for any single HAP or combination of HAPs; and pound per day on an emission unit basis for any single HAP or combination of HAPs; and pound per day on an emission unit basis for any single HAP or combination of HAPs; and pound per day on an emission unit basis for any single HAP or combination of HAPs; and pound per day on an emission unit basis for any single HAP or combination of HAPs; and pound per day on an emission unit basis for any single HAP or combination of HAPs; and pound per day on an emission unit basis for any single HAP or combination of HAPs; and pound per day on an emission unit basis for any single HAP or combination of HAPs; and pound per day on an emission unit basis for any single HAP or combination of HAPs; and pound per day on an emission unit basis for any single HAP or combination of HAPs; and pound per day of the HAP or combination of HAPs; and pound per day of the HAP or combination of HAPs; and pound per day of the HAP or combination of HAPs; and pound per day of the HAP or combination of HAPs; and pound per day of the HAP or combination of HAPs; and pound per day of the HAP or combination of HAPs; and pound per day of the HAP or combination of HAPs; and pound per day of the HAP or combination of HAPs; and pound per day of the HAP or combination of HAPs; and pound per day of the HAP or combination of HAPs; and pound per day of the HAP or combination of HAPs; and pound per day of the H								
	talled emissions meet the exemption levels specified in the	one that are							
	For lead and lead compounds measured as elemental lead (Pb), potential uncontrolled simple and lead (Pb), poten								
	equal to or less than one (1) pound per day  For carbon monoxide (CO), potential uncontrolled emissions that are equal to or less than one (1) pound per day  For sulfur dioxide (SO <sub>2</sub> ), potential uncontrolled emissions that are equal to or less than one (1)								
<u></u>	The sulfur dioxide (SO <sub>2</sub> ), potential uncontrolled emissions that are equal to or less than one (1)	pound per day							
ì	For volatile organic compounds (VOC), potential uncontrolled emissions that are equal to several terms of the controlled emissions that are equal to several terms of the controlled emissions that are equal to several terms of the controlled emissions that are equal to several terms of the controlled emissions that are equal to several terms of the controlled emissions that are equal to several terms of the controlled emissions that are equal to several terms of the controlled emissions that are equal to several terms of the controlled emissions that are equal to several terms of the controlled emissions that are equal to several terms of the controlled emissions that are equal to several terms of the controlled emissions that are equal to several terms of the controlled emissions that are equal to several terms of the controlled emissions that are equal to several terms of the controlled emissions that are equal to several terms of the controlled emissions that are equal to several terms of the controlled emissions of the controlled emissions of the controlled emissions that are equal to several terms of the controlled emissions of								
	For nitrogen oxides (NO <sub>X</sub> ), potential uncontrolled emissions that are equal to or less than one (1) pound positive.								
	day  For particulate matter with an aerodynamic diameter less than or equal to ten (10) micromete potential uncontrolled emissions that are equal to or less than one (1) pound per day	rs (PM <sub>10</sub> ), 2-7-1(40)(							
	The state of the s								
	Production of hot water for on-site personal use not related to any industrial or production								
	process  Water treatment activities used to provide potable and process water for the plant, excluding any activities associated with wastewater treatment								
	excluding any activities associated with wastewater transfer and safety relief valves  Steam traps, vents, leaks and safety relief valves								
	Cooling ponds     Coo								
	Laundry operations using only water solutions of bleach or detergents								
_,	☑ Demineralized water tanks and demineralizer vents								
-	⊠ Boiler water treatment operations, not including cooling towers								
<u> </u>	Oxygen scavenging (de-aeration) of water								
	Steam cleaning operations and steam sterilizers								
	☑ Pressure washing of equipment								
	Water jet cutting operations								

Part A ide checklist correspon	entifies all trivial activities in operation at the source as defined in 326 IAC 2371(46). The solution is check each item and sub-item that applies. If applicable, provide the Emissions Unit Identification in the Plant Layout and Process Flow diagrams.	Citation							
		(326 IAC)							
Unit ID	Description of Trivial Activity	2-7-1(40)(C)							
See Fable	3. Combustion activities including the following:    Portable electrical generators that can be moved by hand from one location to another. "Moved by hand from one location to another. "Moved by hand from one location to another."	and" means							
16	Portable electrical generators that can be moved by hand from one location to another than the another without the assistance of any motorized or non-motorized vehicle, conveyance, that it can be moved without the assistance of any motorized or non-motorized vehicle, conveyance,	or device							
	☐ Combustion emissions from propulsion of mobile sources								
	∑ Fuel use related to food preparation for on-site consumption								
	☐ Tobacco smoking rooms and areas								
	Blacksmith forges								
		2-7-1(40)([							
	4. Activities related to ventilation, venting equipment and refrigeration, including the following: 2277(45)(5)								
	✓ Ventilation exhaust, central chiller water systems, refrigeration and air conditioning equipments related to any industrial or production process, including natural draft hoods or ventilating systems, represent the process.  The process of								
	Stack and vents from plumbing traps used to prevent the discharge of sewer gases, handli sewage only, excluding those at wastewater treatment plants or those handling any industrial sewage only.	ial waste							
	M Vents from continuous emissions monitors and other analyzers								
	<ul> <li>✓ Vents from continuous emissions monitors and other analyses</li> <li>✓ Natural gas pressure regulator vents, excluding venting at oil and gas production facilities</li> </ul>								
	57 Air rate from air compressors								
<u></u>	Vents for air cooling of electric motors provided the air does not commingle with regulated	air pollutants							
	Vents from equipment used to air blow water from cooled plastics strands or sneets								
	5. Activities related to routine fabrication, maintenance and repair of buildings, structures, equipment or vehicles at the source where air emissions from those activities would not be equipment or vehicles at the source where air emissions from those activities would not be	2-7-1(40)							
	Activities associated with the repair and maintenance of paved and unpaved roads, included accelling or both of parking lots and roadways								
	Painting, including interior and exterior painting of buildings, and solvent use, excluding de operations utilizing halogenated organic solvents	egreasing							
	□ Brazing, soldering, or welding operations and associated equipment								
	Deptable blast-cleaning equipment with enclosures								
	Relast-cleaning equipment using water as the suspension agent and associated equipment	ıt							
<u></u>	57 B. White and betton, charging stations, except at battery manufacturing plants								
	<ul> <li>☑ Batteries and battery charging stations, except at battery managed by Batteries and battery charging stations, except at battery managed by Batteries and battery charges by Batteries and battery charging stations, except at battery managed by Batteries and battery charging stations.</li> <li>☑ Lubrication, including hand-held spray can lubrication, dipping metal parts into lubricating oil, and managed by Batteries and battery charging stations, except at battery managed by Batteries and battery charging stations, except at battery managed by Batteries and battery charging stations, except at battery managed by Batteries and Battery charging stations.</li> </ul>								
	or automated addition of cutting of in machine grant and installation or removal								
	☑ Tarring, retarring and repair of building roofs								
	Bead blasting of heater tubes								
£	☐ Beau Blacking of the Dead B								
	Manual tank gauging	un							
	Open tumblers associated with deburring operations in maintenance shops								

	intended to identify all trivial activities in a checklist. Check each item and sub hat corresponds to the Plant Layout an		cable, provide the E	Hilasiona Othi ideni						
numper t					Citation (326 IAC)					
Unit ID	Description of Trivial Activity				2-7-1(40)(F)					
See	6. Activities performed using hand-	held equipment including t	ne following.							
Table 16	□ Application of hot melt adhesives with no VOC in the adhesive formulation     □ Buffing    □ Grinding    □ Sanding     □ Cutting, excluding cutting torches    □ Buffing    □ Sawing									
10			-	_						
			□ Routing     □	Surface grin     Surface grin	ding					
	☐ Turning wood, metal, or plastic	□ Drilling			2-7-1(40)(G)					
	7. Housekeeping and janitorial act	ivities and supplies including	ig the tollowing.	activities or both	<u> </u>					
	✓ Vacuum cleaning systems u	used exclusively for housek	(eeping of custodial	activities, or both						
	Steam cleaning activities	the thirty than the thirty thad the thirty than the thirty than the thirty than the thirty tha								
	□ Rest rooms and associated	cleanup operations and su	upplies							
		ners and associated equipn	ment	<u> </u>						
	☐ Pest control fumigation									
	Office related activities including	g the following:			2-7-1(40)(H)					
	<ul><li>☑ Paper shredding</li><li>☑ Blueprint machines, photog</li></ul>	arophic equipment, and as	sociated supplies							
	Blueprint machines, photo     Lawn care and landscape mail	graphic equipment, and so	inment including th	ne storage,	2-7-1(40)(I)					
	Lawn care and landscape mail spraying or application of insertions	cticides, pesticides and her	rbicides							
	and oativit				2-7-1(40)(J					
	10. Storage equipment and activit  ☑ Pressurized storage tanks	and associated piping for	the following:		<u>.                                    </u>					
		☐ Inorganic compounds		Naturai gas						
	☐ Acetylene ☑ Anhydrous ammonia		☑ Liquid petroleum gas (LPG) ☐ Nitrogen dioxide							
	☐ Carbon Monoxide	☐ Liquid natural gas (LNG) (		Sulfur dioxide						
	Chlorine									
	Storage tanks, vessels, a									
		, and pumping and handlin- grease, animal fat, and no and covers are utilized	g equipment of any nvolatile aqueous sa	size containing alt solutions,						
			erials							
	☐ Castings									
i	☐ Lance rods									
	⊠ Any non-HAP containing r	material in solid form stored in a s	sealed or covered contai	ner						
	Portable containers used	d for the collection, storage ual to or less than forty-six l pt when the material is add	, or disposal of mate hundredths (0.46) c	erials provided the	e					

	Part A: Trivial Activities (continued)  lentifies to identify all trivial activities in operation at the source as defined in 326 IAC 2-7-1(40). Please use a checklist. Check each item and sub-item that applies. If applicable, provide the Emissions Unit Identification that corresponds to the Plant Layout and Process Flow diagrams.	this ation Sitation		
I Init ID	Description of Trivial Activity	326 IAC)		
Unit ID See	2-7-1(40)(K			
Table 16	Emergency (backup) electrical generators at residential locations, such as dormitories, prisons and hospitals.			
	Safety and emergency equipment, except engine driven fire pumps, including fire suppression systems and emergency road flares.			
	Process safety relief devices installed solely for the purpose of minimizing injury to persons or damage to equipment which could result from abnormal process operating conditions, including the following:			
	⊠ Explosion relief vents, diaphragms or panels    ⊠ Rupture discs    ⊠ Safety relief valves			
	Activities and equipment associated with on-site medical care not otherwise specifically regulated			
	Vacuum producing devices for the purpose of removing potential accidental releases	(40)(1)		
	12. Sampling and testing equipment and activities including the following:	2-7-1(40)(L)		
	Equipment used for quality control/assurance or inspection purposes, including sampling equipment used to withdraw materials for analysis			
	Hydraulic and hydrostatic testing equipment			
	Ground water monitoring wells and associated sample collection equipment			
1	Environmental chambers not using hazardous air pollutant (HAP) gases			
	Shock chambers			
	☐ Humidity chambers			
	☐ Solar simulators			
	Sampling activities including     ■ Sampling activities including activities including activities including activities including activities including activities activit			
	☑ Sampling of waste ☐ Glove box sampling, charging, and packaging			
		2-7-1(40)(M		
	Use of consumer products and equipment where the product or equipment is used at a source in the same manner as normal consumer use and is not associated with any production	2-1-1(40/())		
	process  14. Equipment and activities related to the handling, treating, and processing of animals including:	2-7-1(40)(N		
	Equipment used exclusively to slaughter animals, but not including the following: Rendering cookers, Boilers, Heating plants, Incinerators, and/or Electrical power generating equipment			
	☐ Veterinary operating rooms			
	15. Activities generating limited amounts of fugitive dust including:	2-7-1(40)(C		
	Fugitive emissions related to movement of passenger vehicles, provided the emissions are not counted for applicability purposes under 326 IAC 2-7-1(22)(B), and any required fugitive dust control plan or its equivalent is submitted			
	☐ Soil boring			
	⊠ Road salting and sanding			

	Part A: Trivial Activities (continued)	toble as a
1.11	lentifies all trivial activities in operation at the source as defined in 326 IAC 2-7-1(40). Please use this st. Check each item and sub-item that applies. If applicable, provide the Emissions Unit Identification on the Plant Layout and Process Flow diagrams.	
Correspo		Citation (326 IAC)
Unit ID	Description of Trivial Activity	2-7-1(40)(P)
See	16. Activities associated with production including the following:	
Table 16	Closed, non-vented, tumblers used for cleaning or deburring metal products without abrasive blasting	
	☐ Electrical resistance welding	
	CO <sub>2</sub> lasers, used only on metals and other materials which do not emit HAPs in the process	
	☐ Laser trimmers which do not produce fugitive emissions and are equipped with dust collection devices such as bag filter, cyclone, or equivalent device	
	Application equipment for hot melt adhesives with no VOC in the adhesive formulation	<u></u>
	Drop hammers or hydraulic presses for forging or metalworking	
	⊠ Air compressors and pneumatically operated equipment, including hand tools	
	Compressor or pump lubrication and seal oil systems	
	Equipment used to mix and package soaps, vegetable oil, grease, animal fat, and populatile aqueous salt solutions, provided appropriate lids and covers are utilized	
	Equipment for washing or drying fabricated glass or metal products, if no VOCs or HAPs are used in the process, and no gas, oil or solid fuel is burned	
	Handling of solid steel, including coils and slabs, excluding scrap burning, scarfing, and charging into steel making furnaces and vessels	2-7-1(40)(Q)
	17. Miscellaneous equipment, but not emissions associated with the process for which the	
	Equipment used for surface coating, painting, dipping or spraying operation, except those that will emit VOCs or HAPs	
	Condensate drains for natural gas and landfill gas	<u></u>
	<ul> <li>Electric or steam heated drying ovens and autoclaves, including only the heating emissions and not any associated process emissions</li> </ul>	
	Salt baths using nonvolatile salts including caustic solutions that do not result in emissions of any regulated air pollutants	
	Ozone generators	<u> </u>
	☐ Portable dust collectors	<u></u>
	Scrubber systems circulating water based solutions of inorganic salts or bases which are installed to be available for response to emergency situations	
	Soil borrow pits	
	Manual loading and unloading operations	
	☐ Purging of refrigeration devices using a combination of nitrogen and CFC-22 (R-22) as pressure test media	
	☐ Construction and demolition operations	
	☐ Mechanical equipment gear boxes and vents which are isolated from process materials	
1	Non-volatile mold release waxes and agents	

	a checklist. Indicate which activities are present by checking the appropriate activities are present by checking the appropriate activities. Such as the content of the process of the pr	Citation (326 IAC)
Unit ID	Description of Insignificant Activity  18. Combustion related activities, including the following:	2-7-1(21)(G)(i)
See Table 16	Space heaters, process heaters, or boilers using the following fuels     Space heaters, process heaters, or boilers using the following fuels	
	Natural gas-fired combustion sources with heat input equal to or less than ten millon (10,000,000) Btu per hour	
	Propane or liquified petroleum gas, or butane-fired combustion sources with heat input equal to or less than six million (6,000,000) Btu per hour	
	Fuel oil-fired combustion sources with heat input equal to or less than two million (2,000,000) Btu per hour and firing fuel containing less than five-tenths percent (0.5%) sulfur by weight	
	Wood-fired combustion sources with heat input equal to or less than one million (1,000,000) Btu per hour and not burning wood refuse, treated wood or chemically contaminated wood	
	Equipment powered by diesel fuel fired or natural gas fired internal combustion engines of capacity equal to or less than five hundred thousand (500,000) Btu/hour, except where total capacity of equipment operated by one stationary source exceeds two million (2,000,000) Btu/hour	
	☐ Combustion source flame safety purging on startup	2-7-1(21)(G)(
	19. Fuel dispensing activities, including the following:	2-1-1(21)(0)(
	A gasoline fuel transfer dispensing operation handling less than or equal to one thousand three hundred (1,300) gallons per day and filling storage tanks having a capacity equal to or less than ten thousand five hundred (10,500) gallons. Such storage tanks may be in a fixed location or on mobile equipment	
	A petroleum fuel, other than gasoline, dispensing facility, having a storage tank capacity less than or equal to ten thousand five hundred (10,500) gallons, and dispensing three thousand five hundred (3,500) gallons per day or less	
	20. The following VOC and HAP storage containers:	2-7-1(21)(G)
	Storage tanks with capacity less than or equal to one thousand (1,000) gallons and annual throughputs less than twelve thousand (12,000) gallons	
	✓ Vessels storing the following:     ✓	
	☐ Hydraulic oils ☐ Lubricating oils ☐ Machining oils ☐ Machining fluids	0.7.4(24)(C
	21. Refractory storage not requiring air pollution control equipment	2-7-1(21)(G
	22. Equipment used exclusively for the following	2-7-1(21)(G
	☐ Packaging the following: ☐ Greases ☐ Lubricants	
	Filling drums, pails or other packaging containers with the following:	
l	☐ Greases ☐ Lubricating oils ☐ Waxes	

	Part B: Insignificant Activities (continued)		
Part B ide	entifies all insignificant activities in operation at the source as defined in 326 IAC 2-7-1(21)(G). Plea a checklist. Indicate which activities are present by checking the appropriate box. If applicable, pr is Unit Identification number that corresponds to the Plant Layout and Process Flow diagrams.	se use this ovide the	
		Citation (326 IAC)	
Unit ID	Description of Insignificant Activity	2-7-1(21)(G)(vi)	
See Table 16	23. Production related activities, including the following:    Application of the following as temporary protective coatings:		
	Nonvolatile materials     Oils		
	☐ Machining where an aqueous cutting coolant continuously floods the machining		
	interface  ☐ Degreasing operations that do not exceed one hundred forty-five (145) gallons per twelve (12) months, except if subject to 326 IAC 20-6		
	Cleaners and solvents characterized as follows where the use of which, for all cleaners and solvents combined, does not exceed one hundred forty-five (145) gallons per twelve (12) months		
	Having a vapor pressure equal to or less than two kilo Pascals (2.0 kPa) (fifteen millimeters of mercury (15 mm Hg) or three-tenths pound per square inch (0.3 psi)) measured at thirty-eight degrees Centigrade (38°C) (one hundred degrees Fahrenheit (100°F))		
	Having a vapor pressure equal to or less than seven-tenths kilo Pascals (0.7 kPa) (five millimeters of mercury (5 mm Hg) or one-tenth pound per square inch (0.1 psi)) measured at twenty degrees Centigrade (20°C) (sixty-eight degrees Fahrenheit (68°F))		
	The following equipment related to manufacturing activities not resulting in the emission of HAPs:		
	☐ Brazing equipment ☐ Cutting torches ☐ Soldering equipment ☐ We	elding equipment	
	☐ Infared cure equipment		
	Exposure chambers (towers or columns) for curing of ultraviolet inks and ultra-violet coatings where heat is the intended discharge		
	Any of the following structural steel and bridge fabrication activities:		
	Cutting two hundred thousand (200,000) linear feet or less of one (1) inch plate of equivalent		
	☐ Using eighty (80) tons or less of welding consumables	0.7.4(04)(0)(0)	
	24. Activities associated with the following recovery systems:	2-7-1(21)(G)(v	
<u> </u>	Rolling oil recovery systems		
	Groundwater oil recovery wells	0.74(04)(0)(	
	25. Solvent recycling systems with batch capacity less than or equal to one hundred (100) gallons	2-7-1(21)(G)(v	

the Emis	intended to identify all insignificant activities in operation at the source as defined in the s	Citation
Unit ID	Description of Insignificant Activity	(326 IAC)
See	26. Water-based activities, including the following:	2-7-1(21)(G)(ix)
Table 16	Activities associated with the treatment of wastewater streams with an oil and grease content less than or equal to one percent (1%) by volume	
	Water runoff ponds for petroleum coke-cutting and coke storage piles	
	Activities associated with the transportation and treatment of sanitary sewage, provided discharge to the treatment plant is under the control of the owner/operator, that is, an onsite sewage treatment facility	
	Any operation using aqueous solutions containing less than one percent (1%) by weight of VOCs excluding HAPs	AHI
	Water based adhesives that are less than or equal to five percent (5%) by volume of VOCs excluding HAPs	
	☐ Noncontact cooling tower systems with either of the following:	
	☐ Natural draft cooling towers not regulated under a NESHAP	
	☐ Forced and induced draft cooling tower systems not regulated under a NESHAP	
	Quenching operations used with heat treating processes	I
	27. Repair activities, including the following:	2-7-1(21)(G)(x)
	Replacement or repair of electrostatic precipitators, bags in baghouses and filters in other air filtration equipment	
	□ Process vessel degassing and cleaning to prepare for internal repairs	
	28. Trimmers that do not produce fugitive emissions and that are equipped with a dust collection or trim material recovery device, such as a bag filter or cyclone	2-7-1(21)(G)(xi)
	29. Stockpiled soils from soil remediation activities that are covered and waiting transport for disposal	2-7-1(21)(G)(xii)
	30. Paved and unpaved roads and parking lots with public access	2-7-1(21)(G)(xiii)
	31. Conveyors as follows:	2-7-1(21)(G)(xiv)
<u></u>	Covered conveyors for solid raw material, including the following:	
	Coal or coke conveying of less than or equal to three hundred sixty (360) tons per day	
	Limestone conveying of less than or equal to seven thousand two hundred (7,200) tons pe day for sources other than mineral processing plants constructed after August 31, 1983	•
	Uncovered coal or coke conveying of less than or equal to one hundred twenty (120) tons per day	
	☐ Underground conveyors	
	☐ Enclosed systems for conveying plastic raw materials and plastic finished goods	
х	32. Coal bunker and coal scale exhausts and associated dust collector vents	2-7-1(21)(G)(xv)
	33. Asbestos abatement projects regulated by 326 IAC 14-10	2-7-1(21)(G)(xvi

he Emis	table as a checklist. Indicate which activities are present by checking the approach to the plant Layout and Process Flow diagrams. sions Unit Identification number that corresponds to the Plant Layout and Process Flow diagrams.	Citation (326 IAC)
Unit ID See Fable 16	Description of Insignificant Activity  34. Routine maintenance and repair of buildings, structures, or vehicles at the source where air emissions from those activities would not be associated with any production process,	2-7-1(21)(G)(xvii)
	including the following:	
		2-7-1(21)(G)(xviii)
	35. Flue gas conditioning systems and associated chemicals such as the following:  Sulfur trioxide.	
<u></u>	Sodium suitate	2-7-1(21)(G)(xix)
, <sub>1</sub>	process upset, or spill cleanup, including the following:  Catch tanks Temporary liquid separators Tanks Fluid handling ed	quipment
	Catch tanks Temporary liquid copulation	2-7-1(21)(G)(xx)
	37. Blowdown for the following:  ☐ Sight glass ☐ Boiler ☐ Compressors ☐ Pumps ☐ Cooling tower	
	Sight glass Soller Compressors Soller	2-7-1(21)(G)(xxi)
	or equal to four hundred tifty (450) cubic filtries by voiding	2-7-1(21)(G)(xxii)
	39. Activities associated with emergencies, increasing any same and a second particles and a second particle and a se	
	☐ On-site fire training approved by the IDEM	
	☐ Emergency generators as follows: ☐ Gasoline generators not exceeding one hundred ten (110) horsepower	
	☐ Gasoline generators not exceeding one thousand six hundred (1,600) horsepower	
	☐ Diesel generators not exceeding one tribusarid six riditates (1)essy, the Diesel generators not exceeding one tribusarid six riditates (1)essy, the Diesel generators not exceeding six rights of the Diesel generators not exceeding six rights of the Diesel generators not exceeding one tribusarid six rights of the Diesel generators not exceeding one tribusarid six rights of the Diesel generators not exceeding one tribusarid six rights of the Diesel generators not exceeding one tribusarid six rights of the Diesel generators not exceeding one tribusarid six rights of the Diesel generators not exceeding one tribusarid six rights of the Diesel generators not exceeding six rights of the Diesel generators not exceeding six rights of the Diesel generators of the Diese	
	(16,000) horsepower	
	Stationary fire pump engines     ∴ selfectors	2-7-1(21)(G)(xxiii
	40. Grinding and machining operations controlled with fabric filters, scrubbers, mist collectors, wet collectors and electrostatic precipitators with a design grain loading of less than or equal to three one-hundredths grains per actual cubic foot (0.03 gr/acf) and a gas flow rate less than or equal to four thousand actual cubic feet per minute (4,000 acf/min), including the following:	
	☐ Deburring ☐ Polishing ☐ Pneumatic conveying	
	☐ Buffing ☐ Abrasive blasting ☐ Woodworking operations	
**	41. Purge double block and bleed valves	2-7-1(21)(G)(xxi
	42. Filter or coalescer media changeout	2-7-1(21)(G)(xx
	Vents from ash transport systems not operated at positive pressure	2-7-1(21)(G)(xx
	44. Mold release agents using low volatile products (vapor pressure less than or equal to two kilo Pascals (2kPa) measured at thirty-eight degrees Centigrade (38°C)	2-7-1(21)(G)(xx
ļ	45. Farm operations	2-7-1(21)(G)(xv

	entifies all insignificant activities in operation at the source as defined in 326 IAC 2-7-1(21)(G). Please the checklist. Indicate which activities are present by checking the appropriate box. If applicable, process a checklist. Indicate which activities are present to the Plant I away and Process Flow diagrams.	se use this ovide the	
Emission	s Unit Identification number that corresponds to the Plant Layout and Process Flow diagrams.		
Unit ID	Description of Insignificant Activity	Citation (326 IAC)	
See Table 16	46. Woodworking equipment controlled by a baghouse provided that the following criteria are met:	2-7-1(21)(G)(xxix)	
10010	☐ The baghouse does not exhaust to the atmosphere greater than one hundred twenty-five (125,000) cubic feet per minute	thousand	
	☐ The baghouse does not emit particulate matter with a diameter less than ten (10) micron three-thousandths grains per dry standard cubic feet (0.003 gr/dscf) of outlet air	s in excess of	
	Opacity from the baghouse does not exceed ten percent (10%)	ton, ton, ton,	
	☐ The baghouse is in operation at all times the woodworking equipment is in use		
	□ Visible emissions from the baghouse are observed daily using procedures in accordance 60, Appendix A, Method 22 and normal or abnormal emissions are recorded. In the everence emissions are observed for greater than six (6) minutes in duration, the following shall on the content of the procedures of the procedure of the procedure of the procedures of the procedure of the procedures of the procedures of the procedures of the procedure of the procedure of the procedures of the procedure of the proced	IL CADITOTICS	
	☐ The baghouse shall be inspected		
	Corrective actions, such as replacing or reseating bags, are initiated, when necessary		
	☐ The baghouse is inspected quarterly when vented to the atmosphere		
	The owner or operator keeps the following records:		
	Records documenting the date when the baghouse redirected indoors or to the atmosphere		
	Quarterly inspection reports, when vented to the atmosphere		
	☐ Visible observation reports		
	☐ Records of corrective actions	1	
	47. Woodworking equipment controlled by a baghouse provided that the following criteria are met:	2-7-1(21)(G)(xxx	
	The baghouse does not exhaust to the atmosphere greater than forty thousand (40,000 minute		
1	The baghouse does not emit particulate matter with a diameter less than ten (10) micro one-hundredth grains per dry standard cubic feet (0.01 gr/dscf) of outlet air	ns in excess of	
	Opacity from the baghouse does not exceed ten percent (10%)		
-	The baghouse is in operation at all times the woodworking equipment is in use		
	□ Visible emissions from the baghouse are observed daily using procedures in accordance 60, Appendix A, Method 22 and normal or abnormal emissions are recorded. In the event emissions are observed for greater than six (6) minutes in duration, the following shall the content of the		
	☐ The baghouse shall be inspected		
	Corrective actions, such as replacing or reseating bags, are initiated, when necessary		
	☐ The baghouse is inspected quarterly when vented to the atmosphere		
	☐ The owner or operator keeps the following records:		
-	Records documenting the date when the baghouse redirected indoors or to the atmosphe	re	
	Quarterly inspection reports, when vented to the atmosphere		
4	☐ Visible observation reports	Andrew American	
	Records of corrective actions		

Indiana Department of Environmental Management Office of Air Quality State Form 51596 (R4 / 1-10)

	Part C: Insignifica	nt Laboratory, Research, and Educational Activities
	entifies insignificant activities in ope	eration at the source as defined in 326 IAC 2-7-1(21), paragraph (D), (E), or (F). ate which activities are present by checking the appropriate box. If applicable, or that corresponds to the Plant Layout and Process Flow diagrams.
Unit ID	Description of Insignificant Acti	ettalis filmit - die cole el motta til tom il objecto de la cole forma el mande el latit de tallo de forma de la cole difficati
See		tory as defined in 2-7-1(21)(D).
Table 16	49.   Emissions from research	and development activities as defined in 2-7-1(21)(E).
	50. Emissions from education	nal and teaching activities as defined in 2-7-1(21)(F).
		Part D: Other Insignificant Activities
and (B)	lentifies all other insignificant activit	ies in operation at the source (as defined in 326 IAC 2-7-1(21), paragraphs (A) controlled emissions equal to or less than the thresholds listed below) that are not cable, provide the Emissions Unit Identification number that corresponds to the
Carbor	n Monoxide (CO) ≤ 25 lb/day	Particulate Matter with aerodynamic diameter ≤ 10μm (PM₁0) ≤ 5 lbs/hr or 25 lb/day
	Pb) ≤ 0.6 ton/yr or 3.29 lb/day	Sulfur Dioxide (SO₂) ≤ 5 lbs/hr or 25 lb/day
201 - 12 - 11 - 11 - 1	en Oxides (NO <sub>x</sub> ) ≤ 5 lbs/hr or 25 lb/day	Volatile Organic Compounds (VOC) ≤ 3 lbs/hr or 15 lb/day
		y any "other activities", and provide a brief description.

### Part E: Insignificant Activities with HAP Emissions

Part D identifies all insignificant activities in operation at the source (as defined in 326 IAC 2-7-1(21)(C)) that have the potential to emit hazardous air pollutants (HAP). These activities may or may not be identified above in Parts A, B, or D. **Activities listed in Part C above, need not be listed in this section.** Indicate which type of "Insignificant HAP Activities" are present by checking the appropriate box, and provide a brief description.

52. Individual HA Identify any er per day or 1 to	NP Emissions: missions unit, not regulated on per year of a single HAP.	by a NESHAP, emitting greater than 1	
Emissions Unit	HAP	Brief Description	Applicable Requirements
See Table 16			
Identify any e	h HAP Emissions: missions unit, not regulated ay or 2.5 ton per year of a c	I by a NESHAP, emitting greater than 1	pound per day but less than 12.5
Identify any e	missions unit, not regulated ay or 2.5 ton per year of a c	by a NESHAP, emitting greater than 1 combination of HAPs.  Brief Description	pound per day but less than 12.5  Applicable Requirements
Identify any e pounds per d	missions unit, not regulated ay or 2.5 ton per year of a c	combination of HAPs	
Identify any e pounds per d	missions unit, not regulated ay or 2.5 ton per year of a c	combination of HAPs	
Identify any e pounds per d	missions unit, not regulated ay or 2.5 ton per year of a c	combination of HAPs	
Identify any e pounds per d	missions unit, not regulated ay or 2.5 ton per year of a c	combination of HAPs	
Identify any e pounds per d	missions unit, not regulated ay or 2.5 ton per year of a c	combination of HAPs	
Identify any e pounds per d	missions unit, not regulated ay or 2.5 ton per year of a c	combination of HAPs	

Air Perr, pplication FORM GSD-10 Page 13 of 13

art E: Specifically Regulated Insignificant Activities

Indiana D. timent of Environmental Management Office of Air Quality State Form 51596 (R4 / 1-10)

59. Citation														
	Tons Per Year	2007												
58. Potential to Emit	Standard Units	. 1877)		*******										
suc	Tons Per Year								145					
57. Actual Emissions	Standard Units			- dewin-										
54. Unit ID   55. Stack /   56. Pollutant					a de la companya de			16774			Local Martin, Control of the Control			
55. Stack /	1 1 1 2				1.000							****		
54. Unit ID		See Table 16												



# OAQ GENERAL SOURCE DATA APPLICATION GSD-13: Affidavit of Applicability

State Form 51603 (R2 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003

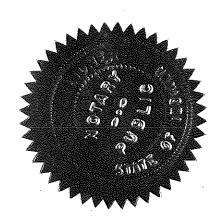
Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 www.IN.gov/idem

- The purpose of GSD-13 is to certify that the requirement to notify adjacent landowners and occupants is applicable to the source of air pollutant emissions.
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims
  of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC
  17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for public
  inspection.

PART A: Affidavit Of Applicability
Complete this form to certify that the requirement to notify adjacent landowners and occupants pursuant to Indiana Code (IC) 13-15-8 is applicable to the source of air pollutant emissions. This form must be notarized by a public notary.
Gregory Merle , being first duly sworn upon oath, deposes and says:
<ol> <li>I live in <u>Fairfield</u> County, State of <u>Connecticut</u>, and being of sound mind and over twenty-one (21) years of age, I am competent to give this affidavit.</li> </ol>
<ol> <li>I hold the position of <u>President</u> for <u>Riverview Energy Corporation</u> (permit applicant's or facility's name).</li> </ol>
<ol> <li>By virtue of my position with <u>Riverview Energy Corporation</u> (permit applicant's name), I am authorized to make the representation contained in this affidavit on behalf of the facility.</li> </ol>
I understand that the notice requirements of Ind. Code §13-15-8 applies to Riverview Energy Corporation permit applicant's or facility's name) for purposes of the accompanying permit application.
5. As required by Indiana Code § 13-15-8, the permit applicant will send written notice to adjacent landowners not more than ten (10) days after submission of the accompanying application for <u>an Air Pollution Source Construction</u> Permit
(briefly describe type of permit application) filed on behalf of Riverview Energy Corporation
(permit applicant's or facility's name).
6. Further Affiant Saith Not.
☑ I affirm under the penalty for perjury that the representations contained in this affidavit are true, to the best of my information and belief.
Gregory Merle President
Name (typed) Title
1-25-18
Signature Date
STATE OF Connecticut COUNTY OF Fairfield

INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT OFFICE OF AIR QUALITY State Form 51603 (2-04)

PA	ART B: Notarization
This section must be completed by a Public Notary.	
efore me a notary Public in and for said County and	State, personally appeared <u>Gregory</u> Merle, and being first in the foregoing instrument are true. Signed and sealed this
Printed: Joyce Weidner	My Commission Expires: <u> </u>
Residence of Indiana	County Marion





State Form 51609 (R2 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 www.IN.gov/idem

- The purpose of GSD-14 is to identify adjacent landowners and occupants that are to be notified that an air permit application has been submitted.
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality.

  Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for public inspection. for public inspection.

Owners And Occi	ipants Notified
Use this table to identify adjacent landowners and occupants the	nat you have notified of your intent to construct pursuant to
Use this table to identify adjacent landowners and occupants to Indiana Code (IC) 13-15-8. If you need additional space, you i	
1. Owner / Occupant Name: Roger L. Payne	2. Date Notified:
3. Address: 4130 East CR 2100 North	47502
City: Dale	State: IN ZIP Code: 47523
4. Electronic Mail:	5. Telephone Number: (812) 937 - 4834
Telephone   Electroni	c Mail 💹 Standard Mail 🗌 Other (specify):
O. Michael	Date Notified:
Owner / Occupant Name.	
Addieso	State: IN ZIP Code: 47579-
City: Santa Claus	Telephone Number: ( ) -
Electronic Mail:	Called Congolds
Method of Notification.	Date Notified:
Owner / Occupant Name: Myron Pugh	I Date to the second se
Address: 779 South Thompson Drive	State: IN ZIP Code: 47454 -
City: Paoli	State.
Electronic Mail:	Telephone Number: ( )  Telephone Number: ( )  Other (specify):
Method of Notification:  Telephone  Electronic	mail at Startours that
Owner / Occupant Name: Hoosier Energy Rural Electric	Cooperative Date Notified:
Address: P.O. Box 908	
	State: IN ZIP Code: 47402 - 0908
City: Bloomington	Telephone Number: (812)876 - 0294
Electronic Mail: jsouders@hepn.com	The state of the s
Method of Nourication.	Date Notified:
Owner / Occupant Name: Winkler, Inc.	I Disco 1
Address: P.O. Box 68	State: IN ZIP Code: 47523_
City: Dale	OLGIO.
Electronic Mail:	Telephone Number: (812 ) 937 - 4421
Method of Notification:  Telephone  Electron	ic Mail 📕 Standard Mail 🗌 Other (specify):



State Form 51609 (R2 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM – Office of Air Quality – Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 www.IN.gov/idem

- The purpose of GSD-14 is to identify adjacent landowners and occupants that are to be notified that an air permit application has been submitted.
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality.
   Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for public inspection.

Owners And Occu	ipants Notified	
the state of the s	nat you have notified of y	our intent to construct pursuant to
Use this table to identify adjacent landowners and occupants a Indiana Code (IC) 13-15-8. If you need additional space, you r	may make copies of this	
1. Owner / Occupant Name: Larry J Gries		2. Date Notified:
3. Address: 20520 North Gries Road	<b></b>	47500
City: Dale	State: N	ZIP Code: 47523
4. Electronic Mail:	5. Telephone Numb	er: (8/2)630 - 2905
Talenhone   Flectroni	c Mail 📕 Standard N	lail Other (specify):
V. 11102170		Date Notified:
Owner / Occupant Name: Sylvester Gries  Address: 20670 North CR 515 East		
	State: IN	ZIP Code: 47523_
City: Dale	Telephone Number: (	) -
Electronic Mail:		il Other (specify):
Method of Nouncation.	Wali Stockistic Co.	Date Notified:
Owner / Occupant Name: Robert and Ruth Gaesser		Date Notinos.
Address: 20861 N CR 500 E	INI	ZIP Code: 47523
City: Dale	State: IN	The same state of the same sta
Electronic Mail:	Telephone Number: (	
Method of Notification:		
Owner / Occupant Name: Alyssa and Sean Sermersheim		Date Notified:
Address: 20569 N CR 500 E		
	State: IN	ZIP Code: 47523 -
City: Dale	Telephone Number:	( ) -
Electronic Mail:		
Method of Notification:	Mail Maranata III	Date Notified:
Owner / Occupant Name: Charles and Janice Gogel		Date House
Address: 3209 Leslie Drive	(N)	ZIP Code: 47546 -
City: Jasper	State: IN	
Electronic Mail:		(812)482-9080
Method of Notification:  Telephone  Electroni	c Mail 🏿 Standard N	Mail Other (specify):



State Form \$1609 (R2 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality -- Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 www.IN.gov/idem

- The purpose of GSD-14 is to identify adjacent landowners and occupants that are to be notified that an air permit application has been submitted.
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality.
   Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for public inspection.

Owners And Occ	upants Notified	
Use this table to identify adjacent landowners and occupants Indiana Code (IC) 13-15-8. If you need additional space, you	that you have notified of y may make copies of this	our intent to construct pursuant to form.
1. Owner / Occupant Name: Rebecca & Grandersen & C	harity James	2. Date Notified:
3. Address: 20333 N CR 500 E		
City: Dale	State: IN	ZIP Code: 47523
4. Electronic Mail:	5. Telephone Numb	er: ( ) -
6. Method of Notification:	ic Mail 🏽 Standard M	ail 🔲 Other (specify):
Owner / Occupant Name: Town of Dale		Date Notified:
Address: P.O. Box 117 103 South Wallace	Street	
City: Dale	State: IN	<b>ZIP Code</b> :47523 _
Electronic Mail:	Telephone Number: 8	12)937-2086
Method of Notification:		· · · · · · · · · · · · · · · · · · ·
Owner / Occupant Name: Vernon Geiss		Date Notified:
Address: 7233 Old Vincennes Road		Australia de la Novembra de Composito de la Composito de la Composito de la Composito de la Composito de Comp
City: Floyd Knobs	State: IN	<b>ZIP Code</b> : 47119-
Electronic Mail:	Telephone Number: (	) -
Method of Notification:	Mail AkStandard Mai	il Other (specify):
Owner / Occupant Name: Tempel Land & Livestock LLC		Date Notified:
Address: 3805 E CR 2000 N		
City: Dale	State:  N	<b>ZIP Code</b> : 47523
Electronic Mail:	Telephone Number: ( <sup>8</sup>	BIZ 1499 - 7862
Method of Notification:	Mail 🙀 Standard Ma	il Other (specify):
Owner / Occupant Name: Gerald and Geraldine Brenner		Date Notified:
Address: 4487 E CR 2000 N		
City: Dale	State: IN	ZIP Code: 47523_
Electronic Mail:	Telephone Number: (	) -
Method of Notification:	Mail Standard Ma	il Dther (specify):



State Form 51609 (R2 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch
100 N. Senate Avenue, MC 61-53 Room 1003
Indianapolis, IN 46204-2251
Telephone: (317) 233-0178 or
Toll Free: 1-800-451-6027 x30178 (within Indiana)
Facsimile Number: (317) 232-6749
www.lN.gov/idem

- The purpose of GSD-14 is to identify adjacent landowners and occupants that are to be notified that an air permit application has been submitted
- · Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality.
   Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for public inspection.

Owners And Occ	upants Notified	
Use this table to identify adjacent landowners and occupants Indiana Code (IC) 13-15-8. If you need additional space, you	that you have notified of y may make copies of this	our intent to construct pursuant to form.
1. Owner / Occupant Name: Nicholas Gerlach		2. Date Notified:
3. Address: 4405 E CR 2000 North		
City: Dale	State: IN	<b>ZIP Code</b> : 47523_
4, Electronic Mail:	5. Telephone Numb	er: (842.) 932-2753-
6. Method of Notification:	c Mail 🍇 Standard M	ail Other (specify):
Owner / Occupant Name: Roger Wilson		Date Notified:
Address: 4443 East CR 2000 N		
City: Dale	State: In	ZIP Code: 47523_
Electronic Mail:	Telephone Number: (	312)937-2753
Method of Notification:		
Owner / Occupant Name: Virlee Waninger		Date Notified:
Address: 4381 E CR 2000 N		
City: Dale	State: IN	ZIP Code: –
Electronic Mail:	Telephone Number: (&	12 1937 -4325
Method of Notification:	Mail XX Standard Mai	I Other (specify):
Owner / Occupant Name: Leander Tempel		Date Notified:
Address: 4327 E CR 2000 N		A
City: Dale	State: IN	ZIP Code: 47523
Electronic Mail:	Telephone Number: (5	312)499 - 7862
Method of Notification:	Mail 🌋 Standard Ma	il Cther (specify):
Owner / Occupant Name: Dennis Forler and Roger Fo		Date Notified:
Address: P.O. Box 465		
city: Santa Claus	State: IN	ZIP Code: 47579_
Electronic Mail: regerforter@gmail, com	Telephone Number: (2	312)639-1001
Method of Notification:		



State Form 51609 (R2 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

iDEM - Office of Air Quality - Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 www.IN.gov/idem

- The purpose of GSD-14 is to identify adjacent landowners and occupants that are to be notified that an air permit application has been submitted
- · Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality.
   Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for public inspection.

Owners And Occ	upants Notified	
Use this table to identify adjacent landowners and occupants Indiana Code (IC) 13-15-8. If you need additional space, you		
1. Owner / Occupant Name: I - 64 Realty LLC		2. Date Notified:
3. Address: 602 Orchard Lane		Y
City: Huntingburg	State: IN	ZIP Code: 47642-
4. Electronic Mail: jimkulbeth@twc.com	5. Telephone Numbe	r. (812) 309-0371
6. Method of Notification: Telephone Electron	ic Mail 🕸 Standard Ma	nil Other (specify):
Owner / Occupant Name: Aneopam, Inc		Date Notified:
Address: 1339 N Washington St		
City: Dale	State: IN	ZIP Code: 47325_
Electronic Mail:	Telephone Number: (	) -
Method of Notification:	Mail Standard Mail	Other (specify):
Owner / Occupant Name: Servus Inc		Date Notified:
Address: 4201 Mannheim Rd Ste A	**************************************	
City: Jasper	State: IN	ZIP Code: 47546_ 9618
Electronic Mail: cmeyer@brsidal_net	Telephone Number: (క	12)634 - 5031
Method of Notification:		
Owner / Occupant Name:		Date Notified:
Address:	**************************************	
City:	State:	ZIP Code: –
Electronic Mail:	Telephone Number: (	) -
Method of Notification:	Mail 🔲 Standard Mail	Other (specify):
Owner / Occupant Name:		Date Notified:
Address:		
City:	State:	ZIP Code: -
Electronic Mail:	Telephone Number: (	) -
Method of Notification:	Mail Standard Mail	Other (specify):



# OAQ GENERAL SOURCE DATA APPLICATION GSD-15: Government Officials Notified

State Form 51608 (R3 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana)

Facsimile Number: (317) 232-6749 www.lN.gov/idem

- The purpose of GSD-15 is to identify local government officials that are to be notified that an air permit application has been submitted.
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality.
   Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for public inspection.

Government Offi	cials Notified	
Use this table to identify local government officials that should be air permit application has been submitted. If you need additions	e notified pursuant to Ind I space, you may make o	iana Code (IC) 13-15-3-1 that an copies of this form.
		2. Date Notified:
Name: Ray Streigel     Title: President, Dale Town Council		
Title: President, Dale Town Council     Address: Dale Town Hall 103 South Wallace Street	P.O. Box 117	
	State: IN	ZIP Code: 47523 _
City: Dale	6. Telephone Number	r. ( 812 <sub>)</sub> 937- 4781
5. Electronic Mail:		
7. Method of Notification: 🔲 Telephone 🔲 Electronic	Man [A] Standard His	Date Notified:
Name: James Seiler		Date Notinos.
Title: President, Spencer County Board of Commissioners		
Address: 2351 North Orchard Road	State: IN	ZIP Code: 47635
City: Rockport	State.	
Electronic Mail:	Telephone Number: (	Other (specify):
Method of Notification:	fail ⊠Standard Mail	Unter (specify).
Method of Notification: Telephone Electronic		en 4. hi - 4761 m.d.
Name: Al Logsdon		Date Notified:
Method of Rothloadox.		Date Notified:
Name: Al Logsdon  Our richieror Spancer County Board of Commission		
Name: Al Logsdon  Title: Commissioner, Spencer County Board of Commissioner, Address: P.O. Box 733	oners  State: IN	ZIP Code:47579 —
Name: Al Logsdon  Title: Commissioner, Spencer County Board of Commission  Address: P.O. Box 733  City: Santa Claus	oners	ZIP Code:47579 —
Name: Al Logsdon  Title: Commissioner, Spencer County Board of Commissioners: P.O. Box 733  City: Santa Claus  Electronic Mail:	State: IN Telephone Number:	ZIP Code:47579 —
Name: Al Logsdon  Title: Commissioner, Spencer County Board of County Boar	State: IN Telephone Number:	<b>ZIP Code</b> : 47579 — 812) 686 - 1289
Name: Al Logsdon  Title: Commissioner, Spencer County Board of Commission  Address: P.O. Box 733  City: Santa Claus  Electronic Mail:  Method of Notification: Telephone Electronic  Name: Tom Brown	State: IN Telephone Number: (	ZIP Code: 47579 812) 686 - 1289  [ Other (specify):
Name: Al Logsdon  Title: Commissioner, Spencer County Board of Commission  Address: P.O. Box 733  City: Santa Claus  Electronic Mail:  Method of Notification: Telephone Electronic  Name: Tom Brown  Title: Commissioner, Spencer County Board of Commissioner	State: IN Telephone Number: (	ZIP Code: 47579 812) 686 - 1289  [ Other (specify):
Name: Al Logsdon  Title: Commissioner, Spencer County Board of Commission  Address: P.O. Box 733  City: Santa Claus  Electronic Mail:  Method of Notification: Telephone Electronic  Name: Tom Brown  Title: Commissioner, Spencer County Board of Commission  Address: 6378 East CR 700 N	State: IN Telephone Number: ( Mail Standard Mail oners	ZIP Code: 47579 —  812) 686 _ 1289  Other (specify):  Date Notified:  ZIP Code: 47615 —
Name: Al Logsdon  Title: Commissioner, Spencer County Board of Commiss	State: IN Telephone Number: ( Mail Standard Mail oners	ZIP Code: 47579 —  812) 686 _ 1289  Other (specify):  Date Notified:  ZIP Code: 47615 —
Name: Al Logsdon  Title: Commissioner, Spencer County Board of Commission  Address: P.O. Box 733  City: Santa Claus  Electronic Mail:  Method of Notification: Telephone Electronic  Name: Tom Brown  Title: Commissioner, Spencer County Board of Commission  Address: 6378 East CR 700 N	State: IN Telephone Number: ( Mail Standard Mail oners  State: IN Telephone Number:	ZIP Code: 47579 —  812) 686 - 1289  Other (specify):  Date Notified:  ZIP Code: 47615 —  (812) 362 - 8302



# OAQ GENERAL SOURCE DATA APPLICATION GSD-15: Government Officials Notified

State Form 51808 (R3 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749

www.IN.gov/idem

- The purpose of GSD-15 is to identify local government officials that are to be notified that an air permit application has been submitted.
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for public inspection.

Government Off	icials Notified	
a crista de la	so notified nursuant to Ind	iana Code (IC) 13-15-3-1 that an
Use this table to identify local government officials that should be air permit application has been submitted. If you need addition	al space, you may make	
1. Name: Gay Ann Harney	,	2. Date Notified:
3. Title: Mayor of Rockport, IN		
4. Address: Rockport City Hall 426 Main Street		47625
City: Rockport	State: IN	ZIP Code: 47635_
5. Electronic Mail:	6. Telephone Numbe	r: (812 )649 _2242
7. Method of Notification: ☐ Telephone ☐ Electroni	c Mail 🗵 Standard Ma	il Other (specify):
Name: Jack Kroeger		Date Notified:
Title: Spencer County Council		
Address: P.O. Box 668		1770
City: Santa Claus	State: IN	ZIP Code: 47579 _
Electronic Mail:	Telephone Number: (	812 ) 544 - 2762
Method of Notification:	Mail 🗵 Standard Mail	Other (specify):
Method of Notification.		Date Notified:
Name: Cindy Morrison  Pala Indiana Clerk Treasurer		Date Notified:
Name: Cindy Morrison  Title: Dale, Indiana Clerk Treasurer		Date Notified:
Name: Cindy Morrison  Title: Dale, Indiana Clerk Treasurer  Address: Dale Town Hall P.O. Box 117	State: IN	Date Notified:  ZIP Code: 47523_
Name: Cindy Morrison  Title: Dale, Indiana Clerk Treasurer  Address: Dale Town Hall P.O. Box 117  City: Dale		ZIP Code: 47523
Name: Cindy Morrison  Title: Dale, Indiana Clerk Treasurer  Address: Dale Town Hall P.O. Box 117  City: Dale  Electronic Mail:	Telephone Number:	<b>ZIP Code</b> : 47523
Name: Cindy Morrison  Title: Dale, Indiana Clerk Treasurer  Address: Dale Town Hall P.O. Box 117  City: Dale  Electronic Mail:  Method of Notification:	Telephone Number:	<b>ZIP Code</b> : 47523
Name: Cindy Morrison  Title: Dale, Indiana Clerk Treasurer  Address: Dale Town Hall P.O. Box 117  City: Dale  Electronic Mail:  Method of Notification:	Telephone Number:	ZIP Code: 47523
Name: Cindy Morrison  Title: Dale, Indiana Clerk Treasurer  Address: Dale Town Hall P.O. Box 117  City: Dale  Electronic Mail:  Method of Notification: Telephone Electronic  Name: Jefferson Lindsey  Title: Spencer County Attorney	Telephone Number:	ZIP Code: 47523
Name: Cindy Morrison  Title: Dale, Indiana Clerk Treasurer  Address: Dale Town Hall P.O. Box 117  City: Dale  Electronic Mail:  Method of Notification: Telephone Electronic  Name: Jefferson Lindsey  Title: Spencer County Attorney  Address: 217 Main Street	Telephone Number: Mail ☑ Standard Mail	ZIP Code: 47523
Name: Cindy Morrison  Title: Dale, Indiana Clerk Treasurer  Address: Dale Town Hall P.O. Box 117  City: Dale  Electronic Mail:  Method of Notification: Telephone Electronic  Name: Jefferson Lindsey  Title: Spencer County Attorney  Address: 217 Main Street  City: Rockport	Telephone Number:  Mail   Standard Mail  State: IN	ZIP Code: 47523  (812) 937 - 2086  Other (specify):  Date Notified:  ZIP Code: 47635
Name: Cindy Morrison  Title: Dale, Indiana Clerk Treasurer  Address: Dale Town Hall P.O. Box 117  City: Dale  Electronic Mail:  Method of Notification: Telephone Electronic  Name: Jefferson Lindsey  Title: Spencer County Attorney  Address: 217 Main Street	Telephone Number:  Mail Standard Mail  State: IN  Telephone Number:	ZIP Code: 47523  (812) 937 - 2086  Other (specify):  Date Notified:  ZIP Code: 47635  (812) 649 - 4571



# OAQ GENERAL SOURCE DATA APPLICATION GSD-15: Government Officials Notified

State Form 51608 (R3 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or Toll Free: 1-800-451-8027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 www.IN.gov/idem

- The purpose of GSD-15 is to identify local government officials that are to be notified that an air permit application has been submitted.
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality.
   Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for public inspection.

Government Off	icials Notified	
to the tabased	so notified nursuant to Ind	iana Code (IC) 13-15-3-1 that an
Use this table to identify local government officials that should a air permit application has been submitted. If you need addition	al space, you may make o	2. Date Notified:
1. Name:		Z. Date Notation.
3. Title:		
4. Address:		ZIP Code: -
City:	State:	
5. Electronic Mail:	6. Telephone Number	
7. Method of Notification:  Telephone  Electroni	c Mail 🔲 Standard Ma	
Name:		Date Notified:
Title:		
ddress:	T	
City:	State:	ZIP Code: -
Electronic Mail:	Telephone Number: (	
Method of Notification:	Mail 🔲 Standard Mail	Other (specify):
Incaroa or notation		Date Notified:
Name:		
Title:		
Address:	State:	ZIP Code: -
City:	Telephone Number: (	) -
Electronic Mail:		Other (specify):
Method of Notification:	Micor Li Colonia	Date Notified:
Name:		
Title:		
Address:		ZIP Code: -
City:	State:	ZIF COUE.
Electronic Mail:	Telephone Number:	
Method of Notification:	Mail Standard Mai	Other (specify):



# OAQ CONTROL EQUIPMENT APPLICATION CE-01: Control Equipment Summary

State Form 51904 (R3 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch

100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or

Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 www.lN.gov/idem

NOTES:

- The purpose of CE-01 is to summarize all of the equipment used to control emissions. This is a required form.
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims
  of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326
  IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for
  any one to inspect and photocopy.

# **Summary of Control Equipment** This table summarizes all of the equipment used to control air pollutant emissions. The identification numbers listed on this form should correspond to the emissions unit identified on the Plant Layout diagram and Process Flow diagram. 6. Applicable 5. Stack / 4. Emission 3. Pollutant **Control Equipment** Rule Control Vent ID **Unit ID** Controlled Description **Equipment ID** See Table 17



# OAQ CONTROL EQUIPMENT APPLICATION CE-02: Particulate Control – Baghouse / Fabric Filter

State Form 51953 (R2 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM – Office of Air Quality – Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749

www.IN.gov/idem

### NOTES:

- The purpose of CE-02 is to identify all the parameters that describe the baghouse or fabric filter. This is a required form.
- Complete this form once for each baghouse or fabric filter (or once for each set of identical baghouses or fabric filters).

PART A: Identification and Description of Control Equipment

- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims
  of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326
  IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for
  any one to inspect and photocopy.

* 10 4 5 5 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	physical prope			
. Control Equipment ID: See Table 18	<u>,,,,,</u>			
. Installation Date:				
. Bags or Cartridges?   Bags   Cartridges				
. Filter Material:	<u></u>			
. Number of Bags/Cartridges per Compartment:	· // // // // // // // // // // // // //			A11 / / / / / / / / / / / / / / / / / /
. Number of Compartments:		□ Cont	inuous	
. Mode of Operation:			Reverse A	ir ∏ Jet Pulse
Shaking Cleaning Method:	Reverse	Pulse	☐ Keveise A	
). Cleaning Cycle / Frequency (specify units):				
10. Is a bag leak detector installed on this device	Yes No		egative Pressu	ıre
11. Type / Description of Bag Leak Detector:	Positive Pressi	ure <u>l</u> Ne	egative Fresso	
12. Air to Cloth Ratio (Ex. 1.3 : 1.0):	<u></u>			
13. Is Lime Injection used on this device? Yes	No			<u></u>
	- I Davamata	rs		
PART B: Operational parameters of the control decrease the operational parameters of the control decrease the control decrease the provided if the standard units are not used. For each	onal Paramete		gas stream. <i>A</i> vide the inlet a	
PART B: Operational parameters of the control decrease the operational parameters of the control decrease the included if the standard units are not used. For each	onal Paramete		gas stream. <i>A</i> vide the inlet a	
PART B: Operational parameters of the control devenues to be included if the standard units are not used. For each provide the differential value.	onal Paramete vice and the poll n applicable par	utant laden ameter, pro		
PART B: Operational parameters of the control devenues be included if the standard units are not used. For each provide the differential value.  15. Gas Stream Flow Rate	onal Paramete vice and the poll n applicable par A. Units	utant laden ameter, pro		D. Differential
PART B: Operational parameters of the control development be included if the standard units are not used. For each provide the differential value.  15. Gas Stream Flow Rate  16. Gas Stream Temperature	onal Paramete rice and the poll n applicable par A. Units	utant laden ameter, pro		
PART B: Operational parameters of the control demust be included if the standard units are not used. For each provide the differential value.  15. Gas Stream Flow Rate  16. Gas Stream Temperature  17. Gas Stream Pressure	onal Paramete vice and the poll n applicable par  A. Units  °F inches of	utant laden ameter, pro		D. Differential
PART B: Operational parameters of the control development be included if the standard units are not used. For each provide the differential value.  15. Gas Stream Flow Rate  16. Gas Stream Temperature  17. Gas Stream Pressure  18. Moisture Content	onal Paramete vice and the poll n applicable para  A. Units  °F  inches of water	utant laden ameter, pro		D. Differential
PART B: Operational parameters of the control devanust be included if the standard units are not used. For each provide the differential value.  15. Gas Stream Flow Rate  16. Gas Stream Temperature  17. Gas Stream Pressure  18. Moisture Content  19. Particle Size Range	onal Paramete vice and the poll n applicable par  A. Units  F inches of water  %	utant laden ameter, pro		D. Differential
PART B: Operational parameters of the control devinust be included if the standard units are not used. For each provide the differential value.  15. Gas Stream Flow Rate  16. Gas Stream Temperature  17. Gas Stream Pressure  18. Moisture Content  19. Particle Size Range  20. Lime Injection Rate (if applicable)	onal Paramete vice and the poll n applicable par  A. Units   °F  inches of water  %  micrometers	utant laden ameter, pro		D. Differential
PART B: Operational parameters of the control devices are included if the standard units are not used. For each provide the differential value.  15. Gas Stream Flow Rate  16. Gas Stream Temperature  17. Gas Stream Pressure  18. Moisture Content  19. Particle Size Range	onal Paramete vice and the poll n applicable para  A. Units	utant laden ameter, pro		D. Differential

art C provides the pollutant concentrations of the	23. Units	24. Inlet	25. Outlet	26. Efficienc	y (%):
	23. Ullus			Capture	Control
a. Lead (Pb)	See Table 18				
b. Hazardous Air Pollutant (HAP) (specify).					
c. Particulate Matter (PM)					
d. Particulate Matter less than 10μm (PM₁₀)					
e. Particulate Matter less than 2.5μm (PM <sub>2.5</sub> )					
f. Other Pollutant (specify):					
PART D: Monitoring part D identifies any existing or proposed monitoring part D identifies any existing or proposed monitoring part D identifies any existing or proposed monitoring part D identifies any existing part D identifies and D identifies any existing part D identifies and D identifies any existing part D identifies any existing part D identifies and	g, Record Kee ring, record ke	eping, & Testi eping, & testin	ng Procedures g procedures tha	at may need to	be included
the permit			<u> </u>		- State - Stat
7. Item(s) Monitored:					<u></u>
8. Monitoring Frequency:					
9. Item(s) Recorded:					
0. Record Keeping Frequency:					
1. Pollutant(s) Tested:					
32. Test Method(s):					
33. Testing Frequency:					
PART E Part E verifies that a complete Preventive Mainte applicable. Use this table as a checklist to ensu 34. Do you have a Preventive Maintenance P	enance Plan (F re that the PM	Maintenance PMP) has beer P is complete.	prepared for th	e control devid	e, if
No PMP is needed. ☐ Yes – the fo	llowing items a	are identified o	n the PMP:		
A. Identification of the individual(s) respo				control devices.	
B. Description of the items or conditions	医克里特氏性小型 医皮肤 医骨髓 抗毒	网络阿拉伯 化二氯化甲基甲基			
☐ <b>C.</b> Schedule for inspection of items or co					
	replacement parts	s that will be maint	ained in inventory fo	r quick replaceme	ent.
		n of Integral (			
PART F Part F provides explanation to determine wheth	er the control	device should	be considered ir	itegral to the p	rocess.
Part F provides explanation to determine when	rol determina	tion for this d	evice?		☐ Yes
35. Has IDEM already made an integral cont If "Yes", provide the following:				No No	
Permit Number: Issuanc	e Date:	Det	ermination:	☐ Integral	Not Integ

Indiana Department of Environmental Management Office of Air Quality	Particulate Control Device – Baghouse / Fabric Filter FORM CE-02 Page 3 of 3
State Form 51953 (R2 / 1-10)	
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# OAQ CONTROL EQUIPMENT APPLICATION CE-06: Organics – Flare / Oxidizer / Incinerator

State Form 52623 (R / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch

100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or

Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 www.IN.gov/idem

- The purpose of CE-06 is to identify all the parameters that describe the oxidizer or incinerator. This is a required form.
- Complete this form once for each oxidizer or incinerator (or once for each set of identical oxidizers or incinerators).
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims
  of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326
  IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for
  any one to inspect and photocopy.

PART A: Identification and Descri	prior of Cont.			
art A identifies the control device and describes its physical pro	perues.	easteada o territorio		
. Control Equipment ID: See Table 19				
. Installation Date:			Other (sp	necify)
i. Incineration Method: ⊠ Flare ☐ Thermal Oxidize	Catalyt	ic Oxidizer	Other (st	cony).
I. Residence Time (specify units):		Manative	Pressure?	☐ Yes ☐ No
5. Hood Static Pressure (specify units):		ivegauve	riessure:	
5. Bed Temperature at the Flame Zone: °F	<u></u>		4 4 DI 005 form	
7. Fuel Used: ☐ Not Applicable ☐ Natural Gas Only			eted PI-02F form.	
8. Is the Gas Stream used as Overnite Air	Yes: Combus			0.00 ft.
9. Location of Flame (flares only): Ground Level 🛛 O	ther (specify elev	ation and units	of measure). 13	0.00 11.
10. Are Flame Arrestors used? (flares only) 🔲 No 🔃 Ye	<u>S</u>			
11. Are Steam Jets used? (flares only) 🔲 No 🔲 Ye			C Other	/if-d)*
12. How is the flare used? (flares only)   Emergency o	nly Norn	nal Operatio	n L Other	(specify):
13. Catalyst Material: None Specify:				☐ Not Applicable
14. Number of Catalyst Beds:		<u></u>		☐ Not Applicable
15. Is the Catalyst Cleaned and reused on-site?		☐ Not Applica	able	
16. Is a Heat Exchanger used to recover heat on this device?	Yes Yes	No	<u> </u>	☐ Not Applicable
17. Heat Exchanger Type: Recuperator Regene	rator U O	ther (specify):		☐ Not Applicable
DART B: Operation	nal Paramete	rs		
Part B provides the operational parameters of the control devi	ce and the poll	utant laden	gas stream.	
Part & provides the open	A. Units	B. Inlet	C. Outlet	D. Differential
18. Organic Vapor Concentration (by volume)	ppmv			
19. Gas Stream Flow Rate	ACFM			
	%			
20. Moisture Content	%			
21. Heat Content (for Flares)	%			
A Conditional				
22. Excess Oxygen (for Oxidizers) 23. Particle Size Range	micrometers			to

C provides the pollutant concentrations of the	25. Units	26. inlet	27. Outlet	28. Efficiency	<i>j</i> (%):
				Capture	Control
a. Carbon Monoxide (CO)	See Table 1	9			
b. Hazardous Air Pollutant (HAP) (specify):					
c. Particulate Matter (PM)					
d. Particulate Matter less than 10μm (PM <sub>10</sub> )					
e. Particulate Matter less than 2.5μm (PM <sub>2.5</sub> )				1	
f. Volatile Organic Compounds (VOC)					
g. Other Pollutant (specify):					
the permit. 9. Item(s) Monitored: 0. Monitoring Frequency:					
PART D: Monitoring Part D identifies any existing or proposed monitor In the permit.  9. Item(s) Monitored: Item(s) Monitored: Item(s) Recorded: Item(s) Rec					
1 the permit.  19. Item(s) Monitored:  10. Monitoring Frequency:  13. Item(s) Recorded:  13. Record Keeping Frequency:  13. Pollutant(s) Tested:  13. Test Method(s):  13. Testing Frequency:	E: Preventive	Maintenance F			
the permit.  9. Item(s) Monitored:  0. Monitoring Frequency:  1. Item(s) Recorded:  2. Record Keeping Frequency:  3. Pollutant(s) Tested:  34. Test Method(s):  35. Testing Frequency:  Part E verifies that a complete Preventive Maintapplicable. Use this table as a checklist to ensure	E: Preventive enance Plan (I	Maintenance F			
1 the permit.  9. Item(s) Monitored:  0. Monitoring Frequency:  1. Item(s) Recorded:  2. Record Keeping Frequency:  3. Pollutant(s) Tested:  34. Test Method(s):  35. Testing Frequency:  PART E  Part E verifies that a complete Preventive Maintapplicable. Use this table as a checklist to ensurance P	E: Preventive enance Plan (I re that the PMP)?	Maintenance F PMP) has been IP is complete.	Plan prepared for th		
1 the permit.  9. Item(s) Monitored:  0. Monitoring Frequency:  1. Item(s) Recorded:  2. Record Keeping Frequency:  3. Pollutant(s) Tested:  34. Test Method(s):  35. Testing Frequency:  Part E verifies that a complete Preventive Maintapplicable. Use this table as a checklist to ensurance Part E verifies a proceded Tyes – the formal proceded to the	E: Preventive enance Plan (I pre that the PMP)?	Maintenance F PMP) has been IP is complete.	Plan prepared for the	e control device	
1 the permit.  9. Item(s) Monitored:  10. Monitoring Frequency:  11. Item(s) Recorded:  12. Record Keeping Frequency:  13. Pollutant(s) Tested:  14. Test Method(s):  15. Testing Frequency:  PARTE  Part E verifies that a complete Preventive Maintapplicable. Use this table as a checklist to ensure as the complete Preventive Maintapplicable. Use the complete Preventive Maintapplicable Preventive Maintapplicable.	E: Preventive enance Plan (I ire that the PM Plan (PMP)? bllowing items onsible for inspecti	Maintenance F PMP) has been IP is complete. are identified or	Plan prepared for the	e control device	

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# OAQ PROCESS INFORMATION APPLICATION PI-02A: Combustion Unit Summary

State Form 52535 (R2 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or

Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 www.IN.gov/idem

- The purpose of this form is to summarize all of the combustion process units.
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 of 1274 to IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for anyone to inspect and photocopy.

Form ID	Form Title	Guidance on when to submit the form
FOUL ID		Complete once for each application.
PI-02A	Combustion Unit Summary	to the appoint each holler or process neater.
PI-02B	Boilers & Process Heaters	Complete once for each turbine or internal combustion
PI-02C	Turbines & Internal Combustion	in o
. ,	Engines	engine.  Complete once for each incinerator or combustor.
PI-02D	Incinerators & Combustors	Complete once for each kilp
PI-02E	Kilns	Complete once for each kiln.
	Fuel Use	Complete once for each emissions unit that burns fuel
PI-02F	ruei Ose	other than natural gas.
	- · · · Fastoro	Complete once for each emissions unit.
PI-02G	Emission Factors	Complete once for each emissions unit.
PI-02H	Federal Rule Applicability	Complete

This table summari	zes all the combustion nd use, you may use or	units at the s ne row to sur	source. If there are multiple nmarize the identical units.		6. Emergency /
1. Combustion Unit Type	2. Number of Identical Units	3. Unit ID(s)	4. Date of Installation or Modification (actual or anticipated)	5. Heat Input Rate of each unit (MMBtu/hr)	Back-Up Unit?
See Table 20					☐ Yes ☐ No
See Table 20					☐ Yes ☐ No
					☐ Yes ☐ No
					☐ Yes ☐ No
					Yes No
					☐ Yes ☐ No
					☐ Yes ☐ N
					☐ Yes ☐ N
					☐ Yes ☐ N
					☐ Yes ☐ N
					☐ Yes ☐ N
					☐ Yes ☐ N



# OAQ PROCESS INFORMATION APPLICATION PI-02B: Combustion – Boilers, Process Heaters & Furnaces

State Form 52536 (R2 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch

100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or

Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 www.IN.gov/idem

- The purpose of this form is to specify details that pertain only to boilers, process heaters and furnaces.
- For the purposes of this form, a process heater is any combustion unit that provides heat directly or indirectly to the process.
- Complete one PI-02B form for each emissions unit. If there are multiple emission units that are identical in nature, capacity, and
  use, you may use one PI-02B form to summarize the units.
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality.
   Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for anyone to inspect and photocopy.

art A specifies operating information of terminology are in	nation that is unique to boilers, noluded in the instructions for th	process heaters and furnaces. Defining form.	
Unit ID: See Table 20			
Type of Combustion Unit	☐ Industrial Boiler	☐ Commercial Bo	
☐ Boiler: ☐ Process Heater:	☐ Institutional Boiler ☐ Dutch Oven ☐ Fuel Cell	☐ Horseshoe Boli ☐ Drying Oven ☐ Space Heater	
☐ Furnace:	☐ Crucible ☐ Cupola ☐ Electric Induction ☐ Open Hearth, Oxygen La	☐ Crucible Pot ☐ Electric Arc ☐ Open Hearth ☐ Pot ☐ Sweat	
3. Combustion Process  ☐ Cyclone Burner ☐ Overfeed Stoker / Trav ☐ Spreader Stoker  4. Heat Transfer Method:	☐ Fluidized Bed	Dry Bottom Pulverized –  toker Other (specify)	Wet Bottom
4. Heat Transfer Metriou.  5. Transfer Surface     Arrangement     (check all that apply):  6. Firing Configuration:	☐ Horizontal ☐	Straight  Bent Tube  ☐ Fluidized Bed Combustor  ☐ Normal ☐ Tangential	☐ Front Wall
7. Heat Transfer Method (process heaters only):	☐ Direct ☐ Indirec	et	

	PART B: Emission Controls and Li	
rt B identifies control technology, c	control techniques or other process lir	mitations that impact air emissions.
Add-On Control Technology: lo	dentify all control technologies used for th	is process. Attach completed CE-01 (unless "none").
<ul> <li>None</li> <li>Baghouse / Fabric Filter − Attach</li> <li>Electrostatic Precipitator − Attach</li> <li>NO<sub>X</sub> Reduction − Attach CE-09.</li> <li>Control Techniques: Identify and None (explain):</li> <li>Ammonia Injection</li> <li>Burners Out Of Service</li> <li>Flyash Reinjection</li> <li>Low Excess Air</li> <li>Reburn</li> <li>Staged Combustion</li> <li>Process Limitations / Addition</li> </ul>	Cycle tach CE-02.	one — Attach CE-03.  orption / Wet Collector / Scrubber — Attach CE-05.  or (specify): — Attach CE-10.  cess.  Burning Oil / Water Emulsions  Flue Gas Recirculation  Load Reduction  Overfire Air  Spray Drying  — Attach completed GSD-09.
information if necessary.		
information if necessary.  Part C identifies all boilers that we	PART C: Previously Installe ere installed prior to submitting this ap	d Boilers oplication.
Part C identifies all boilers that we	PART C: Previously Installe ere installed prior to submitting this ap stalled Boilers present at this source	d Boilers plication
Part C identifies all boilers that we   12. Are there any Previously Ins.  No – Proceed to Part D.	PART C: Previously Installe ere installed prior to submitting this ap stalled Boilers present at this source	d Boilers oplication.
Part C identifies all boilers that we  12. Are there any Previously Ins  ☑ No – Proceed to Part D.  ☐ Yes → ☐ Information	PART C: Previously Installe ere installed prior to submitting this apstalled Boilers present at this source attached.   Information is con	d Boilers  plication ?  tained in operating permit:
Part C identifies all boilers that we  12. Are there any Previously Ins  ☑ No – Proceed to Part D.  ☐ Yes → ☐ Information	PART C: Previously Installe ere installed prior to submitting this apstalled Boilers present at this source attached.   Information is con PART D: Furnace Defain only to furnaces. If there are no fi	d Boilers pplication. ? tained in operating permit: tails urnaces identified with this application, completio
Part C identifies all boilers that we  12. Are there any Previously Ins  ☑ No – Proceed to Part D.  ☐ Yes → ☐ Information  Part D identifies details that perta of this table is not required.	PART C: Previously Installed ere installed prior to submitting this apstalled Boilers present at this source attached. Information is con PART D: Furnace Defain only to furnaces. If there are no fi	d Boilers oplication. ? tained in operating permit: tails urnaces identified with this application, completio
Part C identifies all boilers that we  12. Are there any Previously Ins  ☑ No – Proceed to Part D.  ☐ Yes → ☐ Information  Part D identifies details that perta of this table is not required.	PART C: Previously Installe ere installed prior to submitting this apstalled Boilers present at this source attached.   Information is con PART D: Furnace Defain only to furnaces. If there are no fi	d Boilers oplication. ? tained in operating permit: tails urnaces identified with this application, completio
Part C identifies all boilers that we  12. Are there any Previously Ins  ☑ No – Proceed to Part D.  ☐ Yes → ☐ Information  Part D identifies details that perts of this table is not required.  13. Material Melted:  14. Maximum Melt Rate (specify 15. Flux Type:	PART C: Previously Installed are installed prior to submitting this are stalled Boilers present at this source attached.   Information is con PART D: Furnace Detain only to furnaces. If there are no furnation is confident to furnaces.	d Boilers oplication. ? tained in operating permit: tails urnaces identified with this application, completio
Part C identifies all boilers that we  12. Are there any Previously Ins  ☑ No – Proceed to Part D.  ☐ Yes → ☐ Information  Part D identifies details that perts of this table is not required.  13. Material Melted:  14. Maximum Melt Rate (specify)	PART C: Previously Installed are installed prior to submitting this apstalled Boilers present at this source attached.   Information is compart D: Furnace Detain only to furnaces. If there are no furnits):	d Boilers oplication. ? Itained in operating permit: tails urnaces identified with this application, completion



# OAQ PROCESS INFORMATION APPLICATION PI-02C: Combustion – Turbines & Reciprocating Internal Combustion Engines

State Form 52537 (R2 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 www.IN.gov/idem

NOTES:

- The purpose of this form is to specify details that pertain only to turbines and internal combustion engines.
- Complete one PI-02C form for each emissions unit. If there are multiple emission units that are identical in nature, capacity, and use, you may use one PI-02C form to summarize the units.
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for anyone to inspect and photocopy.

. Unit ID: See Table 20	nation that is unique to turbines and recipiocating inter- nation of terminology are included in the instructions for this form.
Type of Combustion Unit	
	☐ Simple Cycle
	Regenerative Cycle
Turbine:	☐ Cogeneration
	Combined Cycle
	2-stroke lean-burn
Reciprocating Internal	4-stroke lean-burn
Combustion Engine:	4-stroke rich-burn
	☐ Diffusion Flame Combustion
3. Combustion Process:	☐ Lean-Premix Staged Combustion
	☐ Spark
4. Ignition Type:	Compression
	horsepower (hp)
5. Power Output:	megawatts (MW)
6. Duty Cycle:	hours per year (hr/yr)
	☐ Natural Gas Only
7. Fuel Used:	☐ Other — Attach completed PI-02F.  unit supply power to an emergency generator? ☐ Yes ☐ No

This space was intentionally left blank.

Add On Control Technology: Identify all control technology	nologies used for this process. Attach completed CE-01 (unless "none").
Add-On Control Technology: Identify all control techniques on None  Catalytic Oxidation — Attach CE-06 Other (specify): Control Techniques: Identify all control techniques None (explain): Air-To-Fuel Ratio Adjustments Boiling Point adjusted to 10% and 90% Charge Cooling Derating Exhaust Gas Recirculation Fuel Injection Pressure Injection Timing Retard Lean Combustion Oil Consumption Control Rapid Spill Nozzles Two Stage Lean / Lean Combustion Water/Fuel Emulsions	nologies used for this process. Attach completed CE-01 (unless none)  NO <sub>X</sub> Reduction – Attach CE-09  – Attach CE-10.

# PI-02F: Combustion - Fuel Use

# OAQ PROCESS INFORMATION APPLICATION

State Form 52540 (R2 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 IDEM - Office of Air Quality - Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 www.IN.gov/idem

Complete one form PI-02F for each combustion unit. If the unit has any capability of using a fuel, even if on a backup or intermittent basis, complete the applicable section. Using a The purpose of this form is to identify each fuel that will be used in the combustion unit. Definitions and additional explanation of terminology are included in the instructions for this

fuel that is not specified in the permit is a violation of the permit.

NOTES:

Detailed instructions for this form are available on the Air Permit Application Forms website.

All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims of confidentiality must be made at the time the information becoming information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. a public record, available for anyone to inspect and photocopy.

PART A: Process Unit Identification

Part B identifies the gaseous lucis triat with 50 care.  2. Fuel Type:    Dercent of Fuel Use   4. Print	uel Use 4. Primary or Secor			
(by volume) stroleum Gas - Propane Propane (HD-5)		ndary Fuel?	Primary or Secondary Fuel? 5. Component Percentages:	6. Heating value:
<ul> <li>□ Natural Gas</li> <li>□ Liquefied Petroleum Gas</li> <li>□ Commercial- Propane</li> <li>□ Engine Fuel Propane (HD-5)</li> </ul>	\range and	Secondary	Sulfur.	(Btu/ft³)
☐ Liquefied Petroleum Gas ☐ Commercial- Propane ☐ Engine Fuel Propane (HD-5)		1	9	
☐ Liquelled redución Cac ☐ Commercial- Propane ☐ Engine Fuel Propane (HD-5)			Sulfur.	(Rt11/ff <sup>3</sup> )
☐ Commercial- Propaire ☐ Engine Fuel Propane (HD-5)	Primary	Secondary	Butane:	()
Engine Fuer Propare (***)		į	Propane:	
				(D4,,/# <sup>3</sup> )
Commercial- Butane	- Viewing	Secondary	Sulfur.	(Dimir)
Process Gas *				(Btu/ft³)
	Primary	Secondary	Sulfur:	
Landfill Gas *		İ		(Btu/ff³)
Other Consolination	☐ Primary ☐	Secondary		
Other (specify):				
* Indicate the source of the process or landfill gas:	ndfill gas:			

Process Information - Umbustion FORM PI-02F Page 2 of 4

Indiana Dt., ument Of Environmental Management Office Of Air Quality State Form 52540 (R2 / 1-10)

		PART C: Liquid Fuels	5		
Part C identifies the liquid fuels that will be used in the combustion unit.	nat will be used in the combus	stion unit.		44 Cleoding Value	12 Percent Heat:
7. Fuel Type:	8. Percent of Fuel Use (by volume)	9. Primary or Secondary Fuel?	10. Component Percentages:	11, meaning value.	
☐ Residual Fuel Oil ☐ No. 5 – Heavy ☐ No. 5 – Light	See Table 20	☐ Primary ☐ Secondary	Sulfur:	(Btu/gal)	
☐ No. 6 (Bunker C) ☐ Distillate Fuel Oil ☐ No. 1 ☐ No. 2 (Diesel)		☐ Primary ☐ Secondary	Sulfur:	(Btu/gal)	
□ №. 4 □ Gasoline		☐ Primary ☐ Secondary	Sulfur:	(Btu/gal)	
□ Waste Oil		☐ Primary ☐ Secondary	Sulfur: Ash: Lead	(Btu/gal)	
☐ Liquid Waste *		☐ Primary ☐ Secondary	Sulfur: Fluorine: Chlorine:	(Btu/gal)	
Other (specify):		☐ Primary ☐ Secondary		(Btu/gal)	
* RCRA alpha-numeri	* RCRA alpha-numeric codes for Special or Hazardous Waste to be Burned:	dous Waste to be Burned:			

This space was intentionally left blank.

Process Information Abustion FORM PI-02F Page 3 of 4

Indiana Department Of Environmental Management Office Of Air Quality State Form 52540 (R2 / 1-10)

		PART D1: Solid Fuels - Coal	Coal		
in the used in the training of coal that will be used in the	coal that will be used in the c	combustion unit.			.01000
Part D1 Identifies all variations of	14. Percent of Fuel Use	15. Primary of	16. Component Percentages:	17. Heating Value:	10, 02013.
13. Fuel Type:	(by volume)	Secondary ruers			
☐ Anthracite Coal	See Table 20	☐ Primary	Sulfur: Ash:	(Btu/lb)	☐ Dry ☐ Moist
☐ Anthracite		☐ Secondary	Moisture:		
Culm			Sulfur:		:
		☐ Primary	Ash:	(Btu/lb)	Dry Moist
☐ Bituminous Coal		☐ Secondary	Moisture:		
			Sulfur.		<u> </u>
		☐ Primary	Ash:	(Btu/lb)	
Sub-bituminous Coal		☐ Secondary	Moisture:		
			Sulfur:		Moist
		☐ Primary	Ash:	(Btu/lb)	
☐ Lignite Coal		Secondary	Moisture:		
			Sulfur:	(4), .44)	
		Primary	Ash	(aluna)	] ]
□ Coke		Secondary	Moisture:		
			Sulfur:	1000	☐ Drv ☐ Moist
		Primary	Ash:	(BtWgal)	
Other Coal (specify):		☐ Secondary	Moisture:		

This space was intentionally left blank.

Process Information hbustion FORM PI-02F Page 4 of 4

> Indiana Department Of Environmental Management Office Of Air Quality State Form 52540 (R2 / 1-10)

		PART D2: Other Solid Fuels	-uels		
or no identifies the solid fuels, other than coal, that will l	other than coal, that will be us	be used in the combustion unit.			o. Doctor Dost
19. Fuel Type:	20. Percent of Fuel Use	21. Primary or Secondary Fuel?	22. Component Percentages:	23. Heating Value:	Z4. Peloeminous
☐ Wood or Wood Waste	See Table 20	☐ Primary☐ Secondary	Moisture:	(Btu/ton)	
Wood Residue Crity  Wood and Wood Residue			Suffer		
☐ Tires or Tire Derived Fuel ☐ Whole Tires		☐ Primary ☐ Secondary	Chromium:	(Btu/lb)	
☐ Tire Derived Fuel			Ach:	(A), 100	
Bagasse		☐ Primary ☐ Secondary	Moisture:	(BtW/D)	
		Primary		(Btu/lb)	
Solid Waste *		Secondary			
		☐ Primary		(Btu/lb)	
Other (specify):		Secondary			
*RCRA alpha-numeric	*RCRA alpha-numeric codes for Special or Hazardous Waste to be Burned.	lous Waste to be Burned.			

n unit.	
ations combustio	
PART E: Fuel Consumption Limitations in limitations that are acceptable for the combu	
ol Consum at are accep	
ART E: Fue	
eumption lin	
ly fuel cons	
specify an	
PART E: Fuel Consumption Limitations Use the space provided to specify any fuel consumption limitations that are acceptable for the combustion unit.	
the space	
Use	



# OAQ PROCESS INFORMATION APPLICATION PI-02G: Combustion – Emission Factors

State Form 52541 (R2 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch

100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana)

Facsimile Number: (317) 232-6749 www.IN.gov/idem

### NOTES:

- The purpose of this form is to specify the emission factors used to calculate potential to emit from the combustion unit.
- Complete one PI-02G form for each emissions unit. If there are multiple emission units that are identical in nature, capacity, and use, you may use one PI-02G form to summarize the units.
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for anyone to inspect and photocopy.

	Emission Factors			
s table identifies all emission factors used to ca	lculate air emissions from th	e combustion unit		
Unit ID: See Table 20				
Air Pollutant:	3. Emission Fact	or 4. Source ( if not using	of Emission F g AP-42, include c	actor alculations
A A A A A A A A A A A A A A A A A A A	value units	☐ AP-42	☐ Other	□ N/
Carbon Monoxide (CO) Lead (Pb)		☐ AP-42	Other	N/
Hazardous Air Pollutant (HAP) (specify):		☐ AP-42	Other	
Nitrogen Oxides (NO <sub>x</sub> )		☐ AP-42	☐ Other☐ Other☐	N.
Mercury (Hg)		☐ AP-42	Other	N
Particulate Matter (PM)		☐ AP-42	Other	□N
Particulate Matter less than 10μm (PM <sub>10</sub> )  Particulate Matter less than 2.5μm (PM <sub>2.5</sub> )		☐ AP-42	☐ Other	
Sulfur Dioxide (SO <sub>2</sub> )		☐ AP-42	Other	
Volatile Organic Compounds (VOC)		☐ AP-42	Other	
Other (specify):		☐ AP-42	Other	<u> </u>
Other (specify):		☐ AP-42	☐ Other☐ Other☐	<u>'                                    </u>
Other (specify):		☐ AP-42	LJ Other	<u></u>

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# OAQ PROCESS INFORMATION APPLICATION PI-02H: Combustion – Federal Rule Applicability

State Form 52542 (R2 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 www.IN.gov/idem

- The purpose of this form is to identify any federal rules that apply to the emission unit.
- Complete one PI-02H form for each emissions unit. If there are multiple emission units that are identical in nature, capacity, and use, you may use one PI-02H form to summarize the units.
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for anyone to inspect and photocopy.

	Federal Rule Applicability	
is table identifies any federal rules that apply Is a <b>New Source Performance Standard</b> If yes, attach a completed FED-01 for each rule	(NSPS) applicable to this source?   ☐ Yes ☐ No	2. Unit IDs
40 CFR Part 60, Subpart Cb	Large Municipal Waste Combustors (constructed before 9/20/1994)	
☐ 40 CFR Part 60, Subpart Ce	Hospital/Medical/Infectious Waste Incinerators	
40 CFR Part 60, Subpart D	Fossil-Fuel-Fired Steam Generators (constructed after 8/17/1971)	· ·
☐ 40 CFR Part 60, Subpart Da	Electric Utility Steam Generating Units (constructed after 9/18/1978)	EU-2001/4,
☑ 40 CFR Part 60, Subpart Db	Industrial-Commercial-Institutional Generating Units	EU-7001/2
	Small Industrial-Commercial-Institutional Generating Units	EU-6000, EU- 2002/3
☐ 40 CFR Part 60, Subpart E	Incinerators	
40 CFR Part 60, Subpart Ea	Municipal Waste Combustors (constructed after 12/20/1989 and before 9/20/1994)	
☐ 40 CFR Part 60, Subpart Eb	Large Municipal Waste Combustors (constructed after 9/20/1994 or modified / reconstructed after 6/19/1996)	*
☐ 40 CFR Part 60, Subpart Ec	Hospital/Medical/Infectious Waste Incinerators (constructed after 6/20/1996)	
☐ 40 CFR Part 60, Subpart O	Sewage Treatment Plants (sludge burners)	FU-1003/5/6/
☑ 40 CFR Part 60, Subpart Y	Coal Preparation Plants	EO-1003/3/0/
☐ 40 CFR Part 60, Subpart GG	Stationary Gas Turbines	
☐ 40 CFR Part 60, Subpart AAA	New Residential Wood Heaters	
40 CFR Part 60, Subpart AAAA	Small Municipal Waste Combustion Units (constructed after 8/30/1999 or modified / reconstructed after 6/6/2001)	
☐ 40 CFR Part 60, Subpart BBBB	Small Municipal Waste Combustion Units (constructed on or before 8/30/1999)	-
☐ 40 CFR Part 60, Subpart CCCC	Commercial and Industrial Solid Waste Incineration Units (constructed after 11/30/1999 or modified / reconstructed after 6/1/2001)	
☐ 40 CFR Part 60, Subpart DDDD	Commercial and Industrial Solid Waste Incineration Units (constructed on or before 11/30/1999)	
☐ 40 CFR Part 60, Subpart KKKK	Stationary Combustion Turbines	

Is a National Emission Standard for Ha applicable to this source? If yes, attach a completed FED-01 for each ru	le that applies.	4. Unit IDs
☐ 40 CFR Part 63, Subpart MM	Combustion Sources at Kraft, Soda, and Sulfite Pulp & Paper Mills	
40 CFR Part 63, Subpart EEE	Hazardous Waste Combustion	
40 CFR Part 63, Subpart YYYY	Stationary Combustion Turbines	EU-6006/8
☑ 40 CFR Part 63, Subpart ZZZZ	Reciprocating Internal Combustion Engines (RICE)	EU-6000, EU
☑ 40 CFR Part 63, Subpart DDDDD	Industrial, Commercial, and Institutional Boilers and Process Heaters	2001/2/3/4 EU-7001/2
<ul> <li>Non-Applicability Determination: Prov the rule title or the source category), but</li> </ul>	ide an explanation if the process unit appears subject to a r the rule will not apply.	
	ı	

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# OAQ PROCESS INFORMATION APPLICATION PI-03: Storage & Handling of Bulk Material

State Form 52543 (R2 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch

100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana)

Facsimile Number: (317) 232-6749 www.lN.gov/idem

- The purpose of this form is to obtain detailed information about the storage and handling of bulk materials. Complete one form for each process (or group of identical processes). Use additional forms if necessary. This is a required form.
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality.

  Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for express to inspect and photocopy. available for anyone to inspect and photocopy.

art A identifies all proc ocess units that are id . Equipment / Component Type	2. Unit ID	3. Number of Identical Units	4. Installation Date (see instructions)	5.	Material Handled/ Stored	6. Maximum Materia Throughput Rate (tons/year)
See Table 21						
						atod CE-01 (unless "none
Add-On Control	Technology:	Identify all control tech	nologies used for th	us uni	i, and allacir comple	eted CE-01 (unless "none
	recipitator – A	ttach CE-02. Attach CE-04.				/ Scrubber – Attach CE-05 – Attach CE-1
	. 05.07		☐ Othe	r (spe	ecify):	/ Scrubber — Attach CE-0
☐ Adsorber – Att	ach CE-07.  pues: Identify  tions / Addit	Attach CE-04.	☐ Othe	r (spe	ecify): for the process.	– Attach CE-1
Adsorber – Att  Control Techniq  Process Limita	ach CE-07.  pues: Identify  tions / Addit	Attach CE-04. any other air emissio	☐ Othe	r (spe	ecify): for the process.	– Attach CE-1

nd/or handled in this	process.						ch material stored
0. Material Handled/Stored (from table above)	11. Metho Hand		12. Type of Storage	13. Storage Capaci (tons)	·		ent Content
ee Table 21							
			PART C	: Emission Fa	ctors		
Part C identifies all er	mission fact	ors us	ed to calculate a	ir emissions f	rom the proces	s units listed on t	nis form.
17. Process Equipm		TO 1000 - 00 PA	ir Pollutant		ssion Factor	20 Source of I	Emission Factor P-42, include calculations)
(complete for all units Part A of this form)	listed in			value	units	(If not using Ar	42, IIIClude Calculations)
Part A Or Bils John)		Р	M			☐ AP-42	Other
100,		Р	M-10			☐ AP-42	Other
						☐ AP-42	Other
		^				☐ AP-42	Other
					- nlicobility		
	Endoral mile	se that	at the section and the second section is	ederal Rule A	ppileability		
Part D identifies any  21. Is a New Source					this source?		☐ Yes ☐ No
21. Is a New Source If yes, attach a co	mpleted FEL	0-01 for	each rule mar app	0/100.			
40 CFR Par	t 60, Subpa	ırt CC		s Manufacturir	ng Plants		
☐ 40 CFR Par				Elevators	Diamete		
☐ 40 CFR Par				Manufacturin		te	
40 CFR Par					ocessing Plant	ಣ Roofing Manufact	ure
40 CFR Par					ral Processing		
40 CFR Pai			_		ers in Mineral I		
40 CFR Pai	rt 60, Subp	art UUI					☐ Yes ☐ No
	mission Si attach a con	andar ipleted	FED-01 for each i	rule that applies			
00 to a National E							
22. Is a National E source? If yes,	rt <u>61</u> , Subp			cifvi)			
22. Is a National E source? If yes,  40 CFR Pa	462 Subn	art	(Spec	Jily).			to a rule (based on th



# OAQ PROCESS INFORMATION APPLICATION PI-14: Volatile Organic Liquid Compound Storage

State Form 52554 (R2 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana)

Facsimile Number: (317) 232-6749 www.IN.gov/idem

- The purpose of this form is to obtain detailed information about all tanks larger than 250 gallons that are used to store volatile organic liquid compounds. Duplicate this form as necessary.
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. All information submitted to IDEM will be made available to the public unless it is submitted to IDEM, and must follow the requirements set out Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for anyone to inspect and photocopy.

cternal Floatin	g Roof, Domed g Roof, Not Domed ] No ] Vertical	☐ Internal Floating ☐ Variable Vapor S ☐ Pressure Tank	
es	g Roof, Not Domed	☐ Variable Vapor S	
es	g Roof, Not Domed	☐ Variable Vapor S	
es	g Roof, Not Domed	☐ Variable Vapor S	
es [	] No		ppace
		☐ Pressure Tank	
orizontal [	] Vertical		
		100	
pounds pe	r square inch (psi at 20	9°C)	
gallons (b/	lbmole)	140	
gallons pe	r year (gal/yr)		
Submerged	☐ Not Submerged	Other (specify):	
B: Emission (	Controls and Limital	nons and that impact air emi	issions
techniques or	other process inflication	JUS mar impact dir sim	OF 04 (unloss "nono"
all control techni	ologies used for this unit	t, and attach completed C	_E-01 (unless none ,
pecify):			- Attach CE-10.
ol techniques u	ised for this process.		
	☐ Vapor Red	covery System	
t /	gallons (b/gallons per ubmerged  3: Emission (echniques or ll control techniques to pecify):  I techniques to	gallons (b/lbmole) gallons per year (gal/yr)  ubmerged	gallons (b/lbmole) gallons per year (gal/yr)  submerged Not Submerged Other (specify):  3: Emission Controls and Limitations echniques or other process limitations that impact air emill control technologies used for this unit, and attach completed (specify):

□ N/A

Other

☐ Other

Other

☐ AP-42

☐ AP-42

☐ AP-42

Volatile Organic Compounds (VOC)

Other (specify):

Other (specify):

PART C: Informatio	n Specific to Tank Type
Part C identifies the physical properties of the tank.	
17. Tank Diameter (D): See Table 22	
18. Tank Height (Hs): feet (ft)	
19. Tank Volume / Capacity (V): gallons (gallons (gallons )	al) cubic feet (ft³)
20. Maximum Liquid Height (HIX): feet (ft)	
21. External Floating Roof: Complete only if applicable.	
a. Average Liquid Density (WI): pounds pe	er gallon ( <i>lb/gal</i> )
b. Roof Type: ☐ Pontoon Floati	ng Roof
c. Tank Construction: ☐ Welded	☐ Riveted
d. Primary Rim Seal: Uapor Mounted	d
e. Secondary Rim Seal:   Weather Shiele	d Rim Mounted None
22. Internal Floating Roof: Complete only if applicable.	
a. Average Liquid Density (WI):	pounds per gallon ( <i>lb/gal</i> )
b. Roof Type	☐ Double Deck Floating Roof ☐ Other: (specify)
c. Self-supported fixed roof	☐ Yes ☐ No
d. Number of columns supporting the fixed roof	
e. Deck Construction:	☐ Welded ☐ Riveted ☐ Bolted
f. Primary Rim Seal:	☐ Vapor Mounted ☐ Liquid Mounted
g. Is there a Secondary Rim Seal?	☐ Yes ☐ No
23. Variable Vapor Space: Complete only if applicable.	
a. Volume of liquid pumped into the system (V1):	gallons per year (gal/yr)
b. Volume expansion capacity of system (V2):	gallons (gal)
c. Number of Transfers Into the System (N2)	per year (/yr)
PART N.	mission Factors
Part D identifies all emission factors used to calculate air	
24. Air Pollutant:	25. Emission Factor 26. Source of Emission Factor
	value units (if not using AP-42, include calculations)
Hazardous Air Pollutant (HAP): (specify):	☐ AP-42 ☐ Other ☐ N/A

PAR	T E: Federal Rule Applicability	
Part E identifies any federal rules that apply to	the process.	
27. is a New Source Performance Standard If yes, attach a completed FED-01 for each rule	(NSPS) applicable to this source? ☐ Yes ☐ No	28. Unit ID:
☐ 40 CFR Part 60, Subpart K	Petroleum Liquid Storage Vessels (constructed after 6/11/1973 and before 5/19/1978)	
☐ 40 CFR Part 60, Subpart Ka	Petroleum Liquid Storage Vessels (constructed after 5/18/1978 and before 7/23/1984)	
☐ 40 CFR Part 60, Subpart Kb	Volatile Organic Liquid Storage Vessels, Including Petroleum Liquid Storage (constructed after 7/23/1984)	
40 CFR Part 60, Subpart VV	Equipment Leaks of VOC in the Synthetic Organic Chemicals Manufacturing Industry	
☐ 40 CFR Part 60, Subpart GGG	Equipment Leaks of VOC in Petroleum Refineries	
☐ 40 CFR Part 60, Subpart KKK	Equipment Leaks of VOC from On-Shore Natural Gas Processing Plants	
29. Is a National Emission Standard for Hazapplicable to this source? If yes, attach a co	zardous Air Pollutants (NESHAP)  completed FED-01 for each rule that applies.	30. Unit ID:
☐ 40 CFR Part 61, Subpart J	Equipment Leaks (Fugitive Emission Sources) of Benzene	
☐ 40 CFR Part 61, Subpart V	Equipment Leaks (Fugitive Emission Sources)	
☐ 40 CFR Part 61, Subpart Y	Benzene Emissions from Benzene Storage Vessels	
☐ 40 CFR Part 63, Subpart R	Gasoline Distribution (Bulk Gasoline Terminals and Pipeline Breakout Stations)	
40 CFR Part 63, Subpart CC	Petroleum Refineries	
☐ 40 CFR Part 63, Subpart HHH	Natural Gas Transmission and Storage	
☐ 40 CFR Part 63, Subpart EEEE	Organic Liquids Distribution (non-gasoline)	
31. Non-Applicability Determination: Provident the rule title or the source category), but to	de an explanation if the process unit appears subject to a r he rule will not apply.	ule (based on



## **OAQ PROCESS INFORMATION APPLICATION** PI-18: Mineral Processing

State Form 52559 (R2 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch 100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 4620-2251 Telephone: (317) 233-0178 or Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 www.IN.gov/idem

NOTES:

- The purpose of this form is to obtain detailed information about non-metallic mineral processes such as sand and gravel processes, stone quarries, stone processing plants, and slag and kish handing plants. Complete one form for each process material, and duplicate this form as necessary for additional process materials. This is a required form.
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC 17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record, available for anyone to inspect and photocopy.

					eral Process I			5,1,5-15		The groups	
Part A identifies the							cluding co allic Miner		rs, screen	s, crusn	iers, etc.
1. Type of Proces	ss Materia	1: 1	⊠ Non-Me	Hamo	Minerais	☐ Mere	HIIC MILICI	ais		- Tr	
2. Equipment / Process Unit	3. Numb Ident Units	ical	4. Unit ID	5.	Installation Date	6. Open Encid	osed?		Maximun Capacity (tons/hr)	,   . (	Actual Capacity tons/hr)
See Table 23						☐ Open [	☐ Enclosed	Ł			
					A. Marine Control of the Control of	☐ Open !	☐ Enclosed	E			
						☐ Open	☐ Enclosed	d			
			***************************************			☐ Open	☐ Enclosed	d			
						☐ Open	☐ Enclosed	d			
						☐ Open	☐ Enclosed	Enclosed			
	ا حادمالم ا				T B: Dryer Det	ails					
Part B identifies th  9. Dryer 10.U Type:		11.Instal Date		12.P P D	Plate Perforation Diameter / Mesh Size Inches or mm)	13.Volun Capac (ft³)		4.Heat Capa (mmBi	acity	5.Fuel l	Jsed
										Natural G Other – A	ias Only Attach PI-02
										Natural G	Gas Only

Natural Gas Only Other - Attach PI-02F Natural Gas Only Other - Attach PI-02F

PART C: Storage and Handling of Materials								
Part C identifies the details pertaining to aggregate storage and handling.								
16.Material Size & Specification	17.Type of Storage	18.Storage Capacity (tons)	19.Unit ID	20.Installation Date	21.Storage Open or Totally Enclosed/ Covered?			
See Table 23					☐ Open ☐ Enclosed ☐ Covered			
ALL MARKONINI T. T. L.			A A A A A A A A A A A A A A A A A A A		☐ Open ☐ Enclosed ☐ Covered			
1.4.4.000000000000000000000000000000000					☐ Open ☐ Enclosed ☐ Covered			
A Administrative v			}		☐ Open ☐ Enclosed ☐ Covered			

Part D identifies all e PI-02 forms to provid	PAR mission factors used to calcula le the applicable information fo	D: Emission Factors     ate air emissions from the product the dryers.	cess units listed on t	this form. Use the
22.Process Unit (& ID, if applicable)	23.Air Pollutant	24.Emission Factor	25. Source of Emission Factor (if not using AP-42, include calculations)	
		value units	1,110,031,9	
	PM		☐ AP-42	Other
	PM-10		☐ AP-42	☐ Other
	NO <sub>X</sub>		☐ AP-42	Other
	СО		☐ AP-42	☐ Other
	Metals		☐ AP-42	Other
	Organics		☐ AP-42	☐ Other
	Other (specify):		☐ AP-42	☐ Other
	Other (specify):		☐ AP-42	☐ Other

This space was intentionally left blank.

PART E: En	nission Controls and Limitations
Part E identifies the control technologies, techniq Use the PI-02 forms to provide the applicable inf	ues, and other process limitations corresponding to each process. ormation for the dryers.
26.Add-On Control Technology: Identify all cont	trol technologies used for this unit, and attach completed CE-01 (unless "none").
Storage	Handling
☐ None	□ None
☐ Baghouse / Fabric Filter – Attach CE-02.	☐ Baghouse / Fabric Filter — Attach CE-02.
Cyclone – Attach CE-03.	Cyclone — Attach CE-03.
☐ Electrostatic Precipitator — Attach CE-04.	☐ Electrostatic Precipitator – Attach CE-04.
Other (specify): Atta	ach CE-10. Other (specify): Attach CE-10.
27.Control Techniques: Identify all control tech	niques used for this process.
Storage	Handling
28.Process Limitations / Additional Informations / Identify any acceptable process limitations.	
Storage	Handling
PART	F: Federal Rule Applicability
	ne process. Use the PI-02 forms to provide the applicable information
29.ls a New Source Performance Standard (N If yes, attach a completed FED-01 for each rule th	
☐ 40 CFR Part 60, Subpart OOO	Non-Metallic Mineral Processing Plants
☐ 40 CFR Part 60, Subpart UUU	Calciners and Dryers in Mineral Industries
☐ 40 CFR Part 60, Subpart	(Specify)
30.ls a National Emission Standard for Hazar source? If yes, attach a completed FED-01 for e	dous Air Pollutants (NESHAP) applicable to this
☐ 40 CFR Part <u>61</u> , Subpart	(Specify)
☐ 40 CFR Part <u>63</u> , Subpart	(Specify)
	an explanation if the process unit appears subject to a rule (based on
the rule title or the source category), but the	rule will not apply.



# OAQ FEDERAL RULE INCORPORATION APPLICATION FED-02: MACT Pre-Construction Review

State Form 51905 (R2 / 1-10)
INDIANA DEPARTMENT OF ENVIRONMENTAL MANAGEMENT

IDEM - Office of Air Quality - Permits Branch

100 N. Senate Avenue, MC 61-53 Room 1003 Indianapolis, IN 46204-2251 Telephone: (317) 233-0178 or

Toll Free: 1-800-451-6027 x30178 (within Indiana) Facsimile Number: (317) 232-6749 www.IN.gov/idem

NOTES:

- The purpose of this form is to provide a standardized way for sources to request MACT preconstruction approval per 40 CFR 63.5.
- This is a required form for sources subject to the MACT pre-construction review requirements in 40 CFR 63.5.
- Detailed instructions for this form are available on the Air Permit Application Forms website.
- All information submitted to IDEM will be made available to the public unless it is submitted under a claim of confidentiality. Claims
  of confidentiality must be made at the time the information is submitted to IDEM, and must follow the requirements set out in 326 IAC
  17.1-4-1. Failure to follow these requirements exactly will result in your information becoming a public record.

•	Part A: General Informatio	n	
Part A identifie General Provis	s the applicable MACT standard and affected source, and clions is applicable to the affected source.	letermines whether 40 CF	
1. MACT Sub	FFFF for Organic Liquids Distribu	tion (Non-Gasoline), and [ rs,and Process Heaters)	ODDDD (Industrial,
MACT So	irce Category Name:		
2. Affected S	1 30,773, 4111	age Tanks	
DDDDD: F Fractionati	ackage Boiler, Coal Drying Heater, Feed Heater, Treat GA onator Feed Heater	s Heater, Vacuum Columr	i Feed Heater, and
3 Will the n	roposed construction be a major source of HAP emissi	ons? ⊠ Yes □ N	lo
J. Will the p			
	Part B: Emissions Unit Inforr	nation	v racanstructed
Part B identifi	es those emissions units that are part of the affected source	e and will be constructed t	ir reconstructed.
4. Unit ID:	5. HAP Name or Type of HAP	6. Quantity of HAP Er	
		Actual Emissions	Potential To Emit
See Table			
24			
· .			
l .			

	Part C: Compliance Methods for New Affected Sources	
Part C identifie	es the compliance method chosen for each new affected source.	
7. Unit ID:	8. Compliance Method Description	9. Control Efficiency (%)
See Table		
24		

NA		

Indiana Department Of Environmental Management Office of Air Quality State Form 51905 (R2 / 1-10) Attachment B. IDEM Air Permit Application Associated Tables

Table 1. Preliminary Summary of Riverview Energy Facilitywide Potential Emissions

#### **Controlled PTE Emissions**

Controlled PTE Emissions												1 10 11 11 11		74.2-4 K N	Lea		C	02	Total	CO2e	H/	APs
	NO	v	С	ю.	S	02	1	SP	PN	и10		12.5	VOC/NI		(lb/hr)	(tons/yr)	(lb/hr)	(tons/yr)	(lb/hr)	(tons/yr)	(lb/hr)	(tons/yr)
Category	(lb/hr)	(tons/yr)	(lb/hr)	(tons/yr)	2.40E-04	1.05E-03	58433	255937	58629	256794	15.71	5.82										
C. L. C. Li Constant Property	27.98	122,49	18.15	79.44	26.86	117.64	3.91	17.14	3.83	16.80	3.72	16.31	112.51	66.11		0.00	3898	238	3934	241	0.39	0.04
Veba Combi Cracker Process	42.65	2.58	2.35	0.14	0.63	0.04	1.07	0.06	1.07	0.06	1.07	0.06	0.86	0.05	0.00	0.00	451256	1976503	451823	1978988	5.90	25.82
Emergency Equipment	11.34	49.68	38.06	166.73	0.56	2.44	10.11	44.32	10.11	44.32	10.11	44.32	16.42	71.94	0.00		0.00	0.00	0,00	0.00	0.00	0.00
Support Facilities		0.00	0.00	0.00	0.00	0.00	0.12	0.16	0.12	0.16	0.12	0.16	0.00	0.00	0.00	0.00		28490	6518	28549	0.10	0.45
Additive Handling	0.00		2.01	8.80	0.10	0.44	25.09	16.67	14.50	11.68	4.50	5.84	0.30	1.32	0.00	0.00	6505		0.00	0.00	0.00	0.00
Coal Handling	2.23	9.78		0.00	0.00	0.00	0.08	0.35	0.02	0.07	0.00	0.02	0.00	0.00	0.00	0.00	0.00	0.00		2264572	22.10	32.14
Paved Roadways	0.00	0.00	0.00			120.56	40.39	78.71	29.66	73.09	19,53	66.70	130.09	139.42	2.67E-04	1.17E-03	520091	2261168	520904			
Total Emissions Potential	84.20	184.53	60.57	255.12	28.15	120,30	1 40.33							,								

#### Notes

- 1. Diesel firewater pump operation is 200 hours per year
- 2. Emergency Diesel Generator operations is 100 hours per year
- 3. All process related equipment are assumed to operate for 8760 hours annually
- 4. Hydrogen plant emission information has been provided by an outside vendor, based upon vendor's initial conceptual approach. Discussion regarding hydrogen plant design are not finalized.
- 5. Although Hydrogen Reformers are planned to be sized up to 70% of maximum VCC process facility production, maximum pollutant output is limited by VCC facility.
- Thus, emissions potential is based upon the required hydrogen at 100% VCC facility production capacity.
- 6. CO2e includes CO2. They are separately listed to establish that Greenhouse Gas (GHG) impacts have been determined for the spectrum of GHG generating species.
- 7. All non-cooling tower particulates emissions are assumed to be fine particulate matter. Thus TSP = PM10 = PM2.5
- 8. Emissions estimates utilize AP-42 emission factors extensively. These factors provide conservatively high emissions estimates that will be refined with vendor information as it becomes available.
- 9. Smokeless flaring is assumed
- 11. Because a fugitive dust control plan is required by regulation for this facility, potential emissions are determined with the proposed plan in place. Details of plan performance are provided elsewhere in this application package
- 12. Particulate emissions from the hydrogen reformers are uncontrolled in the table. A baghouse will likely be required to satisfy BACT requirements.
- 13. Fugitive VOC emissions from valves, flanges, etc. are separately quantified. They will be addressed in the context of the LDAR program.

Table 2 Itemized Riverview Energy Facilitywide Potential Emissions (Preliminary)

	d Riverview Energy Facilitywide Pote									····	· · · · · · · · · · · · · · · · · · ·		T. 1994	V - 1.25	T	110071	BAUC	Lead		C	02	Total	CO2e	НАР	s	Other	Compound	ds
7 ( 2 A 1 E 1 E 1 E 1		Annual	Unit Rating	NO	x	c	0	sc	2	TS	SP	PN	110	PM	2.5	VOC/N	T		(tons/yr)	(lb/hr)	(tons/yr)	(lb/hr)	(tons/yr)	(lb/hr) (	tons/yr)	Species	(lb/hr)	(tons/yr)
Unit ID	Category	Operating	(Firing on HHV Basis unless noted	(lb/hr)	(tons/yr)	(lb/hr)	(tons/yr)	(lb/hr)	(tons/yr)	(lb/hr)	(tons/yr)	(lb/hr)	(tons/yr)	(lb/hr)	(tons/yr)	(lb/hr)	(tons/yr)	(lb/hr)	(LONS/ y1)	' risainii	. (					·		
		Hours	otherwise)				<u></u>										Ļ			14067.5	65557.4	14998.7	65694.3	0,238	1.041	Metals	0.005	0.024
	Veba Combi Cracker Process		420 444304/b-	2.470	10.800	2,470	10.800	0.229	1.002	0.963	4.218	0.963	4.218	0.963	4.218	0.693	3.037	0.000	0.000	14967.5	——————————————————————————————————————	6167.7	27014.5	0.098	0.428	Metals	0.002	0.010
J-2001	Feed Heater	8760	128.4 MMBtu/hr		9.251	1.901	8,326	0.094	0.412	0.396	1.734	0,396	1.734	0.396	1.734	0,285	1.249	0.000	0.000	6154.8	26958.2		4604.7	0.017	0.073	Metals	0.000	0.002
J-2002	Treat Gas Heater	8760	52.8 MM8tu/hr	2.112		0.324	1.419	0.016	0.070	0.057	0.296	0.067	0.296	0.067	0.296	0.049	0.213	0.000	0.000	1049.1	4595.1	1051.3		0.289	1.265	Metals	0.007	0.029
U-2003	Vac Column Feed Heater	8760	9 MM8tu/hr	0.360	1.577		24.598	0.278	1.217	1.170	5.125	1,170	5.125	1.170	5.125	0.842	3,690	0.000	0.000	18184.8	79649.2	18222.7	79815.5		0.305	Metals	0.002	0.007
U-2004	Fractionator Feed Heater	8760	156 MMBtu/hr	6.240	27.331	5.616		12.507	54,780	0.278	1.216	0.278	1,216	0.278	1.216	0.203	0.890	0.000	0.000	4607.0	20178.7	4616.2	20218.9	0.070	0,303	Sulfuric Acid		<del>                                     </del>
EU-3001	Sulfur Recovery Unit Tail Gas Treatm	8760	37.68 MMBtu/hr	6.782	29.705	1,319	5.775	12.307	34,740	0.270					Ì		[									Mist	0.600	1.940
												<u> </u>					<del></del>		0.000	4607.0	20178.7	4616.2	20218.9	0.070	0.305	Metals	0.002	0.007
			07.00 141.00	6,782	29,705	1.319	5.775	12.507	54.780	0.278	1.216	0.278	1.216	0.278	1.216	0.203	0.890	0.000	0.000	4007.0	20170.7	1020.2				Sulfuric Acid	0.600	1.940
EU-3002	Sulfur Recovery Unit Tail Gas Treatm	8760	37.68 MMBtu/hr	0.752																						Mist		<del> </del>
								<u> </u>			ļ	<del> </del> -	<del> </del>		+		2160	0.000	0.000	819.0	3588.0	886.0	3881.0	0.000	0.000	N/A	N/A	N/A
		8760	70 scfh gas per pilot	0,440	1,930	2.400	10.510	0.010	0.050	0.050	0.240	0.050	0.240	0.050	0.240	0.040	0.160	0,000	0.000	015.0		-	<del>                                     </del>	<del> </del>			N/A	N/A
EU-4004	HP Flare (non-assisted)	8760	6649 scfh purge gas				ļ	<del> </del>		0.040	0.020	0.010	0.030	0.010	0.030	0.020	0.070	0.000	0.000	103.0	452.0	112.0	489.0	0.000	0.000	N/A	N/A	14/74
EU-4002	Sulfur Block Flare	8760	70 scfh gas per pilot gas 683 scfh purge gas	0,060	0.250	0.310	1.340	1,100	4.800	0.010	0.030	0.010	0.030	0.020				<u></u>	+	<del> </del>								Ţ
												1											CT.4	14,532	0.683	N/A	N/A	N/A
			Naphtha loading at 20000 gpm for 93.9 hrs per year + Uncontrolled				0.100	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	98.685	5,603	0.000	0.000	13.8	60.4	14.9	65.4	14,332	0.003	.,,		
EU-4001	Loading Flare	278	Diesel Loading at 20000 gpm for	0.014	0.030	0.040	0.180	0.000	0.000	0.000					Ì	İ			1				1 .					
	-		183.6 hr per year				l					<u> </u>	1	0.510	2.234	0.367	1,608	0.000	0.000	7926.7	34718.8	7943.2	34791.3	0.126	0.551	Metals	0.003	0.013
EU-6000	Package Boiler	8760	68.5 MMBtu/hr	2.720	11.914	2.448	10.722	0.121	0.531	0.510	2.234	0.510	0.492	0.510	<del> </del>	1.282	5.614	0.000	0.000	0.0	0.0	0.0	0.0	0.000	0.000	Ammonia	0.125	0.549
EU-6001/2/3	Cooling Tower (three cells)	8760	32,000 gpm	0.000	0.000	0.000	0.000	0.000	0.000	0.190	0.834	0.112	0.492	0.000	0.002	1.202							1			Chlorine as	1.200	5.220
20-0001/2/3	cooming tower (amount)					İ								ļ			]		1							HOCI	ļ	+
								<u> </u>				<del> </del>	0.000	0.000	0.000	4.196	18.376	0.000	0.000	0.0	0.0	0.0	0.0	0.000	0.000	N/A	N/A	N/A
EU-5001a-04d	Residue Solidification Units	8760	51.5 tons/hr (total operation)	0.000	0.000	0.000	0.000	0,000	0.000	0.000	<del></del>	0.000	+	<del></del>	+	0.756	3,310	0,000	0.000	0.0	0.0	0.0	0.0	0.000	0.000	0.000	0.000	0.000
E0-3001a-040		8760	All storage tanks combined	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	-			<del> </del>	0.0	0.0	0.0	0.0	0.268	1.172	0.000	0.000	0.000
	Storage Tanks	<del> </del>	VCC Process and Product Storage	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	4.886	21.402	0.000	0.000	0.0	0.0	<del>  •</del>		<del> </del>		<del>                                     </del>		+-
İ	Fugitives	8760	and Handling Areas	0.000			<del></del>	+	┼──			+		<b>-</b>								<u> </u>	<del> </del>			N/A	N/A	N/A
	Emergency Equipment					<u> </u>	<u> </u>		0.000	0.840	0.040	0,840	0.040	0.840	0.040	0.680	0.030	0.000	0.000	3028.0	151.0	3056.0	153.0	0.041	0.002	N/A		——
EU-6006	Emergency Diesel Generator	100	2000 kWe	33.640	1,680	1.850	0.090	0,490	0.030	<del></del>		<del> </del>		0.230	0.020	0.180	0.020	0.000	0.000	870.0	87.0	878.0	87.8	0.353	0.040	N/A	N/A	+ 19/4
EU-6008	Emergency Diesel FireWater Pump	200	750 bhp	9.010	0.900	0.500	0.050	0.140	0.010	0.230	0.020	0.230	0.020	ULLEG	_	+	+	<b>—</b> —							<u> </u>			
	Support Facilities									-		-	<del>-  </del>	<del>-</del>			_										İ	
							1		-	1					22.038	5.032	22.038	0,000	0.000	224972.	1 985377.6	225176.1	1 986271.5	0.000	0.000	Ammonia	0.061	0.267
CU 7001	Hydrogen Plant 1 Reformer	8760	838.6 MMBtu/hr	5.451	23.875	16.772	73,462	0.273	1,197	5.032	22.038	5.032	22.038	5.032	22.056	3.052	22.00	,			ļ		_	<u> </u>	<u></u>			
EU-7001	Hydrogen Flant I Reformer		,	1												r 033	22.02	0.000	0.000	224972.	1 985377.6	225176.:	1 986271.5	0.000	0.000	Ammonia	0.061	L 0.26
L	N. J. Slave 2 Defenses	8760	838.6 MMBtu/hr per unit	5,451	23.875	16.772	73.462	0.273	1.197	5.032	22.038	5.032	-	+		<del></del>	<del></del>		0.000	246.5	1080.0	292.5	1282.0	2.950	12.910	Ammoni	a 3.920	3 17.17
EU-7002	Hydrogen Plant 2 Reformer	<del></del>		0.000	0.000	1.060	4.650	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	3.160	13.85	0.000	0.000	2.0%					İ	Acetic aci	id 0.040	0.180
EU-7003	Hydrogen Plant 1 Dearator Vent	8760	2628,36 acfm (Emissions are @100% VCC facility output)							1	ĺ	<u> </u>								2465	1080.0	292.5	1282.0	2.950	12.910	Ammoni	a 3.920	0 17.17
		<u> </u>	groom veerdome, each	0.000	0.000	1.060	4.650	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	3.160	13.85	0.000	0.000	246.5	1080.0	232.3	1202.			Acetic ac	id 0,040	0 0.18
EU-7004	Hydrogen Plant 2 Dearator Vent	8760	2628.36 acfm (Emissions are	0.000	0.000	1.000		"		1															<del>                                     </del>	<del>                                     </del>	N/A	N/A
			@100% VCC facility output)	ļ		-		+		-	0.740	0.050	0.240	0.050	0.240	0.040	0.160	0.000	0.000	819.0	3588.0	886.0	3881.0	0.000	0.000	N/A	N/A	IN/P
EU-4003	LP Flare	8760	70 scfh gas per pilot TBD scfh purge gas	0.440	1.930	2.400	10.510	0.010	0.050	0.050	0.240	0.03	0.240		-			+		<del></del>				<b></b>		0.000	0.000	0.00
	Coal Handling System		18D scin purge gas	-							0 153	0.26	8 0.114	0.00	7 0.003	0.000	0.00	0.000	0.000			0.0	0.0	0.000				
EU-1000	Coal Unloading Station	850	5000 ton/hr	0.000	0.000	0.000	0.000	0.000	0.000										0.000			0.0	0.0	0.000	<del></del>			
EU-1001	Transfer Station 1	850	5000 ton/hr	0.000	0.000	0.000	0.000			2.75					2 0.022		-		0.000			0.0		0.000			0.000	
EU-1002	Stacker 1 Boom Chute	850	5000 ton/hr	0.000	0.000	0.000	0.000		0.000				7 1.882						0.000			0.0		0.000	0.000			
EU-1003	Coal Pile 1A/1B	850	5000 ton/hr	0.000	0.000	0.000	0.000	0.000				2.06	4 0.87						0.000		_+	0.0	0.0	0.000	0.000			
EU-1004	Stacker 2 Boom Chute	850	5000 ton/hr	0.000	0.000	0.000	0.000	0.000				4 4.42							0.000		_	0.0	0.0	0.000	0.000			
EU-1005	Coal Pile 2A/2B	850	500 ton/hr	0.000	0.000	0.000	0.000	0.000			0 2.410	0.41		_+				<del></del>	0.000			6518.	1 28549.	0.103				
EU-1006	Reclaim Transfer Station	8760	500 ton/hr		9.776	2,009	8,799	0.100		6 0.41									0.000			0.0	0.0	0.000	0.000	0.000	0.00	0.00
EU-1007	Coal Dryer Heater	8760	55.8 MMBtu/hr	0.000	0.000	0.000	0.000	0.000			9 2.40	5 0.41	.8 2.40	5 0.41	.8 2.405	5 0,000	0.00	0.000		<del></del>								
EU-1008	Coal Drying Loop Purge (N2 + H2O	Va 8760	300 ton/hr	0.000										<del>,  </del>	9 0.019	9 0.000	0.00	0.000	0.000	0.0	0.0	0.0			5 2.00E-			
	Additive Handling	1 205.5	20 ton/br	0.000	0.000	0.000	0.000	0,000											0.000		0.0	0.0		<del></del>	05 2.00E-			
EU-1501	Coarse Additive Storage Filter	965.5	20 ton/hr	0.000	0.000	0.000	0.000	0.00											0.000		0.0	0.0		0.000				
EU-1502	Fine Additive Storage Filter	1438.8	20 ton/hr 10 ton/hr	0.000	0.000	0.000		0.00											0.000		0.0	0.0			06 3.62E-			
ITTLE STATE	NA2S Additive Storage Filter	67.6	20 ton/hr	0.000	0.000	0.000		0.00													0.0	0.0		0.000				
EU-1503	Fine Additive Production System	8760	~		0.000	0.000		0.00	0.00	0.00	53 0.02								0.000		0.0	0.0	0.0		06 2.40E-			
EU-1504		0700	1259 4 top/br	U.GDO	0.000																							
EU-1504 EU-2005	Coal Handling System Filter	8760	258.4 ton/hr	0.000	0.000	0.000		0.00		_									0.000	$\overline{}$		0.0			06 3.60E-			
EU-1504		ilti 8760	258.4 ton/hr 2.2 ton/hr 3.28 ton/hr				0.000	0.00	0.00	0.00	0.03	0.00	0.03	4 0.00	0.03	4 0.00	0.0	0.000	0.000	0.0	0.0	0.0				<del></del>		

# Table 3 Paved Roadway Particulate Emissions Summary

#### Controlled PTE Emissions

Controlled PTE Emissions	
Line   Rev   PROJECT DEFINITION AND BASIS OF CALCULATIONS	
1 ITEM	
3 1 The vehicle weight used in the calculations are:	
4 Truck (Sami Tractor Trailer) 40 tons 5 Cars =	
6 Other vehicle type = 12 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	
8 3 Plant roads are assumed to be two-laned with a total width of 20 ft.	
9 4 Annual facility operating schedule is 365 days per year  10 24 hours per day	
Fraction of Annual Operating period with no rail availability : 0.05	
13 8 All paved road emission calculations are based on AP-42, Section 13.2.1 "Paved Roads"	
7 Emission Factor (E) for Uncontrolled Emissions is estimated from the Formula 4 in AP 42, Section 13.2.1; E = k(st_usr)/(v=1.02) (1-P4N), where the particle size multiplier for the paved road equation are taken from AP 42, Section 13.2.1, Table 13.2.1-1  15 where, k = particle size multiplier for the paved road equation are taken from AP 42, Section 13.2.1, Table 13.2.1-1	
16 st. will loading values taken from AP-42, Section 13.2.1, Tables 13.2.1.4 (for Pulsor vacades and 10.2.1.4 (for Pulsor vacades an	
17 P = number of 'wet' days with at least 0.01 inclies in presuperior per year and inclies in presuperior per year.  N = number of days in the averaging period (e.g., 365 for annual, 91 for seasonal, 30 for monthly); For this site = 120 days	
19 20	
21 22 22 23 24 25 25 25 25 25 25 25 25 25 25 25 25 25	
23 PAYED ROAD EXISSIONS SUMMARY	
24 Control Efficiency  Road Segment Description Uncontrolled Potential Emissions Efficiency  Control Control Efficiency	
26 ROAD SEGMENT Travel Width Area PMLS PMIQ MAD (TSP PMLS PMIA)	13P:
29 Road 2-1 Na2S Unloading 2133 20 42651 0,00000 0,0000 0,00000 0,00000 0,00007	
30 Nota 2-2 Arquine 1840 20 32808 0.0001 0.0003 0.00015 0 0.0001 0.0003 0.00015 3 0.0001 0.00015 0 0.00010 0.0003 0.00015	
32 Road 2-4 Amine Make-up 1804 20 86989 0,000074 0,00305 0,01589 0 0,00074 0,00305 0,01589	89
34 Road 2-6 Molten Suffur Loading 984 20 19865 0.0003 0.00014 0.00072 0 0.00023 0.00096 0.00049	
35   Road 2-7 residue Loading	
37 Road 1.2 Caustic Unloading 820 20 16404 0.00036 0.00147 0.000765 0 0.00036 0.00147 0.00765	
39 Road 1-4 Diesel Fuel Unitoeding 820 20 16404 0.00096 0.00167 0.00096 0 0.	24
41 Road 1-6 Water Treatment Chemicals Unloading 1312 20 28247 0,00057 0,00235 0,01224 0 0,00057 0,00235 0,01224 1 Road 1-6 Water Treatment Chemicals Unloading 1312 20 28247 0,00057 0,00235 0,01224 0 0,00057 0,00235 0,01224	
42. Nood 1-7 Lime studge classing. 3 Road 1-9 Wastewater Treatment Chemicals Unloading 1540 20 32808 0.00071 0.00294 0.01530 0 0.00071 0.00294 0.01530	
44 Road 1-9 Wastinwater Treatment Biosludge Loading 1640 20 32/eus ULUDITA ULU	856
46 TOTAL = 0.02 0.07 0.35 0.02 0.07	
47 48 PAVED ROAD EMISSIONS CALCULATIONS:	
49 New York Control of the Control o	Particle Size Multiplier (k) Unicontrolled Potential Emission  Controlled Potential Emission
51	Road Segment Description
Ul control to the control of the con	Vehicle Mean,  Specially Number of days  Signment Vehicle Mean,  Signment Vehi
Vehicles pay: Vehicles Per: Operating	Surface SII Longito SII Longito SII Longit
52 Road ID: Plant Block Anthrity Description Service Say year Period Remarks Sile Ditranse / Edit	## Cestingsion in Part III   PART   P
53	VCC Unit 659 2133 26 42651 Paved 1.05 1 1 440 0.15 0.62 3.28 120 355 0.0000 0.0000 0.0000 0.0000 None 00% 0.00001 0.00
55   Road 2-2   2000   Anilline   Regular   0.5   1   1   Tricks every two years   North Entry Gate 2   1   1   2 Trocks every two years   North Entry Gate 2   1   1   2 Trocks every two years   North Entry Gate 2   1   1   2 Trocks every two years   North Entry Gate 2   1   1   2   2   2   2   2   2   2	VCC Unit 500 1540 20 32006 Paved 1.05 2 1 40 0.15 0.52 3.23 120 365 0.0001 0.0004 0.0019 None 066 0.0009 0.0003 0.01589
57 Road 2-4 3000 Amine Make-up Regular 12 1 During start-up and make-up once a mornt in inorm entry ware 2. North Entry Gate 2	Surfur Recovery Units 250 1.05 1.05 1.20 1.08 40 0.15 0.62 3.23 1.20 365 0.000 0.0001 0.0007 None 0% 0.0003 0.00014 0.00009 0.0001 0.00009 0.00014 0.00009 0.00009 0.00014 0.00009 0.0
58 Road 2-5 4000 Ammonia Loading seguer 5 40-25 0.015 Only when rail loading is not available North Entry Gate 2.  59 Road 2-6 4000 Molten Sulfur Loading Emergency 9 164-25 0.05 Only when rail loading is not available North Entry Gate 2.	Sulfur Recovery Unit 300 984 20 19685 Paved 1.05 133 34 40 0.15 0.62 3.23 120 365 0.0002 0.0010 0.0050 None 1.05 0.00032 0.00003 0.00050 None 1.05 0.00032 0.00050 0.00003 0.00050 0.00050 0.00003 0.00050 0.0
60 Road 2-7 S000 Residue Loading Emergency 52 1131.5 G0.05 Only when roat loading to the variable of the control of the contro	Warehouse 250 20 20 16404 Pavel 1.05 208 52 40 0.15 0.62 3.23 1.20 365 0.0004 0.0055 0.0076 None 0.05 0.0036 0.0047 0.0055
62 Road -2 6000 Caustic Unloading Regular 52 2 1 Truck every week default South Entry Gate 1	Warehouse 250 820 20 16404 Paved 1.05 208 52 40 0.15 0.62 3.73 120 365 0.0004 0.0015 0.0076 None 034 0.00036 0.00147 0.00765
0.3   Road 1-9   0000   Diesel Feel Unloading   Regular   52   2   1 Truck every weak default   South Entry Gate 1   1   1   1   1   1   1   1   1   1	Warehouse 250: 820 20 1500 Faved 1.05 206 83 40 0.15 0.62 3.23 120 365 0.0005 0.0023 0.0122 None 0.0023 0.0022 None 0.0023 0.0022 None 0.0023 0.0025
65 Road 1-5 6500 Lime Unloading Regular 52 2 1 Truck every week default South Entry Sate 1 66 Road 1-6 6500 Water Treatment Chemicals Unloading Regular 52 2 1 Truck every week default South Entry Sate 1	Water Treatment Units 1000 1312 20 26:247 Paved 1.05 208 83 40 0.15 0.52 3.23 120 365 0.0003 0.0023 0.0122 None 0.053 0.0023 0.0122 None 0.053 0.0003 0.0122 None 0.053 0.0003 0.0153 None 0.053 0.0003 0.0023 0.01530 0.0003 0.00
67 Road 1-7 6500 Line Studge Loading Regular 52 1710's every week default South entry date 1 52 2 1 Truck every week default South entry date 1 53 2 2 1 Truck every week default South entry date 1	Wastewater Treatment Unit 500 1540 20 32808 Paved 1.05 208 104 40 0.15 0.62 3.23 120 365 0.0007 0.0023 0.0153 None 0% 0.01052 0.0153 0.0007 0.0024 0.01530 0.0007 0.00007 0.00007 0.00007 0.0007 0.00007 0.00007 0.0
68 Road 1-9 6500 Wastewater Treatment Bloglodge Looding Regular 52 2 1 Truck every week default South Entry Gate 1	Westewater Treatment Unit 500 1540 20 32808 Paved 1.05 208 104 - 0.15 0.52 3.23 120 365 0.0105 0.0435 0.266 None CN 0.1052 0.0749 0.2656  Admin Building 200 556 20 13123 Paved 1.05 163520 32704 2 0.15 0.52 3.23 120 365 0.0105 0.0435 0.266 None CN 0.1052 0.0749 0.2656  Building 200 556 20 13123 Paved 1.05 163520 32704 2 0.15 0.52 3.23 120 365 0.0105 0.0435 0.266 None CN 0.1052 0.0749 0.2656
70 Road 1-10 5500 Employee Cars Regular 112 40000 2 2 113 500 1 2 1 2 1 2 1 2 1 2 1 2 1 2 1 2 1 2 1	Public Roads
72 Categor	egory, Provated,
73   g/m2   74   Spring Summer Fall 0.5	0.5 0.75 105
75 Winter 2.4	24 0.25

#### **Table 4 – Paved Roadway Particulate Emissions Summary**

Species: PM-10

Please see table 3 for the PM-10 emissions.

### **Table 5 – Paved Roadway Particulate Emissions Summary**

Species: TSP

Please see table 3 for the TSP emissions.

#### Table 6a: Storage Pile PM2.5 Emissions

Table 6a: S	torage Pile PMZ.	.5 Emissions															Wind Erosion	Emission Control Info	ormation	Load-in En	missions	Load-out I	Emissions	Milita Etrazioni
		Emission Unit Des	ceintian	<del></del>	Param	eters per Storage Pile	Storage	Actual	Number	Maximum		Emissions Paral Max Load-out			Uncontrolled Emi for Pile Load-in &				Effectiveness	,,,,			Annual	Annual Emissions
Emission Unit Designation	Name	Material Stored	Material . Density .	Storage Type	Pile Base Diameter	Theoretical Single Pile Height	Pile Surface Area (acres)	Maximum Pile Ht. (ft)	of Storage Piles	Hourly Throughput (tph)		Wind Speed (mph)	Content (%)	Content	Load-in (ib PM <sub>25</sub> /ton)	Load-out	Emission Factor (lb/acre/year)		(%)	PM 15 (lb/hr)	PM <sub>2.5</sub> (tons/yr)	PM <sub>25</sub> (lb/hr)		(tans/yr)
	Coal storage pile	lilinois basin coal	(lb/cu.ft.) 50	live	(ft) 693	100	19.08	100.00	1	220	48	O	2.2	4.5	0,00389	6,00000	1.45	loading - wet suppression storage - wet suppression	80.00 80.00	0.17	0.750	0.000	0.000	0.003
EU-1003	Coal storage pile	Hinois basin coal	50	live	693	100	19.08	100.00	1	220	48	0	2.2	4.5	0.00389	0.00000	1.45	ioading - wet suppression storage - wet suppression	80.00 80.00	0.17	0.750	0.000	B.005	0.003
EU-1005							<u> </u>			<u> </u>	<u> </u>		<u>l</u>		<u> </u>	<u> </u>			nissions (lb/hr.) neual Emission Total of Annua	s (tons/yr.	1.500	0,000 Erasion Er	0.900 missions (tpy)	0.006 = 1.505

mission Emission Unit Description Parameters per Storage Unit Unit Nome Moterial Material Storage Pile Base Theoretical Single esignation Stored Density Type Diameter Pile Height (lb)/cu.ft.)  Coal storage pile Illinois basin coal 50 live 693 100		Actual Maximum a Pile Ht. (ft)	Number of Storage Piles	Maximum Hourly Throughput (tph)		Wind Speed	Silt Content	Moisture .	Uncontrolled Em for Pile Load-in & Load-in	Load-out		: Emission Control inf Control Description		Hourly PM <sub>10</sub>	PM 10	Hourly PM <sub>10</sub>	Annual PM 10	Annual Emissio
Unit Nome Adderial Material Storage Pite Base Theoretical Single Ignation Storage Diameter Pite Height (ib/cu.ft.) (if) (iff) (iff)  Coal storage pile Illinois basin coal S0 live 693 100	Surface Are	a Pile Ht.	Storage	Throughput	Wind Speed	Wind Speed	Content			Lond-out	Emission Factor		(24)	PW 10				
(tb/cu.ft.) (ft) (ft)  Coal storage pile Illinois basin coal S0 live 693 100	(acres)	(ft)	Piles	(zbu)		(mph)	(%)	(%)	(lb PM <sub>10</sub> /ton)	(lb PM <sub>10</sub> /ton)	(lb/ocre/year)	THE ARREST HEAD		(lb/hr)	(tons/yr)	(lb/hr)	(tons/yr)	(tons/yr)
1-1003 Coal storage pile Jillinois pasiir Coal	19.08	100:00	1	220	48	D	2,2	4.5	0.00973	0.00000	3.63	loading - wet suppression storage - wet	80,00 80.00	0.43	1,875	0.000	0.000	0.007
cont. d. Cont. et compre pile   Illinois hasin cont 50 live 693 100				220	48	0	2.2	4.5	0.00973	0.00000	3.63	loading - wet suppression storage - wet	80.00	0,43	1.875	0.000	0.000	0.007
J-1005 Coa storage pine	19.08	100.00		120								suppression  Total Hourly B	80.00	1 0 856		0.000		

ble 6c: St	orage Pile TSP	Emissions													Uncontrolled Em	ission Factors	Wind Erosion	Emission Control Inf		Load-in Em			missions Annuai	Wind Erosion Annual Emission
mission Unit	Name	Emiss Material Stored	ion Unit Desci Material Density		Pile Base Diameter	rameters per Storage Pile Theoretical Single Pile Height	Pile Surface Area	Maximum Pile Ht.	Number of Storage	Maximum Hourly Throughput	Max. Load-in Wind Speed (meh)	Emissions Parar Max. Load-out Wind Speed			for Pile Load-in & Load-in (Ib TSP/ton)		Uncontrolled TSP Emission Factor (lb/acre/year)	Control Description	Effectiveness (%)	15P	tons/yr)	Hourly TSF (fb/hr)	75P	TSP (tons/yr)
coupe	Coal storage pile	Illinois basin coal	(lb/cu.ft.) 50	live	(ft) 693	100	(acres)	100.00	Piles :	(tph) 220	48	O	2.2	4.5	0.01946	0.00000	7.25	loading - wet suppression storage - wet suppression	80.00 80.00	0.86	3.750	0.000.0	0.000	0.034
<del>cr s,+</del>	Coal storage pile	Illinois basin coal	50	live	693	100	19.08	100.00	1	220	48	o	2.2	4.5	0.01946	600000.0	7.25	loading - wet suppression storage - wet suppression	80.00 80.00	0.86	3.750	0.000	0.000	0.014
J-1005													<u> </u>	<u></u>				Total	missions (lb/hr. Annual Emission Il Total of Annua	s (tons/vr.)	7,499	0.000 Erosion Er	0.000 missions (tpy)	0.028 7,527

- NOTES:

  1. Average coal density of bituminous coal is taken from Table D.9 of the Air Pollution Engineering Manual (AP-40), Second Edition

  2. The load-out operations to the process are conducted in a protected area (due to its location surrounded by the 100 ft. high coal piles), so the load-out which velocity (mph) = 0

  3. The information required to utilize the wind erosion algorithms utilized in AP-42 Chapter 13, Section 13.2.5 is unavailable. The technical approach used is more conservative. It utilizes the maximum wind speed ferorded for Terre Haute (NOAA climatological data for April, 2015) used is more conservative. It utilizes the maximum wind speed ferorded for Terre Haute, in. It is applicable to load-in operations. Load-in wind speed (high) = 4

  5. Material throughput is based upon maximum theoretical process output.

  6. Estimated sit content (2.2%) is from Table 13.2.4-1 of AP-42 for as-received coal.

  7. Moisture content (4.5%) is taken from Table 13.2.4-1 of AP-42 for as-received coal.

  8. Although the potential emissions from pile working are expressed as hourly values, loadout is not a continuous process. Only longer term values (e.g., annual) are representative.

  9. Annual schedule (hrs/yr): 8760

  10. Coal storage piles have a 35 degree angle of repose.

  11. Pile work area has negligible wind erosion emissions (AP-42, Section 13.2.5, page 13.2.5-9 at Step 2).

  12. Pile work area has negligible wind erosion is extracted from Table 11.9.4 of AP-42.

  13. Particle size multiplier (5) used is 0.20 for PM 15 0.50 for PM 15 mand 1.0 for TSP.

  14. The emission factor employed to determine pile wind erosion is extracted from Table 11.9.4 of AP-42.

  15. The control efficiency for wet suppression is based upon the assumption that the outer (wind-exposed pile surfaces are controlled with a chemical suppressant. The wind-exposed pile surfaces are not disturbed unless rail deliveries are interrupted because pile working is performed inside the area enclosed by the twin piles.

**Table 7. Additive Handling Controlled PTE Emissions** 

Unit Designation	Emission Source Description	Design Capacity	Annual Operating Hours	Particulate ( PM2.5) E Sum	
				lb/hr	tpy
EU 4504	Coarse Additive Storage Filter	20 ton/hr	966	0.039	0.019
EU-1501		20 ton/hr	1439	0.039	0.028
	Fine Additive Storage Filter	10 ton/hr	68	0.020	0.001
	NA2S Additive Storage Filter	20 ton/hr	8760	0.008	0.034
EU-1504	Fine Additive Production System	258.4 ton/hr	8760	0.0053	0.023
EU-2005	Coal Handling System Filter		8760	0.005	0.023
EU-2006	Coarse Additive Handling System Filter	2.2 ton/hr			0.034
EU-2007	Fine Additive Handling System Filter	3.28 ton/hr	8760	0.008	
EU-2008	Na2S Handling System Filter	0.077 ton/hr	8760	0.001	0.004
EU-2008	Tota	l Potential Emiss	ions =	0.124	0.165

#### NOTES

- 1 These units are package units. The baghouses are intrinsic to their operation and reclaim process material for use,
- 2 Emissions are based upon a baghouse outlet concentration of 0.003 gr/dscf
- 3 It is conservatively assumed that TSP = PM10 = PM2.5 emissions, since they all are releasased through a baghouse.
- 4 Annual operating hours for process feed equipment =

8760

5 Annual operating hours for feeds to storage silos are based upon storage capacity and usage rate at VCC design.

Table 8: Coal Handling	Emisisons							_					m Potential Hou	why Uncontro	iled Feissi	ons	Ma	ximum Potenti	al Hourly Cont	rolled Emissic	กร	Maximum Pe	otential Hourly	Controlled
Controlled PTE						1			Maxim	um Annual TSP Controlled Err	nissions	Maximu	m Polential 1100	gry discond	Scaling	1		1	[		ļ			, ,
					Nominal	Max Potential	Annual	Reference Source for	Uncontrolled Emission		Primary Design Control		Scaling Factor applied to EF for PM10	PM10	Factor applied to EF for PM2.5	PM2.5	Emission Control	Control Efficiency	TSP	PM10	PM2.5	TSP	PM10	PM2.5
		İ			Capacity	Throughput	Operations	Uncontrolled	Factor	Emission Factor	Effectiveness	ISP	10. 1	lb/hr	fraction	lb/hr	Description		lb/hr	lb/hr	lb/hr	tpy	tpy	tpy
				The second control (6)	ton/hr	ton/hr		Emission Factors	1b/ton	Adjustment Design Element	fraction	lb/hr	fraction	Batti	II BOROII	<del> </del>	1000	<del></del>						
Unit ID	UNIT DESCRIPTION	FROM	TO	AIR POLLUTION CONTROL(S)	DIVIN .	101711									<del> </del>	<del>                                     </del>	<del> </del>							
EU-1000	Coal Unloading Station											35.00	0.75	26.250	0.019	0.6650	Baghouse	0.995	0.1750	0.13	0.00	0.074	0.056	0.001
					2750	5000	860	AP-42 Table 11.9-4	0.028	Dump shed total enclosure	0.75		0.75				Baghouse	0.995	0.1750	0.13	0.00	0.074	0.056	0.001
	Coal Drop Point 1	Unloading Chute 1	Unloading Hopper 1	Enclosure	2750	5000	860	AP-42 Table 11.9-4	0.028	Dump shed total enclosure	0.76	35.00	0.75				Baghouse	0.995	0.0018	0.00	0.00	0,001	0.001	0.000
1	(Continuous Unloading)	Unloading Chute 2	Unfoading Hopper 2	Enclosure	2750	5000	850	AP-42 Table 11.9-4	0.007	Total Enclosure	0.99	0.35					Baghouse	0.995	0.0018	0.00	0.00		0.001	0.000
		Unloading Hopper 1	Drag Flight Feeder 1	Enclosure w/ water Spray Dust Suppression	2750	5000	850	AP-42 Table 11.9-4	0.007	Total Enclosure	0.99	0.35			0.010	0.0067		0.995	0.0018	0.00	0.00	0.001	0,001	0.004 0.000 0.000 0.000 0.000 0.000
1		Unloading Hopper 2	Drag Flight Feeder 2	Enclosure w/ water Spray Dust Suppression	2750	5000	850	AP-42 Table 11.9-4	0.007	Total Enclosure	0.99	0.35		0.263			Baghouse	0.995	0.0018	0.00	0.00	0.001	0.001	0.000
i		Drag Flight Feeder 1	Take-away Conveyor Belt 1	Water Spray Suppression System	2750	5000		AP-42 Table 11.9-4	0.007	Total Enclosure	0.99	0.35					Baghouse	0.995	0.0018	0.00	0.00	0.001	0.001	0.000
1		Drag Flight Feeder 2	Take-away Conveyor Belt 2	Water Spray Suppression System	2750	5000		AP-42 Table 11.9-4	0.007	Total Enclosure	0.99	0,35		0.263			Baghouse	0.995	0.0018	0.00	0.00	0.001	0.001	0.000
		Take-away Conveyor Belt 1	Transfer Station	Enclosure	2750	5000		AP-42 Table 11.9-4	0.007	Total Enclosure	0,99	0.35	0.75	0,263	0.019	0,0007	Dayiibuse	0,030						
		Take-away Conveyor Belt 2	Transfer Station	Enclosure	2150	3050	- 500	To the total of the same						0.000		0.0067	Baghouse	0.995	0.0018	0.00	0.00		0.001	0.00001
					2750	5000	850	AP-42 Table 11.9-4	0.007	Total Enclosure	0.99	0.35	0.75	0,263	0.019	0.0007	Baghouse		0.0018	0.00	0.00	0.001	0,001	
EU-1001	Transfer Station 1	Conveyor 1	Stacker 1 Boom	Enclosure	2750	5000		AP-42 Table 11.9-4	0.007	Total Enclosure	0.99	0.35		0.263	0.019	0.0007	Deshours	0.995	0.0002	0.00	0,00	0.000	0.000	0.00000
20-1001	110101010101	Conveyor 2	Stacker 2 Boom	Enclosure	500	500		AP-42 Table 11.9-4	0.007	Total Enclosure	0.99	0.04	0.75	0.026	0.019	0.0007	Baghouse	0.000						<u> </u>
		Conveyor 9	Reclaim Transfer Station	Baghouse Filter	500	500	1440	AF-12 TUDIC TT.0-4						<u> </u>		0.0500	<del> </del>	0.600	2 7500	2.06	0.05	1,169	0.877	
						5000	950	AP-42 Table 13,2,4	0.0011	Water Spray on Shroud	0.5	2.76	0.75	2.063	0,019	0.0523	NA.	0,000	0.86	0.43	0.17	3.764	1,882	0.753
EU-1002	Stacker 1 Boom Chute	Stacker 1 Boom	Stacker 1 Chute to Coal Piles 1A & 1B	Water Spray Suppression System	2750	5000		6 for emissions from Coal P				1							<del> </del>	<del> </del>				
EU-1002	Otacker I Booth Orlace	Coal Piles 1A & 1B	Coal Pile Fugitive Dust to Atmosphere	Water Spray Suppression System (runoff to Coal Pile Pond)	2750	BUUU	Promeable	E TOT CHINGS DISTRIBUTE COOLS	<u>"I</u>									0.000	2,7500	2.06	0.05	1,169	0,877	0.022
EO-1003		God in the little in the littl			ļ	5000	950	AP-42 Table 13.2.4	0.0011	Water Spray on Shroud	0.5	2.75	0.75	2.063	0.019	0.0523	NA.	0.000	0.86		0.17	3,764	1.862	0.753
E11 +004	Stacker 2 Boom Chute	Stacker 2 Boom	Stacker 2 Chute to Coal Piles 2A & 2B	Water Spray Suppression System	2750			6 for emissions from Coal P											- 0.00			<b></b>		
EU-1004 EU-1005	Stacker 2 Booth Cride	Coal Piles 2A & 2B	Coal Pile Fugitive Dust to Atmosphere	Water Spray Suppression System (runoff to Coal Pile Pond)	2750	5000	From Lable	6 for entissions from Goarv	1				1				<del> </del>	0.000	0.5500	0.41	0.01	2.409	1.807	0,046
EQ-1005		COMIT INSTITUTE					0.700	AP-42 Table 13.2.4	0.0011	None	0	0.55				0.0105			0.5500		0.01		0.000	0,046 0,000 0.000 0.000
	Reclaiming	Coalpiles 1A & 1B Reclaimer 1	Reclaim Conveyor 6	Enclosure	500			AP-42 Table 13.2.4	0.0011	None	0	0.55				0.0105		0.000	0.0002	0.00	0.00	0.001	0.000	0.000
EU-1006	Reclaiming	Coalpiles 2A & 2B Reclaimer 2	Reclaim Conveyor 7	Enclosure	500	500		AP-42 Table 11.9-4	0.007	Total Enclosure	0.99	0.04					Baghouse		0.0002		0.00		0,000	0.000
	1	Redaim Conveyor 6	Reclaim Transfer Station	Baghouse Filter	500				0.007	Total Enclosure	0.99	0.04	0.75	0.026	0.019	0.0007	Baghouse	0.995	0.0002	0,00	0.00	0.000		
1		Redaim Conveyor 7	Recialm Transfer Station	Baghouse Filter	500			AP-42 Table 11.9-4	0.007	rotal Cholodare				T	1				0.55	0.55	0.55	2,405	2,405	2.405
	<del></del>	INECIAITI CONVEYOR /	ALA	Fired Heater to Heat Coal Drying Loop Gas	NA.				+			T		T			Baghouse	0,995						
EU-1007	Coal Dryer Heater	Reclaim Transfer Station	Coal Mill and Pulverizer	Coal Dryer Baghouse Used to Direct Fines to Process	500	500	8760											Sume	9 232	#	1.023	distribution of the second	*****************	317014
EU-1008	Coal Drying Loop	Reciaim   Tansfer Station	COSI MILI SIN I UNCHEST	1000-1-1																				

Table 9. GSD-01 Basic Source Level Information

Part O: New or Modified Emission Units

est tellversted if	1 1 1 1 1 1 1 1			78.		
4. Emission Unit	75. New	76, Old	77. Type of Emissions Unit	Begin Construction	Complete Construction	Begin operation
ID.						
	tive triplet i	+ 1 3.4 N 1 I	G. LUCIA diag Station	1Q2021	1Q2023	3Q2023
U-1000	<u> </u>	NA NA	Coal Unloading Station	102021	1Q2023	3Q2023
U-1001	X	NA	Transfer Station 1	1Q2021	1Q2023	3Q2023
ป-1002	X	NA NA	Stacker 1 Boom Chute			
	v	NA	Coal Pile 1A/1B	1Q2021	1Q2023	3Q2023
U-1003	X X	NA NA	Stacker 2 Boom Chute	1Q2021	1Q2023	3Q2023
U-1004			Coal Pile 2A/2B	1Q2021	102023	3Q2023
EU-1005	X	NA NA	Reclaim Transfer Station	1Q2021	1Q2023	3Q2023
EU-1006	X	NA	Coal Dryer Heater	102021	1Q2023	3Q2023
EU-1007	X	NA_	Coal Drying Loop Purge (N2 + H2O Vapor)	102021	1Q2023	3Q2023
EU-1008	X	NA NA	Coarse Additive Storage Filter	1Q2021	102023	3Q2023
EU-1501	Х	NA NA	Fine Additive Storage Filter	102021	102023	3Q2023
EU-1502	Х	NA NA	NA2S Additive Storage Filter	102021	102023	3Q2023
EU-1503	Х	NA NA	NAZS Additive Broduction System	1Q2021	1Q2023	3Q2023
EU-1504	X	NA NA	Fine Additive Production System	1Q2021	1Q2023	3Q2023
EU-2001	X	NA NA	Feed Heater	102021	1Q2023	3Q2023
EU-2002	<u> </u>	NA NA	Treat Gas Heater Vacuum Column Feed Heater	102021	1Q2023	3Q2023
EU-2003	X	NA NA	Fractionator Feed Heater	1Q2021	1Q2023	3Q2023
EU-2004	X	NA NA	Coal Handling System Filter	102021	1Q2023	3Q2023
EU-2005	X	NA NA	Coarse Additive Handling System Filter	1Q2021	1Q2023	3Q2023
EU-2006	X	NA NA	Fine Additive Handling System Filter	1Q2021	1Q2023	3Q2023
EU-2007	x	NA_	Na2S Handling System Filter	1Q2021	1Q2023	3Q2023
EU-2008	X	NA_		1Q2021	1Q2023	3Q2023
EU-3001	x	NA NA	TGTU Stack A	1Q2021	1Q2023	3Q2023
EU-3002	X	NA NA	TGTU Stack B Loading Flare (8 loading spots naphtha	102021	102023	3Q2023
EU-4001	X	NA	service; each at 2500 gpm)	102021	102023	3Q2023
EU-4002	X	NA	Sulfur Block Flare	1Q2021	1Q2023	3Q2023
EU-4003	X	NA	LP Flare	102021	102023	302023
EU-4004	X	NA	HP Flare	102021	102023	3Q2023
EU-5001A/B/C/D		NA.	Residue Pastilators Stack1	1Q2021	1Q2023	3Q2023
EU-5002A/B/C/D		NA	Residue Pastilators Stack2	102021	1Q2023	3Q2023
EU-5003A/B/C/E		NA NA	Residue Pastilators Stack3	102021	102023	3Q2023
EU-5004A/B/C/[		NA NA	Residue Pastilators Stack4	102021	1Q2023	3Q2023
EU-5005	x	NA NA	Residue Railcar Loading	102021	1Q2023	3Q202
EU-5006	X	NA_	Residue Rail/Truck Loading	102021	1Q2023	3Q202
EU-5007	X	NA_		102021	102023	3Q202
EU-5008	X	NA_	Residue Rail/Truck Loading Residue Bulk Container Loading	1Q2021	1Q2023	3Q202
EU-5009	X	NA NA	Residue Bulk Container Loading Residue Rail Silo Filter	1Q2021	102023	3Q202
EU-5010	X	NA NA	Residue Swing Silo Filter	102021	1Q2023	3Q202
EU-5011	<u> </u>	NA NA	Package Boiler	1Q2021	102023	3Q202
EU-6000	X	NA NA	Cooling Tower Celi A	1Q2021	1Q2023	3Q202
EU-6001	X	NA NA	Cooling Tower Cell B	1Q2021	1Q2023	3Q202
EU-6002	X	NA NA	Cooling Tower Cell C	1Q2021	1Q2023	3Q202
EU-6003	X	NA NA	EDG Diesel Tank	1Q2021	1Q2023	3Q202
EU-6005	X	NA NA	Emergency Diesel Generator	1Q2021	1Q2023	3Q202
EU-6006	X	NA NA	EDFWP Diesel Tank	1Q2021	1Q2023	3Q20
EU-6007	X	NA.	Emergency Diesel FireWater Pump	102021	102023	3Q20:
EU-6008	X	NA NA		1Q2021	1Q2023	3Q20:
EU-6501	X	NA.	Lime Silo Fifter	1Q2021	1Q2023	3Q20
EU-6502	Х	NA.	Deaerator Vent	102021	1Q2023	3Q20
EU-7001	X	NA NA	Hydrogen Plant 1 Reformer	1Q2021		3Q20
EU-7002	Х	NA	Hydrogen Plant 2 Reformer Hydrogen Plant 1 DA Vent	1Q2021		3Q20
EU-7003	Х	NA.	invorogen Plant I DA Vent		1Q2023	3Q20

Distace (ft) 29 29 598 309 304 409 437 292 451 346 380 414 359 383 300 82 22 398 675 25 £3 340 729 349 209 1186 309 254 4225470 4225470 4225470 4225470 4225470 4225470 4225820 4227133 4227133 4227133 4227133 4225820 422682 4226879 Coordinate (North) 4225479 4227138 4225479 4227138 4225479 \$02342 \$02342 \$02342 \$02342 \$01810 \$01810 \$02076 \$02076 \$01810 \$02478 \$02477 \$02477 \$02477 \$02477 \$02477 \$02477 \$02477 \$02477 \$02477 \$02477 \$02477 Coordinate (East 502498 502477 502498 502477 Direction to the nearest residence (feet & compass coordinate) Residence at E County Rd 2000 N
Bursess Trucking 1296 N Washington St
Residence at E County Rd 2000 N
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Baymont Inn and Suites, Dale
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Baymont Inn and Suites, Dale
Residence on County Rd 2100N
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Baymont Inn and Suites, Dale Transportation Department Building
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Residence at E County Rd 2000 N ransportation Department Building esidence at E County Rd 2000 N Residence at E County Rd 2000 N esidence at E County Rd 2000 N esidence at E County Rd 2000 N Baymont Inn and Suites, Dale Building south of Winkler Residence at E County Rd 2000 Building south of Winkler 19. Distance & direction to the nearest property 4226893 4226725 4226725 4226783 4226763 4226684 4226684 4226069 4226725 Contribute Coordinate (North) 422556 422777 422777 422777 422777 4226190 4226431 4226652 4226778 4226893 The or access Uniting feature 502225 501898 502178 502213 502195 502167 502193 502219 502325 502357 502341 502143 502108 502108 Compast Coordinate (East) 502588 502327 502560 502560 502559 502117 Distace (ft) 145 208 28 Height (ft.) 47.9 47.9 47.9 47.9 47.9 8 8 치용 6 18. Building Dimensions (ff) 196.8 147.6 98.4 82 131.2 Diameter (ft) 160.1 160.1 160.1 160.1 160.1 160.1 42.7 42.7 42.7 69.9 69.9 69.9 25.9 25.9 7.9 쑀음 21.3 80.1 80.1 80.1 80.1 80.1 80.1 8 R 669 (ft) (ft) 131.2 295.2 164 131.2 Phenolic Sour Water Storage Tank Stripped Non-Phenolic Sour Water Surge Tank Stripped Phenolic Sour Water Surge Tank Non-Phenolic Sour Water Storage Tank 1 Non-Phenolic Sour Water Storage Tank 2 Non-Phenolic Sour Water Storage Tank 3 Coarse Additive Storage Silo Sodium Sulfide Additive Storage Silo 17, Building Description Maintenance Workshop Laboratory and Analytical Building Amine Surge/Deinventory Tank Moiten Sulfur Tank 2 Residue Surge Tank (VR LPH) 1 Water Trt Sulfuric Acid Tank Water Trt Caustic Tank Potable Water Storage Tank Residue Surge Tank (VR LPH) Demin Water Storage Tank Fine Additive Storage 5110 Diesel Product Swing Tank (Circular Cross-Section)
Naphtha Product Tank 1
Naphtha Product Tank 2 Diesel Fuel Storage Tank Storage Tanks and Silos iesel Product Tank 1 yesel Product Tank 2 lesel Product Tank 3 Soda Ash Mix Tank Molten Sulfur Tank 1 Warehouse/Storage Fresh Amine Tank Residue Feed Tank dmin Buildin VGO Tank 2 VGO Tank 1 Slop Tank 16. Building ۵

Table 10, GSD-02 Plant Layout Diagram Part A Source Building Information

25 Distance & direction to the nearest building on the plant site (feet & compass coordinate) 348 696 797 797 Distance (Feet) 303 203 1018 1021 1118 & 821 419 346 304 515 476 479 260 38 23 237 4226889 4226889 4226689 4226069 4226069 422656 4225656 4225656 4225656 Compass Coordinate (North) 4226763 4226763 4226763 4226763 4226763 4227072 4227072 4227072 4227072 502575 502588 502588 502588 502588 50250 50150 501898 501898 Compass
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502108 502575 502389 502389 502389 502389 502417 502417 502417 502575 24, Building ID of nearest building on the Dant Site Stripped Phenolic Sour Water Surge Tank
Stripped Phenolic Sour Water Surge Tank
Stripped Phenolic Sour Water Surge Tank
Stripped Phenolic Sour Water Surge Tank
Stripped Phenolic Sour Water Surge Tank
Control Room Laboratory and Analytical Building
Laboratory and Analytical Building
Laboratory and Analytical Building
Soda Ash Mix Tank
Soda Ash Mix Tank Laboratory and Analytical Building Laboratory and Analytical Building Soda Ash Mix Tarık
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Admin Compass Coordinate 23. Distance & direction to the nearest property line or access limiting feature (feet & compass coordinate) 4225343 4225551 4226280 4226251 4226296 4227138 4227401 4227401 422703 422703 422637 422637 422642 422642 422642 422642 422643 422643 422643 422643 422643 422643 (North) 4226820 4226866 4226866 4226945 4227133 503636 503568 503404 502607 502477 502435 501740 501122 501135 Compass Coordinate 502763 503074 503431 502601 503480 502585 (East) 501810 501604 501643 501665 502076 Height (ft) 22, Surrounding Building / Residence Property Dimensions ž Š ž ≨ ž Ž ž ž ž ž ¥ ¥ ž \$ \$ 8 8 8 8 Width (ff) 37 23 34 40 32 32 49 8 8 8 8 8 8 8 2 47 ង្គ 15 22 Length (ft) 166 286 233 238 233 103 1103 1182 49 49 56 60 60 60 80 8 8 68 76 꼾 2 2 3 8 228 21 Surrounding Building / Residence Description Bollermakers Union Building
Residence at 20042 N County Rd 500 E
Residence at 20042 N County Rd 500 E
Residence at 20359-2037S N County Rd 500 E
Residence on N County Rd 500 E
Residence on N County Rd 500 E
Residence at 20000 N County Rd 500 E
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Residence at E County Rd 2000 N
Residence at E County Rd 2000 N
Residence at E County Rd 2000 N
Residence at E County Rd 2000 N
Residence at E County Rd 2000 N Buress Trucking 1296 N Washington : Deny's, Dale Wendy's, Dale Transportation Department Building Universal Package Building Winkler Commercial Refrigeration Building south of Winkler Chuckles 23 Residence on County Rd 2100N Baymont Inn and Suites, Dale Motel 6, Dale Chrome Dome Store Taylor Oil

Table 10, GSD-02 Plant Layout Diagram Part B Surrounding Bullding / Residence Information

Table 11. GSD-04 Stack / Vent Information

1. Stack / vent ID	2. Type	3. Shape	4. Outlet Dimensions	5. Height	6. Maximum Outlet Flow Rate	7. Outlet Gas Temperature	8. Related Stacks / Vents
	(V H W O)	(C R O)	(feet)	(feet)	(acfm)	(Degrees F)	(B P O)
THE PURE STORY HAVE			TBD	40	TBD	Ambient	NA NA
U-1000	v	C C	TBD	50	TBD	Ambient	NA NA
U-1001	V	NA NA	TBD	100	TBD	Ambient	NA NA
U-1002	<u> </u>	NA NA	693	100	9697.6	Ambient	NA NA
U-1003	Stockpile	NA NA	TBD	100	TBD	Ambient	NA NA
U-1004	<u>H</u>	NA NA	693	100	9697.6	Ambient	NA NA
U-1005	Stockpile	C	TBD	40	TBD	Ambient	NA NA
U-1006	<u>v</u>	C	3	150	21273	525	NA NA
U-1007	V	c	TBD	40	27917	220	NA
U-1008			1	115	1668	120	NA
U-1501		<u> </u>	1	115	1668	120	NA NA
U-1502	V		0.67	75	834	120	NA NA
U-1503	V	<u> </u>	TBD	TBD	TBD	Ambient	NA NA
EU-1504	V	<u> </u>	5.25	200	48885	525	NA NA
EU-2001		C C	3.17	200	17676	405	NA
EU-2002	V	<u> </u>	1.58	200	4416	800	NA NA
EU-2003	V	C	5.50	200	53051	420	NA NA
EU-2004	V	<u> </u>	TBD	TBD	TBD	Ambient	NA
EU-2005	V	<u> </u>	0.33	115	221	120	NA
<u> </u>	V	C	0.5	115	329	120	NA NA
EU-2007	V	<u> </u>		75	39	120	NA NA
EU-2008	V	<u> </u>	0.17	200	18894	529	NA
EU-3001	V			200	18894	529	NA NA
EU-3002	V		3				
	V	С	1.17	150	3	70	NA NA
EU-4001	+ v	c	2.5	150	11	70	NA NA
EU-4002	<del> </del>	c	On Hold	150	On Hold	On Hold	NA NA
EU-4003		+ <u>c</u>	8	150	111	70	NA NA
EU-4004	<del></del>	<u>c</u>	2	50	8000	500	NA
EU-5001A/B/C/D	V	<del>  c</del>	2	50	8000	500	NA NA
EU-5002A/B/C/D		$+\frac{c}{c}$		50	8000	500	NA_
EU-5003A/B/C/D		C	2	50	8000	500	NA NA
EU-5004A/B/C/D		- c	TBD	TBD	TBD	Ambient	NA_
EU-5005		$\frac{c}{c}$	TBD	TBD	TBD	Ambient	NA_
EU-5006		—— <del>c</del>	TBD	TBD	TBD	Ambient	NA NA
EU-5007		<del></del>	TBD	TBD	TBD	Ambient	NA NA
EU-5008	<u>v</u>	- <del></del>	TBD	TBD	TBD	Ambient	NA NA
EU-5009		c	TBD	TBD	TBD	Ambient	NA NA
EU-5010		—— <u>c</u>	TBD	TBD	TBD	Ambient	
EU-5011		- <del>- c</del>	3.5	100	30300	400	NA_
EU-6000		<del></del>	21	76	545586	110	NA NA
EU-6001	V	<del></del>	21	76	545586	110	NA NA
EU-6002	V	$-\frac{c}{c}$	21	76	545586	110	NA_
EU-6003	V		NA NA	NA NA	NA	NA NA	NA NA
EU-6005	NA NA	NA C	1	16	15234.8	770	NA NA
EU-6006			NA NA	NA.	NA	NA_	NA_
EU-6007	NA	NA C	<u>N7</u>	16	15234.8	770	NA.
EU-6008	V	C	TBD	TBD		Ambien	
EU-6501	V	<u> </u>	TBD	TBD		Ambien	
EU-6502		<u>C</u>	11.25	110		319	NA NA
EU-7001			11.25	110			NA NA
EU-7002	V			45			NA_
EU-7003	V		1.67 1.67	45			NA.

Table 12. GSD-05 Emissions Unit Information

1. Unit ID	2. Model Number	3. Serial Number	4. Description	5. Manufacturer	6. Installation Date	7. Maximum Capacity (MMBtu/hr- HHV or as indicated)	i. Stack / Vent ID
					102021	5000 ton/hr	EU-1000
	TBD	TBD	Coal Unloading Station	TBD	1Q2021	5000 ton/hr	EU-1001
EU-1000	TBD	TBD	Transfer Station 1	TBD	1Q2021	5000 ton/hr	EU-1002
EU-1001	TBD	TBD	Stacker 1 Boom Chute	TBD	1Q2021	93010 tons	EU-1003
EU-1002	TBD	TBD	Coal Pile 1A/1B	TBD	1Q2021	5000 ton/hr	EU-1004
EU-1003	TBD	TBD	Stacker 2 Boom Chute	TBD	1Q2021	93010 tons	EU-1005
EU-1004	TBD	TBD	Coal Pile 2A/2B	TBD	102021	500 ton/hr	EU-1006
EU-1005	TBD	TBD	Reclaim Transfer Station	TBD	1Q2021	55.8	EU-1007
EU-1006	TBD	TBD	Coal Dryer Heater	TBD	1Q2021	NA NA	EU-1008
EU-1007		TBD	Coal Drying Loop Purge (N2 + H2O Vapor)	TBD	102021	20 ton/hr	EU-1501
EU-1008	TBD	TBD	Coarse Additive Storage Filter	TBD	1Q2021		EU-1502
EU-1501	TBD	TBD	Fine Additive Storage Filter	TBD	1Q2021	20 ton/hr	EU-1503
EU-1502	TBD	TBD	NA2S Additive Storage Filter	TBD	1Q2021	10 ton/hr	EU-1504
EU-1503	-U-15U3 Fine Additive Product		Fine Additive Production System	TBD	1Q2021	20 ton/hr	EU-2001
EU-1504	U-1504 TRD Feed Heater		Feed Heater	TBD	1Q2021	128.4	EU-2002
EU-2001	J-2001 TBD TBD Feed Heater		Treat Gas Heater	TBD	1Q2021	52.8	EU-2003
EU-2002	TBD	TBD	Vacuum Column Feed Heater	TBD	1Q2021	9	EU-2003
EU-2003	TBD	TBD	Fractionator Feed Heater	TBD	1Q2021	156	EU-2005
EU-2004	TBD	TBD	Coal Handling System Filter	TBD	1Q2021	300 ton/hr	EU-2005
EU-2005	TBD		Coarse Additive Handling System Filter	TBD	102021	2.2 ton/hr	
EU-2006	TBD	TBD	Fine Additive Handling System Filter	TBD	1Q2021	3,28 ton/hr	EU-2007
EU-2007	TBD	TBD	Na2S Handling System Filter	TBD	1Q2021	0.077 ton/hr	EU-2008
EU-2008	TBD	TBD	TGTU Stack A	TBD	1Q2021	21.4	EU-3001
EU-3001	TBD	TBD	TGTU Stack B	TBD	1Q2021	21.4	EU-3002
EU-3002	TBD	TBD	Loading Flare (8 loading spots naphtha				
			service; each at 2500 gpm)	TBD	1Q2021	99.5 (LHV)	EU-4001
EU-4001	TBD	TBD	Sulfur Block Flare	TBD	1Q2021	100.6 (LHV)	EU-4002
EU-4002	TBD	TBD	LP Flare	TBD	1Q2021	8550 (LHV)	EU-4003
EU-4003	TBD	TBD	HP Flare	TBD	1Q2021	3377 (LHV)	EU-4004
EU-4004	TBD	TBD	Residue Pastilators Stack1	TBD	1Q2021	12.9 ton/hr	EU-5001A/B/C/
EU-5001A/B/C/0	TBD	TBD	Residue Pastilators Stack2	TBD	1Q2021	12.9 ton/hr	EU-5002A/B/C/
EU-5002A/B/C/I	) TBD	TBD	Residue Pastilators Stack2  Residue Pastilators Stack3	TBD	1Q2021	12.9 ton/hr	EU-5003A/B/C/
EU-5003A/B/C/I	O TBD	TBD		TBD	1Q2021	12.9 ton/hr	EU-5004A/B/C/
EU-5004A/B/C/		TBD	Residue Pastilators Stack4	TBD	1Q2021	40 ton/hr	EU-5005
EU-5005	TBD	TBD	Residue Railcar Loading	TBD	102021	40 ton/hr	EU-5006
EU-5006	TBD	TBD	Residue Railcar Loading	ТВО	102023	40 ton/hr	EU-5007
EU-5007	TBD	TBD	Residue Rail/Truck Loading	TBD	1Q2021	40 ton/hr	EU-5008
EU-5008	TBD	TBD	Residue Rail/Truck Loading	TBD	1Q202		EU-5009
EU-5009	TBD	TBD	Residue Bulk Container Loading	TBD	1Q202		EU-5010
EU-5010	TBD	TBD	Residue Rail Silo Filter	TBD	10202		EU-5011
EU-5011	TBD	TBD	Residue Swing Silo Filter	TBD	1Q202		EU-6000
EU-6000	TBD	TBD	Package Boiler	TBD	10202		EU-6001
EU-6001	TBD	TBD	Cooling Tower Cell A		10202		
EU-6001	TBD	TBD	Cooling Tower Cell B	TBD	1Q202	<del></del>	EU-6003
	TBD	TBD	Cooling Tower Cell C	TBD	1Q202		EU-6005
EU-6003	TBD	TBD	EDG Diesel Tank	TBD	1Q202		EU-6006
EU-6005	TBD	TBD	Emergency Diesel Generator	TBD			
EU-6006	TBD	TBD	EDFWP Diesel Tank	TBD	1Q202		EU-6008
EU-6007		TBD	Emergency Diesel FireWater Pump	TBD	1Q202		EU-6501
EU-6008	TBD	TBD	Lime Silo Filter	TBD	1020		EU-6502
EU-6501	TBD	TBD	Deaerator Vent	TBD	1020		EU-7001
EU-6502	EU-6502 TBD		Hydrogen Plant 1 Reformer	TBD	1020		EU-7002
EU-7001	TBD		Hydrogen Plant 2 Reformer	TBD	1Q20		
EU-7002	TBD	TBD	Hydrogen Plant 1 DA Vent	TBD	1Q20		
EU-7003	TBD	TBD	Hydrogen Plant 2 DA Vent	TBD	1Q20	21 2628.36 ac	fm EU-7004

Table 13. GSD-06 Particulate Emissions Summary Table 13a. Part A: Particulate Emissions Summary

	Emission Point			Potential	To Emit (tons p	er year)	<del></del>	1
1. Unit ID	2. Description	3. PM	4. PM-10	5. PM-2.5	6. TSP	7. Fugitive Dust	8. Fugitive PM	9. HAP PM
					4 1			1
EU-1000	Coal Unloading Station	0.152	0.114	0.003	0.152			
EU-1000 EU-1001	Transfer Station 1	0.002	0.001	0	0.002			
EU-1002	Stacker 1 Boom Chute	1.169	0.877	0.022	1.169	1		
EU-1003	Coal Pile 1A/1B	3.7635	1.8815	0.7525	3.7635	ŧ		
EU-1004	Stacker 2 Boom Chute	1.169	0.877	0.022	1.169			
EU-1005	Coal Pile 2A/2B	3.7635	1.8815	0.7525	3.7635	ļ		
EU-1006	Reclaim Transfer Station	2.41	1.807	0.046		4		
EU-1007	Coal Dryer Heater	1.835	1.835			4		
EU-1008	Coal Drying Loop Purge (N2 + H2O Vapor)	2.405	2.405	2.405		-1		
EU-1501	Coarse Additive Storage Filter	0.019	0.019			-{		
EU-1502	Fine Additive Storage Filter	0.028	0.028			1		
EU-1503	NA2S Additive Storage Filter	0.001	0.001			4		
EU-1504	Fine Additive Production System	0.034	0.034			-		
EU-2001	Feed Heater	4.218	4.218			-1		
EU-2002	Treat Gas Heater	1.74	1.74			⊣		
EU-2003	Vacuum Column Feed Heater	0.3	0.3			<b>-</b> ∔		
EU-2004	Fractionator Feed Heater	5.12	5.12 0.023			⊣		
EU-2005	Coal Handling System Filter	0.023	0.023			-1		
EU-2006	Coarse Additive Handling System Filter	0.023	0.023			-1		
EU-2007	Fine Additive Handling System Filter	0.034	0.034			<b>⊣</b> i		
EU-2008	Na2S Handling System Filter	0.004			<del></del>	⊣		
EU-3001	TGTU Stack A	1.216				<b>⊣</b>		
EU-3002	TGTU Stack B	1.216	1.210	1.2.1	-	1		
	Loading Flare (8 loading spots naphtha	0.007	0.007	0.007	0.00	7		
EU-4001	service; each at 2500 gpm) Sulfur Block Flare	0.03	<del></del>	<del></del>	0.0	3 s	ee Fugitive Du	st Plan
EU-4002	LP Flare	0.24		4 0.24	4 0.2	4		
EU-4003	HP Flare	0.235	<b>—</b> ——	5 0.23	5 0.23	5		
EU-4004 EU-5001A/B/C/D	Residue Pastilators Stack1	Trace	Trace	Trace	Trace			
EU-5001A/B/C/D	Residue Pastilators Stack2	Trace	Trace	Trace	Trace	2		
EU-5003A/B/C/D	Residue Pastilators Stack3	Trace	Trace	Trace	Trace	티		
EU-5004A/B/C/D	Residue Pastilators Stack4	Trace	Trace	Trace	Trace	<u>e</u>		
EU-5005	Residue Railcar Loading	Trace	Trace	Trace	Trac	е		
EU-5006	Residue Railcar Loading	Trace	Trace	Trace	e Trac	e		
EU-5007	Residue Rail/Truck Loading	Trace	Trace	e Trace				
EU-5008	Residue Rail/Truck Loading	Trace	Trace	e Trace		_		
EU-5009	Residue Bulk Container Loading	Trace	Trace	e Trace		-1		
EU-5010	Residue Rail Silo Filter	Trace	Trace					
EU-5011	Residue Swing Silo Filter	Trace						
EU-6000	Package Boiler	2.23						
EU-6001	Cooling Tower Cell A	0.278						
EU-6002	Cooling Tower Cell B	0.27						
EU-6003	Cooling Tower Cell C	0.27						
EU-6005	EDG Diesel Tank	N/				IA 51		
EU-6006	Emergency Diesel Generator	0.046				1		
EU-6007	EDFWP Diesel Tank	N <sub>i</sub>				17		
EU-6008	Emergency Diesel FireWater Pump	0.024						
EU-6501	Lime Silo Filter	TBI				NA NA		
EU-6502	Deaerator Vent	N.						
EU-7001	Hydrogen Plant 1 Reformer	22.0						
EU-7002	Hydrogen Plant 2 Reformer	22.0				NA		
EU-7003	Hydrogen Plant 1 DA Vent	N N				NA NA		
EU-7004	Hydrogen Plant 2 DA Vent	N N	A  N	NA NA	NA	***		

Table 13. GSD-06 Particulate Emissions Summary Table 13b. Part B: Control of Particulate Emissions

			13. Control Plan
10. Unit ID	11. Control Measures	12. Control Measures Description	15, CUILLOI FIBIT
		[전 12 기존] 그 이 발표보다 보다 보고 모으는 그 모드다.	
		[보는 회사는 경기는 사고를 한다면 가능하고 모든 모양]	
	Boghouso		
U-1000	Baghouse Baghouse		
U-1001	Water spray on chute		
U-1002	Wetting		
U-1003 U-1004	Water spray on chute		!
EU-1005	Wetting		
EU-1005 EU-1006	Baghouse		
EU-1006 EU-1007	NA	NA .	
EU-1007	Baghouse	Moisture vent with trace PM	
EU-1501	546,1445		
EU-1502	1	Solid storage shall be provided with dust filters on the top to separate	
EU-1503	Baghouse	nitrogen from the solid.	
EU-1504	1		
EU-2001	NA	NA	
EU-2002	NA	NA	Į
EU-2003	NA	NA .	-
EU-2004	NA	NA	
EU-2005			
EU-2006	7	Solid handling systems shall be provided with dust filters to separate	}
EU-2007	Baghouse	nitrogen from the solid.	
EU-2008			4
EU-3001	NA	NA .	4
EU-3002	NA	NA .	1
EU-4001	NA	NA .	┪
EU-4002	NA	NA	-
EU-4003	NA	NA	Yes. Fugitive dust
EU-4004	NA	NA	plan.
EU-5001A/B/C/D	NA	NA	-
EU-5002A/B/C/D	NA	NA .	1
EU-5003A/B/C/D	NA	NA .	1
EU-5004A/B/C/D	NA	NA NA	
EU-5005	NA	NA .	1
EU-5006	NA	NA	1
EU-5007	NA NA	NA .	1
EU-5008	NA	NA	- ·
EU-5009	NA NA	NA .	┪
EU-5010	Baghouse	Baghouse	<b>-</b>
EU-5011	Baghouse	Baghouse	7
EU-6000	NA	NA	
EU-6001	<u></u>	Drift eliminators are capable of achieving drift to 0.0005% of the cooling	
EU-6002	Drift Eliminators	tower's recirculation rate.	
EU-6003			
EU-6005	NA	NA	7
EU-6006	NA	NA	
EU-6007	NA	NA NA	
EU-6008	NA .	NA	
	Baghouse	Baghouse	
EU-6501			
EU-6502	NA	NA	
EU-6502 EU-7001	NA NA	NA .	7
EU-6502	NA		

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Table 14 GSD-07 Criteria Pollutant Emissions Summary - Potential To Emit

Table 14 GSD-	4 GSD-07 Criteria Pollutant Emissions Summary - Potential To Emit					Criteria Po					Criteria Po	a Pollutants - Potential to Emit									1					
Unit ID	Stack ID	NO	)v		:o	sc	)2	TS	P	PN	110	PM	2.5	VOC/N	мнс	Le	ad	cc	)2	Total	CO2e	HA	Ps	Other	Compound	2t
OHI ID	JIACK ID	(lb/hr)	(tons/yr)	(lb/hr)	(tons/yr)	(lb/hr)	(tons/yr)	(lb/hr)	(tons/yr)	(ib/hr)	(tons/yr)	(lb/hr)	(tons/yr)	(ib/hr)	(tons/yr)	(lb/hr)	(tons/yr)	(lb/hr)	(tons/yr)	(lb/hr)	(tons/yr)	(lb/hr)	(tons/yr)	Species	(lb/hr)	(tons/yr)
EU-2001	EU-2001	2.470	10.800	2,470	10.800	0.229	1.002	0.963	4.218	0.963	4.218	0.963	4.218	0.693	3.037	0.000	0.000	14967.5	65557.4	14998.7	65694.3	0.238	1.041	Metals	0.005	0.024
	EU-2002	2.112	9.251	1.901	8.326	0.094	0.412	0.396	1.734	0.396	1.734	0.396	1.734	0.285	1.249	0.000	0.000	6154.8	26958.2	6167.7	27014.5	0.098	0.428	Metals	0.002	0.010
EU-2002		<del>                                     </del>	1.577	0.324	1.419	0.016	0.070	0.067	0.296	0.067	0.296	0.067	0.296	0.049	0.213	0.000	0.000	1049.1	4595.1	1051.3	4604.7	0.017	0.073	Metals	0.000	0.002
EU-2003	EU-2003	0.360	<del> </del>				-		5.125	1.170	5.125	1.170	5.125	0.842	3.690	0.000	0.000	18184.8	79649.2	18222.7	79815.5	0.289	1.265	Metals	0.007	0.029
EU-2004	EU-2004	6.240	27.331	5.616	24.598	0.278	1.217	1.170			1.216	0.278	1.216	0.203	0.890	0.000	0.000	4607.0	20178.7	4616.2	20218.9	0.070	0.305	Metals	0.002	0.007
EU-3001	EU-3001	6.782	29.705	1.319	5.775	12.507	54.780	0.278	1.216	0.278	1.216	0.278	1.210	0.203								-		Sulfuric Acid Mist	0,600	1.940
			1		ļ <u></u>		54.700	0.270	1 216	0.270	1 216	0.278	1.216	0.203	0.890	0.000	0.000	4607.0	20178.7	4616.2	20218.9	0.070	0.305	Metals	0.002	0.007
EU-3002	EU-3002	6.782	29.705	1.319	5.775	12,507	54.780	0.278	1.216	0.278	1.216	0.276	1.210	0.200	0.020									Sulfuric Acid Mist	0.600	1.940
EU-4004	EU-4004	0.440	1.930	2.400	10.510	0.010	0.050	0.050	0.240	0.050	0.240	0.050	0.240	0.040	0.160	0.000	0.000	819.0	3588.0	886.0	3881.0	0.000	0.000	N/A	N/A	N/A
EU-4002	EU-4002	0.060	0.250	0.310	1.340	1.100	4.800	0.010	0.030	0.010	0.030	0.010	0.030	0.020	0.070	0.000	0.000	103.0	452.0	112.0	489.0	0.000	0.000	N/A	N/A	N/A
EU-4001	EU-4001	0.014	0.030	0.040	0,180	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	98.685	5.603	0.000	0.000	13.8	60.4	14.9	65.4	14.532	0.683	N/A	N/A	N/A
		2.720	45.014	2.440	10.722	0.121	0.531	0.510	2.234	0.510	2.234	0.510	2.234	0.367	1.608	0.000	0.000	7926.7	34718.8	7943.2	34791.3	0.126	0:551	Metals	0.003	0.013
EU-6000	EU-6000	0.000	0.000	0.000	0.000	0.000	0.000	0.190	0.834	0.112	0.492	0.000	0.002	1.282	5.614	0.000	0.000	0.0	0.0	0.0	0.0	0.000	0.000	Ammonia	0.125	0.549
EU-6001/2/3	EU-6001/2/3	0.000	0.500	0.000	0.000	0.000	0.000	0.250						-										Chlorine as HOCl	1.200	5.220
					0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	4.196	18.376	0.000	0.000	0.0	0.0	0.0	0.0	0.000	0.000	N/A	N/A	N/A
EU-5001a-04d	EU-5001a-04d	0.000	0.000	0.000	0.000	0.000	0.000					0.840	0.040	0.680	0.030	0.000	0.000	3028.0	151.0	3056.0	153.0	0.041	0.002	N/A	N/A	N/A
EU-6006	EU-6006	33.640	1.680	1.850	0.090	0.490	0.030	0.840	0.040	0.840	0.040	1		0.180	0.020	0.000	0.000	870.0	87.0	878.0	87.8	0.353	0.040	N/A	N/A	N/A
EU-6008	EU-6008	9.010	0.900	0.500	0.050	0.140	0.010	0.230	0.020	0.230	0.020	0.230	0.020			<del> </del>	+	224972.1	985377.6	225176.1	986271.5	0.000	0.000	Ammonia	0.061	0.267
EU-7001	EU-7001	5.451	23.875	16.772	73.462	0.273	1.197	5.032	22.038	5.032	22.038	5.032	22.038	5.032	22.038	0.000	0.000	<del>                                     </del>				ļ		Ammonia	0.061	0.267
EU-7002	EU-7002	5.451	23.875	16.772	73.462	0.273	1.197	5.032	22.038	5.032	22.038	5.032	22.038	5.032	22.038	0.000	0.000	224972.1	985377.6	225176.1	986271.5	0.000	0.000		<del> </del>	17.170
EU-7003	EU-7003	0.000	0.000	1.060	4.650	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	3.160	13.850	0.000	0.000	246.5	1080.0	292.5	1282.0	2.950	12.910	Ammonia	3,920	
											İ										ļ			Acetic acid	0.040	0.180
EU-7004	EU-7004	0.000	0.000	1.060	4.650	0.000	0.000	0.000	0.000	0.000	0.000	0.000	0.000	3.160	13.850	0.000	0.000	246.5	1080.0	292.5	1282.0	2.950	12.910	Ammonia	3.920	17.170
1.0-7004	10.7004	0.500	0.000	*******																				Acetic acid	0.040	0.180
EU-4003	EU-4003	0.440	1.930	2.400	10.510	0.010	0.050	0.050	0.240	0.050	0.240	0.050	0.240	0.040	0.160	0.000	0.000	819.0	3588.0	886.0	3881.0	0.000	0.000	N/A	N/A	N/A
EU-1000	EU-1000	0.000	0.000	0.000	0.000	0.000	0.000	0.358	0.152	0.268	0.114	0.007	0.003	0.000	0.000	0.000	0.000	0.0	0.0	0.0	0.0	0.000	0.000	0.000	0.000	0.000
EU-1001	EU-1001	0.000	0.000	0.000	0.000	0.000	0.000	0.005	0.002	0.002	0.001	0.000	0.000	0.000	0.000	0.000	0.000	0.0	0.0	0.0	0.0	0.000	0.000	0.000	0.000	0.000
EU-1002	EU-1002	0.000	0.000	0.000	0.000	0.000	0.000	2.751	1.169	2.064	0.877	0.052	0.022	0.000	0.000	0.000	0.000	0.0	0.0	0.0	0.0	0.000	0.000	0.000	0.000	0.000
EU-1003	EU-1003	0.000	0.000	0.000	0.000	0.000	0.000	8.855	3.764 1.169	4.427 2.064	0.877	0.052	0.753	0.000	0.000	0.000	0.000	0.0	0.0	0.0	0.0	0.000	0.000	0.000	0.000	0.000
EU-1004	EU-1004	0.000	0.000	0.000	0.000	0.000	0.000	2.751 8.855	3.764	4.427	1.882	1,771	0.753	0.000	0.000	0.000	0.000	0.0	0.0	0.0	0.0	0.000	0.000	0.000	0.000	0.000
EU-1005	EU-1005 EU-1006	0.000	0.000	0.000	0.000	0.000	0.000	0.550	2.410	0.413	1.807	0.011	0.046	0.000	0.000	0.000	0.000	0.0	0.0	0.0	0.0	0.000	0.000	0.000 Metals	0.000	0.000
EU-1006 EU-1007	EU-1007	2.232	9.776	2.009	8.799		0.436			0.418	1.833	0.418	1.833	0.301	1.320	0.000	0.000	6504.5	28489.9	6518.1	28549.4	0.103	0.452	0.000	0.002	
EU-1008	EU-1008	0.000	0.000	0.000	0.000	0.000	0.000	0.549	2.405			_	2.405	0.000	0.000	0.000	0.000	0.0	0.0	0.0	0.0		5 2.00E-05		0.000	
EU-1501	EU-1501	0.000	0.000	0.000	0.000	0.000	0.000	0.039	0.019	0.039			0.019	0.000	0.000	0.000	0.000	0.0	0.0	0.0	0.0		5 2.00E-05		0.000	0.000
EU-1502	EU-1502	0.000	0.000	0.000	0.000	0.000	0.000	0.039	0.028	0.039			0.028	0.000	0.000	0.000	0.000	0.0	0.0	0.0	0.0	0.000	0.000	0.000	0.000	
EU-1503	EU-1503	0.000	0.000	0.000	0.000	0.000	0.000	0.020	0.001	0.020			0.034	0.000	0.000	0.000	0.000	0.0	0.0	0.0	0.0		6 3.62E-05		0.000	
EU-1504	EU-1504	0.000	0.000	0.000	0.000	0.000	0.000	0.0053		0.0053			0.023	0.000	0.000	0.000	0.000	0.0	0.0	0.0	0.0	0.000			0.000	
EU-2005 EU-2006	EU-2005 EU-2006	0.000	0.000	0.000	0.000	0.000	0.000	0.005	0.023	0.005			0.023	0.000	0.000	0.000	0.000	0.0	0.0	0.0	0.0		6 2,40E-05		0.000	
EU-2007	EU-2007	0.000	0.000	0.000	0.000	0.000	0.000		0.034	0.008			0.034	0.000	0.000	0.000	0.000	0.0	0.0	0.0	0.0	0.000	6 3.60E-09		0.000	
EU-2008	EU-2008	0,000	0.000	0.000	0.000	0.000	0.000	0.001	0.004	0.001	0.004	0.001	0.004	0.000	0.000	0.000	0.000	0.0	0.0	1 0.0	1 0.0	1 0.000	3,000			

- 1. Diesel firewater pump operation is 200 hours per year
- 2. Emergency Diesel Generator operations is 100 hours per year
- 3. All process related equipment are assumed to operate for 8760 hours annually
- 4. Hydrogen plant emission information has been provided by an outside vendor, based upon vendor's initial conceptual approach. Discussion regarding hydrogen plant design are not finalized.
- 5. Although Hydrogen Reformers are planned to be sized up to 70% of maximum VCC process facility production, maximum pollutant emissions are limited by VCC facility.
- The potential emissions are invariant, since maximum pollutant putput is limited by the VCC facility and the hydrogen plant is an auxiliary operation. Thus, emissions potential is based upon the required hydrogen at 100% VCC facility production capacity.
- 6. CO2e includes CO2. They are separately listed to establish that Greenhouse Gas (GHG) impacts have been determined for the spectrum of GHG generating species. The 40 CFR Part 98 Global Warming Potentials (GWPs) have been used to determine CO2e.
- 7. All non-cooling tower particulates emissions are assumed to be fine particulate matter. Thus TSP = PM10 = PM2.5 8. Emissions estimates utilize AP-42 emission factors extensively. These factors provide conservatively high emissions estimates that will be refined with vendor information as it becomes available.
- 9. Smokeless flaring is assumed
- 10. Diesel fuel is USLD
- 11. Storage tank emissions were determined using TANKS 4.09d. The results are provided elsewhere in this application.

Table 15 GSD-08 Hazardous Air Pollutants Summary

Table 15a. Part A: Unit Emissions Summary

1. Unit ID	2. Stack / Vent ID		3. Hazardous Air Pollutant	4. CAS Number	5. Actua	l Emissions	6. Potential t	o Emit
					Standard Unit	Tons per Year	Standard Unit, lb/hr	Tons per Year
EU-1007	EU-1007	Coal Dryer Heater	Total HAPs	NA	TBD	TBD	1,03E-01	0.45
EU-1007	50-1007	Coar bryer (lease)	n-Hexane	110543			9.86E-02	0.432
İ		<u> </u>	Formaldehyde	50000	1	Į i	4.11E-03	0.018
		i F	Toluene	108883			1.86E-04	8.15E-04
			Benzene	71432	1		1.15E-04	5.04E-04
			Nickel	7440020			1.15E-04	5.04E-04
EU-1501	EU-1501	Coarse Additive Storage Filter	Total HAPs are manganese compounds	NA	TBD	TBD	4.19€-05	2.00E-05
EU-1502	EU-1502	Fine Additive Storage Filter	Total HAPs are manganese compounds	NA	TBD	ТВО	4.19E-05	2.00E-05
EU-1504	EU-1504	Fine Additive Production System	Total HAPs are manganese compounds	NA	TBD	TBD	8.27E-06	3.62E-05
EU-2001	EU-2001	Feed Heater	Total HAPs	NA	TBD	TBD	2.38E-01	1.04
20 2001		ļ	n-Hexane	110543	_	1	2.27E-01	0.992
			Formaldehyde	50000	4		9.44E-03	4.13E-02
		1	Toluene	108883	_		4.28E-04	1.87E-03
			8enzene -	71432			2.64E-04	1.16E-03
			Nickel	7440020		****	2.64E-04 9.78E-02	0.43
EU-2002	EU-2002	Treat Gas Heater	Total HAPs	NA	TBD	TBD	9.33E-02	0.48
			n-Hexane	110543			3,89E-03	0,017
			Formaldehyde	50000 108883	-	Į	1,76E-04	7.72E-04
			Toluene	71432		1	1.09E-04	4.77E-04
			Benzene Nickel	7440020	-		1,09E-04	4.77E-04
EU-2003	EU-2003	Vacuum Column Feed Heater	Total HAPs	NA NA	TBD	TBD	1.67E-02	0.07
		reed ricates	п-Нехапе	110543	7		1.59E-02	0.0698
		1	Formaldehyde	50000	1		6.64E-04	2.91E-03
			Toluene	108883			3.01E-05	1.32E-04
			Benzene	71432		ļ	1.86E-05	8.14E-05
		Fractionator Feed	Nickel Total HAPs	7440020 NA	ТВО	TBD	1.86E-05 0.29	8.14E-0
EU-2004	EU-2004	Heater				1	0.28	1.21
			n-Hexane	110543			1.50E-02	5.02E-0
			Formaldehyde	50000	-	ļ	5.20E-04	2.28E-0
			Toluene	108883		1	3.21E-04	1.41E-0
			Benzene	71432 7440020			3,218-04	1.41E-0
EU-2006	EU-2006	Coarse Additive Handling System	Nickel Total HAPs are manganese compounds	NA.	TBD	TBD	5.55E-06	0.00002
EU-2007	EU-2007	Filter Fine Additive Handling System	Total HAPs are manganese compounds	NA NA	TBD	TBD	8.27E-06	0.00003
		Filter	Total HAPs	NA NA	TBD	TBD	0.07	0.31
EU-3001	EU-3001	TGTU Stack A	n-Hexane	110543	٠		0.07	0.291
		Į	Formaldehyde	50000	_		2.77E-03	0.01213
			Toluene	108883		1	1.26E-04	5.50E-0
			Benzene	71432			7.76E-05	3.40E-0
			Nickel	7440020			7,76E-05	3.40E-0
EU-3002	EU-3002	TGTU Stack B	Total HAPs	NA	TBD	TBD	0.07	0.31
			n-Hexane	110543			0.07	0.291
			Formaldehyde	50000		1	2,77E-03	0.01213 5.50E-0
		.1	Toluene	108883			1.26E-04 7.76E-05	3,40E-0
		1	Benzene	71432			7.76E-05	3.40E-0
			Nickel	7440020	700	TBD	14.532	0.683
EU-4001	EU-4001		Total HAPs	NA 71422	TBD	1917	1.48	0.07
			Benzene	71432	-	1	3.947	0.185
	İ	Loading Flare (8	Toluene	108883 1330207	$\dashv$		4,934	0.23
	1	loading spots	Xylenes Phonois	108952	-	<b>-  </b>	0.049	0.00
		naphtha service;	Phenols p-cresol	95487		1	0.118	0.00
		each at 2500 gpm)	m+p-cresol	1319773	$\dashv$		0.049	0.00
	1	1	111. p. c. c. c. c. c.		<b>—</b> i	i i	3.947	0.18

#### Table 15 GSD-08 Hazardous Air Pollutants Summary

Table 15a. Part A: Unit Emissions Summary

1. Unit ID	2. Stack / Vent ID		3. Hazardous Air Pollutant	4. CAS Number	5. Actua	l Emissions	5. Potential to Emit		
					Standard Unit	Tons per Year	Standard Unit, Ib/hr	Tons per Year	
EU-6000	EU-6000	Package Boiler	Total HAPs	NA	TBD	TBD	0.127	0.555	
50 0000			n-Hexane	110543	1		0.12	0.526	
			Formaldehyde	50000			0.005	0.022	
	ļ		Toluene	108883	1		2.27E-04	9.93E-04	
			Benzene	71432	1		1.40E-04	6.13E-04	
			Nickel	7440020	1	<u> </u>	1.40E-04	6.13E-04	
EU-6006	EU-6006	Emergency Diesel Generator	Total HAPs		TBĐ	TBD	0.041	0.002	
EU-6008	EU-6008	Emergency Diesel FireWater Pump	Total HAPs		TBD	TBD	0.353	0.04	
EU-7003	EU-7003	Hydrogen Plant 1 DA Vent	Methanol	67561	TBD	TBD	2.95	12.19	
EU-7004	EU-7004	Hydrogen Plant 2 DA Vent	Methanol	67561	TBD	TBD	2.95	12.19	
FUGVCC	FUGVCC	VCC Process Unit	Benzene	71432	TBD	TBD	0.02	0.11	
,			Toluene	108883			0.07	0.29	
			Xylenes	1330207			0.08	0.36	
			Phenols	108952	1		0.00	0.00	
			o-cresol	95487	1		0.00	0.01	
			m+p-cresol	1319773			0.00	0.00	
			n-hexane	110543			0.07	0.29	
FUGPRD	FUGPRD	Product Storage and Handling	8enzene	71432	TBD	TBD	0.00	0.01	
			Toluene	108883			0.01	0.03	
			Xylenes	1330207			0,01	0.03	
			Phenols	108952			0,00	0.00	
	1		o-cresol	95487	1		0.00	0.00	
			m+p-creso	1319773	٦		0.00	0.00	
			n-hexane	110543		1	0.01	0.03	

Table 15b. Part B: Pollutant Emissions Summary

7. Hazardous Air Pollutant	8. CAS Number	9. Actua	al Emissions	10. Potential to Emit			
		Standard Unit	Tons per Year	Standard Unit, lb/hr	Tons per Year		
Hexane (-n)	110543	TBD	TBD	4.98	4.79		
Formaldehyde	50000	TBD	TBD	0.04	0.18		
Toluene	108883	TBD	TBD	4.02	0.51		
Benzene	71432	TBD	TBD	1.51	0.19		
Nickel	7440020	TBD	TBD	0.001	0.005		
Xylenes	1330207	TBD	TBD	5.02	0.63		
Phenol	108952	TBD	TBD	0.05	0.01		
o-Cresol	95487	TBD	TBD	0.12	0.02		
m-, p-Cresois	1319773	TBD	TBD	0.05	0.01		
Methanol	67561	TBD	TBD	5.9	24.38		

Table 15c. Part C: Fugitive HAPs Emissions

11. Fugitive Emission Source	12. Hazardous Air Poliutant	13. Emission Factor	14. Number Leaking	15. Uncontrolled Potential to Emit				
				Pounds per hour	Tons per year			
Compressor Seals			4					
Flanges			1177	1				
Open-Ended Lines			94					
Pressure Relief Seals		achments -CAL-EV2-0001,	109	*See attachments H102-2000-EV-CAL-EV2-0				
Pump Seals	H102-4000-EV	-CAL-EV2-0002	41	H102-4000-EV-CAL-EV2-0				
Sampling			213					
Connections		•	317					
Valves			222					
Other (specify): - Drains			213					

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# FUGITIVE AIR EMISSION INVENTORY CALCULATIONS

	LOGITIAE VIIVEINIOO						T	4
	DOC NO.: H102-2000-EV-CAL-EV2-0001	Rev:	A	0	11	22	3	4
JOB NO.: H102		Date:	8-Jan-18	15-Jan-18	23-Jan-18			
CLIENT: Riverview Energy Corporation		By:	RN	RN	RN			
PROJECT: DCH Facility	BASIS: Reference & PFD Factored Equipment	Check:	SAL	SAL	SAL			
LOCATION: Daie, IN								
UNIT: VCC		Appr.:	151	IEI	IF!			
		Purpose:	]FI	ļ IFI	Н.			
UNIT No. 2000								

UNIT No. 2	2000						Pur	pose:	FI	FI	IF I								
		govalena esse Messa.	***************************************						PROJE	CT DEFINITION				ANGE PROPERTY.	The state of the s	The second secon	A STATE OF THE STA	A A STATE OF THE S	
LINE REV				COMPANION CONTRACTOR	engliste (Angles							entime in Ad	ausay S	SUM	10	M Coordinates	for Process L	Jnit	
1 2	Revision H	listory					SHADING LE	GEND:	ENTRY	LINKED	CALC G	OAL SEEK	CHECK	SUM			Easting (m)		
3	Α	Initial Setup	for Checking												Co	orner 1			
4	0	T&C PFD Ba	asis, MatBal Str	eams Aggrega	ated										C	orner 2			
5	1															orner 3			
6	2														-	orner 4			
7	3														-	orner 5			
8	4														1-	orner 6 orner 7			
9																orner 8			
10	TABLE OF	CONTENTS													12	V. 1.44			
12	SECTION	LINE	DESCRIPTION																
13	1	35	Emissions Su	ummary															
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15	3	78	Federal Regu	Ilatory Applic	ability - Eval	uation Basis	Remarks	uetrial Sacto	re										
16	4.	141	Reference En	mission Facto	ors for Piping	Component	Design Speci	ifications	,, 3										
17	5	204	Reference Pr	rimary Contro	of Credit % 10	for I DAR P	odrams	mouneme											
18	6	250	Evaluation B	econdary Cor	n Factors F	auinment De	sian Specific	ations, and l	LDAR Progra	ims									
19	7	277 327	Available Ma	terial Balance	e Data Inout		· -	-	-										
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25	13	595	Fugitive Equ	tipment Coun	its and Facto	ring Basis, Ir	lieu of Direc	I PAID COUN	ıı										
26	14	712	Final Equipm Undifferentia	nent Counts I	Evaluated	A VIOCI Deci	d linos initis	d Source Co	unt Totals										
27	15	762	Undifferentia Controlled F	ated Fugitive	Emissions (a	inment Tuna	Process Str	eam or Area											
28	16	816	Speciated Fu	·ugnive Emis:	sions by ⊏qu	ess Stream	or Area												
29	17	866	NOTES	ugitive cimiss	Sions by Frod	ess Otteam (	,, ,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,												
30	18	926	NOTES																
31	4								<u> </u>							-			
32																			
34	1																		
35	1	Emissions	Summary							[	Primary	Secondary							
36	1									i	Equipment	LDAR Program	Overall Fugitive						
37		Emission	Factor Set Use	ed :	TCEQ-R	enning					Design Control	Control	Control						1
38	1			1	Em. Factor	Equipment	Un	controlled Fug	itive Emissions	5	Efficiency	Efficiency	Efficiency	Contingency		Controlled Fug MT/yr	Ib/hr	ton/yr	<del> </del>
39	_	Sustitus Em	ission Source	Service	kg/hr	Counts	kg/hr	MT/yr	lb/hr	ton/yr	%	%	%	%	kg/hr	0.36470	0.09178	0.40200	Streams wit
40	_		issidit dource	Gas	0.0268	3	0.08	0.70	0,18	0.78	0	97	97	50%	0,04163	0.09155	0.02304	0.10092	Final valve
41 42	-	Valves		Light Liquid	0.0109	32	0.35	3.05	0,77	3,36	0	97 97	97 97	50% 50%	0.04997	0.43772	0.11016	0.48250	
42	-			Heavy Liquid	0,0109	153	1.67	14.59	3.67	16.08	0	85	97	0%	0.07424	0.65037	0.16368	0.71690	Double Med
44	1	Pumps		Light Liquid	0.1139	18	2.05	17.95	4.52	19.79 3.83	80	0	80	0%	0.12291	1,07667	0,27096	1,18681	
45		(Includes Ve	ssel Agitators)	Heavy Liquid	0.0209	19	0.40	3,47 2.26	0,87 0.57	2.50	0	30	30	25%	0.30599	2.68044	0.67458	2.95465	Reactor and
46		Flanges / C	onnectors	All	0.00025	1036	0.26	58.25	14.66	64.21	100	97	100	15%	0.00000	0.00000	0,00000	0.00000	
47	_	Pressure R	elief Valves	Gas	0.3500	19	6.65 31,50	275.94	69.44	304.17	100	0	100	15%	0.00000	0.00000	0.00000	0.00000	
48	4			Liquids All	0,3500	90	1,40	12.26	3.08	13.51	100	85	100	15%	0.00000	0.00000	0.00000	0.00000	
49		Compresso		All	0.00510	90	0.46	4,02	1.01	4.43	100	85	100	15%	0.00000	0,00000	0.00000		
50	_		d Lines/Valves Connections	All	0.03300	205	6.77	59.26	14,91	65.32	100	85	100	15%	0.00000	0.00000	0.00000		
51	_		onnections s - Miscellaneous	A.11	0.00025	0	0.00	0.00	0.00	0.00	0		-	15%	1,49479	13.09438	3.29542		
52	-	Drains		All	0.02917	205	5.98	52.38	13.18	57.74	50	50	75	15% 15%	0.00000	0.00000	0.00000	0.00000	
54	1	Others			0.00000	0	0.00	0.00	0.00	0.00	0	0		15%	0.00000	0.00000	0.00000	0.00000	
55	7		ers - Gas/Vapor	All	000000	0	0,00	0.00	0,00	0.00	0			15%	0.00000	0,00000	0,00000		
56	]	O&G Othe	ers - Liquid	All	0.00000	0	0.00	0.00	125.88	555,72	ľ	<u> </u>			2,100	18.396	4,630	20.278	
57					Totals >	1871	57.55	504.14		E-1-2-2-2-1-2-1-2-2-2-2-2-2-2-2-2-2-2-2-	2								
58																			
59	_1 _	D===t=+-	d Emiocions C	ummarv							_								
60	2	Speciate	d Emissions S	uning y						Contingency				11.75-	tenher	7			
61	-	Compo	und	Fugitive	gram/s	kg/hr	MT/yr	lb/hr	ton/yr	%	gram/s	kg/hr	MT/yr	1b/hr	0.109	1			
62	-	Benzene		HAP	0.0025	0.009	0.079	0.020	0.087	ļ	0.0031	0.011	0.099	0.025		<b>⊣</b>			
63 64	┥	Toluene		HAP	0.0067	0.024	0.211	0.053	0.233	1	0.0084	0.030	0.264	0.083					
65	-1	Xylenes		HAP	0.0084	0.030	0.264	0.067	0.291	4	0.0105	0.000		0.001	0.004	[			
66	-1	Phenois		HAP	0.0001	0.000	0.003	0.001	0.003	-	0.0001	0.000	0.003	0.002		7			
67	7	o-cresol		HAP	0.0002	0.001	0.006	0.002	0.007	25%	0.0003	0.000		0.001		<b></b>			
68		m+p-cre		HAP	0.0001	0.000	0.003	0.001	0.003	1 27	0.0083	0.030							
69		n-hexan	е	HAP	0.0067	0.024	0.211	0.053	0.232	1	5,000				-	_			
70	_					<del> </del>		<del> </del>	<u> </u>	1						-1			
71					<del> </del>	<del> </del>	<del>                                     </del>			]					+	-1			
72	_				1	+										100			
73	-1	-	***	≖ HAP	0.025	0.089	0,777	0.196	0,856		9.031	0,111	0.971	0.244	1.071				
	1		SHARESTEEN	000 TO VIEW TO A STREET TO	A AND DESCRIPTION OF THE PARTY										Page 1				
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1	<b>Emissions Summary</b>
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mission Factor Set Use	d :	TCEQ-R	lefining -					Equipment Design Control	LDAR Program Control Efficiency	Overall Fugitive Control Efficiency	Contingency		Controlled Fugit	ive Emissions		
		Em, Factor	Equipment	U	ncontrolled Fug	gitive Emission:		Efficiency	Entitleticy	Linetenoy	B/	kg/hr	MT/vr	lb/hr	ton/yr	Remarks
ugitive Emission Source	Service	kg/hr	Counts	kg/hr	MT/yr	lb/hr	ton/yr	%	%	%	70	0.04163	0.36470	0.09178	0.40200	Streams with vapor pressure less than 0.002 psla @ 68 degF are excluded from fugitive evaluations
	Gas	0.0268	3	0.08	0.70	0,18	0.78	0	97	97	50%		0.09155	0.02304	0.10092	Final valve counts have most uncertainty until P&ID's are available in later engineering phases.
lives		0.0208	32	0.35	3.05	0,77	3,36	0	97	97	50%	0.01045		0.11016	0.48250	
	Light Liquid	0.0109	153	1.67	14.59	3.67	16.08	0	97	97	50%	0.04997	0.43772		0.71690	Double Mechanical Seals per API Seal Plans provided on all LL & HL pumps due to process conditions
	Heavy Liquid		,33	2.05	17.95	4,52	19.79	80	85	97	0%	0.07424	0.65037	0.16368	1.18681	Double tree details
imps	Light Liquid	0.1139	18	0.40	3.47	0,87	3,83	80	0	80	0%	0.12291	1,07667	0,27096	1,18061	Reactor and other large vessel flanges are welded due to high process pressures
cludes Vessel Agitators)	Heavy Liquid	0.0209	19		2.26	0.57	2.50	0	30	30	25%	0.30599	2.68044	0.67458		Reactor and other large vesses number
inges / Connectors	All	0.00025	1036	0.26			64.21	100	97	100	15%	0.00000	0,00000	0.00000	0.00000	
essure Relief Valves	Gas	0.3500	19	6.65	58.25	14.66	304.17	100	n	100	15%	0.00000	0.00000	0.00000	0.00000	
	Liquids	0,3500	90	31,50	275.94	69.44		100	85	100		0.00000	0.00000	0.00000	0.00000	Venting controlled by flare
ompressors	All	1,3990	1	1.40	12.26	3.08	13.51		85	100		0.00000	0,00000	0,00000	0.00000	Capped, biinded, or double block primary design.
pen-Ended Lines/Valves	Ali	0.00510	90	0.46	4.02	1,01	4.43	100		100		0.00000	0.00000	0.00000	0.00000	Closed loop system designs used
	All	0.03300	205	6.77	59.26	14,91	65.32	100	85	100		0.00000	0.00000	0.00000	0.00000	
ampling Connections		0.00025	0	0.00	0.00	0.00	0.00	. 0	0	0	15%	1,49479	13.09438	3,29542	14,43393	50% of Drains are hardpiped with 100% control efficiency (entered as Secondary Efficiency)
onnectors - Miscellaneous	All	0.02917	205	5.98	52.38	13.18	57.74	50	50	75				0.00000	0.00000	
rains	All		200	0.00	0.00	0.00	0.00	0	0	0	15%	0.00000	0.00000		0.00000	
thers		0.00000	- 0	0.00	0.00	0,00	0.00	0	0	0	15%	0.00000	0.00000	0,00000		
O&G Others - Gas/Vapor	All	000000,0	0		0.00	0.00	0.00	0	0	0	15%	0,00000	0.00000	0,00000	0.00000	
O&G Others - Liquid	All	0,0000,0	0	0.00			655,72					2,100	18.396	4.630	20.278	
		Totals =	1871	57.55	504.14	125.88	230.72									

							Contingency		1	MThe	lb/hr	ton/yr
A	Fugitive	gram/s	kg/hr	MT/vr	lb/hr	ton/yr	%	gram/s	kg/hr	MT/yr		
Compound			0.009	0.079	0.020	0.087		0.0031	0.011	0.099	0.025	0.109
Benzene	HAP	0.0025			0.053	0.233	1	0.0084	0.030	0.264	0.066	0.291
Toluene	HAP	0.0067	0,024	0.211			1 !	0.0105	0,038	0.330	0.083	0.364
Xylenes	HAP	0.0084	0.030	0.264	0.067	0.291	-[	0.0001	0.000	0.003	0.001	0.004
Phenois	HAP	0.0001	0.000	0.003	0.001	0.003	4			0.008	0.002	0.009
o-cresol	HAP	0.0002	0.001	0.006	0,002	0.007	1	0.0003	0.001		0.002	0.004
	HAP	0.0001	0.000	0.003	0.001	0.003	25%	0.0001	0.000	0.003		
m+p-cresol		0.0067	0.024	0.211	0.053	0.232	1	0.0083	0.030	0.263	0.066	0.290
n-hexane	HAP	0.0067	0.024	U.E.I.I	5.000		1					<u> </u>
							1					
							-					
		1					-	<b></b>				<u> </u>
							ļ <u> </u>	21.10.00 AND MARKET STATES	and the second second	0.971	0.244	1.07
Alexander	Sum = HAP	0.025	0.089	0,777	0,196	0,856	8	0.031	9,313	0.211		
Same	Sum of hear	A PROCESSION OF THE PARTY OF THE	4 Northment Invanto (1995) Annual	Practice of the last								Pane 1

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## FUGITIVE AIR EMISSION INVENTORY CALCULATIONS

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	DOC. NO.: H102-4000-EV-CAL-EV2-0002	Rev:	A	0	1	2	3	- 4
JOB NO.: H102	SUBJECT: Piping and Equipment Fugitives	Date:	8-Jan-18	23-Jan-18				
CLIENT: Riverview Energy Corporation		By:	RN	RN				ļ
PROJECT: DCH Facility	BASIS: Reference & PFD Factored Equipment	Check:	SAL	SAL				
LOCATION: Date, IN								Ì
UNIT: Offsites Product Storage and Handling		Anpr.:	IFI.	1FI				
UNIT No. 4000		Purpose:	1151					

UNIT No.	4000							rpose:						*****************		25000000000000000000000000000000000000			
ECONOMIC EDITOR	on George States	5 5 2 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5							PROJE	CT DEFINITION			3/3/1-1/4 6/3/3/3/1-1/3/9/4/3/3/3/3/3/3/3/3/3/3/3/3/3/3/3/3/3		100 mm 100 mm 100 mm 100 mm 100 mm 100 mm 100 mm 100 mm 100 mm 100 mm 100 mm 100 mm 100 mm 100 mm 100 mm 100 mm			**************************************	
LINE REV	E EFFESTERSES		KOLEKRONOPARBANYNE XIDENERE	CONTRACTOR SERVICES											ច្រ	M Coordinates	for Process Ur	eit	
1	-  <sub> 1-1-</sub>	!am I link					SHADING LE	GEND:	ENTRY	LINKED	CALC C	OAL SEEK	CHECK 38	SUM			asting (m) N		l
2	A REVISION	ion Histo	tial Setup for Checking												<b>⊢</b>	orner 1			ļ
3	1 6		C PFD Basis, MatBal S	reams Aggreg	ated											orner 2			1
4	-  ĭ	100	KC I T D Dasis, Matca. C	. oa											ļ	orner 3			ļ
5	- '2														<b>—</b>	orner 4			1
6 7	3														-	orner 5			ļ
8	-  ŭ														-	orner 6			
	-{ `															orner 7			-
9 10	┪															omer 8			
11	TABLE	E OF CO	ONTENTS												L				
12	SECTIO		LINE DESCRIPTION																
13	1 32016		35 Emissions S																
14	- '2		60 Speciated E	missions Sun	nmary														
15	$-\frac{1}{3}$		79 Federal Ren	ulatory Applie	cability - Eval	uation Basis	Remarks												
16	<b>−</b>   4		141 Reference F	mission Fact	ors for Piping	Component	t Types in Inc	lustrial Secto	ors										
17	5		204 Reference F	rimary Contro	ol Credit % fo	r Equipment	Design Spec	ifications											
18	6		asa Bafaranca S	econdary Co	ntrol Credit %	for LDAR P	rograms		I DAD D-A	me									
19	7	,	277 Evaluation	Basis (Emissi	on Factors, E	quipment De	esign Specific	anons, and	LUAR FIUGIC	mið									
20	8	1	327 Available M	aterial Balanc	e Data Input														
21	9	)		Data for Adjus		Balance													
22	10	0	420 Adjusted M	aterial Balanc	e	6 Dec	Arose Ac No	hoha											
23	11		464 Material Ba	ance Stream	Aggregation	IOI PIOCESS I	nicas • Mə iki İlity Determin	ations											
24	12		529 Process St	eam or Area s uipment Cour	ste and Facts	rina Raeie II	n lieu of Dire	ct P&ID Cour	ıt										
25	13		595 Fugitive Eq	urpment Cour	RS and Pacto Evaluated	1111y pasis, 11	., 1104 01 0116												
26	14		712 Final Equip	ment Counts iated Fugitive	Evaluated Emissions (s	s VOCI Bac	ed Upon Initi	al Source Co	unt Totals										
27	15		762 Undifferent	iated Fugitive Fugitive Emis	cione by For	inment Type	Process Str	eam or Area											
28	16		816 Controlled	rugitive Emis Fugitive Emiss	sions by Equ	ess Stream	or Area												
29	17			ugilive Enils:	Sions by 1 100	coo otroum													
30	18	8	926 NOTES																
31																			
32																			
33	┪																		
34 35	┦ 1	1 F	missions Summary							r	Primary	Secondary		ı					
36							_				Equipment	LDAR	Overall						
37		Œ	mission Factor Set Us	ed:	TCEQ-R	efining					Design	Program	Fugitive						
38					A														
											Control	Control	Control	Contingency		Controlled Fugi	itive Emissions		
					Em. Factor	Equipment	υ	ncontrolled Fug			Efficiency	Efficiency	Efficiency	Contingency %		Controlled Fugi	tive Emissions Ib/hr	ton/yr	
39		F	ugitive Emission Source	Service	Em. Factor kg/hr	Equipment Counts	kg/hr	MT/yr	lb/hr	ton/yr	Efficiency %	Efficiency %	Efficiency %	%	kg/hr				Streams with
39 40		_ <b>⊢</b>		Service Gas	4 3		kg/hr 0.00	MT/yr 0,00	lb/hr 0.00	ton/yr 0.00	Efficiency % 0	Efficiency % 97	Efficiency % 97	% 50%		MT/yr	lb/hr	0,00000 0,10722	
39 40 41		_ <b>⊢</b>	ugitive Emission Source /alves	Gas Light Liquid	kg/hr 0.0268 0.0109	Counts 0 34	kg/hr 0.00 0.37	MT/yr 0.00 3.24	ib/hr 0.00 0.82	0.00 3.57	Efficiency % 0	# 97 97	Efficiency %	%	kg/hr 0.00000	MT/yr 0.00000	1b/hr 0.00000	0.00000 0.10722 0.00000	Final valve o
39 40		_ <b>⊢</b>		Gas	kg/hr 0.0268 0.0109 0.0109	Counts 0 34 0	kg/hr 0.00 0.37 0.00	MT/yr 0.00 3.24 0.00	1b/hr 0.00 0.82 0.00	0.00 3.57 0.00	Efficiency % 0 0	# 97 97 97 97	### Efficiency	% 50% 50%	kg/hr 0.00000 0.01110	MT/yr 0.00000 0.09727	1b/hr 0.00000 0.02448 0.00000 0.03289	0.00000 0.10722 0.00000 0.14404	Final valve o
39 40 41 42		<u>V</u>	/alves	Gas Light Liquid Heavy Liquid Light Liquid	kg/hr 0.0268 0.0109 0.0109 0.1139	0 34 0 4	kg/hr 0.00 0.37 0.00 0.46	MT/yr 0.00 3.24 0.00 3.99	0.00 0.82 0.00 1.00	0.00 3.57 0.00 4.40	% 0 0 0 80	# 97 97	### 97 97	% 50% 50% 50%	0.00000 0.01110 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000	ton/yr 0.00000 0.10722 0.00000 0.14404 0.00000	Final valve o
39 40 41 42 43		<u>V</u>	/alves	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209	0 34 0 4 0	kg/hr 0.00 0.37 0.00 0.46 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00	0.00 0.82 0.00 1.00 0.00	0.00 3.57 0.00 4.40 0.00	% 0 0 0 80	97 97 97 97 85	### 87 97 97 97 97	% 50% 50% 50% 0%	kg/hr 0.00000 0.01110 0.00000 0.01492	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110	0.00000 0.02448 0.00000 0.03289 0.00000 0.07074	ton/yr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986	Final valve o
39 40 41 42 43 44		<u>v</u> F ()	/alives  Pumps (Includes Vessel Agitators) Flanges / Connectors	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025	0 34 0 4 0 141	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31	0.00 0.82 0.00 1.00 0.00	0.00 3.57 0.00 4.40 0.00 0.34	% 0 0 0 80 80	97 97 97 97 85 0	% 97 97 97 97 80	% 50% 50% 50% 0%	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03208 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110	0.00000 0.02448 0.00000 0.03289 0.00000 0.07074	ton/yr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000	Final valve o
39 40 41 42 43 44 45		<u>v</u> F ()	/alves Pumps (Includes Vessel Agitators)	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500	0 34 0 4 0 141 0	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00	0.00 0.82 0.00 1.00 0.00 0.00	0.00 3.57 0.00 4.40 0.00 0.34	% 0 0 0 80	97 97 97 97 85	% 97 97 97 97 80 30	% 50% 50% 50% 0% 0% 25%	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03208 0.00000 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000	ton/yr 0,00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000	Double Med
39 40 41 42 43 44 45 46		V	/alves  Pumps (Includes Vessel Agitators) Flanges / Connectors  Pressure Relief Valves	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid Heavy Liquid All Gas Liquids	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500	0 34 0 4 0 141 0 0 0 0 0	kg/hr 9.00 0.37 9.00 0.46 0.00 0.04 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00	1b/hr 0.00 0.82 0.00 1.00 0.00 0.08 0.00	0.00 3.57 0.00 4.40 0.00 0.34	### Efficiency  ### 0  0  0  0  80  80  100	97 97 97 97 97 85 0	97 97 97 97 97 97 80 30	% 50% 50% 50% 0% 0% 25% 15% 15%	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000	ton/yr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000	Double Med Reactor and Venting con
39 40 41 42 43 44 45 46 47 48 49		V	/alves  Pumps (Includes Vessel Agitators) Flanges / Connectors  Pressure Relief Valves  Compressors	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid Heavy Liquid All Gas Liquids All	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 1.3990	Counts  0 34 0 4 0 141 0 0 3	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 4.20	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77	1b/hr 0.00 0.82 0.00 1.00 0.00 0.08 0.00 0.00 9.25	0.00 3.57 0.00 4.40 0.00 0.34 0.00	% 0 0 0 0 80 80 100	97 97 97 97 85 0 30	97 97 97 97 97 97 100 100 100 100	% 50% 50% 50% 0% 0% 25% 15% 15% 15%	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000 0.00000 0.000000 0.000000 0.000000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000	Double Med Reactor and Venting con Capped, bil
39 40 41 42 43 44 45 46 47 48 49 50		V   F   F   C   C   C   C   C   C   C   C	/alves  Pumps (Includes Vessel Agitators) Flanges / Connectors  Pressure Relief Valves  Compressors  Open-Ended Lines/Valves	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 1.3990 0.00510	Counts  0 34 0 4 0 141 0 0 34	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.04 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18	1b/hr 0.00 0.82 0.00 1.00 0.00 0.08 0.00	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53	## Efficiency    %   0   0   0     0   0   80     80   0   100     100   100	### Efficiency ###  97  97  97  85  0  30  97  0  85	97 97 97 97 97 80 30 100 100 100 100	% 50% 50% 50% 0% 0% 25% 15% 15% 15%	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000	ton/yr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med Reactor and Venting con Capped, bil
39 40 41 42 43 44 45 46 47 48 49 50 51			Jalves  Pumps Includes Vessel Agitators) Flanges / Connectors  Pressure Relief Valves  Compressors  Open-Ended Lines/Valves  Sampling Connections	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 1.3990 0.00510 0.03300	Counts  0 34 0 4 0 141 0 0 3 4 8	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 0.00 36.77 0.18 2.31	1b/hr 0.00 0.82 0.00 1.00 0.00 0.08 0.00 0.00 9.25	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20	## Efficiency  %  0  0  0  80  80  100  100  100  100	### Efficiency ### 97 97 97 97 85 0 30 97 0 85 85	97 97 97 97 97 80 30 100 100 100 100 0	% 50% 50% 50% 0% 0% 25% 15% 15% 15% 15% 15%	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0,00000 0,10722 0,00000 0,14404 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Double Med Reactor and Venting con Capped, bit
39 40 41 42 43 44 45 46 47 48 49 50 51			Jalves  Pumps Includes Vessel Agitators) Flanges / Connectors  Pressure Relief Valves  Compressors  Open-Ended Lines/Valves  Sampling Connections  Connectors - Miscellaneou	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid Heavy Liquid All Gas Liquids All All All All	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 1.3990 0.000510 0.03300 0.00025	Counts  0 34 0 4 0 141 0 0 34 8 0 0	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 4.20 0.02 0.02	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 3.6.77 0.18 2.31 0.00	1b/hr 0.00 0.82 0.00 1.00 0.00 0.08 0.00 0.00 0.00 9.25 0.04	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55	## Efficiency    %   0   0   0   0   0   0   0   0   0	97 97 97 97 85 0 30 97 0 85 0 0	### Efficiency    97	% 50% 50% 50% 0% 0% 25% 15% 15% 15% 15% 15%	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03288 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med Reactor and Venting con Capped, bit
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53			/alves  Pumps  Includes Vessel Agitators   Flanges / Connectors  Pressure Relief Valves     Compressors   Open-Ended Lines/Valves   Sampling Connections   Connectors - Miscellaneous   Drains	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 1.3990 0.00510 0.03300 0.0025	Counts  0 34 0 4 0 141 0 0 3 4 8 0 8	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 4.20 0.02 0.28 0.00 0.23	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 2.04	1b/hr 0.00 0.82 0.00 1.00 0.00 0.08 0.00 0.00 0.00 0.00	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00	## Efficiency	### Efficiency    97	### Efficiency ### 97 97 97 97 97 80 30 100 100 100 100 0 75	% 50% 50% 50% 0% 0% 25% 15% 15% 15% 15% 15%	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03208 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.9727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.12860 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med Reactor and Venting con Capped, bit
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54			/alves  Pumps (Includes Vessel Agitators) Flanges / Connectors  Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid Aul Gas Liquids All All All All	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 1.3990 0.00510 0.03300 0.00025 0.00025	Counts  0 34 0 4 0 141 0 0 33 4 8 0 8 0 0 8	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 4.20 0.02 0.02	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 3.6.77 0.18 2.31 0.00	1b/hr 0.00 0.82 0.00 1.00 0.00 0.00 0.00 0.00 0.00 0.0	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.25	## Efficiency    %   0   0   0   0   0   0   0   0   0	### Efficiency ### 97 97 97 97 85 0 30 97 0 85 85 85 0 0 0 0 0 0 0	### Efficiency    97	% 50% 50% 50% 0% 0% 25% 15% 15% 15% 15% 15% 15% 15%	kg/hr 0.00000 0.01110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.12860 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med  Reactor and  Venting con Capped, bill Closed loop
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54			Pumps Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Okhers O&G Others - Gas/Vapor	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 1.3500 0.00510 0.03300 0.00257 0.002917	Counts  0 34 0 4 0 141 0 0 3 4 8 0 8	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.04 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 2.04	ib/hr 0.00 0.82 0.00 1.00 0.00 0.08 0.00 0.00 0.00 0.00	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 4.953 0.20 2.55 0.00 2.25 0.00 0.00	## Efficiency    %   0   0     80   80     0   100     100   100     100   100     50   0	97 97 97 97 85 0 30 97 85 0 30 97 0 85	### Efficiency    97	% 50% 50% 50% 0% 0% 25% 15% 15% 15% 15% 15% 15% 15%	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med  Reactor and  Venting con Capped, bill Closed loop
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55			/alves  Pumps (Includes Vessel Agitators) Flanges / Connectors  Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid Aul Gas Liquids All All All All	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 0.3500 0.00510 0.03300 0.0025 0.02917 0.00000	Counts  0 34 0 4 0 1441 0 3 3 4 8 0 6 0 0 0 0 0 0 0 0 0	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 2.04 0.00	1b/hr 0.00 0.82 0.00 1.00 0.00 0.08 0.00 0.00 9.25 0.04 0.58 0.00 0.51 0.00	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 0.00	## Efficiency    %   0   0   0   0   0   0   0   0   0	### Efficiency ### 97 97 97 97 85 0 30 97 0 85 85 85 0 0 0 0 0 0 0	### Efficiency    97	% 50% 50% 50% 0% 0% 25% 15% 15% 15% 15% 15% 15% 15%	kg/hr 0.00000 0.01110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.12860 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med  Reactor and  Venting con Capped, bill Closed loop
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 64 55 56			Pumps Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Okhers O&G Others - Gas/Vapor	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 1.3500 0.00510 0.03300 0.00257 0.002917	Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 0 0 0 0 0 0	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 38.77 0.18 2.31 0.00 2.04 0.00 0.00	1b/hr 0.00 0.82 0.00 1.00 0.00 0.00 0.00 0.00 0.00 0.0	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 4.953 0.20 2.55 0.00 2.25 0.00 0.00	## Efficiency    %   0   0   0   0   0   0   0   0   0	### Efficiency ### 97 97 97 97 85 0 30 97 0 85 85 85 0 0 0 0 0 0 0	### Efficiency    97	% 50% 50% 50% 0% 0% 25% 15% 15% 15% 15% 15% 15% 15%	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med  Reactor and  Venting con Capped, bill Closed loop
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57			Pumps Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Okhers O&G Others - Gas/Vapor	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid Heavy Liquid All Gas Liquids All All All All All All All	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 0.3500 0.00510 0.03300 0.0025 0.02917 0.00000	Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 0 0 0 0 0 0	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 38.77 0.18 2.31 0.00 2.04 0.00 0.00	1b/hr 0.00 0.82 0.00 1.00 0.00 0.00 0.00 0.00 0.00 0.0	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 4.953 0.20 2.55 0.00 2.25 0.00 0.00	## Efficiency    %   0   0   0   0   0   0   0   0   0	### Efficiency ### 97 97 97 97 85 0 30 97 0 85 85 85 0 0 0 0 0 0 0	### Efficiency    97	% 50% 50% 50% 0% 0% 25% 15% 15% 15% 15% 15% 15% 15%	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med  Reactor and  Venting con Capped, bill Closed loop
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 64 55 56 57 58 59			Jalves  Pumps Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Okhers O&G Others - Gas/Vapor O&G Others - Liquid	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 0.3500 0.00510 0.03300 0.0025 0.02917 0.00000	Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 0 0 0 0 0 0	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 38.77 0.18 2.31 0.00 2.04 0.00 0.00	1b/hr 0.00 0.82 0.00 1.00 0.00 0.00 0.00 0.00 0.00 0.0	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 0.00 0.00 53.84	## Efficiency    %	### Efficiency ### 97 97 97 97 85 0 30 97 0 85 85 85 0 0 0 0 0 0 0	### Efficiency    97	% 50% 50% 50% 0% 0% 25% 15% 15% 15% 15% 15% 15% 15%	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med  Reactor and  Venting con Capped, bill Closed loop
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58			Pumps Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Okhers O&G Others - Gas/Vapor	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 0.3500 0.00510 0.03300 0.0025 0.02917 0.00000	Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 0 0 0 0 0 0	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 38.77 0.18 2.31 0.00 2.04 0.00 0.00	1b/hr 0.00 0.82 0.00 1.00 0.00 0.00 0.08 0.00 0.00 0.00	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 0.00 0.00	## Efficiency    %	### Efficiency % 97 97 97 97 85 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	### Efficiency ### 97 97 97 97 97 80 30 100 100 100 100 0 75 0 0 0	% 50% 50% 50% 0% 0% 25% 15% 15% 15% 15% 15% 15% 15% 15%	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03208 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med  Reactor and  Venting con Capped, bill Closed loop
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61			Jalves  Pumps Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions \$	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All All Al	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 0.3500 0.00510 0.03300 0.0025 0.02917 0.00000	Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 0 0 0 0 0 0	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 0.01 2.01 0.00 0.00 0.00 0.0	1b/hr 0.00 0.82 0.00 1.00 0.00 0.00 0.00 0.00 0.00 0.0	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 0.00 0.00 53.84	## Efficiency    %   0   0   0   0   0   0   0   0   0	### Efficiency  ### ### ### ### ### ### ### ### ###	### Efficiency ### 97 97 97 97 97 80 30 100 100 100 100 0 75 0 0 MT/yr	% 50% 50% 50% 0% 0% 0% 15% 15% 15% 15% 15% 15% 15% 15% 15%	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med  Reactor and  Venting con Capped, bill Closed loop
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62			Jalves  Pumps Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneou Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions S Compound	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All Figure All All Figure Figure Fugitive	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 0.3500 0.00510 0.00300 0.00025 0.02917 0.00000 0.00000	Counts  0 34 0 4 0 1441 0 0 33 4 8 0 0 8 0 0 202	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 2.04 0.00 0.00 48.84	ib/hr 0.00 0.82 0.00 1.00 0.08 0.00 0.00 0.00 0.00 0.01 0.00 0.00	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 0.00 0.00	## Efficiency    %   0   0   0   0   0   0   0   0   0	### Efficiency ###  97  97  97  85  0  30  97  0  85  85  85  85  0  0  0  0  0  0  kg/hr  0.001	### Efficiency ### 97 97 97 97 97 80 30 100 100 100 100 0 75 0 0 MT/yr 0.009	% 50% 50% 50% 0% 0% 0% 25% 15% 15% 15% 15% 15% 15% 15% 15% 15% 1	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med  Reactor and  Venting con Capped, bill Closed loop
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 64 55 66 57 58 59 60 61 61 62 63			Jalves  Pumps Includes Vessel Agitators) Flanges / Connectors  Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions \$ Compound Benzene	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All All Al	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 0.3500 0.00510 0.003300 0.00025 0.02917 0.00000 0.00000 0.000000 Totals	Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 0 202	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 0.00 0.00 48.84	Ib/hr	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 0.00 0.00	### Efficiency    %   0   0   0   0   0   0   0   0   0	### Efficiency   97	### Efficiency   97   97   97   97   97   97   97   97	% 50% 50% 50% 50% 0% 0% 0% 25% 15% 15% 15% 15% 15% 15% 15% 15% 15% 1	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000	MT/yr 0.00000 0.9727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med  Reactor and  Venting con Capped, bill Closed loop
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 64 55 66 57 58 59 60 61 62 63 64			Jalves  Pumps  Includes Vessel Agitators   Includes Vessel Agitators   Includes Vessel Agitators   Includes Vessel Agitators   Includes Vessel Agitators   Includes Vessel Agitators   Includes Vessel Agitators   Includes Includes Vessel Agitators   Includes Includes Vessel Agitators   Includes Includes Includes Vessel Agitators   Includes Includes Vessel Agitators   Includes Includes Includes Vessel Agitators   Includes Includes Vessel Agitators   Includes In	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All All Al	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 1.3990 0.00510 0.03300 0.00025 0.02917 0.00000 0.00000 Totals	Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 8 0 202	kg/hr 0.00 0.37 0.00 0.46 0.00 0.00 0.00 4.20 0.02 0.02 0.02 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 2.04 0.00 0.00 48.84	1b/hr 0.00 0.82 0.00 1.00 0.08 0.00 0.00 0.00 0.00 0.05 0.00 0.51 0.00 0.00	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 0.00 0.00	### Efficiency    %   0   0   0   0   0   0   0   0   0	### Efficiency    97	### Efficiency   97   97   97   97   97   97   97   80   30   100   100   100   100   100   0   75   0   0   0   0   0   0   0   0   0	% 50% 50% 50% 0% 0% 0% 25% 15% 15% 15% 15% 15% 15% 15% 15% 0.002 0.002	kg/hr 0.00000 0.01110 0.001192 0.00000	MT/yr 0.00000 0.9727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med  Reactor and  Venting con Capped, bill Closed loop
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 64 55 66 57 58 59 60 61 62 63 64 65			Jalves  Pumps Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions S  Compound Benzene Toluene Xylenes	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All All Al	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 1.3990 0.00510 0.03300 0.00025 0.00000 0.00000 Totals:	Counts  0 34 0 4 0 1441 0 0 3 4 8 0 0 8 0 0 202	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 4.20 0.02 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 2.04 0.00 0.00 48.84	Ib/hr	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 0.00 0.00	### Efficiency    %   0   0   0   0   0   0   0   0   0	### Efficiency   %   97     97     97     97     85     0     85     85     85     0     0     0     0     kg/hr     0.001     0.003     0.004     0.004     0.000	### Efficiency ### 97 97 97 97 97 80 30 100 100 100 100 0 0 75 0 0  MT/yr 0.009 0.025 0.031	% 50% 50% 50% 60% 0% 0% 0% 25% 15% 15% 15% 15% 15% 15% 15% 0.002 0.002 0.008	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03208 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.05833 0.00000 0.00000 0.05833 0.00000 0.00000 0.05833 0.00000 0.00000 0.05833	MT/yr 0.00000 0.9727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med  Reactor and  Venting con Capped, bill Closed loop
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62 63 64 65 66			Jalves  Pumps Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions S  Compound Benzene Toluene Xylenes Phenols	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All Hall All All All All All All All All All	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 1.3500 0.00510 0.03300 0.00510 0.02917 0.00000 0.00000 Totals=	Counts  0 34 0 4 0 1441 0 3 3 4 8 0 0 8 0 202 8 kg/hr 0,001 0,002	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.36.77 0.18 2.31 0.00 2.04 0.00 0.00 48.84	Ib/hr	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 3.84	### Efficiency    %	### Efficiency ### 97 97 97 97 85 0 30 97 0 85 85 85 0 0 0 0 0 0 0 0 0 0 0 0 0 0	### Efficiency   97   97   97   97   97   80   80   80   80   80   80   80   8	% 50% 50% 50% 0% 0% 0% 15% 15% 15% 15% 15% 15% 15% 15% 0.002 0.008 0.000	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med Reactor and Venting con Capped, bit
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 66 67			Jalves  Pumps Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneou Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions S  Compound Benzene Toluene Xylenes Phenols o-cresol	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All Hand All All All All All All All All All Al	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 0.00510 0.00300 0.00025 0.02917 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Counts  0 34 0 4 0 1441 0 3 3 4 8 0 0 8 0 0 2002	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.02 0.02 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 0.00 0.00 0.00 48.84	Ib/hr	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 0.00 0.00	### Company   Co	### Efficiency %  97  97  97  85  0  30  97  0  85  85  85  0  0  0  0  0  0    kg/hr  0.001  0.003  0.004  0.0000  0.0000  0.0000	### ##################################	% 50% 50% 50% 0% 0% 0% 0% 15% 15% 15% 15% 15% 15% 15% 10% 10% 10% 10% 10% 10% 10% 10% 10% 10	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 1.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med Reactor and Venting con Capped, bit
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 66 67 68			Jalves  Pumps Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions S  Compound Benzene Toluene Xylenes Phenols	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All All Al	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 0.3500 0.00510 0.00300 0.00025 0.02917 0.00000 0.00000 Totals 0.0002 0.00002 0.00002 0.00000 0.00000 0.00000 0.00000	Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 0 202  kg/hr 0,001 0,002 0,003 0,000	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.36.77 0.18 2.31 0.00 2.04 0.00 0.00 48.84	Ib/hr	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 3.84	### Efficiency    %	### Efficiency %  97  97  97  85  0  30  97  0  85  85  85  0  0  0  0  0  0    kg/hr  0.001  0.003  0.004  0.0000  0.0000  0.0000	### Efficiency   97   97   97   97   97   80   80   80   80   80   80   80   8	% 50% 50% 50% 0% 0% 0% 0% 15% 15% 15% 15% 15% 15% 15% 10% 10% 10% 10% 10% 10% 10% 10% 10% 10	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 1.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med Reactor and Venting con Capped, bit
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 64 55 66 67 68 67 68 69			Jalves  Pumps Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions S  Compound Benzene Toluene Xylenes Phenols O-cresol m+p-cresol	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All All Al	kg/hr   0.0268   0.0108   0.0109   0.1139   0.0209   0.00025   0.3500   1.3990   0.00510   0.00510   0.00000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.00000	Counts  0 34 0 4 0 141 0 0 33 4 8 0 8 0 0 202  kg/hr 0,001 0,002 0,000 0,000 0,000	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 0.00 0.00 0.00 48.84	Ib/hr	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 3.84	### Company   Co	### Efficiency %  97  97  97  85  0  30  97  0  85  85  85  0  0  0  0  0  0    kg/hr  0.001  0.003  0.004  0.0000  0.0000  0.0000	### ##################################	% 50% 50% 50% 0% 0% 0% 0% 15% 15% 15% 15% 15% 15% 15% 10% 10% 10% 10% 10% 10% 10% 10% 10% 10	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 1.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med Reactor and Venting con Capped, bit
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 64 55 66 67 68 65 66 67 68 69 70			Jalves  Pumps Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions S  Compound Benzene Toluene Xylenes Phenols O-cresol m+p-cresol	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All All Al	kg/hr   0.0268   0.0108   0.0109   0.1139   0.0209   0.00025   0.3500   1.3990   0.00510   0.00510   0.00000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.00000	Counts  0 34 0 4 0 141 0 0 33 4 8 0 8 0 0 202  kg/hr 0,001 0,002 0,000 0,000 0,000	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 0.00 0.00 0.00 48.84	Ib/hr	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 3.84	### Company   Co	### Efficiency %  97  97  97  85  0  30  97  0  85  85  85  0  0  0  0  0  0    kg/hr  0.001  0.003  0.004  0.0000  0.0000  0.0000	### ##################################	% 50% 50% 50% 0% 0% 0% 0% 15% 15% 15% 15% 15% 15% 15% 10% 10% 10% 10% 10% 10% 10% 10% 10% 10	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 1.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med Reactor and Venting con Capped, bit
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 67 68 69 67 68 69 70 71			Jalves  Pumps Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions S  Compound Benzene Toluene Xylenes Phenols O-cresol m+p-cresol	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All All Al	kg/hr   0.0268   0.0108   0.0109   0.1139   0.0209   0.00025   0.3500   1.3990   0.00510   0.00510   0.00000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.00000	Counts  0 34 0 4 0 141 0 0 33 4 8 0 8 0 0 202  kg/hr 0,001 0,002 0,000 0,000 0,000	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 0.00 0.00 0.00 48.84	Ib/hr	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 3.84	### Company   Co	### Efficiency %  97  97  97  85  0  30  97  0  85  85  85  0  0  0  0  0  0    kg/hr  0.001  0.003  0.004  0.0000  0.0000  0.0000	### ##################################	% 50% 50% 50% 0% 0% 0% 0% 15% 15% 15% 15% 15% 15% 15% 10% 10% 10% 10% 10% 10% 10% 10% 10% 10	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 1.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Double Med  Reactor and  Venting con Capped, bill Closed loop
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 64 55 66 67 68 69 70 71 72			Jalves Pumps Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Okhers O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions S Compound Benzene Toluene Xylenes Phenols O-cresol m+p-cresol n-hexane	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All All Al	kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 1.3990 0.00510 0.03300 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Counts  0 34 0 4 0 141 0 0 3 4 8 0 8 0 0 8 0 0 0 0 0 0 0 0 0 0 0 0 0	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.02 0.02 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 2.04 0.00 0.00 0.00 0.00 0.00 0.00	Ib/hr	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 0.00 0.00 33.84	### Efficiency   %   0   0   0   0   0   0   0   0   0	### Efficiency %  97 97 97 97 85 0 30 97 0 85 85 85 85 0 0 0 0 0 0 0 0 0 0 0 0 0	### Efficiency % 97 97 97 97 80 30 100 100 100 100 0 75 0 0 0  ####  MT/yr 0.009 0.025 0.031 0.000 0.0001	% 50% 50% 50% 0% 0% 0% 25% 15% 15% 15% 15% 15% 15% 15% 0.002 0.006 0.008 0.000 0.000	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000	MT/yr 0.00000 0.9727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 1.5026	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Streams with Final valve of Double Medical Reactor and Venting con Capped, bit Closed loop 50% of Drain Capped (Control of Drain Capped) (Control of
39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 67 68 69 67 68 69 70 71			Jalves Pumps Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Okhers O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions S Compound Benzene Toluene Xylenes Phenols O-cresol m+p-cresol n-hexane	Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All All Al	kg/hr   0.0268   0.0108   0.0109   0.1139   0.0209   0.00025   0.3500   1.3990   0.00510   0.00510   0.00000   0.0000   0.0000   0.0000   0.0000   0.0000   0.0000   0.00000	Counts  0 34 0 4 0 141 0 0 33 4 8 0 8 0 0 202  kg/hr 0,001 0,002 0,000 0,000 0,000	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.02 0.02 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 2.04 0.00 0.00 0.00 0.00 0.00 0.00	Ib/hr	ton/yr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 0.00 0.00 33.84	### Company   Co	### Efficiency %  97 97 97 97 85 0 30 97 0 85 85 85 85 0 0 0 0 0 0 0 0 0 0 0 0 0	### Efficiency % 97 97 97 97 80 30 100 100 100 100 0 75 0 0 0  ####  MT/yr 0.009 0.025 0.031 0.000 0.0001	% 50% 50% 50% 0% 0% 0% 25% 15% 15% 15% 15% 15% 15% 15% 0.002 0.006 0.008 0.000 0.000	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.151100 0.00000 0.00000 0.00000 0.10200	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	tonlyr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Final valve of Double Med Reactor and Venting con Capped, bill Closed loop

mission Factor Set Use	<u>"                                      </u>		Refining :				_	Design Control Efficiency	Program Control Efficiency	Control Efficiency	Contingency	(	Controlled Fugit			Remarks
		Em. Factor	Equipment	Ur		gitive Emission		Litioneries	0/	8/.	9%	kg/hr	MT/yr	lb/hr	ton/yr	
ugitive Emission Source	Service	kg/hr	Counts	kg/hr	MT/yr	lb/hr	ton/yr	%	70	70	50%	0.00000	0.00000	0.00000	0.00000	Streams with vapor pressure less than 0.002 psia @ 68 degF are excluded from fugitive evaluations
alves	Gas	0.0268	0	0.00	0.00	0.00	0.00	0_	97	97	50%	0.01110	0.09727	0.02448	0.10722	Final valve counts have most uncertainty until P&ID's are available in later engineering phases.
	Light Liquid	0.0109	34	0.37	3.24	0.82	3.57	0_	97	97	50%	0.00000	0.00000	0.00000	0.00000	and the second times
	Heavy Liquid	0.0109	0	0.00	0.00	0.00	0.00	0	85	97	0%	0.01492	0.13067	0.03289	0.14404	Double Mechanical Seals per API Seal Plans provided on all LL & HL pumps due to process conditions
umps	Light Liquid	0.1139	4	0.46	3.99	1.00	4.40	80	85	80	0%	0.00000	0.00000	0.00000	0.00000	
includes Vessel Agitators)	Heavy Liquid	0.0209	0	0.00	0.00	0.00	0.00	80	30	30	25%	0.03209	0,28110	0.07074	0.30986	Reactor and other large vessel flanges are welded due to high process pressures
langes / Connectors	AJI	0.00025	141	0.04	0.31	0,08	0.34	100	97	100	15%	0.00000	0.00000	0.00000	0.00000	ساري حملون بالمساور ال
ressure Relief Valves	Gas	0.3500	. 0	0.00	0.00	0.00	0.00	100	97	100		0.00000	0.00000	0.00000	0.00000	
	Liquids	0.3500	0	0.00	0.00	0.00	0.00	100	85	100		0.00000	0.00000	0.00000	0.00000	Venting controlled by flare
Compressors	All	1.3990	3	4.20	36.77	9.25	40.53 0.20	100	85	100	15%	0,00000	0.00000	0.00000	0.00000	Capped, biinded, or double block primary design.
Opeπ-Ended Lines/Valves	All	0.00510	4	0.02	0.18	0.04	2,55	100	85	100	15%	0.00000	0.00000	0.00000	0.00000	Closed loop system designs used
Sampling Connections	All	0.03300	8	0.26	2.31	0.58	0.00	100	0	0	15%	0.00000	0,00000	0.00000	0.00000	50% of Drains are hardpiped with 100% control efficiency (entered as Secondary Efficiency)
Connectors - Miscellaneous	All	0.00025	0	0.00	0.00	0,00 0,51	2.25	50	50	75	15%	0.05833	0.51100	0.12860	0.56328	50% of Drains are hardpiped with 100% control endertry (cited as 55
Orains	All	0.02917		0,23	2.04	0.00	0.00	1 0	0	0	15%	0.00000	0.00000	0.00000	0.00000	
Others		0.00000	0	0.00	0.00	0.00	0.00	0	0	0	15%	0.00000	0.00000	0.00000	0,00000	
O&G Others - Gas/Vapor	Ali	0.00000	0	0.00	0.00	0.00	0.00	0	0	0	15%	0.00000	0.00000	0.00000	0,00000	
O&G Others - Liquid	All	0.00000	0	0.00	0.00	12.29	53.84		1	-		0.116	1.020	0.257	1,124	
		Totals =	202	5,58	48.84	12.29	JJ.64									

						Contingency					
111		kalbe	MT/or	lb/hr	ton/vr	1 % [	gram/s	kg/hr	MT/yr	lb/hr	ton/yr
Fugitive							0.0003	0.001	0.009	0.002	0.01
HAP	0.0002	0.001				- I		0.003	0.025	0.006	0.02
HAP	0,0006	0.002	0.020			-					0.03
HAP	0.0008	0.003	0.025	0.006	0.027						0.00
	0.0000	0.000	0.000	0.000	0.000	ا ا	0.0000				0.00
			0.001	0.000	0.001	1 1	0.0000	0.000			
					0.000	25%	0.0000	0.000	0.000	0.000	0.00
HAP						1	0.0008	0.003	0.025	0.006	0.02
HAP	0.0006	0.002	0.020	0.005	0.022	-	0.000				
						-					
						4					
						]					
<del></del>	<del>                                     </del>					l	İ				250000000000000000000000000000000000000
	7.505	0.762	8.073	0.018	0,081		0,003	0.010	0,092	0,023	0.10
um =  HAP	B.VUZ	ลมขอ	W.414	222 X 400 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	22.00		- Annual Control				Page 1 of
	HAP HAP HAP HAP HAP HAP	HAP 0.0002 HAP 0.0006 HAP 0.0000 HAP 0.0000 HAP 0.0000 HAP 0.0000 HAP 0.0000 HAP 0.0000	HAP 0.0002 0.001 HAP 0.0006 0.002 HAP 0.0008 0.003 HAP 0.0000 0.000 HAP 0.0000 0.000 HAP 0.0000 0.000 HAP 0.0000 0.000 HAP 0.0000 0.000	HAP         0.0002         0.001         0.007           HAP         0.0008         0.002         0.020           HAP         0.0008         0.003         0.025           HAP         0.0000         0.000         0.000           HAP         0.0000         0.000         0.001           HAP         0.0000         0.000         0.000           HAP         0.0000         0.000         0.000           HAP         0.0006         0.002         0.020	HAP 0.0002 0.001 0.007 0.002  HAP 0.0006 0.002 0.020 0.020 0.005  HAP 0.0008 0.003 0.025 0.006  HAP 0.0000 0.000 0.000 0.000  HAP 0.0000 0.000 0.001 0.001  HAP 0.0000 0.000 0.001 0.001  HAP 0.0000 0.000 0.000 0.000  HAP 0.0000 0.000 0.000 0.000  HAP 0.0006 0.000 0.000 0.000	HAP 0.0002 0.001 0.007 0.002 0.008 HAP 0.0006 0.002 0.020 0.005 0.022 HAP 0.0008 0.003 0.025 0.006 0.027 HAP 0.0000 0.000 0.000 0.000 0.000 HAP 0.0000 0.000 0.001 0.000 0.001 HAP 0.0000 0.000 0.001 0.000 0.001 HAP 0.0000 0.000 0.001 0.000 0.001 HAP 0.0000 0.000 0.001 0.000 0.000 HAP 0.0000 0.000 0.001 0.000 0.000	HAP	HAP	HAP	HAP	HAP

# Table 19. CE-06. Organics - Flare/Oxidizer/Incinerator

Table 19a. Part A. Identification and Description of Control Equipment

1.Control	2.Installation Date:	3.Incineration Method:	4.Residence Time	5.Hood Static	6.Bed		8.ls the Gas	10 (4) (4) (4) (4) (4) (4) (4) (4) (4)	10.Are Flame	11.Are Steam Jets	12.How is the flare used?	13.Catalyst Material;	14.Number of Catalyst		16.ls a Heat Exchanger	17.Heat Exchanger
Equipment ID:				Pressure	Temperature at the Flame Zone		Stream used as Overfire Air?		Arrestors used?	used?			Beds:	Cleaned and reused on- site?	Hashiman di Bad	Type:
								NA	No	No	Safety Relief	None	NA	NA NA	No	NA
EU-4004	1Q2021	Flare	NA	NA	NA NA	Natural Gas Only		NA NA	No	No	Safety Relief	None	NA	NA	No	NA
EU-4002	1Q2021	Flare	NA NA	NA NA	NA NA	Natural Gas Only Natural Gas Only		NA NA	No	No	Safety Relief	None	NA	NA	No	NA
EU-4001	102021	Flare	NA NA	NA	IVA	Matarar das omy	1.1.				<u> </u>					

#### Table 19b. Operational Parameters

1.Control	18.Organic Vapor	19.Gas Stream Flow	20.Moisture	21.Heat Content (for	22.Excess Oxygen	23, Particle Size	24.Other
Equipment	Concentration (%)	Rate	Content	Flares) MMBtu/hr	(for Oxidizers)	Range	(specify):
ID: EU-4004	2	6649.4 scfh	NA	6.70551	NA	<2.5 um	NA
EU-4002	2	683.4 scfh	NA	0.68931	NA	<2.5 um	NA
EU-4001	2	154 scfh	NA	0.1554	NA	<2.5 um	NA

#### Table 19c. Part C. Pollutant Concentrations

1.Control Equipment ID:	Pollutant	Units	26. Inlet	27. Outlet	28. Efficiency (%):
	voc	lb/hr	1.8	0.036	98
	PM	lb/hr	2.7	0.054	98
EU-4004	со	lb/hr	120	2.4	98
	NO <sub>x</sub>	lb/hr	22.05	0.441	98
Ψ	SO <sub>2</sub>	lb/hr	0.6	0.012	98
	VOC	lb/hr	0.75	0.015	98
<u></u>	PM	lb/hr	0.35	0.007	98
EU-4002	СО	lb/hr	15.3	0.306	98
	NO <sub>x</sub>	lb/hr	2.8	0.056	98
	SO <sub>2</sub>	lb/hr	54.75	1.095	98
	VOC	lb/hr	4944.7	98.685	98
	PM	lb/hr	0.1	0.002	98
EU-4001	со	lb/hr	2212.4	44.248	98
<del></del>	NO <sub>x</sub>	lb/hr	406.6	8.132	98

#### Table 19d. Parts D and E

1.Control Equipment ID:	29.ltem(s) Monitored:	30.Monitoring Frequency:	31.ltem(s) Recorded:	32.Record Keeping Frequency:	33.Pollutant(s) Tested:	34.Test Method(s):	35.Testing Frequency:	36. Do you have a Preventive Maintenance Plan (PMP)?
EU 4004	TBD	TBD	TBD	TBD	TBD	TBD	TBD	TBD
度J-4004 定J-4002	TBD	TBD	TBD	TBD	TBD	TBD	TBD	TBD
EU-4002	TBD	TBD	TBD	TBD	TBD	TBD	TBD	TBD

#### Table 16. GSD-10 Insignificant Activities

\* This table identifies for the listed sources which pollutants are emitted in trivial amounts. A number of these emitters have significant potential emissions of other criteria pollutants.

Emission Unit	Description	PM10/ PM2.5	NOx	co	SO2	VOCs	HAPs	Lead
		X	NA	NA	NA	NA	Х	х
	Coal Unloading Station	<u>x</u>	NA NA	NA	NA	NA	X	Х
	Transfer Station 1 Stacker 1 Boom Chute	<u>x</u>	NA.	NΑ	NA	NA	X	X
EU-1002	Stacker I Boom Cridte		· · · · · · · · · · · · · · · · · · ·					.,
EU-1003	Coal Pile 1A/1B	X	NA	NA	NA	NA	X	x
EU-1004	Stacker 2 Boom Chute	X	NA NA	NA	NA	NA NA	X	^_
EU-1005	Coal Pile 2A/2B	×	NA NA	NA	NA	NA	х	Х
511 5005	Reclaim Transfer Station	X	NA	NA	NA	NA	Х	NA
EU-1006	Coal Dryer Heater	Х	<del>  _</del>		Х	x	Х	X
EU-1007	Coal Drying Loop Purge (N2 + H2O Vapor)	X	NA	NA	NA	NA_	NA	NA
EU-1008	Coarse Additive Storage Filter	X	NA	NA NA	NA	NA NA	Х	NA_
EU-1501		X	NA	NA	NΑ	NA NA	X	NA NA
EU-1502	Fine Additive Storage Filter NA2S Additive Storage Filter	1 x	NA	NA.	NA	NA	NA	NA
EU-1503		<del>  ^</del>	NA NA	NA	NA	NA	X	NA
EU-1504	Fine Additive Production System	X	-		Х	X	Х	х
EU-2001	Feed Heater	<del>\\ \x</del>			X	X	Х	Х
EU-2002	Treat Gas Heater	x	X	X	X	X	х	Х
EU-2003	Vacuum Column Feed Heater	<del>- ^</del>			Х	X	X	Х
EU-2004	Fractionator Feed Heater	X	NA	NA	NA	NA	X	X
EU-2005	Coal Handling System Filter	<del>                                     </del>	NA NA	NA NA	NA	NA	Х	NA
EU-2006	Coarse Additive Handling System Filter	<del>X</del>	NA	NA NA	NA	NA	X	NA
EU-2007	Fine Additive Handling System Filter	X	NA NA	NA NA	NA	NA	NA	NA
EU-2008	Na2S Handling System Filter	1 ×				X	X	X
EU-3001	TGTU Stack A	+ ^-		<del> </del>		X	X	Х
EU-3002	TGTU Stack B	<del>  ^-</del>	+		<del>-   </del>		T .	x
EU-4001	Loading Flare (8 loading spots naphtha service; each at 2500 gpm)	X	X	X   X	X	X	X	
EU-4002	Sulfur Block Flare	X X	X	$+\frac{\hat{x}}{x}$	X	×	X	Х
EU-4003	LP Flare		X	$\frac{1}{x}$	×	х	X	X
EU-4004	HP Flare	X	NA NA	NA NA	NA.	X	X	NA
EU-5001A/B/C/D	Residue Pastilators Stack1	X	NA NA	NA NA	NA NA	Х	X	NA
EU-5002A/B/C/D	Residue Pastilators Stack2	X		NA NA	NA NA	X	×	NA
EU-5003A/B/C/D	Residue Pastilators Stack3	X	NA NA	NA NA	NA NA	X		NA.
EU-5004A/8/C/D	Residue Pastilators Stack4	X	NA NA		NA NA	X	X	NA.
EU-5005	Residue Railcar Loading	X	NA NA	NA NA	NA NA	X	- x	NA NA
EU-5006	Residue Railcar Loading	<u> </u>	NA NA	NA NA	NA NA	X	x	NA NA
EU-5007	Residue Rail/Truck Loading	<u> </u>	NA NA	NA NA	NA NA	X	X	NA
EU-5008	Residue Rail/Truck Loading	X	NA NA	NA NA	NA NA	x	$\frac{\hat{x}}{x}$	NA.
EU-5009	Residue Bulk Container Loading	<u></u>	NA NA	NA NA	NA NA	- x	- X	NA.
EU-5010	Residue Rail Silo Filter	X	NA NA	NA NA	NA NA	- <del>`</del> x	- x	NA.
EU-5011	Residue Swing Silo Filter	X	NA.	NA NA	INA	- x	X	X
EU-6000	Package Boiler					$\frac{\hat{x}}{x}$	NA NA	NA NA
EU-6001	Cooling Tower Cell A	X	NA NA	NA NA	NA_NA	<del></del>	NA NA	NA NA
EU-6002	Cooling Tower Cell B	X	NA NA	NA NA	NA NA		NA	NA
EU-6003	Cooling Tower Cell C	X	NA NA	NA NA	NA NA	<del>- ^</del>	NA NA	NA
EU-6005	EDG Diesel Tank	NA.	NA NA	NA NA	NA V	- X	X	X
EU-6006	Emergency Diesel Generator	Х			X 210		NA NA	N/A
EU-6007	EDFWP Diesel Tank	NA	NA_	NA NA	NA V	X	X X	X
EU-6008	Emergency Diesel FireWater Pump	Х			X	X X		N/
EU-6501	Lime Silo Filter	Х	NA.	NA_	NA_	NA NA	NA NA	N/
EU-6502	Deaerator Vent	NA	NA	NA NA	NA_	NA NA	NA V	
EU-7001	Hydrogen Plant 1 Reformer		<u></u>				X	<del>-                                    </del>
EU-7001 EU-7002	Hydrogen Plant 2 Reformer						X	<u>X</u>
£U-7002	Hydrogen Plant 1 DA Vent	NA	NA		NA			N/
EU-7003	Hydrogen Plant 2 DA Vent	NA	NA		NA		-	N/

Table 17. CE-01 Control Equipment Summary

**Summary of Control Equiment** 

1. Control Equipment ID	2. Control  Equipment  Description	3. Pollutant Controlled	4. Emission Unit ID	5. Stack / Vent ID	6. Applicable Rule
	Baghouse	PM	EU-1000	ี €U-1000	40 CFR 60 Part Y 60.254
EU-1000	Baghouse	PM	EU-1001	EU-1001	40 CFR 60 Part Y 60.254
EU-1001	NA				
EU-1002	NA NA				
EU-1003	NA NA				
EU-1004	NA NA				
EU-1005		PM	EU-1006	EU-1006	40 CFR 60 Part Y 60.254
EU-1006	Baghouse				
EU-1007	NA NA	PM	EU-1008	EU-1008	40 CFR 60 Part Y 60.254
EU-1008	Baghouse	PM, HAPs	EU-1501	EU-1501	
EU-1501	Baghouse	PM, HAPs	EU-1502	EU-1502	
EU-1502	Baghouse		EU-1503	EU-1503	
EU-1503	Baghouse	PM, HAPs	EU-1504	EU-1504	
EU-1504	Baghouse	PM, HAPs	LO 130,		
EU-2001	NA				<b></b>
EU-2002	NA NA				
EU-2003	NA NA		+		T
EU-2004	NA NA		EU-2005	EU-2005	40 CFR 60 Part Y 60.254
EU-2005	Baghouse	PM	EU-2006	EU-2006	
EU-2006	Baghouse	PM, HAPs	EU-2007	EU-2007	
EU-2007	Baghouse	PM, HAPs		EU-2008	
EU-2008	Baghouse	PM, HAPs	EU-2008		
EU-3001	NA				
EU-3002	NA		<del></del>	<del></del>	
EU-4001	NA NA				
EU-4002	NA				
EU-4003	NA				
EU-4004	NA NA				
	NA NA				<del>+</del>
EU-5001A/B/C/D	NA NA				
EU-5002A/B/C/D	NA NA				
EU-5003A/B/C/D	NA NA				
EU-5004A/B/C/D				and the	
EU-5005	NA NA				
EU-5006	NA NA				
EU-5007	NA NA				
EU-5008	NA NA				
EU-5009	NA NA		EU-5010	EU-5010	
EU-5010	Baghouse	PM PM	EU-5011	EU-5011	
EU-5011	Baghouse				
EU-6000	NA NA		EU-6001	EU-6001	
EU-6001	Drift Eliminators	PM_	EU-6002	EU-6002	
EU-6002	Drift Eliminators	PM	EU-6002	EU-6003	
EU-6003	Drift Eliminators	PM	E0-0003		
EU-6005	NA	<del></del>			-
EU-6006	NA				
EU-6007	NA				
EU-6008	NA			#U. CC01	
EU-6501	Baghouse	PM	EU-6501		
EU-6502	NA NA	T		 TU 7001	
EU-7001	SCR	NOx	EU-7001		
EU-7001	SCR	NOx	EU-700		
EU-7002	NA NA				
EU-7003	NA NA				

Table 18. CE-02 Particulate Control - Baghouse / Fabric Filter

Table 18a. Part A: Identification and Description of Control Equipment

1. Control E	quipment ID	2. Installation Date	3. Bags or Cartridges?	4. Filter Material	5. Number of bags per Compartment	6. Number of Compartments	
			Bags	TBD	TBD	TBD	
EU-1000		1Q2021		TBD	TBD	TBD	
EU-1001		1Q2021	Bags	TBD	TBD	TBD	
EU-1006		102021	Bags	TBD	TBD	TBD	
EU-1008		102021	Bags	TBD	ТВР	TBD	
EU-1501		1Q2021	Bags	TBD	TBD	TBD	
EU-1502	Used for material	102021	Bags		TBD	TBD	
EU-1503	recovery, not a	102021	Bags	TBD	TBD	TBD	
EU-1504	control device	102021	Bags	TBD		TBD	
		102021	Bags	TBD	TBD	TBD	
EU-2005	Used for material		Bags	TBD	TBD		
EU-2006		102021	Bags	TBD	TBO	TBD	
EU-2007	recovery, not a		Bags	TBD	18D	TBD	
EU-2008	control device	102021	Bags	TBD	TBD	TBD	
EU-5010		102021		TBD	TBD	TBD	
EU-5011		1Q2021	Bags	TBD	TBD	TBD	
EU-6501		102021	Bags	I I I I I I I I I I I I I I I I I I I			

1. Control Equipment ID	7. Mode of Operation	escription of Contr 8. Cleanign Method	9. Cleaning Cycle / Frequency	10. is a bag leak detector installed on a device	11. Type / Description of Bag Leak Detector	12, Air to Cloth Ratio	13. Is Lime Inkection used on this device	14. Is Carbon Injection used on this device
				Yes	TBD	TBD	No	No
EU-1000	Continuous	Reverse Pulse	As Needed	Yes	TBD	TBD	No	No
EU-1001	Continuous	Reverse Pulse	As Needed	1	TBD	TBD	No	No
EU-1006	Continuous	Reverse Pulse	As Needed	Yes	TBD	TBD	No	No
FU-1008	Continuous	Reverse Pulse	As Needed	Yes	TBD	TBD	No	No
EU-1501	Continuous	Reverse Pulse	As Needed	Yes	TBD	TBD	No	No
EU-1502	Continuous	Reverse Pulse	As Needed	Yes	TBD	TBD	No	No
EU-1503	Continuous	Reverse Pulse	As Needed	Yes		TBD	No	Nio
EU-1504	Continuous	Reverse Pulse	As Needed	Yes	TBD	TBD	No	No
	Continuous	Reverse Pulse	As Needed	Yes	TBD	TBD	No	No
EU-2005	Continuous	Reverse Pulse	As Needed	Yes	TBD	TBD	No	No
EU-2006	Continuous	Reverse Pulse	As Needed	Yes	TBD	TBD	No	No
EU-2007	Continuous	Reverse Pulse	As Needed	Yes	TBD		No.	No
EU-2008		Reverse Pulse	As Needed	Yes	TBD	TBD	No	No
EU-5010	Continuous	Reverse Pulse	As Needed	Yes	TBD	TBD	No	No
EU-5011	Continuous		As Needed	Yes	TBD	TBD	1 NO	
EU-6501	Continuous	Reverse Pulse	As Needed	1 163				

Table 18b. Part B: Operational Parameters

1. Control	15. Gas Stream	16. Gas Stream Temperature deg	17. Gas Stream	18. Moisture	19. Particle Size Range Inlet	19, Particle Size Range Outlet	20. Lime Injection Rate (if applicable)	21. Carbon Injection Rate (if applicable)	22. Other (specify):
Equipment ID	Flow Rate acfm	F	71030410		≤ 2.5 microns	≤ 2.5 microns	NA	NA NA	NA
EU-1000	TBD	Ambient	TBD	0		≤ 2.5 microns	NA	NA NA	NA
	TBD	Ambjent	TBD	0	≤ 2.5 microns	≤ 2.5 microns	NA	NA NA	NA
EU-1001	TBD	Ambient	TBD	0	≤ 2.5 microns		NA NA	NA	NA
EU-1006		220	TBD	0	≤ 2.5 microns	≤ 2.5 microns	NA NA	NA NA	NA
EU-1008	27916.6	120	TBD	0	≤ 2.5 microns	≤ 2.5 microns		NA NA	NA
EU-1501	1668		TBD	0	≤ 2.5 microns	≤ 2.5 microns	NA	NA NA	NA
EU-1502	1668	120	TBD	0	≤ 2.5 microns	≤ 2.5 microns		NA NA	NA.
EU-1503	834	120		0	≤ 2.5 microns	≤ 2.5 microns	NA NA		NA.
EU-1504	TBD	Ambient	TBD	0	≤ 2.5 microns	≤ 2.5 microns	NA NA	NA NA	
EU-2005	TBD	Ambient	TBD	0	≤ 2.5 microns		NA NA	NA NA	NA_
EU-2006	221	120	TBD		≤ 2.5 microns		NA	NA NA	NA NA
EU-2007	329	120	TBD	0	≤ 2.5 microns			NA NA	NA NA
EU-2008	39	120	TBD	0				NA	NA.
	TBD	Ambient	TBD	0	≤ 2.5 microns			NA	NA
EU-5010	TBD	Ambient	TBD	0	≤ 2.5 microns			NA NA	NA
EU-5011		Ambient	TBD	0	≤ 2.5 microns	≤ 2.5 microns	NA .	1	
EU-6501	TBD	Amblene							

Table 18c. Part C: Pollutant Concentrations

1. Control Equipment ID	Pı	ollutant Potential t	26. Capture Efficiency (%)	26. Control Efficiency (%)		
	PM	PM10	PM2.5	HAPs		
EU-1000	0.152	0.114	0.003	NA	100	99.5
EU-1001	0.002	0.001	0.000	NA	100	99.5
	2.410	1.807	0.046	NA NA	100	99.5
EU-1006	2,405	2,405	2,405	NA	100	99.5
EU-1008		0.019	0.019	2.00E-05	100	99,5
EU-1501	0,019	0.028	0.028	2.00E-05	100	99.5
EU-1502	0.028		0.001	NA.	100	99.5
EU-1503	0.001	0.001		3.62E-05	100	99.5
EU-1504	0.034	0.034	0.034	NA NA	100	99.5
EU-2005	0.023	0,023	0.023		100	99.5
EU-2006	0.023	0.023	0.023	2.40E-05		99.5
EU-2007	0.034	0.034	0.034	0.000	100	
EU-2008	0.004	0.004	0.004	NA NA	100	99.5
		Trace	Trace	NA.	100	99.5
EU-5010	Trace		Trace	NA NA	100	99.5
EU-5011	Trace	Trace		NA.	100	99.5
EU-6501	TBD	TBD	TBD	NA	1	

#### Table 18d. Parts D, E, F

1. Control Equipment ID	27. Item(s) Monitored	28. Monitoring Frequency	29. Item(s) Recorded:	30. Record Keeping Frequency:	31. Pollutant(s) Tested:	32. Test Method(s)	33. Testing Frequency:	34. Do you have a Preventive Maintenance Plan (PMP)	35. Has IDEM aiready made an integral determination for this device?	36, is this device integral to the process?
				Continuous	PM	Method 5	Every 5 years	No - in development	No	Yes
EU-1000	Pressure	Continuous	Delta P		PM	Method 5	Every 5 years	No - in development	No	Yes
EU-1001	Pressure	Continuous	Delta P	Continuous	PM	Method 5	Every 5 years	No - in development	No	Yes
EU-1006	Pressure	Continuous	Delta P	Continuous		Method 5	Every 5 years	No - in development	No	Yes
EU-1008	Pressure	Continuous	Delta P	Continuous	PM	Method 5	Every 5 years	No - in development	No	Yes
EU-1501	Pressure	Continuous	Delta P	Continuous	PM	Method 5	Every 5 years	No - in development		Yes
EU-1502	Pressure	Continuous	Delta P	Continuous	PM		Every 5 years	No - in development		Yes
EU-1503	Pressure	Continuous	Delta P	Continuous	PM	Method 5		No - in development		Yes
EU-1504	Pressure	Continuous	Delta P	Continuous	PM	Method 5	Every 5 years	No - in development		Yes
EU-2005	Pressure	Continuous	Delta P	Continuous	PM	Method 5	Every 5 years	No - in development		Yes
	Pressure	Continuous	Delta P	Continuous	PM	Method 5	Every 5 years			Yes
EU-2006	Pressure	Continuous	Delta P	Continuous	PM	Method 5	Every 5 years	No - in development		Yes
EU-2007		Continuous	Delta P	Continuous	PM	Method 5	Every 5 years	No - in development		Yes
EU-2008	Pressure	Continuous	Delta P	Continuous	PM	Method 5	Every 5 years	No - in development		Yes
EU-5010	Pressure		Delta P	Continuous	PM	Method 5	Every 5 years	No - in development		
EU-5011	Pressure	Continuous		Continuous	PM	Method 5	Every 5 years	No - in developmen	t No	Yes
EU-6501	Pressure	Continuous	Delta P	Continuous	1					

Table 20. PI-02 Combustion

Table 20a. Summary of Combustion Units

1. Combustion Unit Type	2. Number of Identical Units	3. Unit ID(s)	4. Date of Installation or Modification	5. Heat input rate of each unit (MMBtu/hr)	6. Emergency Back-Up Unit?
- 1	1	EU-1007	102021	55.8	No
Coal Dryer Heater	1	EU-2001	102021	128.4	. No
Feed Heater Treat Gas Heater	1	EU-2002	102021	52.8	No
Vacuum Column Feed	1	EU-2003	102021	9	No
Heater		EU-2004	102021	156	No
Fractionator Feed Heater	1	EU-6000	102021	68.5	No
Package Boiler Emergency Diesel Generator	1	EU-6006	1Q2021	17.86	Yes
Emergency Diesel FireWater Pump	1	EU-6008	1Q2021	5.14	Yes
Hydrogen Plant 1 Reformer	1	EU-7001	· 1Q2021	838.6	No
Hydrogen Plant 2 Reformer	1	EU-7002	102021	838.6	No

# Table 20b. PI-02B: Combustion - Boilers, Process Heaters & Furnaces Part A: Process Unit Details

Part B: Emission Controls and Limitation

2. Unit Type	3. Combustion	4. Heat Transfer	5. Transfer Surface Arrangement	6. Firing Configuration	7. Heat Transfer Method	8. Fuel Used	9. Add-On Control Technology	10. Control Technique
		Method	11-11-1-1	Up-fired	Indirect	Natural Gas	None	Ultra Low NOx Burners
Coal Dryer Heater	Gas Combustion				Indirect	Natural Gas	None	Ultra Low NOx Burners
Feed Heater	Gas Combustion					Natural Gas	None	Ultra Low NOx Burners
Treat Gas Heater	Gas Combustion		Horizontal	Ор-шец				
Vacuum Column			Madeantol	Un-fired	Indirect	Natural Gas	None	Ultra Low NOx Burners
Feed Heater	Gas Combustion	Sections	RUGIZORICAL	OP 1/1/25				
Fractionator Feed			I I I untral	Lin-fired	Indirect	Natural Gas	None	Ultra Low NOx Burners
Heater					NA.	Natural Gas	None	Ultra Low NOx Burners
Package Boller	Gas Combustion	Watertube	Horizontal	Horizonta		Process Tail Gas		
Hydrogen Plant 1		Radiant and	Manager	Down-fired	Indirect	supplemented by Natural Gas	Yes	Selective Catalytic Reduction (SCR)
Reformer	Gas Combustion	Convection	Horizontal	powinting cu		Process Tail Gas		1
Hydrogen Plant 2		Sections	Hasirontal	Down-fired	Indirect	supplemented by Natural Gas	Yes	Selective Catalytic Reduction (SCR)
	Coal Dryer Heater Feed Heater Treat Gas Heater Vacuum Column Feed Heater Fractionator Feed Heater Package Boiler Hydrogen Plant 1 Reformer	2. Unit Type Process  Coal Dryer Heater Gas Combustion Feed Heater Gas Combustion Treat Gas Heater Gas Combustion Vacuum Column Freed Heater Gas Combustion Fractionator Feed Heater Gas Combustion Pyckage Boller Gas Combustion Hydrogen Plant 1 Reformer Gas Combustion Hydrogen Plant 2	2. Unit Type Process Method  Coal Dryer Heater Gas Combustion Freed Heater Gas Combustion Treat Gas Heater Gas Combustion Treat Gas Heater Gas Combustion Treat Gas Heater Gas Combustion Treat Gas Heater Gas Combustion Treat Gas Heater Gas Combustion Treat Gas Heater Gas Combustion Treat Gas Heater Gas Combustion Treat Gas Combustion Transfer Method  Radiant and Convection Treat Gas Combustion Treatser Method  Radiant and Convection Treatser Method  Radiant and Convection Sections	2. Unit Type  3. Combustion Process  Coal Dryer Heater Gas Combustion Feed Heater Gas Combustion Freed Heater Freed Heater Gas Combustion Freed Heater Gas Combustion Freed Heater Freed Heater Freed Heater Gas Combustion Freed Heater Freed Heater Freed Heater Gas Combustion Freed Heater	2. Unit Type 3. Combustion Process Method Arrangement Method Arrangement Horizontal Up-fired Horizontal Up-fired Horizontal Up-fired Horizontal Up-fired Horizontal Up-fired Horizontal Up-fired Up-fired Horizontal Up-fired Horizontal Up-fired Horizontal Up-fired Horizontal Up-fired Horizontal Up-fired Horizontal Up-fired Horizontal Up-fired Horizontal Horizontal Up-fired Horizontal Horizontal Up-fired Horizontal Down-fired Dow	2. Unit Type 3. Combustion Process Method Arrangement	2. Unit Type   3. Combustion   Process   Transfer   Method   Arrangement   Method   Arrangement   Method   Arrangement   Method	2. Unit Type Process Coal Dryer Heater Gas Combustion Freed Heater Gas Combustion Freed Heater Gas Combustion Seed Heater Gas Combustion Freed Heater Gas Combustion Freed Heater Gas Combustion Seed Heater Gas Combustion Freed Heater Gas Combustion Seed Heater Gas Combustion Freed Fre

### Table 20c. PI-02C: Combustion - Turbines & Reciprocating Internal Combustion Engines

table foci i i and i amo			<del>, ,                                    </del>		and the second	A STATE OF THE STA	8. Supply power
	2. Type of	3. Combustion		5. Power Output	6. Duty Cycle (hr/yr)	7. Fuel Used	to an emergency
1. Unit ID	Combustion Unit	Process	4. Ignition Type	3. FUREI Duipat			generator?
			Compression	2800 BHP	100	Diesel Fuel	Yes
EU-6006	RICE	,50		750 BHP	200	Diesel Fuel	Yes
EU-6008	RICE	TBD	Compression	750 0111			

#### Table 20c. PI-02F: Combustion - Fuel Use Part A, Part B, Part C

1. Unit ID	2. Fuel Type	3. Percent of Fuel Use	4. Primary or Secondary Fuel?	5. Component Percentages	6. Heating Value (Btu/scf)	
	Natural Gas	100%	Primary	Sulfur: 10ppmv	909	
EU-1007	Natural Gas	100%	Primary	Sulfur: 10ppmv	909	
EU-2001		100%	Primary	Sulfur: 10ppmv	909	
EU-2002	Natural Gas	100%	Primary	Sulfur: 10ppmv	909	
EU-2003	Natural Gas	100%	Primary	Sulfur: 10ppmv	909	
EU-2004	Natural Gas	100%	Primary	Sulfur: 10ppmv	909	
EU-6000	Natural Gas	81.5%	Primary	Sulfur: 0	251	
EU-7001	Process Tail Gas	18.5% (100% during Start up)		Sulfur: 10 ppmv	909	
	Natural Gas	81.5%	Primary	Sulfur: 0	251	
EU-7002	Process Tail Gas  Natural Gas	18.5% (100% during Start up)		Suifur: 10 ppmv	909	

#### Table 20c. Pl-02F: Combustion - Fuel Use Continued

1. Unit ID	7. Fuel Type	8. Percent of Fuel Use	9. Primary or Secondary Fuel?	10. Component Percentages	11. Heating Value (Btu/gal)	12. Percent Heat:
	Diesel Fuel	100%	Primary	Sulfur: 0.05wt%	137030	100%
EU-6006 EU-6008	Diesel Fuel	100%	Primary	Sulfur: 0.05wt%	137030	1.00%

Table 20d. PI-02G: Combustion - Fuel Use Emission Factor

1. Unit ID	2. Air Pollutant	3. Emission Factor (lb/MM8tu HHV)	4. Source of Emission Factor
FU-1007	VOC	0.0054	AP42
E0-1007	PM	0.0075	AP42
	PM10	0.0075	AP42
	PM2.5	0.0075	AP42
	co	0,036	Performance
	NOx	0.04	Bid
	SOZ	0.0018	Specification
	Pb	4.90E-07	AP42
	HAPs	0.0019	AP42
CIL BOOK	VOC	0.0054	AP42
EU-2001	PM	0.0075	AP42
	PM10	0.0075	AP42
	PM2.5	0.0075	AP42
	co	0.036	Performance
	NOx	0,04	] Bid
	502	0.018	Specification
	Ph	4.90E-07	AP42
	HAPs	0.0019	AP42
EU-2002	voc	0.0054	AP42
EU-2002	PM	0.0075	AP42
	PM10	0.0075	AP42
	PM2.5	0.0075	AP42
	co	0.036	Performance
	NOx	0.04	Bid
	502	0.018	Specification
	Pb	4.90E-07	AP42
	HAPs	0.0019	AP42
EU-2003	VOC	0.0054	AP42
E0-2003	PM	0,0075	AP42
	PM10	0.0075	AP42
	PM2.5	0.0075	AP42
	co	0.036	Performance
	NOx	0.04	Bid
	SO2	0.018	Specification
	Pb	4.90E-07	AP42
	HAPs	0.0019	AP42

Table 20d. PL02G: Combustion - Fuel Use Continued

1. Unit ID	2. Air Pollutant	3. Emission Factor (lb/MMBtu HHV)	4. Source of Emission Factor
U-2004	VOC	0.0054	AP42
U-200 <del>4</del>	PM	0.0075	AP42
	PM10	0.0075	AP42
	PM2.5	0.0075	AP42
	CO	0.036	Performance
	NOx	0.04	8id
	SO2	0,018	Specification
	Pb	4.90E-07	AP42
	HAPs	0.0019	AP42
U-6000	voc	0.0054	AP42
0-0000	PM	0.0075	AP42
	PM10	0,0075	AP42
	PM2.5	0.0075	AP42
	CO	0.036	Performance
	NOx	0.04	Bid
	502	0.018	Specification
	Pb	4.90E-07	AP42
	HAPs	0.0019	AP42
U-7001	VOC	0.006	
.0.7001	PM	0.006	
	PM10	0.006	Performance
	PM2.5	0.006	- Bid
	CO	0,02	Specification
	NOx	0.007	Specification
	502	3.26E-04	
	Ammonia	10 ppmvd	
	Pb	4.90E-07	AP42
	HAPs	0.0019	AP42
EU-7002	VOC	0.006	
	PM	0.006	
	PM10	0.006	Performance
	PM2.5	0.006	Bld
	co	0.02	Specification
	NOx	0.007	
	SO2	3.26E-04	
	Ammonia	10 ppmvd	
	Pb	4.90E-07	AP42
i	HAPs	0,0019	AP42

# Table 21. PI-03 Storage & Handling of Bulk Material

ble 21a. Part A: Storage & Handling Information

Date of installation for the listed equipment is expected to be 1Q2021

1. Equipment/ Component Type	2. Unit ID	3. Number of Identical Units	4. Installation Date	5. Material Handled/Stored	6. Maximum Materials Throughput Rate	7. Add on Control Technology	8. Control Technique	9. Process Limitations/ Additional Information				
Coarse Additive Handling System	EU- <del>1001</del> 1501		-2/4/2016*	Coarse Additive	20 ton/hr	Baghouse	NA	]				
		0			20 ton/hr	Baghouse	NA	1				
Fine Additive Handling System	EU- <del>1002</del> 1502	0	<del>2/4/2016</del>	Fine Additive	20 (01)10			1				
Coal Handling System	ystem EU- <b>1000</b> 2005				258.4 ton/hr	Baghouse	NA.	Refer to Emissions				
		C	2/1/2010	Dried Coal	230,4 (01)/12			Summary Table for				
Na2S Handling System	EU-1005 1503		3/1/2015	Sodium Sulfide additive	10 ton/hr	Baghouse	NA	Handling Information				
				VCC Fine Additive	3,28 ton/hr	Baghouse	NA					
Fine Additive Handling System	EU- <del>1007</del> 2007	0	9/1/2015	VCC FRIE Additive	T	<u> </u>	1					
Coarse Additve Handling System	EU-1-000-2006	0	B/4/2016	VCC Coarse Additive	2.2046 ton/hr	Baghouse	NA NA	_				
Na25 Handling System	System EU-1000 2008			a is a substantiation	.077161 ton/hr	Baghouse	NA					
Maza Indireding System		0	3/1/2016	Sodium Sulfide additive		Baghouse	NA.					
Fine Additive Production System	EU-1504	0	1Q2021	Fine additives	3.28 ton/hr	pagiouse .						

e 21b. Part B: Process Mat to. Material Handled/Stored	al management at the STA 7	12. Type of Storage	13. Storage Capacity	14. Pile Acreage	15. Silt Content	16. Moistur Content
Coarse Additive	Rail Transport to storage vessel	Silo	TBD	NA	100 % 20-450 um	0
Fine Additive	Rail transport to storage vessel	Silo	TBD	NA NA	100 % 20-450 um	0
Dried Coal	Continuous rapid unloading from 100 car unit trains to hoppers	Stackpile	ТВО	38.16	2.20%	4.50%
Sodium Sulfide additive	Truck transport to storage vessel	Silo	TBD	NA NA	100 % 20-450 um	0
VCC Fine Additive	Rail Transport to storage vessel and to pro		TBD	NA NA	100 % 20-450 um	0
VCC Coarse Additive	Rail Transport to storage vessel	Silo	TBD	NA NA	100 % 20-450 um	C
Sodium Sulfide additive	Truck transport to storage vessel	Silo	TBD	NA_	100 % 20-450 um	0

#### Table 21c. Part C: Emission Factors

### Table 21d. Part D. Federal Rule Applicability

ble 21c. Part C: Emission Fac 17. Process Equipment & ID	18. Air Pollutant	19. Emission Factor	20, Source of Emission Factor	21. NSPS Applicability	22. NESHAP Applicability	23. Non- Applicability Determination NA	
	PM	.003 gr/dscf	AP-42	No	No		
EU- <del>1001</del> 1501		.003 gr/dscf	AP-42	No	No	NA	
	PM-10	.003 gr/dscf	AP-42	No	No	NA_	
EU-1 <del>002-</del> 1502	PM	.003 gr/dscf	AP-42	No	No	NA	
	PM-10	1.45 lb/acre/year	AP-42	No	No	NA NA	
EU-1005 2005	PM 2.5	3.63 lb/acre/year	AP-42	No	No	NA	
	PM-10		AP-42	No	No	NA	
EU- <del>#860-</del> 1503	PM	.003 gr/dscf	AP-42	No	No	NA	
	PM-10	.003 gr/dscf	AP-42	No	No	NA	
EU-1007 2007	PM	.003 gr/dscf	AP-42	No	No	NA	
	PM-10	.003 gr/dscf	AP-42	No	No	NA	
Eบ- <del>1088</del> 2006	PM	.003 gr/dscf		No No	No	NA	
	PM-10	.003 gr/dscf	AP-42	No	No	NA.	
EU- <b>1009</b> 2008	PM	.003 gr/dscf	AP-42	No	No	NA	
	PM-10	.003 gr/dscf	AP-42	No No	No	NA.	
EU-1504	PM	003 gr/dscf	AP-42 AP-42	No No	No	NA.	
	PM-10	.003 gr/dscf	I Ar-12				

# Table 22. PI-14 Volatile Organic Liquid Compound Storage Parts A through E: Note this table is a comprehensive list, non organic storage is also included below

	Parts A throug	h E: Note this ta	able is a compreh	ensive list, iit	of Organic :	itorage is diso in	ond does a cons			Commence of the second second second second				N.B. STYPE STREET
1. Tank/ Unit ID	2. Installation Date	3. Tank Location: UTM EASTING COORDINATE (m)	3. Tank Location: UTM NORTHING COORDINATE (m)	4. Tank Type:	S. Above	6. Tank Orientation	7. Tank Color	8. Materials Stored	9. True Vapor Pressure	10. Vapor Molecular Weight	11. Annual Throughput (gal/yr)	12. Venting Method	13. Filling Method	14. Add-On Control Technology
NULL IN SE	- Paus		Marketing of the Control of the Control of	VI II-II-III-II-II-II-II-II-II-II-II-II-I							:		:	
	102021	502225	4226190	IFR	Yes	Vertical	Default	Naphtha Product Tank 1	2.03 psia at 100 degF	91.5	4,629,879	TBD	Submerged	None
	1Q2021	302223					D ()	Northbo Brodust Tapk 2	2.03 psia at 100 degF	91.5	4,629,879	TBD	Submerged	None
	1Q2021	502150	4226190	IFR	Yes	Vertical	Default	Naphtha Product Tank 2						
3	1Q2021	502150	4226114	Fixed Roof	Yes	Vertical	Default	Diesel Product Tank 1	0.002 psia at 100 degF	198.7	4,525,796	Conservation Vent	Submerged	None
	102021	302230						Di I Dundush Tonk 2	0.002 psia at 100 degF	198.7	4,525,796	Conservation Vent	Submerged	None
	1Q2021	502225	4226114	Fixed Roof	Yes	Vertical		Diesel Product Tank 2		198.7	4,525,796	Conservation Vent	Submerged	None
	1Q2021	502301	4226114	Fixed Roof	Yes	Vertical	Default	Diesel Product Tank 3	0.002 psia at 100 degF	150.7	4,323,730			
								Tank	0.002 psia at 100 degF	198.7	4,525,796	Conservation Vent	Submerged	None
ò	1Q2021	502301	4226190	IFR	Yes	Vertical		Diesel Product Swing Tank	TBD	TBD	342,367	Conservation Vent	Submerged	None
	1Q2021	502116	4226652	Fixed Roof		Vertical		Molten Sulfur 1 Molten Sulfur 2	TBD	TBD	342,367	Conservation Vent	Submerged	None
	1Q2021	502116	4226671	Fixed Roof		Vertical Pressurized Horizontal		Ammonia Product Storage Bullets	TBD	17.03	36,720	Closed	Submerged	None
İ	1Q2021	501954	4226698	NA NA	Yes	FIQUIZOIILAI			TD0	386.7	926,980	VENT TO ATM Temp = 505 F Heavy Material	Submerged	None
LO	1Q2021	502167	4226778	Fixed Roof		Vertical		Residue Surge Tank (VR LPH) 1	TBD TBD	386.7	926,980	VENT TO ATM Temp = 505 F Heavy Material		None
.1	1Q2021	502193	4226778	Fixed Root		Vertical		Residue Surge Tank (VR LPH) 2	TBD	386.7	926,980	VENT TO ATM Temp = 505 F Heavy Material	Submerged	None
L2	1Q2021	502219	4226778	Fixed Roo		Vertical		Residue Feed Tank	0.001 pisa at 300 degF		926,980	VENT TO ATM Temp = 505 F Heavy Material	Submerged	None
13	1Q2021	502325	4226893	Fixed Roo		Vertical		VGO Tank 2	0.001 pisa at 300 degF		926,980	VENT TO ATM Temp = 505 F Heavy Material	Submerged	None
14	1Q2021	502357	4226893	Fixed Roo	f Yes	Vertical Pressurized		VGO Tank 2			40.070	TBD	Submerged	None
15	1Q2021	502548	4226789	NA NA	Yes	Horizontal	Default	LPG Storage Bullets	TBD	TBD TBD	48,872 4,195,581	Vent to Flare	Submerged	
16	1Q2021 1Q2021	502341	4226190	Fixed Roo		Vertical	Default	Slop Tank	TBD	עמו	4,133,361			
							:				22.77	Vent to ATM	Submerged	i None
17	1Q2021	501898	4226431	Fixed Roo	of Yes	Vertical		Diesel Fuel Storage Tank	TBD	198.7 18.01	23,775 1,268,026	Vent to ATM  Vent to flare	Submerged	
18	1Q2021		4226725	Fixed Roc		Vertical	Default	Non-Phenolic Sour Water Storage Tank 1	TBD	18.01	1,208,020			

# Table 22. PI-14 Volatile Organic Liquid Compound Storage Parts A through E: Note this table is a comprehensive list, non organic storage is also included below

	The state of the s			The same of the sa		2750 - 275 - 275 - 01 - 1									
							21. External								
Tel: Was Nill			ALL PLANTS OF THE PROPERTY OF		Part of the second of the seco		Floating							THE PROPERTY OF STREET STREET, AS	31.
						20.	Roof:	22.	23.						Applicabilit
			17. Tank	18. Tank	19. Tank	Maximum	Complete	Internal	Variable		And the second of the second o	26. EF	27/28	The state of the s	Determina
			Diameter:	Height:	Volume /	Liguid	only if	Floating	Vapor				NSPS?	29/30 NESHAP?	on
Tank/	15. Control Techniques	16. Process Limitations/Additional Information	<b>(ft)</b>	(11)	Capacity:	Height:	applicable.	Roof	Space	24, Air Pollutant	Secretary Communication Commun				
nit ID	am tecamichesas											1			
		TANKS 4.0.9d DEFAULTS Applied - Primary Seal: Vapor-Mounted,								n-Hexane,		1			
		Secondary Seal: None; Deck Type: Welded, Deck Fitting					!			Benzene,					
		Category: Typical.								Toluene,					
		2 tanks listed at size and construction details given. Tank						B	TBD	Xylenes,	Emission Factor values				
	IFR	turnovers represents total production through single tank	160.1	47.9	4,629,879	N/A	NA	Dome	100	Phenol, o-Cresol,	from EPA's Tanks 4.0.9				
			160.1	47.9	4,629,879	N/A	NA.	Dome	TBD	m-, p-Cresols	used	AP 42	NA	40 CFR 63.2343(b)	NA
	IFR	NA 3 OF 4 Diesel Tanks are fixed roof. 1 OF 4 Diesel Tanks as IFR, for	10012												
		use as swing tank in naphtha service - SEE LINE BELOW.													
		2 tanks listed at size and construction details given. Tank								:			1		
,	IFR	turnovers respresents is total production through single tank.	160.1	47.9	4,525,796	46.9	NA NA	NA	NA						
3	1110	turnove) 3 respice 3 respi									Emission Factor values				
								NA	NA NA	Product Diesel	from EPA's Tanks 4.0.9	AP 42	NA	40 CFR 63.2343(b)	NA
1	NA NA	NA	160.1	47.9	4,525,796	46.9	NA	INA	11/0	11000012101	used	i			
		NA.	160.1	47.9	4,525,796	46.9	NA	NA	NA						
)	NA NA	NA .								n-Hexane,					
									1	Benzene,					
										Toluene,					
				-						Xylenes,	Emission Factor values				
		Primary Seal: Vapor-Mounted, Secondary Seal: None; Deck Type:			ļ					Phenol,	from EPA's Tanks 4.0.9				
		Welded,								o-Cresol,	used	AP 42	NA	40 CFR 63.2343(b)	NA NA
6	IFR	Deck Fitting Category: Typical	160.1	47.9	4,525,796	N/A	NA	Dome	TBD	m-, p-Cresols	uscu				
7	NA NA	NA .	42.7	47.9	342,367	46.9	NA	NA NA	N N				1		
8	NA	NA	42.7	47.9	342,367	46.9	NA NA	NA_	N						
			10.8	69.2	36,720	N/A	NA	NA	NA						
9	NA NA	NA .									7.3 E-7 lb benzene/ton				
10	None	NA	69.9	47.9	926,980	46.9	NA NA	NA NA	NA NA	Hydrogen Residue	asphalt loaded	AP 42	. NA	NA NA	NA NA
10	None										aspirate (baucu				
11	None	NA .	69.9	47.9	926,980	46.9	NA NA	NA	NA		7.3 E-7 lb benzene/ton				
						46.0	NA	NA	NA.		asphalt loaded	AP 42	NA NA	NA NA	NA NA
12	None	NA	69.9	47.9	926,980	46.9	INA .	110	103						
			69.9	47.9	926,980	46.9	NA NA	NA.	NA.	V(CC)/CO	7.3 E-7 lb benzene/ton	AP 42	2 NA	NA NA	NA
13	None	NA	6.50	+/.3	720,300	1	T -			VCC VGO	asphalt loaded				
			69.9	47.9	926,980	46.9	NA	NA	NA			-	-		
14	None	NA	55.5		1										
15	NA	Pressurized vessels	10.8	83.7	48,872	N/A	NA	NA NA	NA NA	1			+		
16	NA NA	NA	160.1	40	4,195,581	1 39	NA_	NA.	NA	Hexane (-n),					
	177									Benzene,					
			-							Toluene,	Emission Factor values				
										Ethylbenzene,	from EPA's Tanks 4.0.9				
											i .		1	1	LII NIA
			21.3	16.1	23,775	15.1	NA NA	NA.	NA.	Xylene (-m)	used	AP 4	2 NA	40 CFR 63.2343(I	b) NA

Table 22. PI-14 Volatile Organic Liquid Compound Storage
Parts A through E: Note this table is a comprehensive list, non organic storage is also included below

	, 0.125 / 0.110 - 2	,,,	•		_			No. of the state o	The state of the s	AND THE LOCAL PROPERTY OF THE PARTY OF THE P				
1. Tank/	2. Installation	3. Tank Location: UTM EASTING COORDINATE	3. Tank Location: UTM NORTHING COORDINATE	4. Tank	5. Above	6. Tank	7. Tank	8. Materials Stored	9. True Vapor Pressure	10. Vapor Molecular Weight	11. Annual Throughput (gal/yr)	12. Venting Method	13. Filling Method	14. Add-On Control Technology
Unit ID	Date :	(m)	(m)	Туре:	ground?	Orientation	Color	THE PARTY OF THE P	TBD	18.01	1,268,026	Vent to flare	Submerged	None
T19	1Q2021	502178	4226725	Fixed Roof	Yes	Vertical		Non-Phenolic Sour Water Storage Tank 2	TBD	18.01	1,268,026	Vent to flare	Submerged	None
T20	1Q2021	502213	4226725	Fixed Roof	Yes	Vertical		Non-Phenolic Sour Water Storage Tank 3	TBD	18.01	40,947	Vent to flare	Submerged	None
T21	1Q2021	502108	4226725	Fixed Roof	Yes	Vertical		Phenolic Sour Water Storage Tank	TBD	18.01	1,268,026	Vent to ATM. < 10 ppm H2S, < 10 ppm NH3; Conservation Vent. Head space concentration based on Henry's Law.	Submerged	None
T22	1Q2021	502117	4226783	Fixed Roof	Yes	Vertical  Vertical		Stripped Non-Phenolic Sour Water Surge Tank Stripped Phenolic Sour Water Surge Tank	TBD	18.01	13,737	Vent to ATM. < 10 ppm H2S, < 10 ppm NH3; Conservation Vent. Head space concentration based on Henry's Law.	Submerged	None
T23	1Q2021	502108	4226763	Fixed Roof	Yes	Vertical		Amine Surge/Deinventory Tank	0.01 psia at 100 degF	18	63,943	Vent to flare	Submerged	None
T24 T25	1Q2021 1Q2021	502195	4226684	Fixed Roof	Yes	Vertical		Fresh Amine Tank	0.01 psia at 100 degF	18	63,943	Vent to ATM as Lean Amine  Vent to ATM. Low Vapor Pressure Material.  Drain drum located in sump, vent not	Submerged	None
Tac	1Q2021	502210	4226665	Fixed Roof	Yes	Horizontal	Default	Amine Containment Tank	0.01 psia at 100 degF	18	793	modeled. TBD	Submerged Submerged	None None
T26	1Q2021 1Q2021	502552	4226069	Fixed Roof		Vertical	Default	Water Trt Sulfuric Acid Tank	TBD	TBD	6,076	TBD	Submerged	None
T27	1Q2021 1Q2021	502575	4226069	Fixed Roof		Vertical	Default	Water Trt Caustic Tank	TBD	TBD	6,076	TBD	Submerged	None
T28 T29	1Q2021 1Q2021	502575	4225919	Fixed Roof		Vertical	Default	Potable Water Storage Tank	TBD	TBD	10,567	IBU		
	icals Storage	5025/3	1							TDD	TBD	TBD	Submerged	None
T30	1Q2021	502451	4226873	Container	Yes	NA		DMDS Storage Tank	TBD	TBD	218,735	TBD	Submerged	None
T31	1Q2021	502417	4226889	Fixed	Yes	Vertical	Default	Soda Ash Mix Tank	TBD	I IBU	210,/33			
	s Inventory								NA.	NA NA	TBD	TBD	Submerged	None
T32	1Q2021	502282	4226493	NA	Yes	Vertical		Raw Coal Bunker (Milling Feed)	NA NA	NA NA	TBD	TBD	Submerged	None
T33	1Q2021	502318	4226533	Fixed Roof	f Yes	Vertical		Fine Additive Storage Silo	NA	NA NA	TBD	TBD	Submerged	None
T34	1Q2021	502298	4226533	Fixed Roof	f Yes	Vertical	Default		NA NA	NA NA	TBD	TBD	Submerged	None
T35	1Q2021	502338	4226533	Fixed Root	f Yes	Vertical	Default	Sodium Sulfide Additive Storage Silo	INA					-

Table 22. PI-14 Volatile Organic Liquid Compound Storage
Parts A through E: Note this table is a comprehensive list, non organic storage is also included below

	raits A tinough	E: Note this table is a comprehensive last, non organic storage is				manager and a second and an a	puillally gravillation						100 4 VILLE OF THE	THE PARTY OF THE P	TARAGE STATE OF TH
1. Tank/ Unit ID	15, Control Techniques	16. Process Limitations/Additional Information	17. Tank Diameter: (ft)	18. Tank Height: (ft)	19. Tank Volume / Capacity:	20. Maximum Liquid Height:	21. External Floating Roof: Complete only if applicable.	22. Internal Floating Roof	23. Variable Vapor Space	24. Air Pollutant	25, Emission Factor	26, EF Source		29/30 NESHAP?	31, Applicability Determinati
T19	and different and a second and	NA	80.1	47.9	1,268,026	46.9	NA	NA	NA						
T20		NA	80.1	47.9	1,268,026	46.9	NA	NA	NA						
T21		NA	21.3	24	40,947	23	NA	NA	NA			<u> </u>	<del> </del>		
T22	Flare	NA	80.1	47.9	1,268,026	46.9	NA NA	NA NA	NA NA						
T23	Flare	NA	21.3	16.1	13,737	15.1	NA	NA	NA						
T24		NA	25.9	16.1	63,943	15.1	NA	NA	NA		Emission Factor values		<del>                                     </del>		
T25	N2 Blanket	NA	25.9	16.1	63,943	15.1	NA	NA	NA.	Lean Amine	from EPA's Tanks 4.0.9 used	AP 42	NA	NA	NA NA
T26	N2 Blanket		3.9	5.9	793	4.9 15.1	NA NA	NA NA	NA NA						
T27		98% H2SO4 Concentration; NO POLLUTANTS TO MODEL	7.9	16.1	6,076	15.1	NA NA	NA NA	NA NA						
T28		50% NaOH Concentration; NO POLLUTANTS TO MODEL	7.9	16.1	6,076 10,567	15.1	NA NA	NA NA	NA NA						
T29		NA	15.1	16.1	10,367	13,1	117	1	1						
Chemi			-	<del> </del>		NA NA	NA NA	NA	NA						
T30	NA TOO	NA	37	40	218,735	NA NA	NA	NA	NA						
T31	TBD	NA .	<del> </del>			<del>                                     </del>									
Solids	TBD	NA .	-			NA	NA	NA	NA						_
T32	TBD	NA NA	30	100	NA	NA	NA	NA	NA						
T33		NA NA	26	100	NA	NA	NA	NA	NA						
T34	TBD	NA NA	10	35	NA	NA	NA	NΑ	NA						
T35	TBD	INA													

## Table 23. Pl-18 Mineral Processing

Table 23a. Part A. Mineral Processing Information						8. Actual Capacity
1. Type of Process Material  Non Metallic Non Metallic Non Metallic Non Metallic Non Metallic Non Metallic Non Metallic Non Metallic Non Metallic Raw Coal Bunker	0 0	4. Unit ID EU-1501 EU-1502 EU-1503 EU-1000	5. Installation Date  1Q2021 1Q2021 1Q2021 1Q2021 1Q2021	6. Open/ Enclosed?  Enclosed  Enclosed  Enclosed  Enclosed  Enclosed	20 20 10 5000	20 20 20 10 5000

Table 23b. Part B. Dryer Details	12. Pate	13 Volume 14 Near Capacity	
9, Dryer Type: 100, Unit ID	11, installation Perforation Date Diameter / Mesh Size	Capacity (mmBtu/hr) 15. r	uel Used ural Gas
Coal Drying Heater EU-1007	1Q2021 NA	21273 55.8 Nat	ulai cas

able 23c. Part C. Storage a	17 Type of Storage	18. Storage Capacity (tons)	19. Unit ID	20. Installation Date	21 Storage Open of Totally Enclosed/ Covered?
Specification			<u>in krasing kanangan menin</u>	102021	Enclosed
oarse Additive 400-	Silo	1672	EU-1501		<b>↓</b>
2000 microns		<del> </del>	EU-1502	1Q2021	Enclosed
ine Additive <500	Silo	2576	E0-1302		<del></del>
nicrons		+	FU-1503	1Q2021	Enclosed
Sodium Sulfide mm sized	Silo	43	\	102021	Open
crystaline flakes		93010	EU-1003		Open
Illinois Basin Coal	Coal Pile Coal Pile	93010	EU-1005	1Q2021	<u>1</u> <u>Opci.</u>
Illinois Basin Coal	COBITIE				

## Table 23d. Part D. Emission Factors

Process Unit & (ID, if	23. Air Pollutant	24. Emission Factor	25. Source of Emission Factor
applicable)		0.003 gr/scf	AP-42
1	PM		AP-42
EU-1501.	PM-10	0.003 gr/scf	AP-42
	PM	0.003 gr/scf	AP-42
EU-1502	PM-10	0.003 gr/scf	AP-42
	PM 2.5	1.45 lb/acre/year	AP-42
EU-1503	PM-10	3.63 lb/acre/year	
	PM	0.028 lb/ton	AP-42
EU-1000	PM-10	0.021 ib/ton	AP-42

# Table 23e. Part E. Emission Controls and Limitations

		28. Process
26. Add-On Control	27. Control	Limitations:
Technology	NA NA	None
Baghouse	NA NA	None
Baghouse	NA NA	None
Baghouse	NA NA	None
Baghouse	<u>N</u>	

# Table 23f. Part F. Federal Rule Applicability

NA NA	NA	NA
source?	source	
applicable to this	applicable to this	
Standard (NSPS)	(NESHAP)	Determination
Performance	Hazardous Air Poliutants	
23.1.	Ettiission project	31140117
29. Is a New Source	Emission Standard for	31. Non-
	30. Is a National	

#### Table 24. FED-02 MACT Pre-Construction Review

#### Part B Emission Unit Information

#### Part C Compliance Method for New Affected Sources

4. Unit ID	5. HAP Name or Type of HAP	6. Quantity o	f HAP Emitted	7. Unit ID	8. Complaince Method Description	9. Control Efficiency
		Actual Emissions (tpy)	Potential to Emit (tpy)			(%)
EU-1007	Total HAPs	TBD	0.45	EU-1007	None	NA
20 200,	n-Hexane		0.432		İ	
	Formaldehyde		0.018			
	Toluene		8.15E-04			
	Benzene		5.04E-04			
	Nickel		5.04E-04			
EU-1501	Total HAPs are manganese compounds	TBD	2.00E-05	EU-1501	Baghouse	Typically >99.5% for PM
EU-1502	Total HAPs are manganese compounds	TBD	2.00E-05	EU-1502	Baghouse	Typically >99.5% for PM
EU-1504	Total HAPs are manganese compounds	TBD	3.62E-05	EU-1504	Baghouse	Typically >99.5% for PN
EU-2001	Total HAPs	TBD	1.04	EU-2001	None	NA
20 200	n-Hexane	_	0.992			
	Formaldehyde		0.0413			
	Toluene		1.87E-03	1		
	Benzene		1.16E-03	4		
	Nickel		1.16E-03		B.L.	NA NA
EU-2002	Total HAPs	TBD	0.43	EU-2002	None	IVA
	n-Hexane	_	0.48	-		
	Formaldehyde	_	0.017 7.72E-04	-		
	Toluene		4.77E-04			
	Benzene Nickel	_	4.77E-04	1		
EU-2003	Total HAPs	TBD	0.07	EU-2003	None	NA
	n-Hexane		0.0698			
	Formaldehyde		2.91E-03			
	Toluene		1.32E-04		1	
	Benzene	_	8.14E-05	4		
	Nickel		8.14E-05	<b>-</b>		
EU-2004	Total HAPs	TBD	1.26	EU-2004	None	NA
	n-Hexane Formaldehyde	$\dashv$	0.0502			
	Toluene		2.28E-03			
	Benzene		1.41E-03	7	1	
	Nickel	<del></del>	1.41E-03			
EU-2006	Total HAPs are manganese compounds	TBD	2.40E-05	EU-2006	Baghouse	Typically >99.5% for P
EU-2007	Total HAPs are manganese compounds	TBD	3.60E-05	EU-2007	Baghouse	Typically >99.5% for P
EU-3001	Total HAPs	TBD	0.31	EU-3001	None	NA NA
	n-Hexane		0.29	_		
	Formaldehyde		0.01	_		
	Toluene		5.50E-04			
	Benzene		3.40E-04		1	
	Nickel		3.40E-04			

Table 24. FED-02 MACT Pre-Construction Review

#### Part B Emission Unit Information

# Part C Compliance Method for New Affected Sources

4. Unit ID	5, HAP Name or Type of HAP	6, Quantity o	f HAP Emitted	7. Unit ID	8. Complaince Method Description	9. Control Efficiency
		Actual Emissions (tpy)	Potential to Emit (tpy)			(%)
	Total HAPs	TBD	0.31	EU-3002	None	NA NA
EU-3002	n-Hexane	-	0.29		[ ]	
	Formaldehyde		0.01		ļ	
	Toluene		5.50E-04	•		}
		┪	3,40E-04	1		
	Benzene	-{	3.40E-04	1		
	Nickel	TBD	0.683	EU-4001	Flare	98% DRE
EU-4001	Total HAPs	- '''	0.07	1		
	Benzene	-	0.185			
	Toluene		0.232	1	1	
	Xylenes	_	0.002	1		
	Phenols		0.006	4		
	o-cresol		0.002	+		
	m+p-cresol		0.185		1	_
	n-hexane			EU-6000	None	NA
EU-6000	Total HAPs	TBD	0.555	- 50-0000	"	
	n-Hexane	_	0.526		1	
	Formaldehyde		0.022		1	
	Toluene		9.93E-04	_		
	Benzene		6.13E-04	4		
	Nickel		6.13E-04		<del></del>	
EU-6006	Total HAPs	TBD	0.002	EU-6006	None	NA NA
EU-6008	Total HAPs	TBD	0.04	EU-6008	None	NA NA
EU-7003	Methanol	TBD	12.19	EU-7003	None	NA
EU-7004	Methanol	TBD	12.19	EU-7004	None	NA
	Benzene	TBD	0.10930395	7 FUGVCC	LDAR	*See attachments
FUGVCC	Toluene	_	0.29065694	17		H102-2000-EV-CAL-EV
	Xylenes		0.36418246	58		0001,
	Phenols		0.00372549	92	1	·
	o-cresol		0.0088033	76	ļ	H102-4000-EV-CAL-EV
	m+p-cresol	<b>-</b>	0.0037254	92	l	0001
	n-hexane		0.2901647	85		
FUGPRD	Benzene	TBD	0.0103088	38 FUGPRD	LDAR	*See attachments H102-2000-EV-CAL-EV
	Toluene		0.0274617		ļ	0001,
	Xylenes		0.0343570	99	1	
	Phenols		0.0003464	74	1	H102-4000-EV-CAL-EV
	o-cresol		0.0008267	756		0001
	m+p-cresol		0.0003464	174		

#### KBA

### FUGITIVE AIR EMISSION INVENTORY CALCULATIONS

BRIK ADMIT DOMINAL	Melana, mare water			,				-	1 4 '
JOB NO.:	H102	DOC. NO.: H102-2000-EV-CAL-EV2-0001	Rev:	A	0	1			
CLIENT:	Riverview Energy Corporation	SUBJECT: Piping and Equipment Fugitives	Date:	8-Jan-18	15-Jan-18	23-Jan-18			
		BASIS: Reference & PFD Factored Equipment	By:	RN	RN	RN			
PROJECT:	DCH Facility	DASIS. Relationed and the factorial Equipment	Check:	SAL	SAL	SAL			
LOCATION:	Dale, IN			+					
UNIT:	VCC	100	Appr.:			·F)			
UNIT No.	2000		Purpose:	IF1	IFI	(11)	L	1	

UNIT NO. A	2000												
LINE REV		ST STANFISHER		NEIDEN DE LE CONTROL DE LA CON	PR	OJECT DEFINITI	ON			The state of the s			
1	*3274.	***************************************									UTM Coordina	ton for Droposs	Unit
2	Revision	History		SHADING LEGEND:	ENTRY	LINKED	CALC	GOAL SEEK	CHECK	SUM	Perimeter		Northing (m)
3	Α		for Checking								Corner 1	Lusting (sin)	1
4	0	T&C PFD B	asis, MatBal Streams Aggregated								Corner 2		
5	1										Corner 3		
6	2										Corner 4		
7	3										Corner 5		
8	4										Corner 6		
9											Corner 7		
10											Corner 8		
11	TABLE O	F CONTENT											
12	SECTION	LINE	DESCRIPTION										
13	1	35	Emissions Summary										
14	2	60	Speciated Emissions Summary	i- D									
15	3	78	Federal Regulatory Applicability - Evaluation Bas	SIS Remarks	Contore								
16	4	141	Reference Emission Factors for Piping Compone	ett Types III muusukat et Dooien Coocification	ne								
17	5	204	Reference Primary Control Credit % for Equipme	Decarame	113								
18	6	250	Reference Secondary Control Credit % for LDAR Evaluation Basis (Emission Factors, Equipment	Docian Specifications	and I DAR Pro	grams							
19	7	277	Available Material Balance Data Input	Design opeometrons,	, und LDrux	g. w							
20	8	327 371	Speciation Data for Adjusting Material Balance										
21	9	420	Adjusted Material Balance										
22	10 11	464	Material Balance Stream Aggregation for Proces	s Areas - As Needed									
23	12	529	Process Stream or Area Service & LDAR Applica	bility Determinations									
24 25	13	595	Fugitive Equipment Counts and Factoring Basis	, In lieu of Direct P&ID	Count								
26	14	712	Final Equipment Counts Evaluated										
27	15	762	Undifferentiated Fugitive Emissions (as VOC) Ba	ased Upon Initial Source	ce Count Totals								
28	16	816	Controlled Fugitive Emissions by Equipment Ty	pe, Process Stream or	Area								
29	17	866	Speciated Fugitive Emissions by Process Stream	n or Area									
30	1 18	926	NOTES										
31	1					-							
32	1												

1 Emissions Summary

Emission Factor Set Use	d :	TCEQ-F	Refining					Equipment Design Control	Program Control	Overall Fugitive Control			Controlled Fugi	tive Emissions		
		Em. Factor	Equipment	u	Incontrolled Fug	gitive Emission		Efficiency	Efficiency	Efficiency	Contingency	ka/hr	MT/vr	lb/hr	ton/yr	Remarks
ugitive Emission Source	Service	kg/hr	Counts	kg/hr	MT/yr	lb/hr	ton/yr	%	%	%	%	0.04163	0.36470	0.09178	0.40200	Streams with vapor pressure less than 0.002 psia @ 68 degF are excluded from fugitive evaluations
lives	Gas	0.0268	3	0.08	0.70	0.18	0,78	0	97	97	50%		0.09155	0.02304	0.10092	Final valve counts have most uncertainty until P&ID's are available in later engineering phases.
	Light Liguid	0.0109	32	0.35	3.05	0.77	3.36	0	97	97	50%	0.01045	0.09133	0.11016	0.48250	
	Heavy Liquid	0.0109	153	1.67	14.59	3,67	16.08	0	97	97	50%	0,04997	0.45772	0,16368	0.71690	Double Mechanical Seals per API Seal Plans provided on all LL & HL pumps due to process conditions
ımps	Light Liquid	0,1139	18	2.05	17.95	4.52	19.79	80	85	97	0%	0.07424	1,07667	0.27096	1,18681	Diddo Aldonalina.
cludes Vessel Agitators)	Heavy Liquid	0.0209	19	0.40	3.47	0.87	3.83	80	0	80	0%	0.12291	2,68044	0.67458	2,95465	Reactor and other large vessel flanges are welded due to high process pressures
anges / Connectors	Ali	0.00025	1036	0.26	2.26	0.57	2.50	0	30	30	25%	0.30599		0.00000	0.00000	(0.000)
ressure Relief Valves	Gas	0.3500	19	6,65	58.25	14.66	64.21	100	97	100	15%	0.00000	0.00000	0.00000	0.00000	
	Liquids	0.3500	90	31.50	275.94	69.44	304.17	100	0	100	15%	0.00000	0.00000	0.00000	0.00000	Venting controlled by flare
ompressors	All	1.3990	1	1.40	12.26	3,08	13.51	100	85	100	15%	0,00000	0.00000	0.00000	0.00000	Capped, biinded, or double block primary design.
pen-Ended Lines/Valves	Ali	0.00510	90	0.46	4,02	1.01	4.43	100	85	100	15%	0.00000	0.00000	0.00000	0.00000	Closed loop system designs used
ampling Connections	All	0.03300	205	6.77	59.26	14.91	65.32	100	85	100	15%	0.00000	0.00000	0,00000	0.00000	
onnectors - Miscellaneous	All	0.00025	0	0.00	0.00	0.00	0.00	0	0	0	15%	1,49479	13.09438	3,29542	14,43393	50% of Drains are hardpiped with 100% control efficiency (entered as Secondary Efficiency)
rains	All	0.02917	205	5.98	52.38	13,18	57.74	50	50	75	15%		0,00000	0,00000	0.00000	
thers		0.00000	0	0.00	0.00	0.00	0,00	0	0	0	15%	0.00000	0,00000	0,00000	0.00000	
O&G Others - Gas/Vapor	All	0.00000	0	0.00	0.00	0.00	0.00	0	0	0	15%	0.00000	0.00000	0.00000	0.00000	
O&G Others - Liquid	All	0.00000	0	0.00	0.00	0.00	0.00	0	1 0	1 0	15%	W-1-7-W-12-1-W-12-1-W-12-1-W-12-W-12-W-1	18.396	4.630	20.278	
		Tatalone	4974	57.55	504.14	126.88	555,72	100				2.100	10.000	**************************************	Transfer Corners	· · · · · · · · · · · · · · · · · · ·

2 Speciated Emissions Summar

							Contingency				13-75-4	ton/yr
Compound	Fugitive	gram/s	kg/hr	MT/yr	lb/hr	ton/yr	%	gram/s	kg/hr	MT/yr	lb/hr	
-	HAP	0.0025	0.009	0.079	0.020	0.087		0.0031	0.011	0.099	0.025	0.109
Benzene	HAP	0.0067	0,024	0.211	0.053	0.233		0.0084	0.030	0.264	0.066	0.291
Toluene		0.0084	0.030	0.264	0.067	0.291	1 I	0.0105	0.038	0.330	0.083	0.364
Xylenes	HAP		0.000	0.003	0.001	0.003		0.0001	0.000	0.003	0.001	0.004
Phenois	HAP	0.0001			0.002	0.007	!	0.0003	0,001	0.008	0.002	0.009
o-cresol	HAP	0.0002	0.001	0.006			25%	0.0001	0.000	0.003	0,001	0.004
m+p-cresol	HAP	0,0001	0.000	0.003	0.001	0.003	23/8		0.030	0.263	0,066	0.290
n-hexane	HAP	0.0067	0,024	0.211	0.053	0.232		0.0083	0,030	0,203	0.000	
							<b>l</b>					
							1					
							1					
With the contract of	Sum = HAP	0,025	0.089	0,777	0,196	0,856		0,031	0.111	0.971	0.244	1.071



### FUGITIVE AIR EMISSION INVENTORY CALCULATIONS

-	MM					1				
JOB NO.:	H102	DOC. NO.:	H102-4000-EV-CAL-EV2-0002	Rev:	A	0	1		- 3	
CLIENT:	Riverview Energy Corporation	SUBJECT:	Piping and Equipment Fugitives	Date:	8-Jan-18	23-Jan-18				
	DCH Facility	BASIS:	Reference & PFD Factored Equipment	By:	RN	RN				
LOCATION:				Check:	SAL	SAL		!		
				Appr.:						i
UNIT:	Offsites Product Storage and Handling		A177	Purpose:	IEI	(F)				
UNIT No.	4000			şғигрозе.		1 ",				

UNIT No.	40	000																	
ESPONSONAL RESIDE	155 K.O 213	KSSECTED TO THE SECOND		SANGER AND THE SANGER					PROJ	GT DEFINITIO	N COLUMN		A THE STATE OF THE						
LINE R	EV	PARTICIONE PROPERTY OF			Name of the Party	.,									-				
1	┥.	Davisian H	lintamı			Γ	SHADING L	EGEND:	ENTRY	LINKED	CALC	GOAL SEEK	CHECK	SUM	-	TM Coordinate			
2	_   -	Revision H	Initial Setup for Checking			٠									P	erimeter	Easting (m)	Northing (m)	
3			T&C PFD Basis, MatBal St	rooms Aggreg	ated										<u>[0</u>	omer 1			-
4		_	T&C PFD Basis, Matbai St	learns Aggreg	lated										<u>ic</u>	orner 2			
5	_	1													c	corner 3			
6	ļ	2													ļc	Corner 4			1
7		3													įc	Corner 5			
8		4														Corner 6			
9	_														c	Corner 7			
10															Ī	Corner 8			
11			CONTENTS												_				
12		SECTION	LINE DESCRIPTION																
13		1	35 Emissions S	-															
14	_	2	60 Speciated Er	missions Sun	nmary	lucation Donie	Domarke												
15		3	78 Federal Regi 141 Reference E	ulatory Applic	cabinly - Eva	- Composes	t Tunne in In	dustrial Sort	ors										
16		4		mission Fact	ors for Pipili	y Componen	Docion Sne	uusuus occi rifirations	010										
17		5	204 Reference P	rimary Contri	of Credit % ic	/ for IDADD	rograme	CHICAGONS											
18		6		econdary Co	ntro: Credit 7	o IUI LUAK F	rograms neign Specifi	cations and	I DAR Progr	ems									
19	_	7					esign opecin	Cadono, and	LD/III 1 10g.										
20	_	8		iterial Balanc															
21		9	•	ata for Adjus		Dalaite													
22		10	•	terial Balanc	v Δααroastion	for Process	Areas . As N.	eeded											
23		11	464 Material Bali	eam or Area S	nggregation Service & I D	AR Annlicahi	ility Determin	ations											
24		12		soment Corr	ofe and Facto	ring Basis I	n lieu of Dire	ct P&ID Com	nt										
25		13		nent Counts		Dagio, i	0, 0,10												
26	-	14 15	712 Final Equipr 762 Undifferenti	nem Counts ated Fugitive	Emissione f	as VOCI Base	ed Upon Initi	al Source Co	unt Totals										
27		15 16	816 Controlled F	ugitive Emis	sions by For	ipment Tyne	Process St	ream or Area	i										
28		17	866 Speciated F	ugitive Emiss	sions by Proc	ess Stream	or Area												
29		18	926 NOTES	ugiuve Limes	510113 DJ 1 100	ococ otroum													
30		10	920 NOTES																
31	$\dashv$																		
32	<b>-</b>																		
33																			
34 35		1	Emissions Summary																
		•	Ettinooioilo odittiive																
											Primary	Secondary	Overali						
36 37			Emission Factor Set Use	ed :	TCEQ-F	Refining	l				Equipment	LDAR	Overali Fugitive						
37			Emission Factor Set Use	ed:	TCEQ-R	Refining					Equipment Design Control	LDAR Program Control	Fugitive Control				uha Emissione		1
37 38			Emission Factor Set Use	ed :	TCEQ-R	Refining Equipment	U	ncontrolled Fu	gitive Emission		Equipment Design Control Efficiency	LDAR Program Control Efficiency	Fugitive Control Efficiency	Contingency		Controlled Fug			419
37 38 39				ed :			U kg/hr	ncontrolled Fu MT/yr	gitive Emission lb/hr	ton/yr	Equipment Design Control	LDAR Program Control Efficiency %	Fugitive Control Efficiency %	%	kg/hr	MT/yr	lb/hr	ton/yr	Change with
37 38 39 40			Fugitive Emission Source		Em. Factor	Equipment				ton/yr 0.00	Equipment Design Control Efficiency %	LDAR Program Control Efficiency %	Fugitive Control Efficiency %	% 50%	kg/hr 0,00000	MT/yr 0.00000	1b/hr 0.00000	ton/yr 0,00000	
37 38 39 40 41				Service	Em. Factor kg/hr	Equipment Counts 0	kg/hr 0,00 0,37	MT/yr 0.00 3.24	1 <b>b/hr</b> 0.00 0.82	ton/yr 0.00 3.57	Equipment Design Control Efficiency % 0	LDAR Program Control Efficiency % 97	Fugitive Control Efficiency % 97	% 50% 50%	kg/hr 0,00000 0,01110	MT/yr 0.00000 0.09727	1b/hr 0.00000 0.02448	0,00000 0.10722	
37 38 39 40			Fugitive Emission Source	Service Gas	Em. Factor kg/hr 0.0268	Equipment Counts	<b>kg/hr</b> 0,00	MT/yr 0.00 3.24 0.00	0.00 0.82 0.00	0.00 3.57 0.00	Equipment Design Control Efficiency % 0 0	LDAR Program Control Efficiency % 97 97	Fugitive Control Efficiency % 97 97	% 50% 50% 50%	kg/hr 0,00000 0.01110 0.00000	MT/yr 0.00000 0.09727 0.00000	1b/hr 0.00000 0.02448 0.00000	0,00000 0,10722 0,00000	Final valve co
37 38 39 40 41 42			Fugitive Emission Source	Service Gas Light Liquid	Em. Factor kg/hr 0.0268 0.0109	Equipment Counts  0 34 0 4	kg/hr 0,00 0,37	MT/yr 0.00 3.24 0.00 3.99	0.00 0.82 0.00 1.00	0.00 3.57 0.00 4.40	Equipment Design Control Efficiency % 0 0 0 80	LDAR Program Control Efficiency % 97 97 97 85	Fugitive Control Efficiency % 97 97 97	% 50% 50% 50% 0%	kg/hr 0,00000 0,01110 0,00000 0,01492	MT/yr 0.00000 0.09727 0.00000 0.13067	1b/hr 0.00000 0.02448 0.00000 0.03289	0,00000 0,10722 0,00000 0,14404	Final valve co
37 38 39 40 41 42 43			Fugitive Emission Source Valves	Service Gas Light Liquid Heavy Liquid	Em. Factor kg/hr 0.0268 0.0109 0.0109	Equipment Counts  0 34 0 4 0	kg/hr 0.00 0.37 0.00 0.46 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00	1b/hr 0.00 0.82 0.00 1.00 0.00	0.00 3.57 0.00 4.40 0.00	Equipment Design Control Efficiency % 0 0 0 0 80 80	LDAR Program Control Efficiency % 97 97 97 97 055	Fugitive Control Efficiency % 97 97 97 97	% 50% 50% 50% 0%	kg/hr 0,00000 0,01110 0,00000 0,01492 0,00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000	0,00000 0.10722 0.00000 0.14404 0.00000	Final valve of Double Mech
37 38 39 40 41 42 43 44			Fugitive Emission Source Valves	Service Gas Light Liquid Heavy Liquid Light Liquid	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139	Equipment Counts  0 34 0 4 0 141	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04	MT/yr 0.00 3.24 0.00 3.99 0.00	0.00 0.82 0.00 1.00 0.00	0.00 3.57 0.00 4.40 0.00 0.34	Equipment Design Control Efficiency % 0 0 0 0 80 80 0	LDAR Program Control Efficiency % 97 97 97 85 0	Fugitive Control Efficiency % 97 97 97 97 80	% 50% 50% 50% 0% 0% 25%	kg/hr 0,00000 0.01110 0.00000 0.01492 0.00000 0.03209	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074	0,00000 0,10722 0,00000 0,14404 0,00000 0,30986	Final valve or Double Mech
37 38 39 40 41 42 43 44 45			Fugitive Emission Source Valves  Pumps (Includes Vessel Agilators)	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025	Equipment Counts  0 34 0 4 0 141	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31	b/hr	0.00 3.57 0.00 4.40 0.00 0.34	Equipment Design Control Efficiency % 0 0 0 80 80 0	LDAR Program Control Efficiency % 97 97 97 97 97 97 97 97 97	Fugitive Control Efficiency % 97 97 97 97 80 30	% 50% 50% 50% 0% 0% 25%	kg/hr 0,00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074	0,00000 0.10722 0.00000 0.14404 0.00000	Final valve of Double Mech
37 38 39 40 41 42 43 44 45 46			Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500	Equipment Counts  0 34 0 4 0 141 0 0	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00	0.00 0.82 0.00 1.00 0.00 0.08 0.00	0.00 3.57 0.00 4.40 0.00 0.34 0.00	Equipment Design Control Efficiency % 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	LDAR Program Control Efficiency % 97 97 97 97 95 0 30 97	Fugitive Control Efficiency % 97 97 97 97 90 30 100 100	% 50% 50% 50% 0% 0% 25% 15%	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000	ton/yr 0,00000 0.10722 0,00000 0.14404 0,00000 0.30986 0,00000	Pinal valve of Double Mechanical Reactor and
37 38 39 40 41 42 43 44 45 46			Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500	Equipment Counts  0 34 0 4 0 141 0 0 33 34 0 34 0 34 0 3	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 4.20	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77	1b/hr 0.00 0.82 0.00 1.00 0.00 0.08 0.00 0.00 9.25	0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53	Equipment Design Control Efficiency % 0 0 0 0 80 80 0 100 100 100 100 100 100	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85	Fugitive Control Efficiency % 97 97 97 97 90 30 100 100 100	% 50% 50% 50% 0% 0% 25% 15% 15%	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000	ton/yr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000	Pinal valve of Double Mech Reactor and Venting control
37 38 39 40 41 42 43 44 45 46 47 48			Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 1.3990 0.00510	Equipment Counts  0 34 0 4 0 141 0 0 34	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 4.20 0.02	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 96.77 0.18	1b/hr 0.00 0.82 0.00 1,00 0.00 0.08 0.00 0.00 9.25	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20	Equipment Design Control Efficiency % 0 0 0 80 80 0 100 100 100 100 100 100 1	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85	Fugitive Control Efficiency % 97 97 97 97 97 90 100 100 100	% 50% 50% 50% 0% 0% 25% 15% 15% 15%	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000 0.00000 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000	ton/yr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000	Pinal valve of Double Mech Reactor and Venting control Capped, biln
37 38 39 40 41 42 43 44 45 46 47 48			Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves Compressors	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 1.3990 0.00510	Equipment Counts  0 34 0 4 0 141 0 3 3 4 8	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55	Equipment Design Control Efficiency % 0 0 0 80 80 0 100 100 100 100 100 100 1	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85	Fugitive Control Efficiency % 97 97 97 97 97 90 30 100 100 100 100 100 100 100 100 100	% 50% 50% 50% 0% 0% 25% 15% 15% 15%	kg/hr 0,00000 0,01110 0,00000 0,01492 0,00000 0,03209 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000	ton/yr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000	Pinal valve of Double Mech Reactor and Venting cont Capped, biln
37 38 39 40 41 42 43 44 45 46 47 48 49 50			Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 1.3990 0.00510	Equipment Counts  0 34 0 4 0 141 0 0 34	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 4.20 0.02	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 96.77 0.18 2.31 0.00	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00	Equipment Design Control Efficiency % 0 0 0 0 80 80 80 100 100 100 100 100 10	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85 85	Fugitive Control Efficiency % 97 97 97 97 97 80 30 100 100 100 100 100 100 100 0 0	% 50% 50% 50% 60% 60% 60% 60% 60% 60% 60% 60% 60% 6	kg/hr 0,00000 0,01110 0,00000 0,01492 0,00000 0,03209 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000	ton/yr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000	Pinal valve or  Double Mech  Reactor and  Venting cont Capped, bin Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51			Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00525 0.3500 1.3990 0.00510 0.00300 0.00025	Equipment Counts  0 34 0 4 0 141 0 0 3 4 6 0 8	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 4.20 0.02 0.26 0.00 0.23	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 96.77 0.18 2.31 0.00 2.04	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25	Equipment Design Control Efficiency % 0 0 0 0 80 80 80 100 100 100 100 100 50	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85 85 85	Fugitive Control Efficiency % 97 97 97 97 97 99 100 100 100 100 100 100 100 100 100	% 50% 50% 50% 60% 60% 60% 60% 60% 60% 60% 60% 60% 6	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,14404 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Final valve or  Double Mech  Reactor and  Venting cont Capped, biln  Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52			Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All	Em. Factor kg/hr 0.0268 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 1.3990 0.00510 0.03300 0.0025 0.02917	Equipment Counts  0 34 0 4 0 141 0 0 33 4 0 8 0 8	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.04 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 96.77 0.18 2.31 0.00 2.04	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25	Equipment Design Control Efficiency % 0 0 0 80 80 0 100 100 100 100 100 0 50 0 0 0 0 0 0	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85 85 85 65 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 80 30 100 100 100 100 0 75	% 50% 50% 50% 60% 60% 60% 60% 60% 60% 60% 60% 60% 6	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,14404 0,00000 0,30985 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Final valve or  Double Mech  Reactor and  Venting cont Capped, biln  Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53			Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 1.3990 0.00510 0.03300 0.0025 0.00217 0.00000	Equipment Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 0 0 0 0 0 0 0 0 0 0	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 4.20 0.02 0.26 0.00 0.23 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 96.77 0.18 2.31 0.00 2.04 0.00	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.26 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 0 80 80 0 100 100 100 100 0 50 0 0 0 0 0 0 0 0	LDAR Program Control Efficiency % 97 97 97 985 0 30 97 0 85 85 85 0 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 80 30 100 100 100 100 0 75 0 0 0	% 50% 50% 50% 60% 60% 60% 60% 60% 60% 60% 60% 60% 6	kg/hr 0.00000 0.01110 0.00000 0.01482 0.00000 0.03208 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.12860 0.00000	ton/yr 0.00000 0.10722 0.00000 0.14404 0.00000 0.30986 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Final valve or  Double Mech  Reactor and  Venting cont Capped, biln  Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54			Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 1.3990 0.00510 0.03300 0.0025 0.02917 0.00000 0.00000	Equipment Counts  0 34 0 4 0 141 0 0 33 4 6 0 6 8 0 0 0 0 0	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 2.04 0.00 0.00	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 80 80 0 100 100 100 100 100 0 50 0 0 0 0 0 0	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85 85 85 65 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 80 30 100 100 100 100 0 75	% 50% 50% 50% 60% 60% 60% 60% 60% 60% 60% 60% 60% 6	kg/hr 0.00000 0.01110 0.00000 0.01482 0.00000 0.03209 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,0000 0,10722 0,00000 0,14494 0,00000 0,30986 0,00000	Final valve or  Double Mech  Reactor and  Venting cont Capped, biln  Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55			Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 0.3500 1.3990 0.00510 0.03300 0.0025 0.00217 0.00000	Equipment Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 0 0 0 0 0 0 0 0 0 0	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 4.20 0.02 0.26 0.00 0.23 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 96.77 0.18 2.31 0.00 2.04 0.00	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.26 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 0 80 80 0 100 100 100 100 0 50 0 0 0 0 0 0 0 0	LDAR Program Control Efficiency % 97 97 97 985 0 30 97 0 85 85 85 0 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 80 30 100 100 100 100 0 75 0 0 0	% 50% 50% 50% 60% 60% 60% 60% 60% 60% 60% 60% 60% 6	kg/hr 0.00000 0.01110 0.00000 0.01482 0.00000 0.03208 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,1404 0,00000 0,30986 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Streams with Final valve or Double Mech Reactor and Venting cont Capped, blin Closed loop 50% of Drain
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56			Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 1.3990 0.00510 0.03300 0.0025 0.02917 0.00000 0.00000	Equipment Counts  0 34 0 4 0 141 0 0 33 4 6 0 6 8 0 0 0 0 0	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 2.04 0.00 0.00	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 0 80 80 0 100 100 100 100 0 50 0 0 0 0 0 0 0 0	LDAR Program Control Efficiency % 97 97 97 985 0 30 97 0 85 85 85 0 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 80 30 100 100 100 100 0 75 0 0 0	% 50% 50% 50% 60% 60% 60% 60% 60% 60% 60% 60% 60% 6	kg/hr 0.00000 0.01110 0.00000 0.01482 0.00000 0.03209 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,1404 0,00000 0,30986 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Pinal valve composite Machine Reactor and Venting control Capped, billing Closed loop in the Closed loop in
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57			Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gast/Vapor O&G Others - Liquid	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 1.3990 0.00510 0.03300 0.0025 0.02917 0.00000 0.00000	Equipment Counts  0 34 0 4 0 141 0 0 33 4 6 0 6 8 0 0 0 0 0	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 2.04 0.00 0.00	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 0 80 80 0 100 100 100 100 0 50 0 0 0 0 0 0 0 0	LDAR Program Control Efficiency % 97 97 97 985 0 30 97 0 85 85 85 0 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 80 30 100 100 100 100 0 75 0 0 0	% 50% 50% 50% 60% 60% 60% 60% 60% 60% 60% 60% 60% 6	kg/hr 0.00000 0.01110 0.00000 0.01482 0.00000 0.03209 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,1404 0,00000 0,30986 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Final valve or  Double Mech  Reactor and  Venting cont Capped, biln  Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 68		2	Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 1.3990 0.00510 0.03300 0.0025 0.02917 0.00000 0.00000	Equipment Counts  0 34 0 4 0 141 0 0 33 4 6 0 6 8 0 0 0 0 0	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 2.04 0.00 0.00	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 0 80 80 0 100 100 100 100 0 50 0 0 0 0 0 0 0 0	LDAR Program Control Efficiency % 97 97 97 985 0 30 97 0 85 85 85 0 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 80 30 100 100 100 100 0 75 0 0 0	% 50% 50% 50% 60% 60% 60% 60% 60% 60% 60% 60% 60% 6	kg/hr 0.00000 0.01110 0.00000 0.01482 0.00000 0.03209 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,1404 0,00000 0,30986 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Final valve or  Double Mech  Reactor and  Venting cont Capped, biln  Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59		2	Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gast/Vapor O&G Others - Liquid	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 1.3990 0.00510 0.03300 0.0025 0.02917 0.00000 0.00000	Equipment Counts  0 34 0 4 0 141 0 0 3 4 8 0 0 2 202	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 2.04 0.00 0.00 0.00	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 0 80 80 0 100 100 100 100 0 0 0 0	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85 85 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 80 30 100 100 100 0 75 0 0	% 50% 50% 50% 60% 60% 60% 60% 60% 60% 60% 60% 60% 6	kg/hr 0.00000 0.01110 0.00000 0.01482 0.00000 0.03209 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,1404 0,00000 0,30986 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Final valve or  Double Mech  Reactor and  Venting cont Capped, biln  Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60		2	Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gast/Vapor O&G Others - Liquid	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All Figure All All All Figure All All All All All All All All All Al	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.00025 0.3500 1.3990 0.0051 0.03500 0.0051 0.03500 0.00000 0.00000 0.000000 0.000000 0.000000	Equipment Counts  0 34 0 4 0 141 0 0 3 4 8 0 0 8 0 0 8 0 0 0 0 0 0 0 0 0 0 0 0	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 4.20 0.02 0.26 0.00 0.23 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 0.00 36.77 0.18 2.31 0.00 2.04 0.00 0.00 0.00 0.00 0.00	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 0 80 80 100 100 100 100 0 0 0 0 0	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 5 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 97 90 100 100 100 100 100 0 75 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	% 50% 50% 50% 60% 0% 0% 0% 15% 15% 15% 15% 15% 15% 15% 15% 15%	kg/hr 0,00000 0,01110 0,00000 0,01492 0,00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,1404 0,00000 0,30986 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Final valve or  Double Mech  Reactor and  Venting cont Capped, biln  Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 68 59 60 61		2	Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor O&G Others - Liquid	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid Haavy Liquid All Gas Liquids All All All All All All Figure All All All All All All All All All Al	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.3500 0.3500 1.3990 0.0051 0.00300 0.00000 Totals =	Equipment Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 8 0 0 202	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 4.20 0.02 0.26 0.00 0.00 0.00 0.00 0.00 0	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 96.77 0.18 2.31 0.00 2.04 0.00 0.00 48.34	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 0 80 80 0 100 100 100 100 100 100	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85 85 85 0 0 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 80 30 100 100 100 100 0 0 75 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	% 50% 50% 50% 60% 60% 60% 60% 60% 60% 60% 60% 60% 6	kg/hr 0,00000 0,01110 0,00000 0,01492 0,00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,1404 0,00000 0,30986 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Final valve or  Double Mech  Reactor and  Venting cont Capped, biln  Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62		2	Fugitive Emission Source Valves  Pumps (Includes Vessel Agilators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions St Compound	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All Figure All All All Figure All All All All All All All All All Al	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.0055 0.3500 0.3500 0.3500 0.00510 0.03000 0.00000 0.00000 0.00000 0.00000 Totals **	Equipment Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 202  kg/hr 0,001 0,002	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 4.20 0.02 0.28 0.00 0.00 0.00 0.00 5.58	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 2.04 0.00 0.00 3.90 0.00 0.00 0.00 0.00 0.00	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 0.00 0.00	Equipment Design (Control Efficiency) % 0 0 0 0 80 80 0 100 100 100 100 100 100	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85 85 85 0 0 0 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 99 97 80 30 100 100 100 100 100 100 100 100 100	% 50% 50% 50% 60% 0% 0% 25% 15% 15% 15% 15% 15% 15% 15% 15% 15% 1	kg/hr 0,00000 0,01110 0,00000 0,01492 0,00000 0,03209 0,00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,1404 0,00000 0,30986 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Final valve or  Double Mech  Reactor and  Venting cont Capped, biln  Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62 63		2	Fugitive Emission Source Valves  Pumps (Includes Vessel Agilators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions St  Compound Benzene	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid Haavy Liquid All Gas Liquids All All All All All All Figure All All All All All All All All All Al	Em. Factor kg/hr 0.0268 0.0109 0.1139 0.0209 0.0025 0.3500 0.3500 0.3500 0.3500 0.00510 0.00350 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Equipment Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 202    kg/hr 0.001 0.002 0.003	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 4.20 0.02 0.28 0.00 0.00 0.00 5.58	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 2.04 0.00 0.00 48.84	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 0 80 80 0 100 100 100 100 100 0 0 0	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85 85 0 0 0 0 0 0 0 0 0 0 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 99 100 100 100 100 100 100 100 100 100	% 50% 50% 50% 60% 0% 0% 25% 15% 15% 15% 15% 15% 15% 15% 15% 15% 1	kg/hr 0.00000 0.01110 0.00000 0.01492 0.00000 0.03209 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,1404 0,00000 0,30986 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Final valve or  Double Mech  Reactor and  Venting cont Capped, biln  Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62 63 64		2	Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions St  Compound Benzene Toluene	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All All Al	Em. Factor kg/hr 0.0268 0.0109 0.1139 0.00025 0.3500 0.3500 1.3990 0.00051 0.00310 0.00025 0.2217 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Equipment Counts  0 34 0 4 0 141 0 0 33 4 8 0 8 0 0 8 0 0 8 0 0 0 0 8 0 0 0 0 0	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 4.20 0.02 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 36.77 0.18 2.31 0.00 0.00 0.00 0.00 1.00 0.00 0.00 0	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 2.25 0.00 0.00 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85 85 0 0 0 0 0 0 0 0 0 0 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 80 30 100 100 100 0 75 0 0 0 MTf/yr 0.009 0.025 0.031	% 50% 50% 50% 60% 0% 0% 0% 15% 15% 15% 15% 15% 15% 15% 0.000 0.000	kg/hr 0.00000 0.01110 0.00000 0.011110 0.00000 0.03209 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,1404 0,00000 0,30986 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Final valve or  Double Mech  Reactor and  Venting cont Capped, biln  Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62 63 64 65		2	Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gast/Vapor O&G Others - Liquid  Speciated Emissions St  Compound Benzene Toluene Xylenes	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All All All All All All All All Hall All Hall All Hall All Hall Ha	Em. Factor kg/hr 0.0268 0.0109 0.1139 0.0209 0.0025 0.3500 0.3500 0.3500 0.3500 0.00510 0.00350 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Equipment Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 8 0 202    kg/hr 0.001 0.002 0.003 0.000	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 0.00 0.00 0.00 0.00	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 0.00 0.00 0.00 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 80 30 100 100 100 100 0 75 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	% 50% 50% 50% 60% 6% 6% 6% 6% 15% 15% 15% 15% 15% 15% 15% 15% 15% 15	kg/hr 0,00000 0,01110 0,00000 0,011110 0,00000 0,03209 0,000000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,1404 0,00000 0,30986 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Pinal valve or  Double Mech  Reactor and  Venting cont Capped, bin Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62 63 64 65 66		2	Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions St  Compound Benzene Toluene Xylenes Phenois	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All All Al	Em. Factor kg/hr 0.0268 0.0109 0.1139 0.00025 0.3500 0.3500 1.3990 0.00051 0.00310 0.00025 0.2217 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Equipment Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 8 0 0 202    kg/hr 0.001 0.002 0.000 0.000 0.000	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.02 0.26 0.00 0.23 0.00 0.00 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 96.77 0.18 2.31 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 0.00 0.00 0.00 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85 85 85 0 0 0 0 0 0 0 0 0 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 80 30 100 100 100 100 0 75 0 0 0 MT/yr 0.009 0.025 0.031 0.000 0.001	% 50% 50% 50% 60% 0% 0% 0% 15% 15% 15% 15% 15% 15% 15% 0.002 0.006 0.008 0.000	kg/hr 0,00000 0,01110 0,00000 0,01492 0,00000 0,03209 0,000000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,1404 0,00000 0,30986 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Pinal valve or  Double Mech  Reactor and  Venting cont Capped, bin Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62 63 64 65 66 67		2	Fugitive Emission Source Valves  Pumps (Includes Vessel Agilators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions St Compound Benzene Toluene Xylenes Phenols O-cresoi	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All All Al	Em. Factor kg/hr 0.0268 0.0109 0.1139 0.0209 0.00025 0.3500 1.3990 0.0051 0.03500 0.0051 0.00000 0.00000 Etais =   gram/s 0.0002 0.0000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Equipment Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 8 0 202    kg/hr 0.001 0.002 0.003 0.000	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 0.00 0.00 0.00 0.00	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 0.00 0.00 0.00 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 80 30 100 100 100 100 0 75 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	% 50% 50% 50% 60% 6% 6% 6% 6% 15% 15% 15% 15% 15% 15% 15% 15% 15% 15	kg/hr 0.00000 0.01110 0.00000 0.011110 0.00000 0.03209 0.00000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,1404 0,00000 0,30986 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Pinal valve or  Double Mech  Reactor and  Venting cont Capped, bin Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62 63 64 65 66 67 68		2	Fugitive Emission Source Valves  Pumps (Includes Vessel Agilators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions St  Compound Benzene Toluene Xylenes Phenols o-cresol m+p-cresol	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All All Al	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.3500 0.3500 1.3990 0.0051 0.00000 0.00000 Totals =  gram/s 0.0002 0.0000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Equipment Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 8 0 0 202    kg/hr 0.001 0.002 0.000 0.000 0.000	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.02 0.26 0.00 0.23 0.00 0.00 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 96.77 0.18 2.31 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 0.00 0.00 0.00 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85 85 85 0 0 0 0 0 0 0 0 0 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 80 30 100 100 100 100 0 75 0 0 0 MT/yr 0.009 0.025 0.031 0.000 0.001	% 50% 50% 50% 60% 0% 0% 0% 15% 15% 15% 15% 15% 15% 15% 0.002 0.006 0.008 0.000	kg/hr 0,00000 0,01110 0,00000 0,01492 0,00000 0,03209 0,000000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,1404 0,00000 0,30986 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Pinal valve or  Double Mech  Reactor and  Venting cont Capped, bin Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 60 61 62 63 64 65 66 67 68 69		2	Fugitive Emission Source Valves  Pumps (Includes Vessel Agilators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions St  Compound Benzene Toluene Xylenes Phenols o-cresol m+p-cresol	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All All Al	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.3500 0.3500 1.3990 0.0051 0.00000 0.00000 Totals =  gram/s 0.0002 0.0000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Equipment Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 8 0 0 202    kg/hr 0.001 0.002 0.000 0.000 0.000	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.02 0.26 0.00 0.23 0.00 0.00 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 96.77 0.18 2.31 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 0.00 0.00 0.00 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85 85 85 0 0 0 0 0 0 0 0 0 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 80 30 100 100 100 100 0 75 0 0 0 MT/yr 0.009 0.025 0.031 0.000 0.001	% 50% 50% 50% 60% 0% 0% 0% 15% 15% 15% 15% 15% 15% 15% 0.002 0.006 0.008 0.000	kg/hr 0,00000 0,01110 0,00000 0,01492 0,00000 0,03209 0,000000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,1404 0,00000 0,30986 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Final valve of Double Mech Reactor and Venting cont Capped, blin Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62 63 64 65 66 67 68 69 70 71		2	Fugitive Emission Source Valves  Pumps (Includes Vessel Agilators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions St  Compound Benzene Toluene Xylenes Phenols o-cresol m+p-cresol	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All All Al	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.3500 0.3500 1.3990 0.0051 0.00000 0.00000 Totals =  gram/s 0.0002 0.0000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Equipment Counts  0 34 0 4 0 141 0 0 33 4 8 0 0 8 0 0 202    kg/hr 0.001 0.002 0.000 0.000 0.000	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.02 0.26 0.00 0.23 0.00 0.00 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 96.77 0.18 2.31 0.00 0.00 0.00 0.00 0.00 0.00 0.00 0	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 0.00 0.00 0.00 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85 85 85 0 0 0 0 0 0 0 0 0 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 80 30 100 100 100 100 0 75 0 0 0 MT/yr 0.009 0.025 0.031 0.000 0.001	% 50% 50% 50% 60% 0% 0% 0% 15% 15% 15% 15% 15% 15% 15% 0.002 0.006 0.008 0.000	kg/hr 0,00000 0,01110 0,00000 0,01492 0,00000 0,03209 0,000000	MT/yr 0.00000 0.99727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,1404 0,00000 0,30986 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Pinal valve or  Double Mech  Reactor and  Venting cont Capped, bin Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62 63 64 65 66 67 68 69 70 71 72		2	Fugitive Emission Source Valves  Pumps (Includes Vessel Agilators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Connectors - Miscellaneous Drains Others O&G Others - Gas/Vapor O&G Others - Liquid  Speciated Emissions St  Compound Benzene Toluene Xylenes Phenols o-cresol m+p-cresol	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid All Gas Liquids All All All All All All All All All Al	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.3500 0.3500 1.3990 0.0051 0.00000 0.00000 Totals =  gram/s 0.0002 0.0000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Equipment Counts  0 34 0 141 0 141 0 0 3 4 8 0 0 202    kg/hr 0.001 0.002 0.003 0.000 0.0000 0.0002	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.00 4.20 0.02 0.28 0.00 0.00 0.00 0.00 0.00 0	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 96.77 0.18 2.31 0.00 2.04 0.00 0.00 0.00 0.00 0.00 0.00	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 0.00 0.00 0.00 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 0 80 80 80 0 100 100 100 100 100	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85 85 85 85 0 0 0 0 0 0 0 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 80 30 100 100 100 100 0 75 0 0 0 MT/yr 0.009 0.025 0.031 0.000 0.001	% 50% 50% 50% 60% 0% 0% 0% 15% 15% 15% 15% 15% 15% 15% 0.002 0.000 0.000 0.000	kg/hr 0,00000 0,01110 0,00000 0,01492 0,00000 0,03209 0,000000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,1404 0,00000 0,30986 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Final valve or  Double Mech  Reactor and  Venting cont Capped, biln  Closed loop
37 38 39 40 41 42 43 44 45 46 47 48 49 50 51 52 53 54 55 56 57 58 59 60 61 62 63 64 65 66 67 68 69 70 71		2	Fugitive Emission Source Valves  Pumps (Includes Vessel Agitators) Flanges / Connectors Pressure Relief Valves  Compressors Open-Ended Lines/Valves Sampling Connections Others O&G Others - Miscellaneous Drains Others O&G Others - Liquid  Speciated Emissions St  Compound Benzene Toluene Xylenes Phenols o-cresol m+p-cresol n-hexane	Service Gas Light Liquid Heavy Liquid Light Liquid Heavy Liquid Havy Liquid All Gas Liquids All All All All All All All All All Al	Em. Factor kg/hr 0.0268 0.0109 0.0109 0.1139 0.0209 0.3500 0.3500 1.3990 0.0051 0.00000 0.00000 Totals =  gram/s 0.0002 0.0000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	Equipment Counts  0 34 0 141 0 141 0 0 33 4 8 0 0 8 0 0 202    kg/hr 0.001 0.002 0.000 0.000 0.000 0.000	kg/hr 0.00 0.37 0.00 0.46 0.00 0.04 0.00 0.02 0.26 0.00 0.23 0.00 0.00 0.00 0.00 0.00 0.00	MT/yr 0.00 3.24 0.00 3.99 0.00 0.31 0.00 0.00 96.77 0.18 2.31 0.00 0.00 0.00 48.84	Ib/hr	tonlyr 0.00 3.57 0.00 4.40 0.00 0.34 0.00 0.00 40.53 0.20 2.55 0.00 0.00 0.00 0.00 0.00 0.00	Equipment Design Control Efficiency % 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0	LDAR Program Control Efficiency % 97 97 97 85 0 30 97 0 85 85 85 85 0 0 0 0 0 0 0 0 0 0 0 0 0	Fugitive Control Efficiency % 97 97 97 97 97 80 30 100 100 100 100 0 75 0 0 0 MT/yr 0.009 0.025 0.031 0.000 0.001	% 50% 50% 50% 60% 0% 0% 0% 15% 15% 15% 15% 15% 15% 15% 0.002 0.000 0.000 0.000	kg/hr 0,00000 0,01110 0,00000 0,01492 0,00000 0,03209 0,000000	MT/yr 0.00000 0.09727 0.00000 0.13067 0.00000 0.28110 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	1b/hr 0.00000 0.02448 0.00000 0.03289 0.00000 0.07074 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000 0.00000	ton/yr 0,00000 0,10722 0,00000 0,1404 0,00000 0,30986 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000 0,00000	Final valve or  Double Mech  Reactor and  Venting cont Capped, biln  Closed loop

1	Emissions	Summary
1	Emissions	Summary

mission Factor Set Use	d :	TCEQ-F	Refining					Design Control	Program Control	Fugitive Control						
	- 1	Em. Factor	Equipment	Uncontrolled Fugitive Emissions			Efficiency	Efficiency	Efficiency	Contingency		Controlled Fugit			Remarks	
ugitive Emission Source	Service	kg/hr	Counts	kg/hr	MT/yr	lb/hr	ton/yr	%	%	%	%	kg/hr	MT/yr	lb/hr	ton/yr	Streams with vapor pressure less than 0.002 psia @ 68 degF are excluded from fugitive evaluations
	Gas	0.0268	0	0,00	0.00	0.00	0.00	0	97	97	50%	0,00000	0.00000	0.00000	0,00000	Streams with vapor pressure less than 0.002 paia to occur and consider morning the occur.
alves		0,0200	34	0.37	3.24	0.82	3.57	0	97	97	50%	0.01110	0.09727	0.02448		Final valve counts have most uncertainty until P&ID's are available in later engineering phases.
	Light Liquid		34	0.00	0.00	0.00	0.00	0	97	97	50%	0.00000	0.00000	0.00000	0.00000	
	Heavy Liquid	0.0109					4,40	80	85	97	0%	0,01492	0.13067	0.03289	0.14404	Double Mechanical Seals per API Seal Plans provided on all LL & HL pumps due to process conditions
umps	Light Liquid	0.1139	4	0.46	3.99	1.00	0.00	80	0.0	80	0%	0.00000	0.00000	0.00000	0.00000	
ncludes Vessel Agitators)	Heavy Liquid	0.0209	0	00,0	0.00	0.00		00	30	30	25%	0.03209	0.28110	0.07074	0.30986	Reactor and other large vessel flanges are welded due to high process pressures
langes / Connectors	All	0,00025	141	0.04	0.31	0.08	0.34	, , , , , , , , , , , , , , , , , , ,			+	0.00000	0.00000	0.00000	0,00000	
ressure Relief Valves	Gas	0.3500	0	0.00	0,00	0,00	0.00	100	97	100		0.00000	0.00000	0.00000	0.00000	
	Liquids	0.3500	0	0.00	0.00	0.00	0.00	100	0	100	15%		0.00000	0.00000	0.00000	Venting controlled by flare
ompressors	ΑſI	1.3990	3	4.20	36.77	9.25	40.53	100	85	100	15%	0,00000		0.00000	0.00000	Capped, bilnded, or double block primary design.
pen-Ended Lines/Valves	All	0.00510	4	0.02	0.18	0.04	0.20	100	85	100		0.00000	0.00000		0.00000	Closed loop system designs used
Sampling Connections	All	0.03300	8	0.26	2,31	0.58	2.55	100	85	100	15%	0.00000	0.00000	0.00000		Closen loop system designs date
onnectors - Miscellaneous	All	0.00025	0	0.00	0.00	0.00	0.00	0	0	0	15%	0.00000	0.00000	0,00000	0.00000	and the second s
Orains	All	0.02917	B	0.23	2.04	0.51	2.25	50	50	75	15%	0,05833	0.51100	0.12860	0.56328	50% of Drains are hardpiped with 100% control efficiency (entered as Secondary Efficiency)
	2-41	0.00000	-	0.00	0.00	0.00	0.00	0	0	0	15%	0.00000	0.00000	0.00000	0.00000	
Others	A.11			0.00	0.00	0.00	0.00	0	0	0	15%	0.00000	0.00000	0.00000	0.00000	
O&G Others - Gas/Vapor	All	0.00000	0		0.00	0.00	0.00	<u> </u>	<u> </u>	0	15%	0.00000	0.00000	0.00000	0.00000	
O&G Others - Liquid	All	0.00000	90.7	0.00	42.84	13.39	53.84	<u> </u>				0.116	1.020	0.257	1,124	

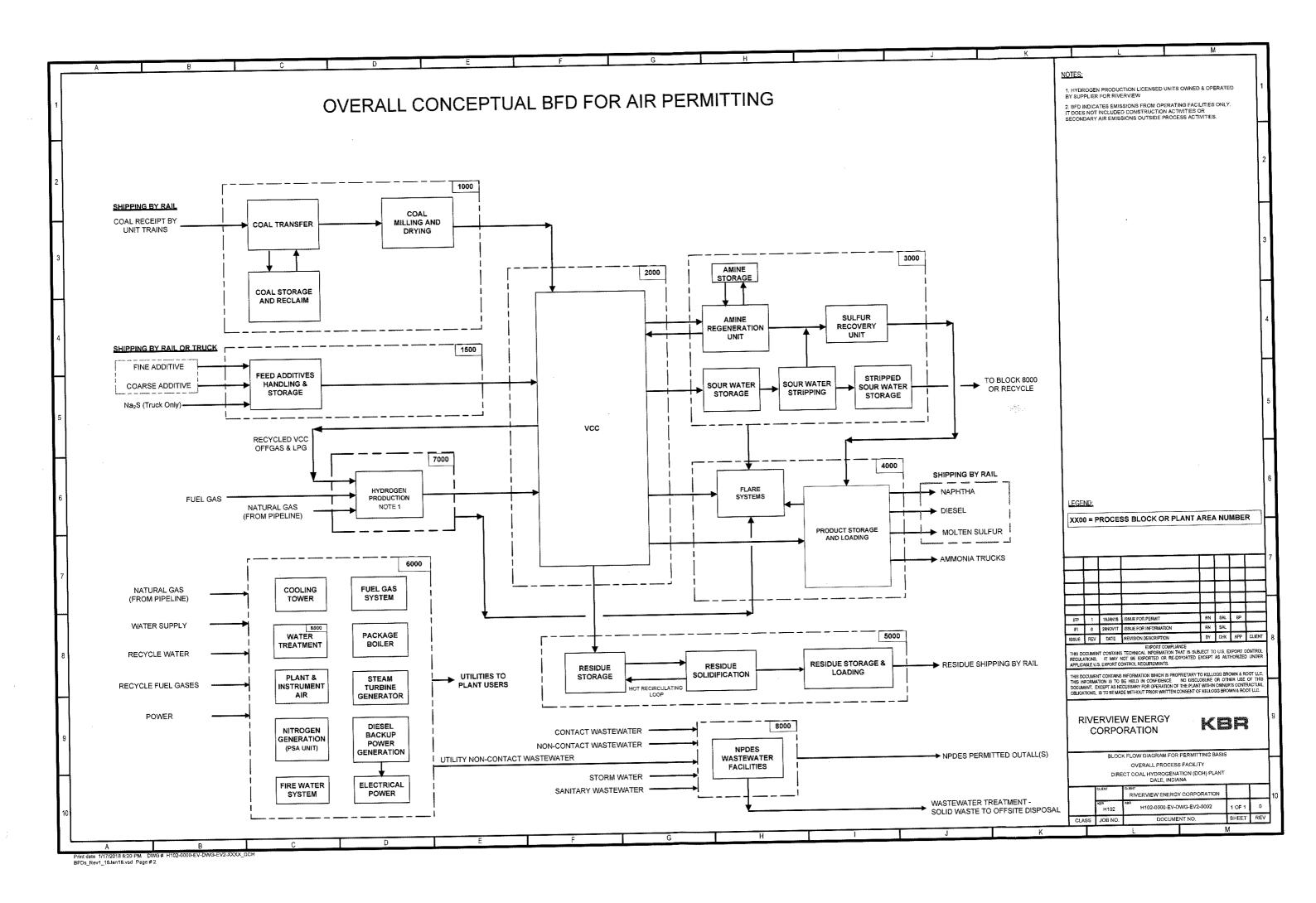
#### 2 Speciated Emissions Summary

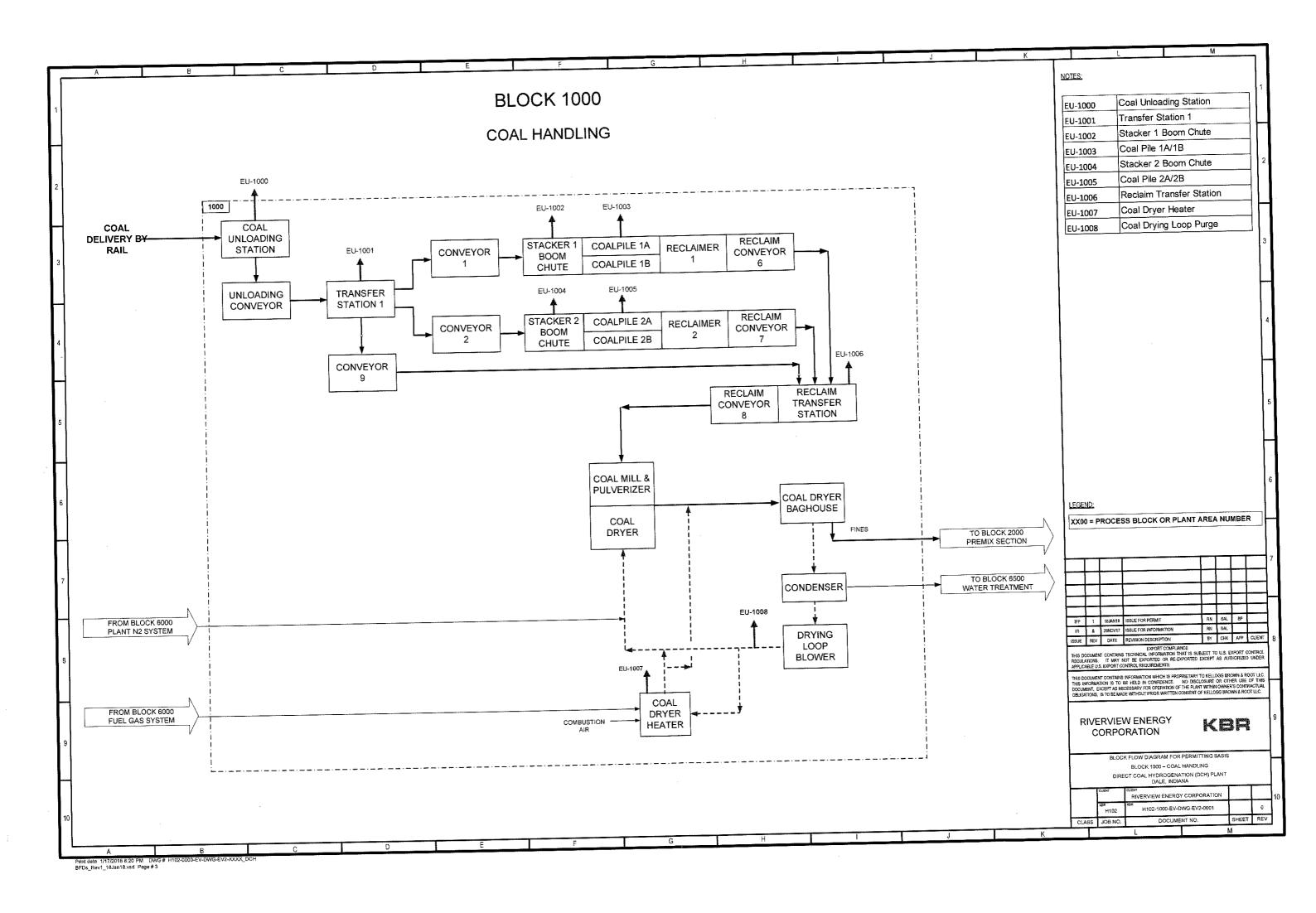
							Contingency			4.57	15-75-	ton/yr
Compound	Fugitive	gram/s	kg/hr	MT/yr	lb/hr	ton/yr	%	gram/s	kg/hr	MT/yr	lb/hr	
Benzene	HAP	0.0002	0.001	0.007	0.002	800.0		0.0003	0.001	0.009	0.002	0.010
Toluene	HAP	0.0006	0,002	0,020	0.005	0.022	1	0.0008	0.003	0.025	0.006	0.027
	HAP	0.0008	0.003	0.025	0.006	0.027		0.0010	0.004	0.031	0.008	0.034
Xylenes Dhonolo	HAP	0.0000	0.000	0.000	0.000	0.000		0.0000	0.000	0.000	0,000	0.000
Phenois	HAP	0.0000	0.000	0.001	0.000	0.001	1 '	0.0000	0.000	0.001	0.000	0.001
o-cresol	HAP	0.0000	0.000	0.000	0.000	0.000	25%	0,0000	0.000	0.000	0.000	0.000
m+p-cresol			0.002	0.020	0.005	0.022	1 !	0,0008	0.003	0.025	0.006	0.027
n-hexane	HAP	0,0006	0,002	0.020	0.003	0.022	1 1	0,000				
							1					
							-					
							4					
						AND ALL OF THE COMMANDER OF THE COMMANDE				35:049.000		0.101
No. of the last of	Sum = HAP	0.002	0.008	0.073	0.018	0.081	3	0,003	0,010	0.092	0.023	高級なるので、

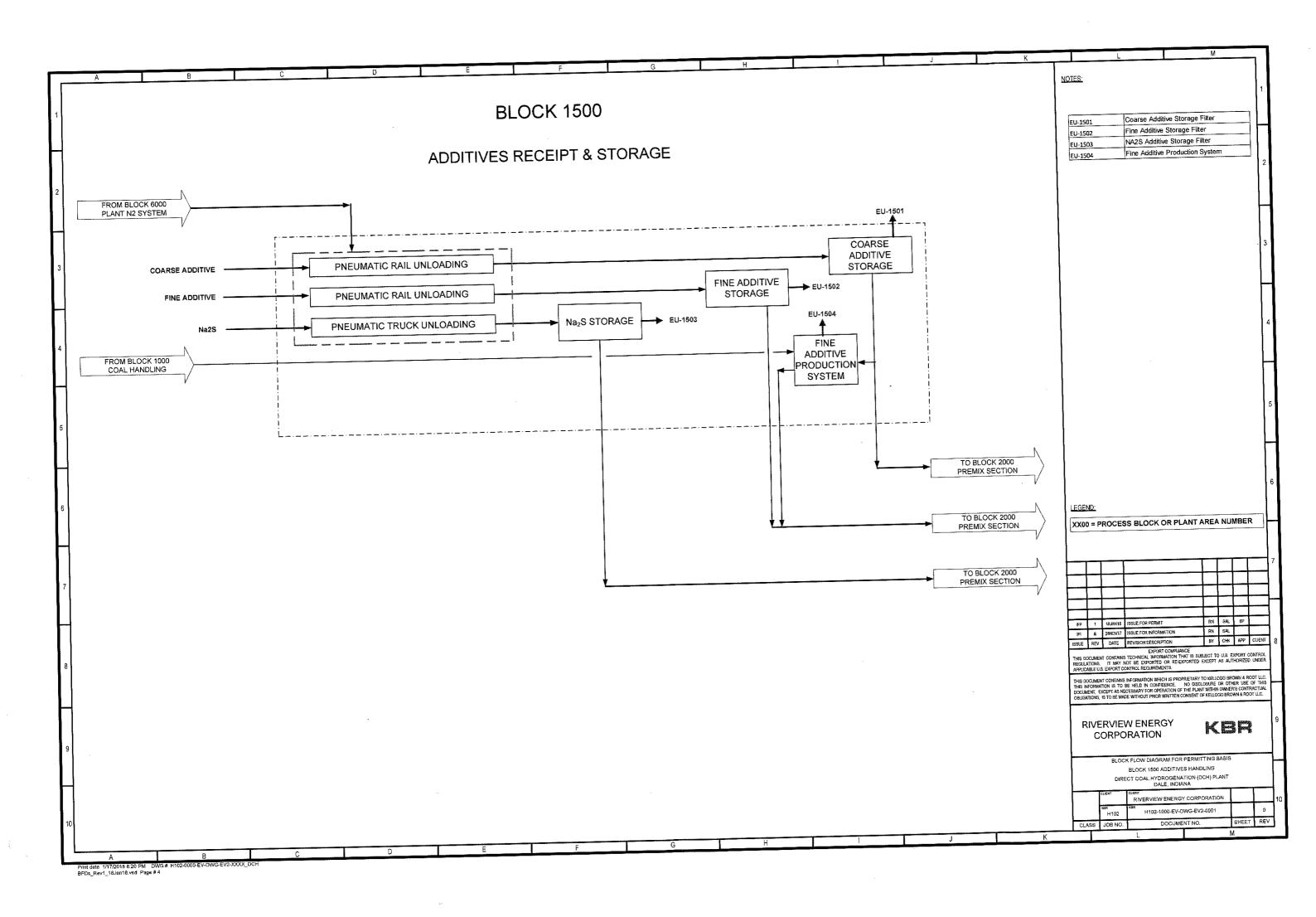
# **Attachment C. Process Diagrams**

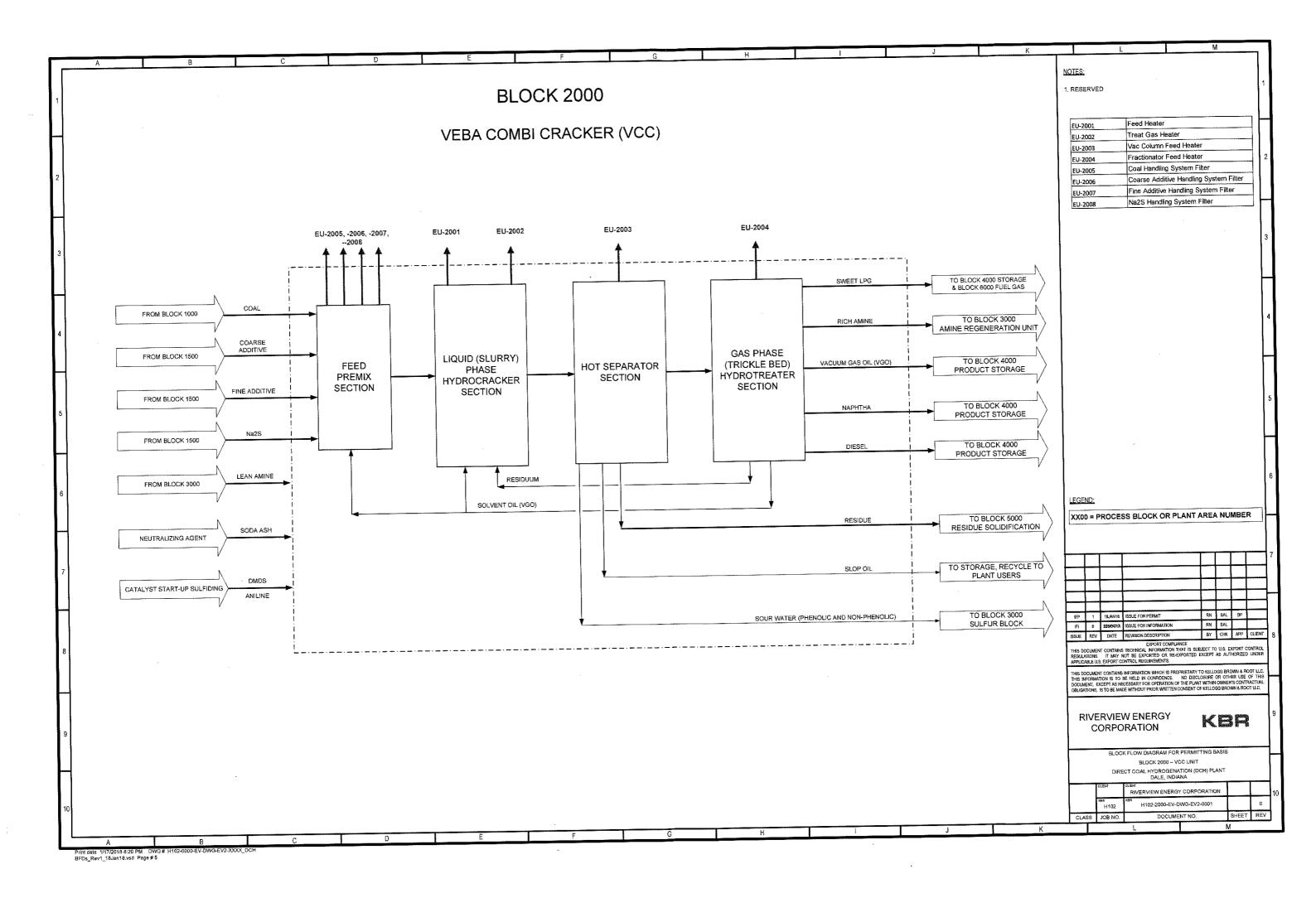
B C D	E F G H		NOTES:
Amount the constraint and the co			
DRAWING NUMBERS	TITLE		
H102-0000-EV-DWG-EV2-0001	Drawing Index		
H102-0000-EV-DWG-EV2-0002	Site Overall Conceptual BFD for Air Permits		
H102-1000-EV-DWG-EV2-0001	Block 1000 Coal Handling BFD		
H102-1500-EV-DWG-EV2-0001	Block 1500 Additives Handling BFD		
H102-2000-EV-DWG-EV2-0001	Block 2000 VCC Unit BFD	ament A	
H102-2000-EV-DWG-EV2-0002	Block 2000 VCC Detail BFD		
H102-3000-EV-DWG-EV2-0001	Block 3000 Sulfur Recovery BFD	3,047.07	
H102-3000-EV-DWG-EV2-0003	Block 3000 Amine Recovery Unit Detail BFD		
H102-3000-EV-DWG-EV2-0004	Block 3000 Amine Storage Detail BFD	siderer	
H102-4000-EV-DWG-EV2-0001	Block 4000 Offsites Unit BFD	ma237	
H102-5000-EV-DWG-EV2-0001	Block 5000 Residue Solidification Unit BFD	igness(f)	
H102-6000-EV-DWG-EV2-0001	Block 6000 Utilities BFD	Name of the state	LEGEND:
H102-6500-EV-DWG-EV2-0001	Block 6500 Water Supply & Treatment BFD	and the state of t	XX00 = PROCESS BLOCK O
H102-7000-EV-DWG-EV2-0001	Block 7000 Hydrogen Production BFD	984.mandrij 1	
H102-8000-EV-DWG-EV2-0001	Block 8000 Waste Water Treatment BFD	grave-radio.	
And the second s			
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			ISSUE REV DATE REVISION DESCRIPTION THIS DOCUMENT CONTAINS TECHNICAL INFORMAT REGULATIONS. IT MAY NOT BE EXPORTED O
			APPLICABLE U.S. EXPORT CONTROL REQUIREMENT THIS DOCUMENT CONTAINS INFORMATION WHICH
			THIS INFORMATION IS TO BE HELD IN CURPILED DOCUMENT, EXCEPT AS NECESSARY POR OPERAT OBLIGATIONS, IS TO BE MADE WITHOUT PRIOR WIR
			RIVERVIEW ENERG CORPORATION
			BLOCK FLOW DIAGRAM
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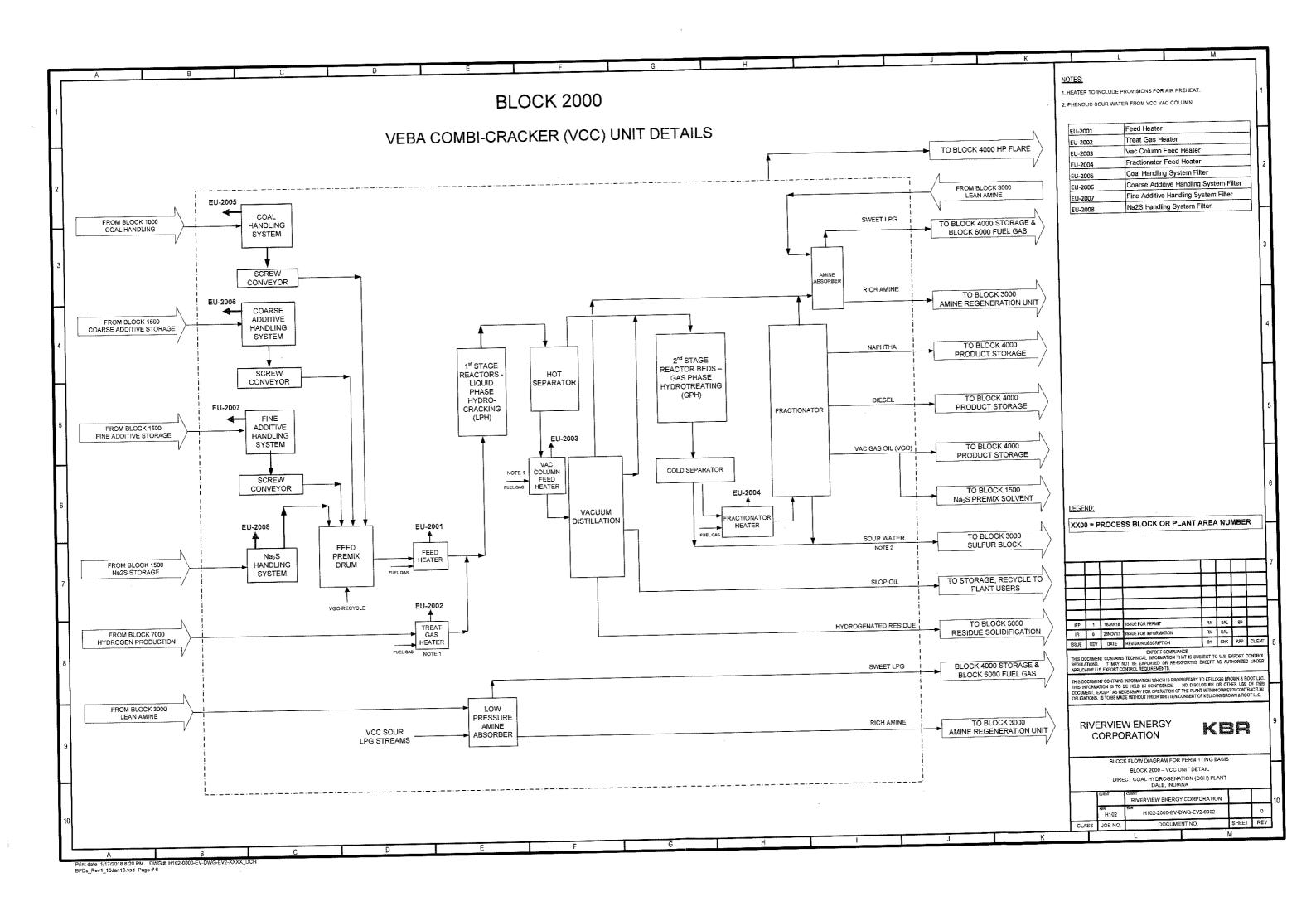
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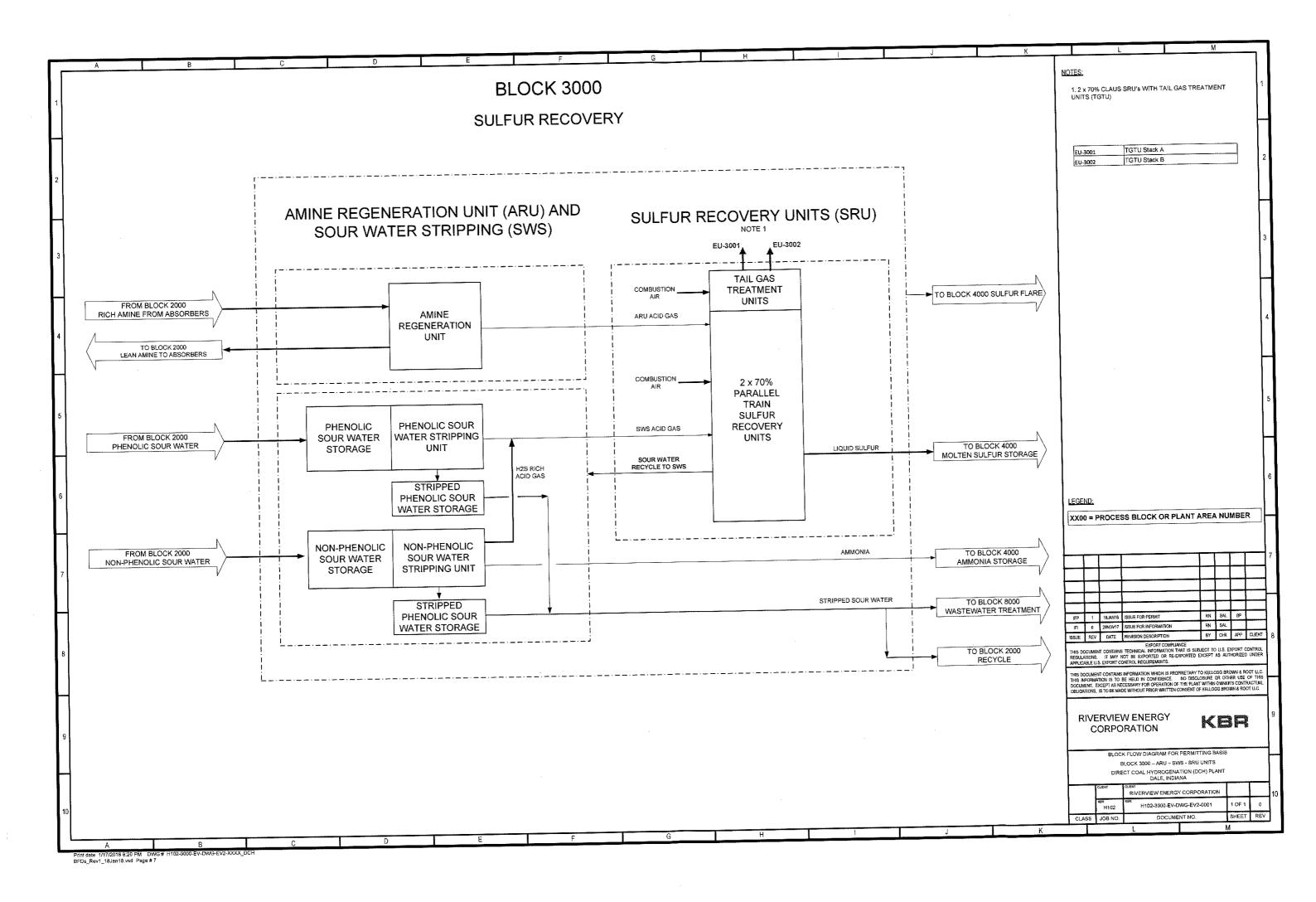


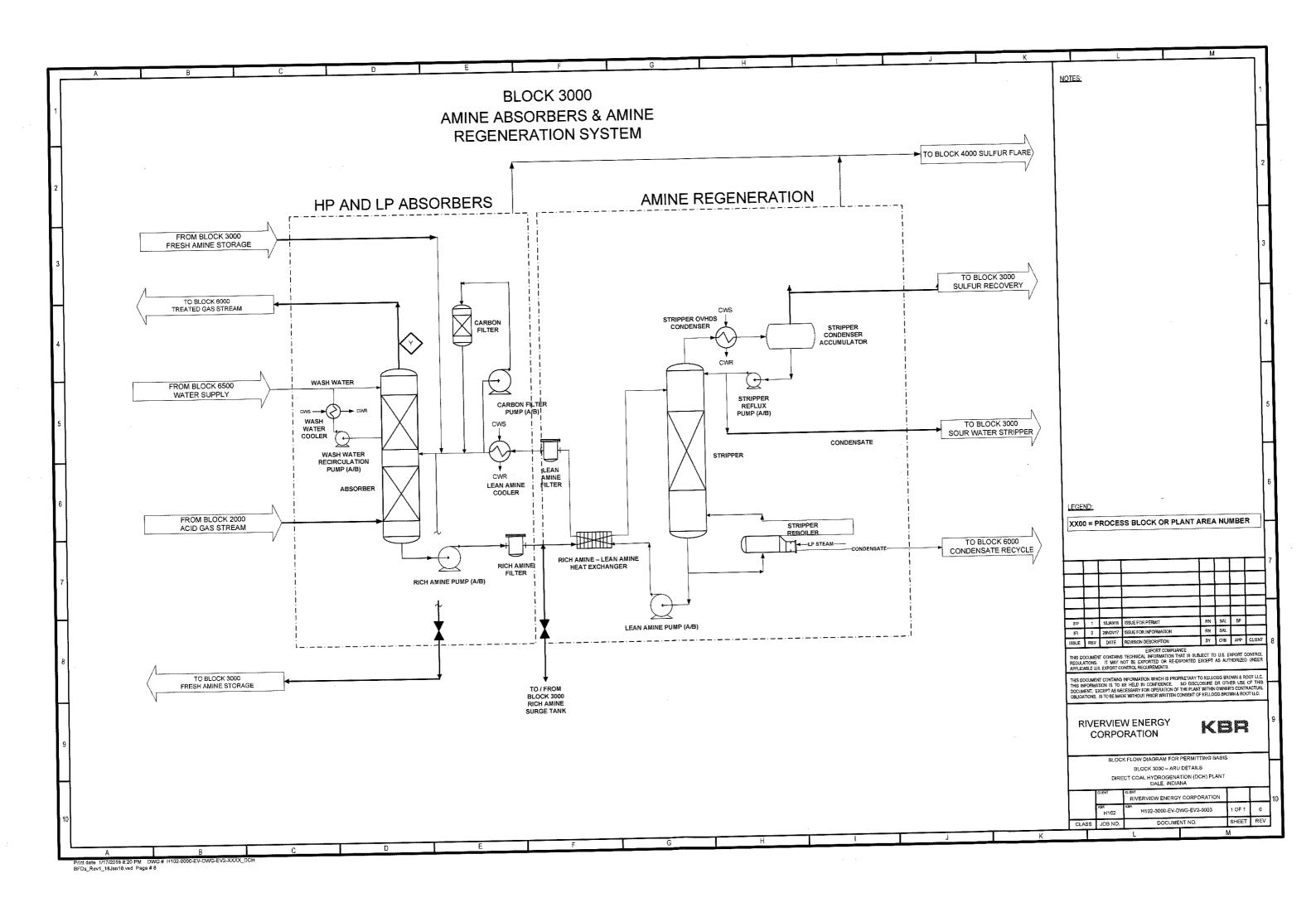


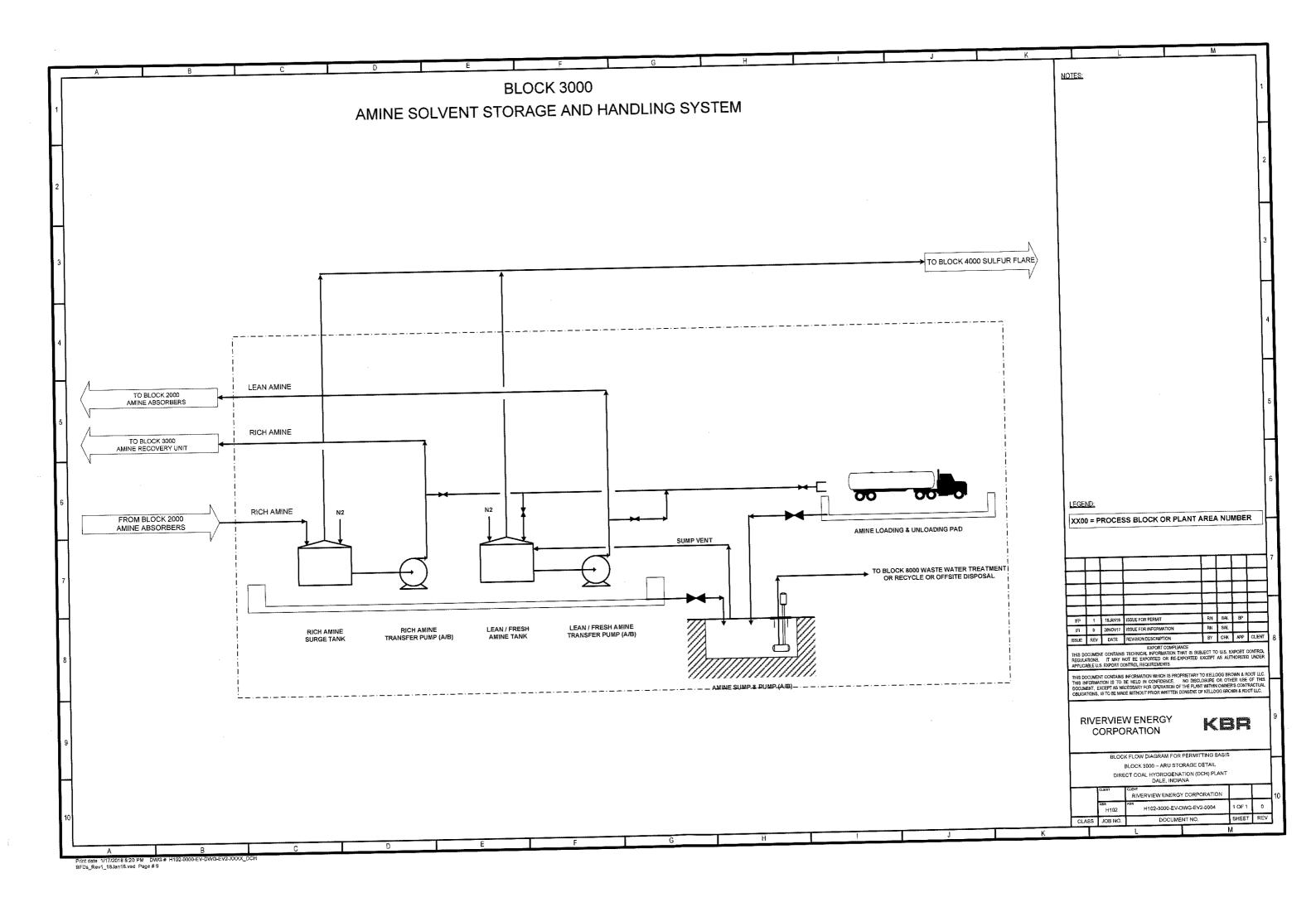


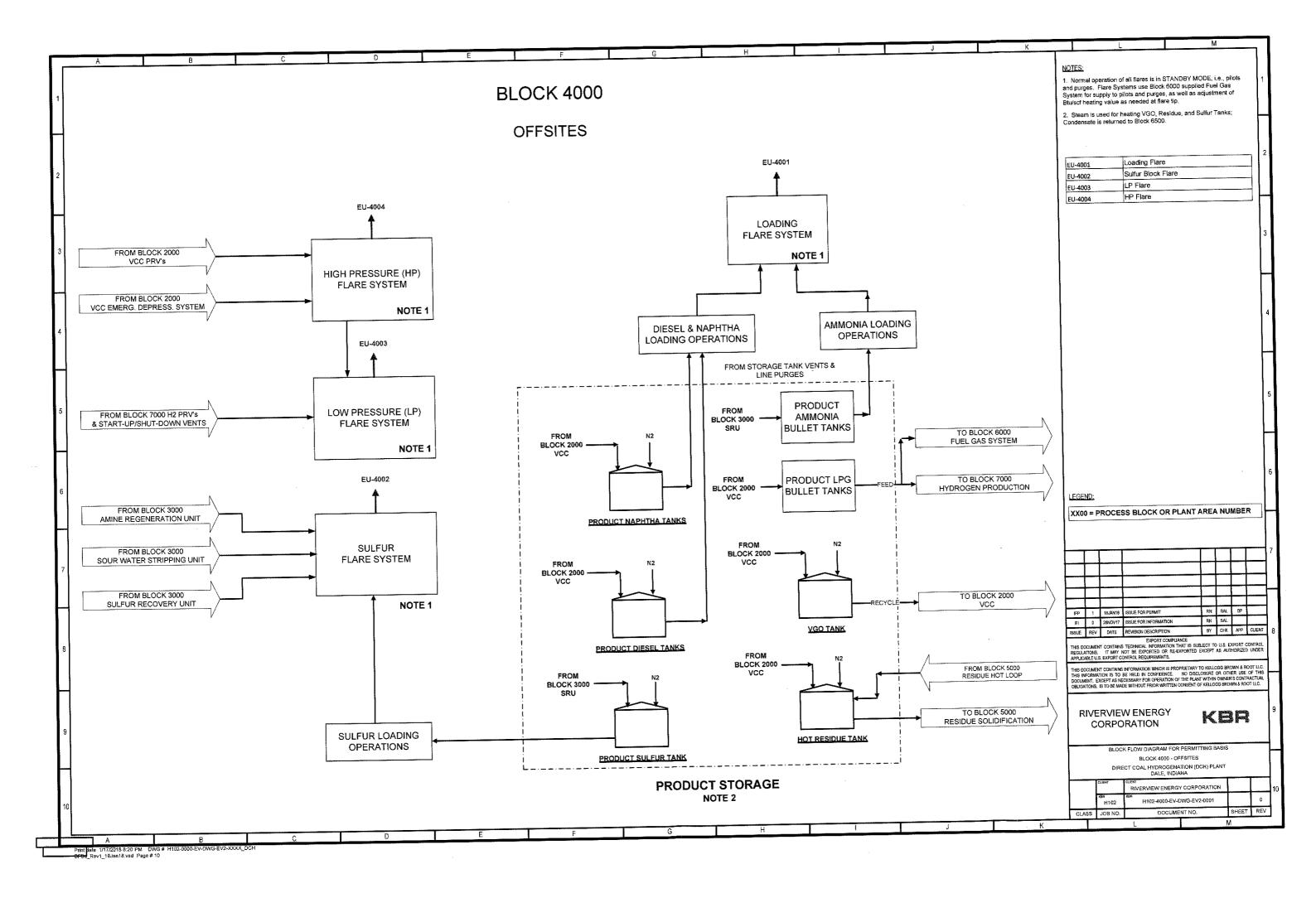


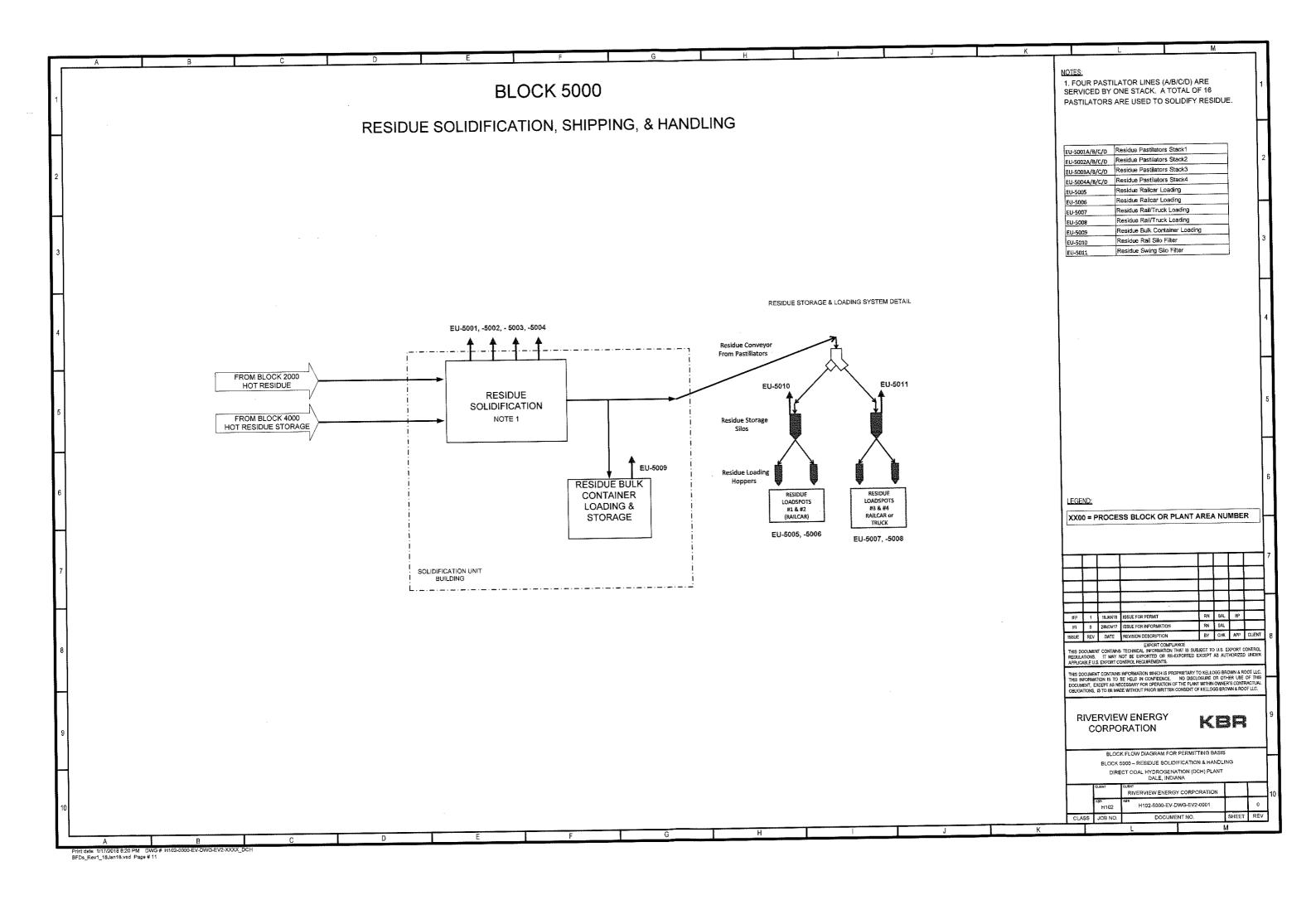


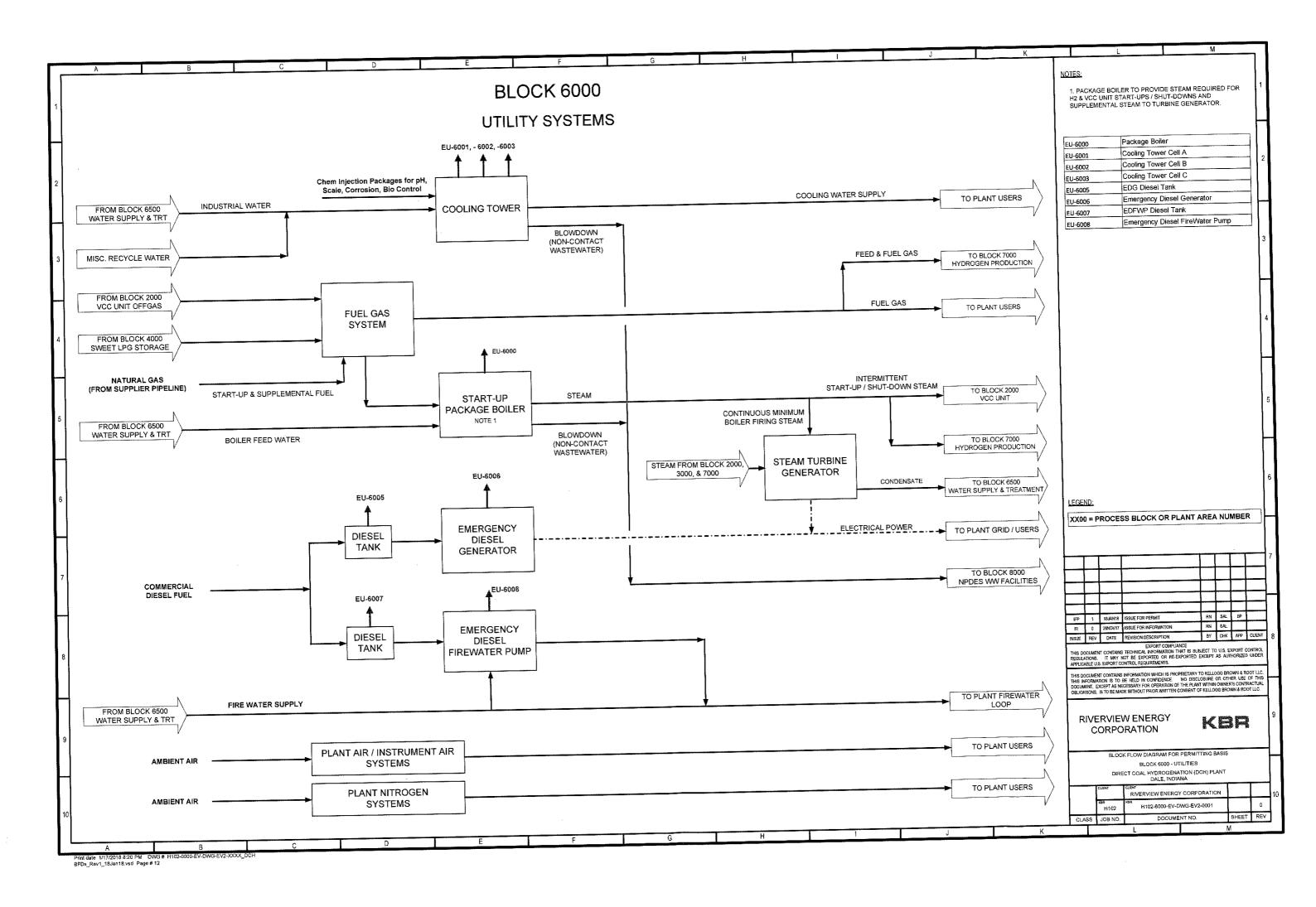


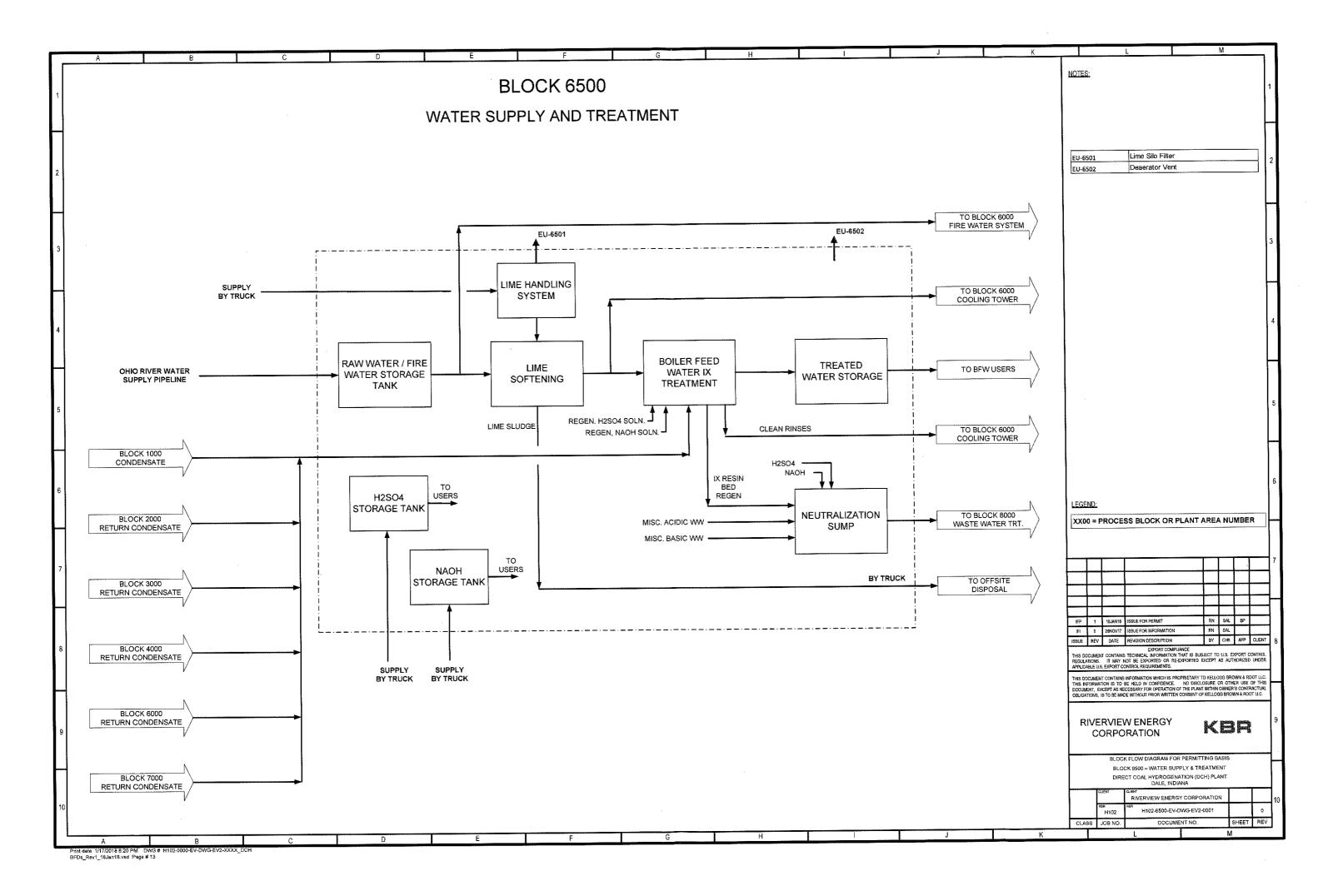


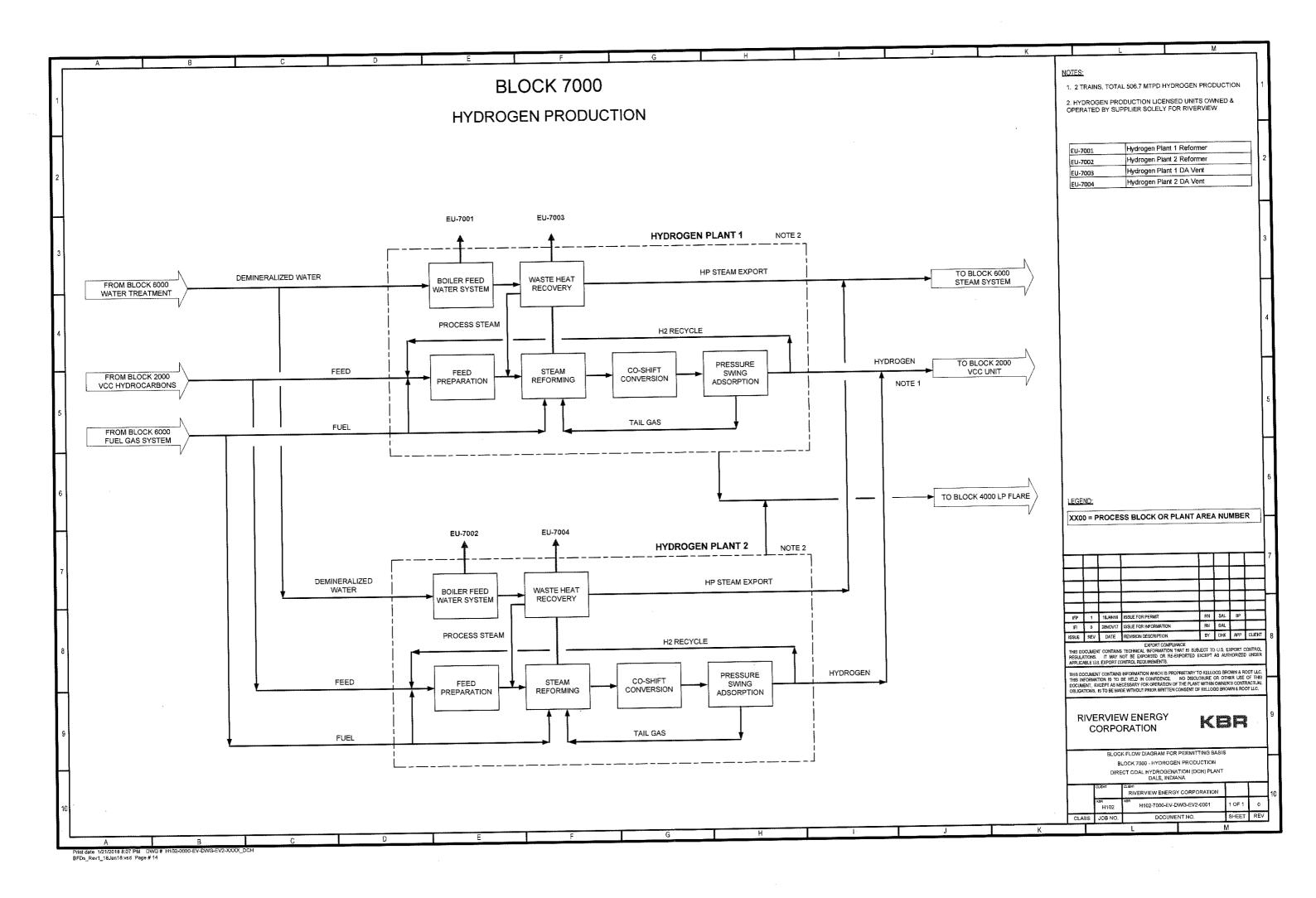


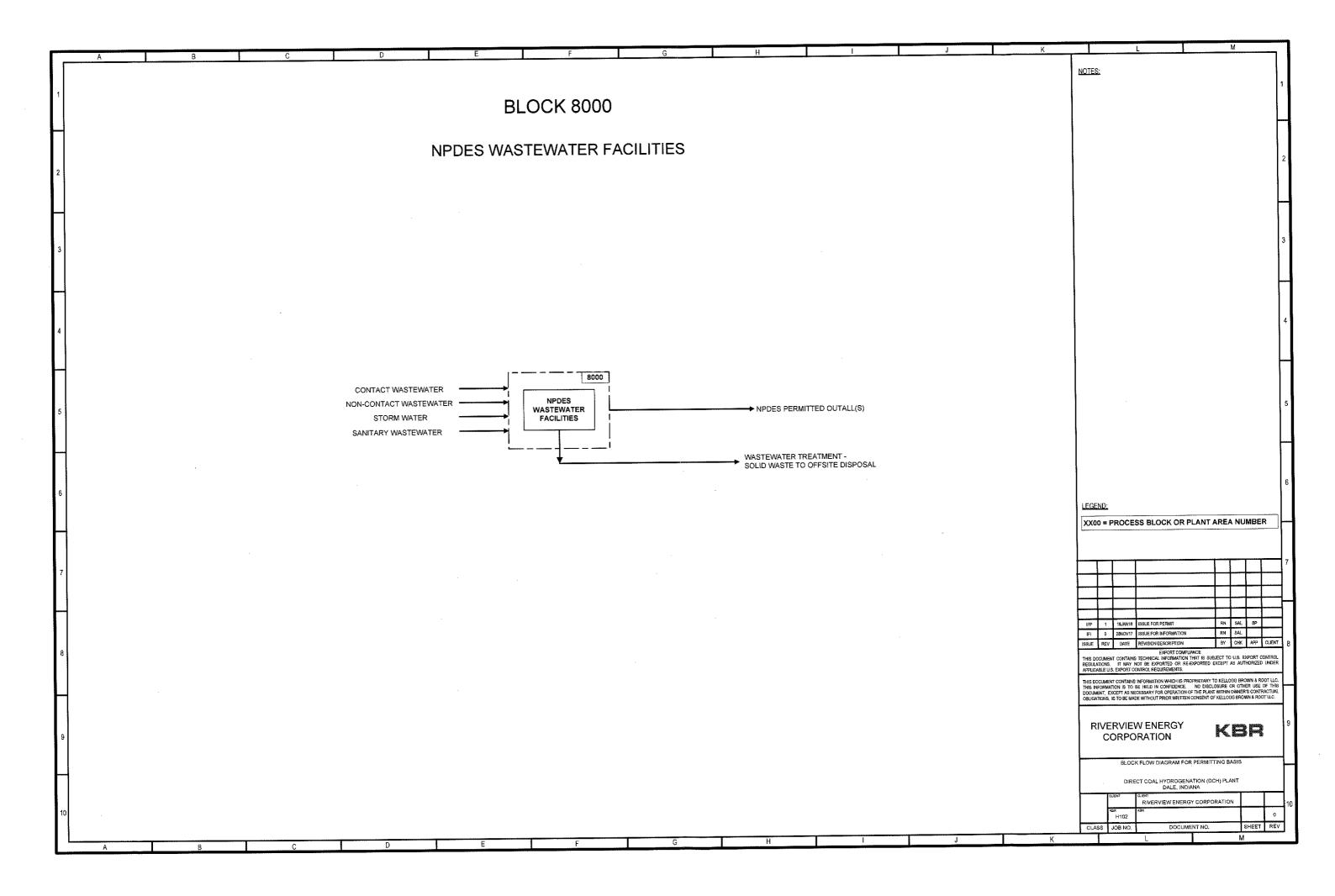












## **Attachment D. Site Plans**

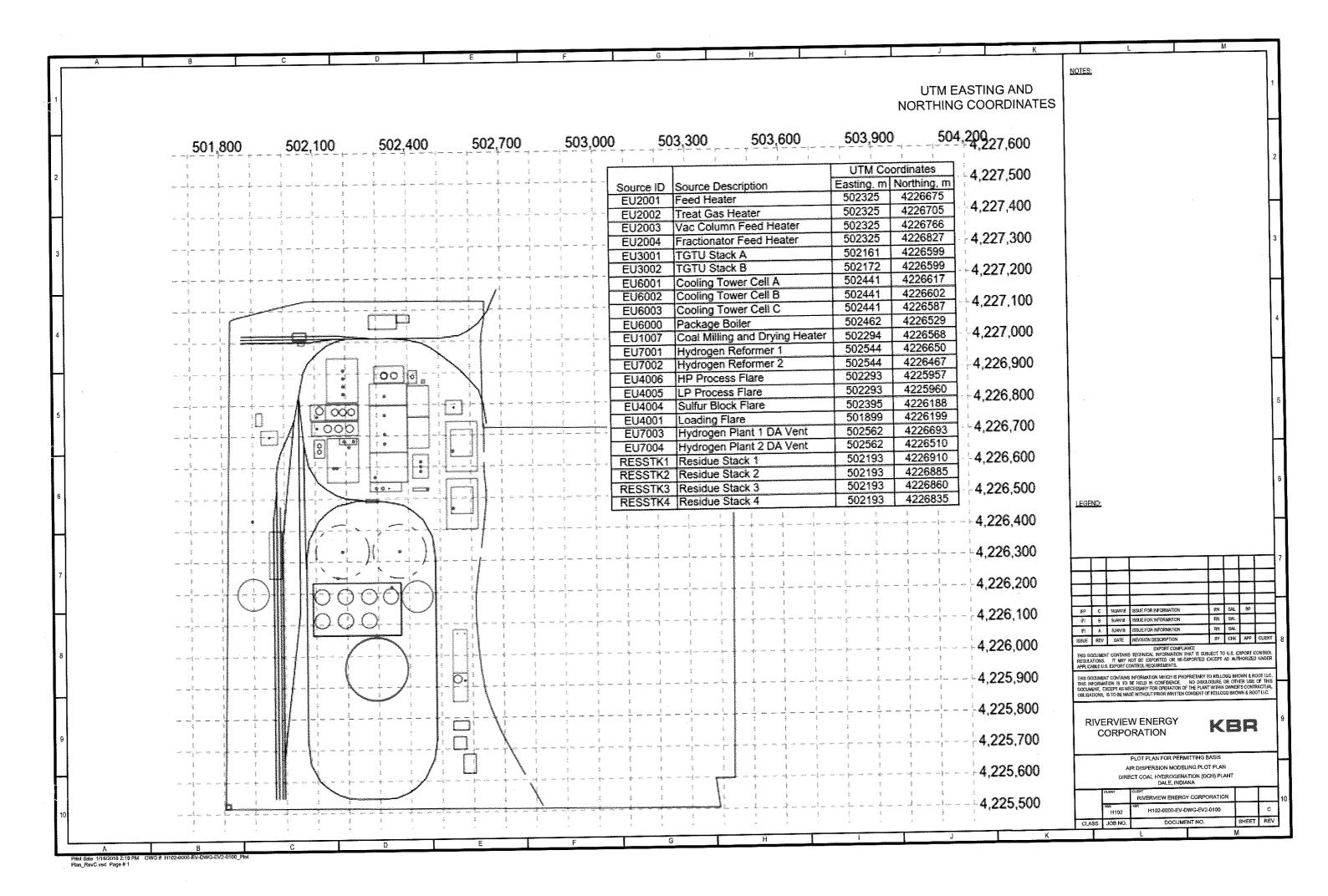


Table 1. Tank Emissions Summary Naphtha Product Tank, Diesel Product Swing Tank

			Loss	es per Tank i	(lbs)		Total Emissions		
Tank Identification	<u>Camponents</u>	Rim Seal Loss	Withdrawl Loss	Deck Fitting Loss	Deck Seam Loss	Total Emissions	Total Tanks Emissions (lbs/yr)	Total Tanks Emissions (tons/yr)	
Naphtha Product Tank - Internal Floating Roof Tank	Product Naphtha	1,040.01	73.68	556,33	0	1,670.03	3,340.06	1.67	
lumber of Tanks	Hexane (-n)	42.86	1,11	22.93	0	66.9	133.8	0.07	
	Benzene	10,36	0.44	5.54	0	16.34	32,68	0.02	
	Toluene	9.56	1.47	5.11	0	16.15	32.3	0.02	
	Ethylbenzene	0.77	0.37	0.41	. 0	1.55	3.1	0.00	
	Xylene (-m)	3.19	1.84	1.71	0	6.74	13.48		
	Isopropyl benzene	0,13	0.15	0.07	0	0.35	0.7		
	Cyclohexane	21.57	0.88	11.54	0	33.99	67.98	0.03	
	Unidentified Components	951.57	67.42	509.02	0	1,528.01	3,056.02	1.53	
Dieset Product Swing Tank - Internal Floating Roof Tank	Product Naphtha	1,040.01	72.02	556.33		1,668.36	1,668.36	0.83	
rioding Roof (unk	Hexane (-n)	42.86	1.08	22.93	3 (	66.87	66.87	0.0	
	Benzene	10.36	0.43	5.54	1 (	16.33	<u> </u>		
Number of Tanks	Toluene	9.56	1.40	5.1	1 (	16.1			
	1 Xylene (-m)	3.19	1.8			6.1			
	Isopropyl benzene	0.13	0.14	0.0	<u> </u>	0.3			
	Cyclohexane	21.5	0.80	3 11.5	4	33.9	7 33.9	7 0.0	
	Unidentified Components	951.5	65.	509.0	2	0 1,526.4			
	Ethylbenzene	0.7	7 0.3	6 0.4	1	0 1.5	4 1.5	4 0.0	

Table 2. Tank Emissions Summary Diesel Product Tank and Fuel Storage Tank, Fresh Amine Tank, VGO Tank, Surge Tank, Vacuum Residue Tank

Tank Identification	Components		Losses(Ibs)		Total Emissions			
запк іденніськог	components	Working Loss	Breathing Loss	Total Emissions per Tank	Total Emissions (libs/vr)	Total Emissions (tons/vr)		
Diesel Product Tank - Vertical Fixed Boof Tank	Product Diesel	26.06	26.72	52.78	158.34	0.07917		
lumber of Tanks								
Diesel Fuel Storage Tank - Vertical Fixed Roof Tank	Distillate fuel oil no. 2	4.92	5.98	10.9	10.9	0.00545		
Ned Roof Tark	Hexane (-n)	0		0	0	)		
Number of Tanks	Benzene	0.01		0.02	0.02	0,0000		
-	1 Toluene	0.12		0.26	0.26	0.0001		
	Ethylbenzene	0.02	<del> </del>	0.03	0.03	0.00001		
	Xylene (-m)	0.28	0.34	0.63	0.63	0.00031		
	1,2,4-Trimethylbenzene	0.22	0.26	0.48	0.48	0.0002		
	Unidentified Components	4.28	5.19	9.47	9.47	0.00473		
Fresh Amine Tank - Vertical Fixed Roof Tank	Lean Amine	0.03	0.23	0.26	0.26	0.0001		
Number of Tanks			<u> </u>		ļ			
	1					0.000		
VGO Tank	VCC VGO	0.10	5 0.08	0.24	0.48	0.0002		
Number of Tanks			ļ		<b></b>	<b> </b>		
	2	<del> </del>	<del> </del>	0.02	0.04	0.000		
Hydrogenated Residue Surge Tank	Hydrogenated	0.0	1	0.02	0.04	0.000		
Number of Tanks			<u> </u>			<del> </del>		
	2	0.2	5 0.0	8 0.33	0.33	0.0001		
Vacuum Residue Feed Tank	VCC Residue	0.2						
Number of Tanks	1			1		<b>1</b>		

Table 3. Total Annual Potential Emissions

		Total Annual Potential Emissions			
Identification	Components	Total VOC Emissions (lbs/vr)	Total VOC Emissions (tons/yr)		
Naphtha Product Tank - Internal Floating Roof Tank	Product Naphtha	3,340	1.67		
Diesel Product Tank - Vertical Fixed Roof Tank	Product Diesel	158	0.08		
Naphtha Product Loadout Diesel Product Loadout	Product Naphtha Product Diesel	3,115 0	1.56 0		
	Overall Total	6,613	3.31		